Official Transcript of Proceedings NUCLEAR REGULATORY COMMISSION

Title: Advisory Committee on Reactor Safeguards

APR1400 Subcommittee

Docket Number: N/A

Location: Rockville, Maryland

Date: April 19, 2017

Work Order No.: NRC-3023 Pages 1-543

NEAL R. GROSS AND CO., INC. Court Reporters and Transcribers 1323 Rhode Island Avenue, N.W. Washington, D.C. 20005 (202) 234-4433

-	
_	L

2

7

7

_

10

11

12

13

14

15

16

17

18

19

2021

22

23

DISCLAIMER

UNITED STATES NUCLEAR REGULATORY COMMISSION'S ADVISORY COMMITTEE ON REACTOR SAFEGUARDS

The contents of this transcript of the proceeding of the United States Nuclear Regulatory Commission Advisory Committee on Reactor Safeguards, as reported herein, is a record of the discussions recorded at the meeting.

This transcript has not been reviewed, corrected, and edited, and it may contain inaccuracies.

UNITED STATES OF AMERICA

NUCLEAR REGULATORY COMMISSION

+ + + + +

ADVISORY COMMITTEE ON REACTOR SAFEGUARDS

(ACRS)

+ + + + +

APR1400 SUBCOMMITTEE

+ + + + +

WEDNESDAY

APRIL 19, 2017

+ + + + +

ROCKVILLE, MARYLAND

+ + + + +

The Subcommittee met at the Nuclear Regulatory Commission, Two White Flint North, Room T2B1, 11545 Rockville Pike, at 8:30 a.m., Ronald G. Ballinger, Chairman, presiding.

COMMITTEE MEMBERS:

RONALD G. BALLINGER, Chairman

DENNIS C. BLEY, Member

MICHAEL L. CORRADINI, Member

WALTER L. KIRCHNER, Member

JOSE MARCH-LEUBA, Member

NEAL R. GROSS

COURT REPORTERS AND TRANSCRIBERS 1323 RHODE ISLAND AVE., N.W. WASHINGTON, D.C. 20005-3701 DANA A. POWERS, Member

JOY REMPE, Member

GORDON R. SKILLMAN, Member

JOHN W. STETKAR, Member

MATTHEW W. SUNSERI, Member

DESIGNATED FEDERAL OFFICIAL:

CHRISTOPHER BROWN

CHRISTIANA LUI

ALSO PRESENT:

ROSS ANDERSON, ENERCON

AARON ARMSTRONG, NRO

ODUNAYO AYEGBUSI, NRO

JEFF CIOCCO, NRO

RAYMOND DREMEL, ENERCON

STEVE D. FLOYD, Jensen Hughes

ANNE-MARIE GRADY, NRO

GARY W. HAYNER, Jensen Hughes

SUN HEO, KHNP

SEOKHWAN HUR, KEPCO E&C

KYUHO HWANG, SGH

TAEHEE HWANG, KEPCO E&C

YOUNG H. IN ENERCON

NEAL R. GROSS

BYUNG JO KIM, KEPCO E&C

JAE GAB KIM, KEPCO E&C

JEFF LEARY, ENERCON

DONGWON LEE, KEPCO E&C

ROBERT LICHTENSTEIN, ENERCON

JAESOO LIM, KHNP

MARK LINTZ, NRO

MICHAEL MCCOPPIN, NRO

JILL MONAHAN, Westinghouse

LYNN MROWCA, NRO

TONY NAKANISHI, NRO

ALISSA NEUHAUSEN, NRO

DAE GEUN OH, KEPCO E&C

JIYONG OH, KHNP

CHAN Y. PAIK, FAI

CHAN EOK PARK, KEPCO E&C

CHANG SUN PARK, KEPCO E&C

HANH PHAN, NRO

STEVE PHILL PPI, ENERCON

MARIE POHIDA, NRO

ROBERT ROCHE-RIVERA, NRO

JAMES ROSS, AECOM

GREGORY ROZGA, ENERCON

IN CHUL RYU, KEPCO E&C

NEAL R. GROSS

SUJIT SAMADDAR, NRO

JASON SCHAPEROW, NRO

RAY SCHNEIDER, Westinghouse

ROB SISK, Westinghouse

COURTNEY ST PETERS, NRO

JAMES STECKEL, NRO

VAUGHN THOMAS, NRO

ANDREA VEIL, Executive Director, ACRS

HANRY WAGAGE, NRO

*Present via telephone

CONTENTS

1.	Opening Remarks & Objectives
	Ronald Ballinger, ACRS7
2.	Staff Opening Remarks
	Jeff Ciocco, NRO11
3.	Chapter 19.1 PRA
	Young In11
	Gregory Rozga25
4.	Break77
5.	Chapter 19.1 PRA (Cont.)
	Taehee Hwang78
	Dongwon Lee104
	Gregory Rozga115
6.	Lunch136
7.	Chapter 19.1 PRA
	Ray Dremel136
	Jae Gab Kim150
8.	Chapter 19.2 Severe Accident Evaluation
	Byung Jo Kim166
9.	Break214

CONTENTS (cont.)

10. Chapter 19.2 Severe Accident Evaluation (cont.)
Hanh Phan
Odunayo Ayegbusi224
Courtney St. Peters235
Tony Nakanishi245
Alissa Neuhausen257
Marie Pohida265
11. Break294
12. Chapter 19.2 Severe Accident Evaluation (cont.)
Hanry Wagage294
Anne-Marie Grady317
Alissa Neuhausen331
13. Public Comments
Adjourn

1	PROCEEDINGS
2	8:31 a.m.
3	CHAIRMAN BALLINGER: The meeting will now
4	come to order. This is a meeting of the APR1400
5	Subcommittee of the Advisory Committee on Reactor
6	Safeguards.
7	I=m Ron Ballinger, Chairman of the
8	APR1400 Subcommittee.
9	ACRS Members in attendance are Mike
10	Corradini, Gordon Skillman, Dana Powers, Matt
11	Sunseri, Dennis Bley, John Stetkar, Jose March-Leuba,
12	Walt Kirchner and Joy Rempe.
13	The purpose of today=s meeting is for the
14	Subcommittee to receive briefings from Korea Electric
15	Power Corporation and Korea Hydro and Nuclear Power
16	Company regarding their design certification
17	application and the NRC staff regarding their Safety
18	Evaluation Report with open items specific to Chapter
19	17, Quality Assurance and Reliability Assurance in 19
20	Probabilistic Risk Assessment and Severe Accident
21	Evaluation.
22	The ACRS was established by statute and
23	is governed by the Federal Advisory Committee Act,
24	FACA. That means that the Committee can only speak

1	through its published letter reports.
2	We hold meetings to gather information to
3	support our deliberations.
4	Interested parties who wish to provide
5	comments can contact our offices requesting time
6	after the meeting announcement is published in the
7	Federal Register.
8	That said, we also set aside ten minutes
9	for spur of the moment from members of the public
10	attending or listening to our meetings.
11	Written comments are also welcome.
12	The ACRS Section of the USNRC public
13	website provides our charter, bylaws, letter reports
14	and full transcripts of all Full and Subcommittee
15	meetings, including slides presented at the meetings.
16	The rules for participation in today=s
17	meeting were announced in the Federal Register on
18	Wednesday, April 12, 2017. The meeting was announced
19	as open/closed to the public meeting.
20	And, I=m reminded that during the
21	presentation today, there=s a session that=s labeled
22	as closed for the end of the day. But, if the
23	questioning that goes on today suddenly gets into
24	something which is proprietary, you=11 need to let us

1	know so that we can take some action.
2	The meeting is announced in open public
3	this means that the Chairman can close the meeting
4	as needed to protect SRI and information proprietary
5	to KHNP and its vendors.
6	No requests for making a statement to the
7	Subcommittee has been received from the public.
8	A transcript of the meeting is being kept
9	and will be made available as stated in the Federal
10	Register Notice. Therefore, we request that
11	participants in this meeting use the microphones
12	located throughout the room and remember to push the
13	button and make it green when addressing the
14	Subcommittee.
15	Participants should first identify
16	themselves and speak with sufficient clarity and
17	volume so that they can be readily heard.
18	We have a bridge line established for
19	interested members of the public to listen in. The
20	bridge number and password were published in the
21	agenda posted on the NRC public website.
22	To minimize disturbance, this public line
23	will be kept in the listen only mode. The public
24	will have an opportunity to make a statement or

	10
1	provide comments at a designated time towards the end
2	of the meeting.
3	Request meeting attendees and
4	participants silence their cell phones and electronic
5	devices.
6	Also, I=ve been reminded on a number of
7	occasions that there are a number lots of slides,
8	a lot to go through. And so, and I thought I was
9	going to be issued a stun gun to keep people in order.
10	But, keep that in mind, although we really need to
11	have a full discussion.
12	MEMBER POWERS: Now, let me understand,
13	we=re supposed to have a full and complete discussion,
14	but not take too much time?
15	CHAIRMAN BALLINGER: You=ve got it right.
16	(Laughter.)
17	MEMBER STETKAR: You have your thoughts
18	well formulated, ust speak every third word.
19	(Laughter.)
20	CHAIRMAN BALLINGER: Chris Brown and
21	Christiana Lui are the Federal Designated Federal
22	Officials and they do have a stun gun.
23	So, let=s see, there was something else
24	I was supposed to be reminded of.

1	Oh, with regard to the slides, the
2	problem is that I have a reputation at MIT for using
3	the most slides for anybody. So, it=s like the pot
4	calling the kettle black.
5	So, I ll turn the meeting over the Jeff.
6	MR. CIOCCO: Yes, thank you.
7	Good morning, my name is Jeff Ciocco.
8	I=m the Lead Project Manager for the APR1400 Standard
9	Design Certification Project. Thank you for having
10	us back to present and defend our Safety Evaluations
11	over these two days on Chapter 17, 19, 19.3, 19.4 and
12	19.5.
13	We will have staff and management in
14	attendance to present and respond to questions.
15	Thank you, and we=re ready to get on with
16	it.
17	CHAIRMAN BALLINGER: And the floor is
18	yours.
19	MR. SISK: And, again, thank you very
20	much, we look forward to a good discussion.
21	I do want to echo the comment, we do have
22	a large amount of material to cover. Chapter 19 is
23	a very busy chapter, so without any undue delay, I=m
24	going to turn it over to Mr. Young In and he=ll get

1	us started off on 19.1.
2	MR. IN: Thank you.
3	My name is Young In from Enercon and I
4	will be providing the general overview of the Chapter
5	19.1, basically a PRA presentation.
6	We have five gentlemen who=s going to be
7	presenting the supparts of the Chapter 19.1 and a few
8	of the names associated with each key topics, in the
9	first section will be the first session in the
10	morning will be covered by Mr. Greg Rozga and Mr.
11	Taehee Hwang.
12	And, then, hopefully, I don=t know if we
13	can cover the third topic which is beyond seismic
14	that would be Mr. Lee Dongwon.
15	And then, the rest of the presentation
16	will be covered in the later part second session
17	of the morning.
18	And then, the next slide shows the
19	presentation that s going to be given this afternoon
20	and tomorrow. So, these are on the 19.3 and 19.3
21	through 19.5.
22	The section overview of the 19.1 is
23	basically taken after the template provided in the
24	Reg Guide 1.46. It=s very similar, basically, it=s

1	the same order and we=ll cover each topic throughout
2	the morning.
3	The PRA scope for the APR1400 is
4	basically a full scope amount except the seismic
5	portion which is a PRA based SMA.
6	The only exception here is that the
7	internal flooding for the Level 2 was, you know,
8	bounded by the Level 1 because, you know, such a, you
9	know, low power in the CDR.
10	The basic methodology is and the
11	tools, you know, that were utilized to perform the
12	PRA, it=s basic methodology, you know, small event
13	tree and large fault tree approaches, linked fall
14	tree method.
15	The computer tools that we used is SAREX,
16	FTREX, CAFTA and the HRA Calculator and MAAP, RELAP
17	and MACCS.
18	And, the HRA Calculator was used, you
19	know, parts of the HRA determination in the second -
20	- played a place in the Phase 1 in the PRA, mainly
21	for the shutdown PRA and now, we are updating that
22	with the 27 update will be using the HRA Calculator.
23	And then, the these next slides the
24	next four slides are really the conclusion portion of

1	the 19.1.
2	MEMBER STETKAR: You just mentioned the
3	word update. Can you tell us what you=re doing from
4	the version of the PRA that=s in Rev 0 of the DCD
5	compared to what you mean by update?
6	MR. IN: Yes.
7	MEMBER STETKAR: I know there=s a Rev 1
8	of the DCD coming out or is out.
9	MR. IN: Yes, basically, the Rev 1 of the
10	DCD that=s coming out is, you know, results of the
11	RAI responses, you know, that we=ve been going
12	through.
13	And, the it=s, you know, basically,
14	you know, all the markups, you know, that we had so
15	far and that incorporates into one clean document.
16	That=s the Rev 1 of the DCD that=s being submitted to
17	the NRC.
18	The 2017 update, PRA update, there=s, you
19	know, actually, update of the PRA model and that
20	includes, you know, any design changes, you know,
21	that occurred, you know, during the last during
22	the Phase 2 review, you know, to the RAI responses.
23	And, we accumulated all that and then the
24	also any RAI responses, you know, that we had in the

	15
1	Chapter 19.1 that impacts the model, we are updating
2	all that.
3	And then, the all the findings, you
4	know, that we had, you know, from the peer review,
5	that=s going into this update.
6	MEMBER STETKAR: Okay, so that update
7	will be documented in some future revision of the
8	DCD, is that
9	MR. IN: Correct.
10	MEMBER STETKAR: Two or later?
11	MR. IN: Yes, hopefully two.
12	MEMBER STETKAR: Hopefully two, okay,
13	thank you.
14	MEMBER REMPE: Before you leave this
15	slide, you have here like you have MAAP and RELAP.
16	Didn=t we hear a couple weeks ago from the staff that
17	RELAP5/MOD3 is not really an accepted NRC code? And
18	that was something that you had actually had in your
19	write-up that it was.
20	And, do you remember what I=m talking
21	about with the folks from the
22	MEMBER CORRADINI: You=re talking to me?
23	MEMBER REMPE: Yes, the South Texas
24	project?

	16
1	So, this is more of a staff question, but
2	
3	MEMBER CORRADINI: But, I
4	MEMBER REMPE: What is the staff=s
5	MEMBER CORRADINI: I=m guessing the staff
6	is going to tell you they=re going to evaluate this
7	as the user using a tool, not as a generic blessing
8	of the tool.
9	MEMBER REMPE: Okay. But, again, in the
10	write-up, it had said that it was an NRC accepted
11	code.
12	MEMBER CORRADINI: Oh, right.
13	MEMBER REMPE: And so, that was something
14	that I was questionable. I can look for the reference
15	on that, but it was something in your write-up.
16	The other thing was, could you talk a
17	little bit about your philosophy for when you used
18	RELAP versus when you used MAAP?
19	MR. IN: Yes, basically, RELAP for PRA
20	was used, you know, to compliment the MAAP code, you
21	know, to determine the success break criterial.
22	MEMBER REMPE: Okay.
23	MR. IN: Because, you know, MAAP, you
24	know, on certain cases like, you know, large LOCA,

1	you know, MAAP code is not sufficient in detail. So,
2	you know, we used, you know, RELAP to do that.
3	MEMBER REMPE: Did you ever do any
4	comparisons where you would do a similar run and say,
5	yes, MAAP could do the thermal hydraulics fine until
6	we got to the core damage? Did you ever look at the
7	water level decrease, for example, and say, yes, they
8	give the same values?
9	MR. IN: Mr. Hwang?
10	MR. T. HWANG: Yes
11	MEMBER CORRADINI: This green light on,
12	sir.
13	MR. T. HWANG: Yes, we have found the
14	success correctly analysis using RELAP code per the
15	logical sequences and some of the low power shutdown
16	sequences.
17	But, pasically, we used the MAAP code for
18	the other LOCA sequences large LOCA and again with
19	small LOCA and other transients or sequences.
20	And, sometimes we compared the reset for
21	compared the reset for RELAP code using the RELAP
22	and MAAP code. But, the success created for core
23	damage is a little bit different because the RELAP
24	code is a detailed code. So, we complied the core

1	damage as a higher than 2,200 Fahrenheit degrees and
2	MAAP code is a little simplified code. So we complied
3	the core damage as 1,800 Fahrenheit degrees.
4	MEMBER REMPE: Thank you.
5	MEMBER MARCH-LEUBA: Just a
6	modification, when in the regulatory basis, when
7	a code is said approved, it means approved to be
8	to do calculations referred to technical
9	specifications.
10	So, it=s approved for it=s called
11	approved for reference because then your technical
12	specs can refer to it and you can only reference it
13	if it=s approved.
14	You can use any code you want for
15	engineering calculations that
16	MEMBER CORRADINI: As long as staff
17	reviews
18	MEMBER MARCH-LEUBA: That calculation
19	for
20	MEMBER CORRADINI: and how it=s used
21	and verified that the user is bona fide.
22	MEMBER MARCH-LEUBA: It=s perfectly
23	acceptable to use a Microsoft Excel worksheet to do
24	calculations. It s not acceptable to do a Microsoft

	19
1	Excel worksheet for set point calculations in tech
2	specs.
3	MR. IN: Can we move on?
4	CHAIRMAN BALLINGER: Yes.
5	MR. IN: Okay, next full slide is, you
6	know, really a conclusion part of the 19.1. I can
7	cover this here now or I can cover it at the end of
8	the after the other presentation is done.
9	MEMBER CORRADINI: So, since I=m sure
10	Member Stetkar has lots of questions, I want to ask
11	a delta question.
12	If I looked at CE80+ and I looked at this
13	since this, with all due respect, is a derivative of
14	CE80+, what=s the delta change? Can you at least
15	identify the delta change from what was CE80+ and
16	that estimate and these?
17	MR. IN: No, sorry.
18	MEMBER CORRADINI: Okay.
19	MR. IN: We haven=t done that comparison.
20	Because, basically, APR1400 has a lot more redundancy
21	range for
22	MEMBER CORRADINI: So, you=d expect it to
23	be different in many places?
24	MR. IN: Yes, it would be different in so

1	many different places.
2	MEMBER CORRADINI: Okay, okay. All
3	right, thank you.
4	MR. IN: So, I=ll just, you know, go
5	ahead with this in four slides and if you think it
6	needs to be covered later, you know, we=ll come back
7	to it.
8	So, basically, for the PRA applications
9	or risk applications defined in the 19.1 sub and
10	basically, there are at the COLA stage, there are two
11	programs, you know, that has a major input to the SOR
12	program. And then the severe accident management
13	design on the SAMDA and that goes into the
14	environmental report.
15	For the COR stage, the PRA will support
16	there reactor oversight program and the MSPI, SDP and
17	so forth and the maintenance role.
18	For the design improvements on the risk
19	insights, basically, the APR1400, for the design
20	certification as a reference plant which is section
21	43 and 4.
22	And, from there, we made some design
23	improvements. And, basically, these are the there
24	are five, but, you know, some may call it four.

1	Basically, the number of diesels went
2	from two diesels to four diesels, one per each, and
3	then to break up the common cause, you know, potential
4	between EDG and the AAC, we made the we changed
5	the AAC from a diesel generator to be a gas turbine
6	generator.
7	And then, also to reduce the contribution
8	from the SBO sequences, we extended the battery
9	capacity from for the 125 volt DC and basically,
10	it went from the - the one that=s, you know, critical
11	to the PRA is to be C&D and that went from 2 hours to
12	16 hours without the load sharing.
13	MEMBER CORRADINI: Again, I=m looking for
14	delta. So, if I go to Shin Kori, where is Shin Kori
15	in comparison? Is it six, five? I can=t remember
16	which one?
17	MR. IN: Three and four.
18	MEMBER CORRADINI: Three and four? Are
19	they two diesel generators, the AAC is a diesel
20	generator and this is a change in the
21	MR. IN: Yes.
22	MEMBER CORRADINI: Okay, all right. So,
23	that was one question.
24	The same question is, is the accumulator

	22
1	the fluidic device and it=s lengthening of the of
2	its operational time allow one to do the second
3	bullet? Is that the reason you can do the second
4	bullet?
5	MR. IN: No. The second bullet was, you
6	know, basically, Shin Kori 3 and 4 has, you know, a
7	common cause between the AAC and the EDG.
8	MEMBER CORRADINI: A common
9	MR. IN: Common cause failure.
10	MEMBER CORRADINI: Oh, okay.
11	MR. IN: And, basically, that comes out
12	to be one of the top causes for the SPOA sequences.
13	MEMBER CORRADINI: Okay. And, I=m sure
14	Member Stetkar knows all this, but just in case.
15	MR. IN: And, basically, because, you
16	know, these, you know, three improvements they are
17	SBO LOOP and the SBO contribution from referenced
18	plant which was about 60 percent, went down to, you
19	know, about 30 percent 36 percent.
20	MEMBER CORRADINI: Okay, thank you.
21	MR. IN: And, the other design
22	improvements that we made was that we made the changes
23	to the Tech Spec 3.67 which is related to the
24	equipment hatch closure in the modified.

	23
1	And, the last one is the from the prior
2	PRA we identified the cables for 75 components to be
3	protected.
4	MEMBER KIRCHNER: May I ask a question?
5	How early did you first do your PRA to decide to make
6	these changes? Because these changes like the first
7	two bullets I think have been in the DCD since Tier
8	1, right?
9	MR. IN: Tier 2.
10	MEMBER KIRCHNER: Tier 2?
11	MR. IN: Yes.
12	MEMBER KIRCHNER: Okay.
13	MR. IN: Yes, so
14	MEMBER KIRCHNER: So, you did the PRA and
15	then you went you looped back and you actually
16	physically changed the design?
17	MR. IN: Actually, we when we started
18	
19	MEMBER KIRCHNER: Or did you do a scoping
20	PRA very early on?
21	MR. IN: Yes, we did the scoping PRA very
22	early and we looked at the, you know, risk profile
23	from the reference plant. And, that=s when it
24	started the process.

1	MEMBER KIRCHNER: Okay.
2	MR. IN: The overall results shown here,
3	I=m not going to read the each individual number,
4	but there are for the CDF, you know, which is, you
5	know, from results for the Level 1, they=re all less
6	around the low $E-06$ and the sum adds up to be about
7	7.8, 7.9 E-06.
8	And, the Level 2 is the results shown
9	here is in a large release frequency. And they are
10	all low E-07 range. The total comes out to be 5.5 E-
11	07.
12	And, this overall CDF profile shows by
13	the operational modes and the hazard, related hazard,
14	and the largest, you know, contribution comes from
15	the shutdown internal events which is, you know, 35
16	percent.
17	And, the second one is at power internal
18	fire which is about 24 percent.
19	MEMBER KIRCHNER: So, I have another
20	question. So, is this good? It is good that the
21	wheel has essentially equal distribution from all the
22	things versus one dominating?
23	I mean, I would think it=s good, but
24	MR. IN: Yes.

	25
1	MEMBER KIRCHNER: am I wrong?
2	MR. IN: Yes, it would be good. Now, it
3	would be good to have them wholly balanced, you know,
4	profile. Here, you know, I was going to say that the
5	shutdown internal events which is, you know, mainly
6	by the operation actions.
7	MEMBER KIRCHNER: Operators, yes.
8	MR. IN: It=s somewhat conservative right
9	now at the design stage. Because, we don=t have, you
10	know, all the procedures, you know, written down.
11	And, for the at power internal fire,
12	there is, you know, somewhat conservative assumptions
13	in there and, you know, Mr. Rozga will discuss that,
14	you know, when the internal fire presentation.
15	But, yes, there are some new
16	conservatisms in the internal fire as well.
17	MEMBER KIRCHNER: I=m a little surprised
18	that the low power shutdown is such a big sector.
19	So, is that being driven mainly by operator error?
20	MR. IN: Yes.
21	MEMBER KIRCHNER: Human reliability
22	issues and so on? Because that=s rather large.
23	So, that becomes a COL task to mitigate
24	that, to reduce that risk.

	1
1	MR. IN: Yes, there are several items to
2	make sure that the shutdown program is, you know,
3	finalized and them that they will have to, you know,
4	redo the shutdown PRA.
5	MEMBER KIRCHNER: So, what were the major
6	contributors there?
7	MR. IN: We have a presentation on this.
8	MEMBER KIRCHNER: You=re going to get to
9	that?
10	MR. IN: Yes.
11	MEMBER KIRCHNER: Thank you.
12	MR. IN: Yes.
13	So, that concludes the overview of the
14	19.1 which is, you know, PRA. And, the next, we=re
15	going to the each subsection.
16	And, the first one is the at power
17	internal events Level 1 which will be presented by
18	Mr. Greg Rozga.
19	MR. ROZGA: Good morning, everyone. I=m
20	Greg Rozga from Enercon supporting KHNP and KEPCO and
21	the fire PRA and internal events PRA.
22	Am I speaking loud enough? Okay, thank
23	you.
24	The first step in any PRA is the

1	initiating events analysis and, generally, it=s
2	there=s three main steps.
3	First, we identify all potential
4	initiators that could occur and we look at various
5	industry generic sources.
6	We also do a failure modes and effects
7	analysis on all the individual systems of the plant
8	to see if failure of that system would result in a
9	unique initiator that=s not in one of the industry
10	generic sources.
11	Those initiators are then grouped
12	together based on similarity of the initiator impacts
13	on the core protection functions, common accident
14	sequence progression and common success criteria.
15	And then, finally, the initiating event
16	frequencies, the =re calculated based on generic
17	industry data and we assumed a 95 percent capacity
18	factor for the design certification.
19	MEMBER SKILLMAN: Greg, how do you know
20	there are no major orphans when you do this review
21	and account for these events? How do you know that
22	you haven=t
23	MR. ROZGA: That we haven=t missed
24	anything?

	1
1	MEMBER SKILLMAN: missed any that are
2	significant.
3	MR. ROZGA: That=s the intent of the FMEA
4	is to look all the individual systems and see a
5	failure of those systems would cause something that
6	isn=t already in the list of the various generic
7	industry sources.
8	MEMBER SKILLMAN: Thank you.
9	CHAIRMAN BALLINGER: Would this be picked
10	up on the peer review as well?
11	MR. ROZGA: Correct, correct.
12	And, there was a peer review done.
13	CHAIRMAN BALLINGER: Did they find
14	anything?
15	MR. ROZGA: Of course, yes.
16	The major list of initiating events are
17	we have various different sized LOCAs, tube
18	rupture, the LOCAs include RCP, seal LOCAs both from
19	random events as well as from system failures, failure
20	of all seal cooling injection.
21	There s a variety of transients, general
22	transient, loss of secondary site cooling, secondary
23	site steam and feedwater pipe breaks, loss of support
24	systems, loss of DC, loss of instrument error, et

1	cetera, loss of offsite power events.
2	And then, there=s also category, I term
3	induced initiators, are not real initiating events,
4	but they are initiators that are induced after the
5	initial initiator, but because these specific
6	failures significantly change the accident sequence
7	progression, we create a separate event treating
8	separate accident sequence for those.
9	And, those include things like ATWS,
10	station blackout, a stuck open POSRV LOCA. In that
11	case, it looks just like the regular LOCA, but it
12	would start and maybe you have a general transient
13	and then you have a stuck open POSRV so then we need
14	to transfer over into a LOCA tree.
15	MEMBER STETKAR: Greg?
16	MR. ROZGA: Yes?
17	MEMBER STETKAR: It struck me that this
18	list is, number one, completely in lock step with
19	NUREG/CR-6928 which it always bothers me.
20	And, number two, that it=s notably
21	lacking support system initiating events other than
22	the ones that are in NUREG/CR-6928.
23	It also bothered me that the
24	identification and grouping of the initiating events

1	was not documented in the DCA, recognizing you can=t
2	document everything in the DC.
3	So, things like, for example, failure of
4	the main transformer, how is that modeled? Is that
5	a general transient?
6	MR. ROZGA: Yes, yes.
7	MEMBER STETKAR: It strikes me that no
8	power from the main transformer is different than a
9	reactor trip on a sunny day. So, why isn=t failure
10	of the main transformer a separate initiating event?
11	Why isn=t failure of the unit auxiliary
12	transformers separate initiating event?
13	What where is the process that
14	systematically shows me that I went through every
15	electrical, fluid and ventilation system and
16	allocated them to an initiating event category?
17	Because they all must be in that general
18	transient case and it can=t be.
19	MR. ROZGA: Well, yes. Some may be a
20	subset of a loss of offsite power. So you could
21	you would say the loss of a UAT is a
22	MEMBER STETKAR: Probably not because you
23	took the frequencies from NUREG/CR-6928 and I don=t
24	know what those frequencies came from.

1	MR. ROZGA: Yes.
2	MEMBER STETKAR: They=re generic
3	frequencies for a generic site and a generic plant,
4	not your plant.
5	MR. ROZGA: Yes. In the initiating event
6	notebook, there is detail of the there are several
7	hundred events that were looked at and it=s documented
8	in there.
9	MEMBER STETKAR: It=s just striking that
10	for a plant, things that I=ve found, for example,
11	I know, and I have to be careful about comments here
12	because, obviously, I have a lot, you can lose locally
13	part of your component cooling water system, not the
14	initiating event PLO CCW.
15	You can locally lose part of your
16	component cooling water system that will give you a
17	plant trip and put you in jeopardy of a seal LOCA and
18	the frequency of that may be comparable to the total
19	frequency that you=ve used for partial loss of
20	component cooling water.
21	Yet, you=ve not identified that as an
22	initiating event.
23	MR. ROZGA: Well, we have partial loss of
24	CCW, partial

1	MEMBER STETKAR: Yes, you do. My that
2	partial loss of CCW, I don=t I know where the
3	frequency came from. You=re using it from NUREG/CR-
4	6928 which, again, is a generic plant.
5	I don=t know how many component cooling
6	water trains or pumps or pipes or valves a generic
7	component cooling water system has because they=re
8	all different.
9	And, I know I read in the DC that you did
10	site specific fault tree analyses, but you didn=t use
11	those for the initiating event
12	MR. ROZGA: Right. And the
13	MEMBER STETKAR: frequencies.
14	MR. ROZGA: The numbers in 6928 were
15	slightly more conservative than the numbers from the
16	fault trees.
17	MEMBER STETKAR: Oh, okay.
18	I=m just curious that the given what
19	I know about the design, the lack of design specific
20	kind of goes to what Dick was saying. The lack of
21	design specific support system initiating events
22	seems striking.
23	And, I=11 ask the staff about that when
24	they come up as far as how much of an audit they did

1	of the initiating events.
2	And, in the interest of time, I=ll be
3	quiet now.
4	MR. ROZGA: Next slide, please?
5	All right, once we have the initiators,
6	the next thing we do for each one of those initiating
7	events is we define the accident sequence analysis
8	and these are modeled in the form of event trees.
9	And, the event trees model, the accident
10	progression and the manner consistent with the plant
11	design, operating procedures and expected plant
12	response, thermal hydraulic analyses are used to
13	determine the systemic success criteria for each
14	branch in the event tree.
15	And, fault trees are used to model the
16	mitigating system failure probabilities with respect
17	to those success criteria.
18	And, the fault trees include both
19	equipment failures as well as human failure events
20	leading to the individual system failures.
21	And, since the fault threes are directly
22	linked to the event tree branches, the inner system
23	and sequence dependencies are inherently considered.
24	MEMBER BLEY: Greg?

1	MR. ROZGA: Yes, sir?
2	MEMBER BLEY: I=m going to follow up on
3	what Mr. Stetkar asked you before.
4	This is a design cert PRA and I know here
5	the requirements are a little different than for COL
6	and certainly different from prior to fuel load PRA.
7	Should there actually be one of these
8	built in the United States someday, at what point do
9	you think it would be necessary to move from generic
10	initiating event frequencies with what might be
11	conservative or might be pessimistic, depending on
12	how the real design turns out to be generic initiating
13	events and groupings, when would that turn into design
14	specific evaluation of initiating event groups and
15	frequencies?
16	MR. ROZGA: In general, once the system
17	design is more 100 percent complete. One of the
18	service water and CCW system are some of the systems
19	that are all tied to the main power block. They have
20	their own buildings and those
21	In fact, in the PRA update that we=re
22	doing now, there have been some changes to those
23	systems. And, those are some of the reasons why,
24	when we initially did the support state initiating

event fault trees, 1 we ended up going with the generic 2 data because we knew that those system designs weren=t 3 completely locked down. 4 I will say that even existing nuclear 5 plants use the generic data for their initiating event 6 frequencies. However, they do update it with plant 7 specific data. things like, you 8 And so, some know, 9 LOCAs, tube ruptures, various other systemic 10 initiators, some will -- well, even at the end of the design certification, we=ll use the generic data when 11 12 those secondary support systems are -- when the design 13 is finalized then those will likely use support state 14 initiating event fault trees which will be a more 15 accurate representation. 16 we felt it was, at this time, okay 17 the generic data for those support state initiators because the numbers were -- they were 18 19 They were a little bit greater than so we close. 20 didn=t think that we were losing anything. 21 MEMBER BLEY: this I=mnot on 22 Subcommittee and Ι admit I haven=t fully 23 everything in detail. Do you make that at all clear 24 in the Chapter 19

	36
1	MR. ROZGA: Make it clear when we I
2	think we identify in Chapter 19 that we=re using the
3	generic data.
4	MEMBER BLEY: Without regard to the
5	design details of the system?
6	MR. ROZGA: Yes, for those support state
7	initiating events, yes.
8	MEMBER BLEY: I=ll have to look because
9	I didn=t see that in the quick look.
10	MR. ROZGA: Yes, I think it=s in a table,
11	but don=t quote me. But, I believe there=s a footnote
12	in the table that says that that=s where they come
13	from.
14	MEMBER BLEY: Okay, thanks.
15	MR. ROZGA: You=re welcome.
16	I think part of this slide, Mr. Hwang
17	already talked about with Joy=s question, but,
18	ultimately the accident sequences and the success
19	criteria analysis that=s done is for the Level 1
20	analysis is based on preventing, trying to prevent
21	core damage.
22	And, the core damage criteria that we use
23	is consistent with supporting requirement SEA 2 of
24	the ASME standard as endorsed by the NRC and Reg Guide

1	1-200.
2	And, there=s the 2,200 degrees for RELAP
3	and 1,800 for MAAP.
4	And, we already kind of discussed
5	earlier, you know, where those codes are used.
6	Before we go any further, there=s some
7	key PRA assumptions that feed into some of the system
8	modeling, some of the event tree modeling. And,
9	there was no good place to put it, so I just kind of
10	put it here and we can go through them and I=m sure
11	John will have many questions on this slide.
12	As much of all the models for the fire,
13	flooding and seismic, as much as we had, we used the
14	APR1400 design information.
15	The reference plant, Shin Kori 3 and 4,
16	we used that design information when the design
17	information was not available.
18	The digital I&C system, that one we
19	specifically are currently using, the hardware model
20	from Shin Kori 3 and 4.
21	Medium LOCA, our medium LOCA is the two
22	to six inch range and the design basis small LOCA
23	goes up to nine inches. So, therefore, we don=t
24	require hot leg injection for medium LOCA. We only

1	require hot leg injection for large LOCA.
2	At the time, the Rev 0 DCD was developed.
3	The model supporting that, the RCP seal LOCA testing
4	NW CAP was not finalized at that time. So, we used
5	some engineering judgment. We do now have that W CAP
6	and we are doing a detailed RCP seal LOCA analysis in
7	the model.
8	But, what we have currently in the model
9	is there is a generic number from 6928 for just a
10	random RCP seal LCCA. You=re running fine and all of
11	a sudden the seal just fails.
12	And, the size of those breaks fall within
13	the small LOCA so we include that frequency within
14	the small LOCA frequency and we evaluate it within
15	the small LOCA event tree.
16	The seal LOCAs caused by post-trip loss
17	of seal injection and thermal barrier cooling, that
18	is based on engineering judgment, just based on
19	experience with other seal LOCA models.
20	We have 1E-3 failure rate per reactor
21	seal and that includes the operator action to trip
22	the reactors, if they need to.
23	Or, I m sorry, the reactor coolant pumps,
24	if they need to.

]
1	And, the actual failure of the seals
2	themselves.
3	For GSI-191, APR1400 is classified as a
4	low fiber plant. And, therefore, although we do
5	model some plugging, we don=t model the chemical
6	effects.
7	CHAIRMAN BALLINGER: The Shin Kori 3 and
8	4 have a very different digital I&C system than
9	APR1400, is that correct? Is it different it=s a
10	COMMON Q, right? Is Shin Kori
11	MR. ROZGA: Yes, the Shin Kori
12	CHAIRMAN BALLINGER: 3 and 4, are the
13	COMMON Q as well?
14	MR. IN: Yes.
15	CHAIRMAN BALLINGER: Oh, okay. I
16	thought they were different.
17	MEMBER STETKAR: Greg, let=s reactor
18	coolant pump sea LOCAs, you said that you=re
19	that=s one of the changes, I think you said, that
20	you=re making to the model based on
21	MR. ROZGA: The PRA update based on the
22	W CAP.
23	MEMBER STETKAR: Our PRA Subcommittee has
24	been briefed rather recently on a Westinghouse model

1	for their Generation 3 shutdown seals. And, I have
2	to be careful because that is all proprietary and,
3	although Rob has Westinghouse, I don=t know who has
4	what information and this is a public meeting, so I
5	can=t say very much.
6	We=ve not seen the W CAP that you=re
7	referring to, nor do we know anything about your
8	particular seal design.
9	The 10 to the minus 3 conditional failure
10	probability per seal after loss of all cooling strikes
11	me as numerically somewhat optimistic compared to
12	many other models for other types of pumps and seals
13	that I=ve seen.
14	So, I m hoping that, at some time, we=11
15	be able to look at the W CAP report and the basis for
16	whatever changes you=re making to your models.
17	MR. ROZGA: Yes, the
18	MEMBER STETKAR: I=ll just leave it at
19	that.
20	MR. ROZGA: Yes, the engineering judgment
21	also, it was based on preliminary information. But,
22	the W CAP wasn=t complete. So, it says in one of the
23	older seal designs that did have higher conditional
24	failure probabilities.

1	MEMBER STETKAR: Let me I don=t know
2	where to at the end, I=m going to let you get
3	through let me just be quiet. I=ll let you get
4	through all of 19.1.4.1 because I have several
5	comments to make on event modeling and it=s better to
6	just let you get through the end and then come back
7	to the discussion
8	MEMBER KIRCHNER: Greg, may I back up one
9	slide
10	MR. ROZGA: Sure.
11	MEMBER KIRCHNER: or two?
12	Just, would you familiarize me with how
13	you apply that success criteria? I don=t know the
14	PRA standard firsthand. So, you have peak
15	temperatures, how do you is it an on/off success
16	criteria?
17	MR. ROZGA: Correct, there=s
18	MEMBER KIRCHNER: Or is there a band.
19	Say you=re running the temperature up to 2,150 degrees
20	or 2,1999, how is that success criteria applied?
21	MR. ROZGA: Yes, well, there=s several
22	success criteria runs that are made to support. And,
23	you change your inputs, basically change the
24	equipment that you = re relying on and you increase the

1	number.
2	And, we tried to ensure that you are at
3	a safe, stable state that we=re not at 1,201 and still
4	increasing by the 24 hours. We don=t stop at that
5	point and say, well, we=re good, because we know that
6	we won=t be.
7	MEMBER KIRCHNER: Maybe I didn=t phrase
8	my question very well.
9	How much uncertainty band is applied to
10	the RELAP and MAAP calculations? In other words, you
11	come up to some thermal limit, regardless of how the
12	systems function or not and so on.
13	When do you say you=ve tripped? You
14	don=t succeed? Is it just on/off at 2,200?
15	MR. ROZGA: Yes.
16	MEMBER KIRCHNER: Interesting. Okay,
17	thank you.
18	MEMBER POWERS: I mean, I don=t think
19	that=s I mean, I think that=s the way the criterion
20	is supposed to be used. That there is a margin
21	inherent in the 2,200 that is claimed by the NRC and
22	doesn=t make available so they didn=t have I
23	mean, it=s okay for him to take
24	MEMBER KIRCHNER: I understand, I was

	43
1	just thinking through the uncertainty in the actual
2	analysis.
3	MEMBER POWERS: Yes, I mean, that=s a
4	very legitimate concern you make. But, I think that
5	the presumption has always been that the NRC=s already
6	built a margin into that number.
7	Now, presume if I came in with a really,
8	really awful code that vastly under predicted
9	temperatures and things like that, that that would
10	get flagged in the process.
11	MEMBER KIRCHNER: All right, yes. Thank
12	you.
13	MEMBER MARCH-LEUBA: So, let me ask the
14	question a different way.
15	Is this a best estimate calculation or
16	best estimate plus uncertainty calculation?
17	MR. ROZGA: Best estimate.
18	MEMBER MARCH-LEUBA: Okay. Not okay.
19	MEMBER KIRCHNER: Okay, thank you.
20	MR. ROZGA: All right.
21	The systems modeled in the PRA, there is
22	several front line systems. You have your secondary
23	side cooling water systems, your safety injection
24	systems, CBCS, reactor protection system.

	44
1	And then, all those systems that support
2	the continued operation of your front line systems,
3	all your cooling water systems, HVAC, chillers,
4	instrument error, SFAS, et cetera.
5	MEMBER CORRADINI: So, can let me ask
6	a question at this point.
7	So, after if you were to look at this
8	PRA before Fukushima and after Fukushima, would you
9	have do you operate or assume operation of the aux
10	feed differently?
11	In other words, a takeaway from Fukushima
12	is, gee, I=d like to find a way to always use aux
13	feed as long as it=s available come hell or high
14	water.
15	Is anything changed in the emergency
16	operating procedures or have you assumed operation
17	actions that essentially try to optimize the use of
18	aux feed so that I don=t get into a, which I=m sure
19	Dr. Rempe will ask a high dry low.
20	MR. ROZGA: With respect to the operating
21	procedures, that I don=t know. I do know that there
22	are guidelines for refilling the aux feed water
23	storage tanks to extend the life of aux feed water.
24	But, the details of the operator action, I don=t know.

	45
1	Young, do you?
2	MR. IN: Yes, my name is Young In.
3	Basically, all the lessons learned, you
4	know, from the Fukushima accident, it=s covered in
5	the 19.3.
6	MEMBER CORRADINI: Oh.
7	MR. IN: But, yes, 19.1 does not go into
8	the extended condition.
9	MEMBER CORRADINI: Okay. But, okay.
10	But, that, in some sense, is changes. What I=m trying
11	to get what I=m kind of searching for is, is there
12	some assumptions about a change in how you try to use
13	aux feed in the PRA or is if I was here in 2017
14	and we were doing this whole thing in 2010, I would
15	still assume the same sorts of things in how aux feed
16	behaves and how I use it as I get beyond the design
17	basis, that=s what I=m trying to ask.
18	MR. IN: Correct, it=s in the PRA space
19	because
20	MEMBER CORRADINI: It doesn=t matter
21	where we are compared to Fukushima on how you do the
22	base PRA?
23	MR. IN: Yes, we haven=t integrated the,
24	you know, Fukushima lessons learned in the, for

	11
1	instance, in because, you know, this is, you know,
2	design certification stage. We didn=t integrate any
3	of the operating guidelines such as, you know, FSG.
4	MEMBER CORRADINI: Okay.
5	MR. IN: So, those went in separately and
6	analyzed in the 19.3.
7	MEMBER CORRADINI: Okay. But, you
8	understand my question?
9	MR. IN: Yes, we understand.
10	MEMBER CORRADINI: Okay, thank you.
11	MEMBER SKILLMAN: Greg, a question,
12	please.
13	For your front line systems, just two as
14	an example, aux feed and main feed, how are the, for
15	instance, lubricating oil systems for those pumps
16	addressed in the PRA?
17	MR. ROZGA: The lubricating system for
18	individual pumps is within the component boundary of
19	the pump with the exception of the external cooling
20	water systems that would cool the lube oil coolers,
21	say for instance.
22	And, that=s a function of the data
23	analysis when the data is collected on the pump if
24	the pump fails because of the lubricating system

	47
1	failure or if it fails because of a bearing wipe of
2	if it fails for whatever reason, that=s all included
3	within the boundary of the individual component.
4	MEMBER SKILLMAN: Thank you.
5	MEMBER STETKAR: Greg, just one question.
6	MR. ROZGA: Yes, sir?
7	MEMBER STETKAR: And, front line systems,
8	you didn=t list ECSBS, I got it right. I always
9	and it=s kind of in there for Level 1, it=s kind of
10	in there for Level 2.
11	MR. ROZGA: We don=t credit it in Level
12	1.
13	MEMBER STETKAR: Oh, okay.
14	MR. ROZGA: We have it in there as a
15	sensitivity.
16	MEMBER STETKAR: Okay, okay. But, it is
17	modeled explicitly for the
18	MR. ROZGA: Yes.
19	MEMBER STETKAR: benefit of the rest
20	of the Committee, ECSBS is, indeed, a FLEX system.
21	It=s an external emergency containment spray backup
22	system. And, it=s it looks like a FLEX system and
23	it is explicitly modeled in the PRA.
24	MR. ROZGA: And, for the Level 1 PRA,

	
1	there is a flag that=s set to trigger that. That
2	fails it for the evel 1 analysis. So, we do it=s
3	explicitly in the model, but we do not credit it
4	MEMBER STETKAR: It=s in the model? It=s
5	just
6	MR. ROZGA: on Level 1, though.
7	MEMBER STETKAR: this just says
8	systems modeled in the PRA and it=s
9	MR. ROZGA: Oh, okay.
10	MEMBER STETKAR: in the PRA.
11	MR. ROZGA: Yes.
12	MEMBER STETKAR: It just isn=t in the
13	Level 1
14	MR. ROZGA: That is correct.
15	MEMBER STETKAR: PRA kind of
16	quantification.
17	MR. ROZGA: Correct, it=s not in the
18	quantification.
19	MEMBER STETKAR: I just wanted to make
20	sure that the Committee was away, especially from
21	what Mike asked about Fukushima and some things.
22	MEMBER CORRADINI: The reason I=m focused
23	on this is for other studies. There=s this great
24	intensity to try to figure out how does aux feed or

1	RCIC work for extended times.
2	And, it strikes me this would be a time
3	to see how it would behave under your situation,
4	particularly because I=m guessing we=re going to come
5	back and ask about steam generator tube rupture and
6	timing of it compared to other things.
7	And, one can delay that or preclude that
8	if you had aux feed working water on the times.
9	MR. ROZGA: That=s fine.
10	Okay, Young, next slide, please?
11	MEMBER BLEY: Let me toss something in.
12	Well, there=s a difference between what=s done in PRA
13	and what=s done in licensing safety analysis.
14	And, PRAs almost forever, all of the
15	systems that are available or could be available are
16	modeled so aux feed water, RCIC would be modeled for
17	different usages.
18	Fan coolers sometimes would be modeled
19	for containment heat removal if they=re there.
20	And, sometimes the probabilistic
21	likelihood of availability over long term is
22	included.
23	So, in the PRA, those kind of things that
24	are, I think, you = re bringing up, have always been

1	part of the modeling.
2	MEMBER CORRADINI: Okay. But, so,
3	here=s where I=m going with this. Is there something
4	in the emergency operating procedures that tell you
5	to shut off aux feed when you should try to keep it
6	on?
7	In other words, is there a directive that
8	you follow now that I would change because of what
9	I=ve learned from Fukushima to keep this thing going
10	longer?
11	MEMBER BLEY: That=s a possibility and
12	it=s certainly design specific and it could even be
13	plant specific at times.
14	MEMBER CORRADINI: Well, and the only
15	reason I ask
16	MEMBER BLEY: And, they don=t have their
17	operating procedures yet, right, or do you?
18	MR. ROZGA: We have EOGs, the Emergency
19	Operating Guidelines at this point.
20	MEMBER BLEY: Okay.
21	MEMBER CORRADINI: Well, the only reason
22	I=m asking the question is, I=m looking back to what
23	we=re going to discuss in other venues about steam
24	generator tube rupture and timing of it relative to

1	a station blackout at high pressure.
2	MEMBER BLEY: No, and I think that=s a
3	really good point and, you know, depending on the
4	PRA, you know, if you=re not if your procedures
5	aren=t built to support it, it at least becomes a lot
6	less likely that you do those kind of things.
7	MR. ROZGA: All right, the data and
8	common cause data are used for equipment failure rates
9	and it=s generally from NUREG-6928. There are some
10	other data sources were used when 6928 did not provide
11	that data.
12	And then, as a last resort, if we had no
13	data source, then we used engineering judgment.
14	An example was the RCP seal failure that
15	we discussed earlier, the 1E to the minus 3 per pump.
16	We don=t have any plant specific data and
17	there is no generic data for air dryer, test and
18	maintenance on availability.
19	So, yes, I don=t know why it=s not in
20	6928, John. But, it wasn=t. So, we have a number
21	in there based on, you know, plant operating
22	experience, what we think would be a reasonable
23	number.
24	Human reliability analysis is a major

	52
1	part of PRAs and the evaluation is based on standard
2	industry methodologies.
3	The model includes about 60 pre-
4	initiator, Type A HRAs and those are things that
5	happened prior to the event that could impact the
6	event.
7	There could be the operators miscalibrate
8	something or they don=t realign a system post-
9	maintenance test correctly.
10	So, we tried to identify those and insert
11	them in the model.
12	Type B initiating events are only for
13	initiating event fault trees. And, since we=re just
14	using generic data, we have no Type B initiators at
15	this point.
16	And, those would normally be if you fail
17	a train, the operator would try to start the alternate
18	train to prevent the trip.
19	Type C, those are the yes, sir?
20	MEMBER STETKAR: In remind me in
21	your internal flooding models, do you include
22	operator actions to either close flood barriers or
23	open drain paths typically of flood?
24	MR. ROZGA: There are a few instances for

	[]
1	specific flooding scenarios.
2	MR. DREMEL: Ray Dremel from Enercon.
3	The answer to that is no. We have
4	operator actions -
5	MEMBER STETKAR: Okay, a few apparently
6	is zero.
7	MR. DREMEL: Yes, we have operator
8	actions to isolate a break before a certain volume of
9	water would be released.
10	MEMBER STETKAR: Okay.
11	MR. DREMEL: But, we have no operator
12	action to open a drain.
13	MEMBER STETKAR: But, that=s okay, the
14	first one is one that I was asking about. Isn=t that
15	an operator action that contributes to the initiating
16	event frequency that you finally quantify in your
17	model such that, if they failed to isolate the break
18	within a certain time window, you would then have
19	enough water entering a compartment to be a flood?
20	MR. DREMEL: Yes.
21	MEMBER STETKAR: Okay.
22	How do you account in your model then for
23	dependencies between that operator action and
24	subsequent operator actions after you draw the dotted

	[]
1	line in the sand and say I now have an initiating
2	event?
3	MR. DREMEL: We do the we do a
4	dependency among all the operator actions and we saw
5	the cut sets with all the human failure events set
6	for relatively high.
7	MEMBER STETKAR: So, do you have a fault
8	tree then that shows that operator action as a basic
9	event in the fault tree model for the flooding
10	initiating event?
11	MR. DREMEL: Yes.
12	MEMBER STETKAR: Okay, thank you.
13	MR. ROZGA: The last type is the post-
14	initiator HEPs and we have about 70 of these. And,
15	these are things like the operator fails to initiate
16	feed and bleed when required.
17	One of the most important things with the
18	operator actions are the dependencies between the
19	actions. You can get several cut sets where you have
20	several operator actions and those cut sets, because
21	there are so many HEPs in them, would tend to get
22	truncated.
23	So, what we do to make sure that we
24	capture them is, prior to quantifying, we set all of

1	the HEPs to a very high number, very close to one.
2	We quantify and then we identify all of
3	the combinations. And then, the potentially
4	dependent HEP combinations are evaluation or, I=m
5	sorry, are evaluated based on dependency level
6	decision trees and NUREG-1921.
7	And, they look at things like timing,
8	crew, recovery from other individuals.
9	And then, the dependencies are inserted
10	then at the end of the model with during the post-
11	processing of the cut sets.
12	So, by doing that, we ensure that we
13	capture the dependencies.
14	Did - all right, make sure we=re on the
15	right slide.
16	The quantification is performed. We
17	already talked before about SAREX and CAFTA, the
18	codes.
19	The truncation level that we quantified
20	at is at E-13 for all models. And that=s about six
21	to seven orders of magnitude below the CDF.
22	We use a variety of flagged files, house
23	events and recovery files, et cetera, during the
24	quantification to control the quantification process

	56
1	for each model. And, those things may turn off ECSBS,
2	for instance, like we were talking about with John
3	before.
4	We used the delete-term logic to remove
5	unrealistic minimal cut sets, LCO, or Tech Spec
6	disallowed maintenance combinations, for example.
7	And then, actually, prior to the
8	quantification, we break circular logic loops that
9	inevitably end up in your logic.
10	The final step in the quantification
11	process is called recovery. And, there=s a recovery
12	file where we read it, each individual cut set and
13	then we apply recovery based on those cut sets.
14	Mainly used for applying the HRA
15	dependencies, but you can all insert offsite power
16	recovery rules and the such.
17	This is a CDF distribution by initiating
18	event. As Young had mentioned earlier, it=s still
19	dominated by SBO and LOOP. It=s much less than it
20	was for the reference plant. There, it was about 60
21	percent, if I=m correct.
22	You see the other TLO, CCW and that=s a
23	total loss of CCW and total loss of ESW system, those
24	lead to RCP seal LOCAs.

	J
1	And, the uncertainty analysis, we did a
2	parametric uncertainty analysis post-quantification.
3	And, there were selected sensitivity analyses that
4	were performed.
5	There is currently an open item on
6	generally overall on the uncertainty analysis and
7	sensitivity analysis and we=re working with the staff
8	at this time at resolving that.
9	And, unless John has no questions, then
10	
11	MEMBER STETKAR: In the words of Leslie
12	Nielsen, surely you jest. Don=t call me Shirley,
13	I=ll be Frank.
14	I promised Ron that I=d try to keep this
15	constrained and short. So, what I=d like to do is
16	highlight three or four issues that I identified
17	during my reviews of the models. And, all of this
18	information is in the DCD.
19	And, I only want to highlight these
20	because I think that they=re I have many, many,
21	many other comments that are kind of lower importance
22	than this. But -
23	The first issue is reactor coolant pump
24	seals. And, I mentioned a number there, that 10 to

	58
1	the minus 3 and I know that you=re changing those
2	models.
3	When went through the models, it struck
4	me that the reactor coolant pump seal LOCAs are
5	questioned in all of the usual suspect event trees.
6	They=re questioned in station blackout.
7	They=re questioned in those partial and total losses
8	of component cooling water and essential service
9	water.
10	They=re not questioned in most other
11	event trees, which is curious.
12	One thing that is notable on this plant
13	compared to many plants is that although it contains
14	four trains of some equipment, and I=ll use the term
15	train here, like t has four component cooling water
16	pumps nominally, and those are part of the certified
17	design because they=re inside the walls.
18	It has nominally four essential service
19	water pumps. Those are not part of the certified
20	design, they=re kind of outside the walls. It has
21	four safety injection plant pumps.
22	It basically, though, has a it=s a two
23	division plant.
24	MR. ROZGA: That=s correct.

1	MEMBER STETKAR: So, for example, there
2	are two divisions of component cooling water once you
3	get all the plumbing taken care of.
4	The - all of the cooling for the reactor
5	coolant pumps, the auto coolers, the motor air
6	coolers, the thermal barrier coolers, is supplied
7	from Division 1, not supplied from Division 1 and
8	Division 2. There-s manual crosstie valves that the
9	model doesn=t account for.
10	So, what I=m getting to is there=s an
11	asymmetry and a pretty strong asymmetry so that, for
12	example, the reactor coolant pump seal failure
13	contribution is much more dependent on failures of
14	component cooling water, essential service water,
15	Division 1 than it would be of Division 2.
16	MR. ROZGA: Correct.
17	MEMBER STETKAR: So, there=s an
18	asymmetry.
19	Because of that asymmetry and the fact
20	that there=s only one division is one of the reasons
21	why perhaps some of those support system initiating
22	events that are grouped with general transients on
23	this particular plant might be more interesting than
24	just a general transient.

1	The real concern I have with lack of
2	completeness, perhaps, in modeling the reactor
3	coolant pump seal LOCA is partially due to what we
4	see in Level 1, core damage frequency.
5	It=s more important, I think, for Level
6	2. And, I wanted to this is why I want to kind of
7	intercept it here as we go from Level 1 to Level 2.
8	We=ll hear in Level 2 that this PRA
9	explicitly does account for consequential tube
10	failures, high dry load scenarios, if you will.
11	This PRA also explicitly accounts for the
12	fact that if you have a reactor coolant pump seal
13	LOCA, there is a very high conditional likelihood
14	that the loop seal in the affected loop will clear.
15	And, if the loop seal clears, there is an
16	extremely high, like guaranteed, probability that you
17	have a thermally induced tube rupture.
18	That makes the reactor coolant pump seal
19	LOCAs really, really interesting in terms of tracking
20	Level 2 large release frequency results.
21	And, I=m not sure that the models
22	completely account for those contributions. Of
23	course, you know, the numerical effects will depend
24	on whatever your revised model of the conditional

1	probability of the seal failure is.
2	But, even without that, there are I think
3	some effects, for example, from the loss of instrument
4	initiating event that may make you vulnerable to
5	more vulnerable to seal LOCA. It may not guarantee
6	a seal LOCA, but within a pump away or something like
7	that for the seal LOCA.
8	But, the seal LOCA is not modeled in that
9	particular event tree.
10	So, my concern about the completeness of
11	the seal LOCA modeling under what initiating events
12	are you asking the question, do the seals fail, is
13	partly a concern about Level 1 core damage frequency.
14	Because, even with the model that=s in there, we see
15	some contribution from it.
16	But, to me, it=s even more important for
17	Level 2 in the sense of, if you do have a seal LOCA
18	and you go to melt at a relative at a high pressure,
19	you get clearing the seals. And, if you then have
20	nothing in the secondary side of one of your steam
21	generators, it=s not a good day.
22	So, that=s one of the issues that I want
23	to bring up. I don=t know if you want to reply to
24	that. I didn=t have a real question in a sense other

1	than trying to get a concern on the record here.
2	MR. ROZGA: The one thing that I will say
3	with respect to the thermal barrier cooling coming
4	directly from the Alpha train, if we were to split
5	and have did one, did two RCPs and did another two
6	RCPs, you basically will double.
7	MEMBER STETKAR: There=s no easy way
8	around the problem.
9	MR. ROZGA: Yes, yes, yes.
10	MEMBER STETKAR: No, that=s what you said
11	is there=s no easy around it.
12	MR. ROZGA: Now, there are crossties that
13	could be credited. Right now, you have, you know,
14	the
15	MEMBER STETKAR: They could that all
16	it=s a timing analysis.
17	MR. ROZGA: It=s a timing analysis and
18	there is
19	MEMBER STETKAR: And, that=s why
20	MR. ROZGA: there is manual valves
21	that would have to be opened. And, without
22	procedures and without knowing exactly how far away
23	the CCW heat exchanger belt.
24	So, at this point, we just

1	MEMBER STETKAR: No, no, I know what=s in
2	the model and I kind of know why it=s there. But,
3	given that asymmetry, that=s, as I said, I don=t
4	really have a question, I just, you know, if I said
5	anything wrong, I would have expected you to come
6	back and say, no, you=re lying, it=s wrong. But, I
7	was pretty sure about that one.
8	So, that=s one issue, the seal LOCA,
9	completeness of the seal LOCA modeling and its
10	relationship to both Level 1 and Level 2.
11	The second one is also related to the
12	consequential tube rupture, Level 2 more than Level
13	1. And, there=s kind of two parts to this one.
14	If you go back to go back to your pie
15	chart. Well, you won=t see it on this, I=m sorry.
16	You won=t see it on Level 1. We=ll see it on Level
17	2, but again, I want to get people sort of oriented
18	before we get into the Level 2 discussion.
19	The current the PRA evaluates large
20	steam line breaks upstream and downstream from the
21	MSIVs and you see a little bit of a contribution here
22	from large steam line breaks downstream. You don=t
23	see any contribution here from large steam line breaks
24	upstream.

	[]
1	When we see Level 2, you=11 see even a
2	larger disparity between those two.
3	At the moment, large steam line breaks
4	upstream of the MSIVs, it is assumed that they are
5	all inside containment. Is that true?
6	MR. ROZGA: Correct.
7	MEMBER STETKAR: Okay.
8	That, in a, to me, in a one sense may be
9	considered, I=m going to try to not use words that I
10	don=t like to use that might be worse for evaluating
11	energy release into the containment.
12	It, however, is much better for
13	consequential tube ruptures because, if I have a steam
14	line break in a steam generator upstream of the MSIVs,
15	I cannot isolate t. It will continue to blow down.
16	And, if the operators isolate feedwater
17	as they=re mostly instructed to and parts of it is
18	automatic, I can get a dry and low condition on that
19	steam generator fairly easy.
20	Right now, that does not contribute to
21	any Level 2 because all the releases are inside the
22	containment.
23	If the break was between the containment
24	wall and the MSIV outside of the containment, all of

1	those releases would go outside, well, they=d go to
2	the main steam valve room and, you know, out that
3	way.
4	So, one of the sources of concern that I
5	have about the steam line break upstream of the MSIV
6	model is the fact that it=s all all of those breaks
7	are allocated to only inside the containment. None
8	of them are allocated between the containment wall
9	and the MSIV, where there are a lot of welds.
LO	There s risers for all of the safety
11	valves. There's risers for the main steam
12	atmospheric dump valve, so there=s a lot of welds in
L3	that line. I don t know how big is a big or how big
L 4	is a small.
L 5	So, that=s another concern that I have,
L 6	more for the Level 2 analysis than the Level 1
L7	analysis.
L 8	Dr. Corradini?
L 9	MEMBER CORRADINI: May I interrupt you in
20	your disposition?
21	MEMBER STETKAR: You may because I=m
22	going to switch gears to a different issue.
23	MEMBER CORRADINI: So, since you kind of
24	educated me before we got together for this about

	[]
1	this, so it=s the procedure you just said about
2	isolating that I don=t understand.
3	In other words, I have a break or a leak
4	and I start depressurizing and the instruction is to
5	isolate aux feed. That=s what I=m confused about.
6	MEMBER STETKAR: At many plants, it is.
7	I don=t know what s assumed in this model. I think
8	it is assumed that they would do that.
9	MEMBER CORRADINI: This why I asked the
10	question earlier. But, he=s much more subtle in
11	whether it=s upstream or downstream.
12	But, I=m just concerned that, if you
13	isolate aux feed when you it=s workable, you would
14	never then generate a low dry condition.
15	MEMBER STETKAR: It=s not at all clear if
16	you got a big hole open to the environment whether
17	you can, you know, keep it full. Eventually you can
18	maybe. I don=t know.
19	MEMBER CORRADINI: But, that=s the reason
20	I was asking the question.
21	MEMBER STETKAR: I know.
22	MEMBER CORRADINI: Because, the way you
23	talk us through this is the aux feed is shut off by
24	procedure.

	II 67
1	MEMBER STETKAR: It=s not I know that
2	it=s not shut of automatically in this plant, aux
3	feed is not. Some plants do it automatically and
4	this plant, I couldn=t find any signals or that
5	isolate it automatically.
6	MR. DREMEL: It=s typical in
7	MEMBER STETKAR: You have to come you
8	still have to come to the microphone.
9	MR. PREMEL: Sorry, Ray Dremel with
10	Enercon again.
11	It=s typical in most U.S. plants that, if
12	you have a secondary side line break, you stop feeding
13	the faulted steam generator for many concerns.
14	One is, the operators are concerned about
15	killing their people. You know, you don=t want the
16	steam going into the people tank, so to say.
17	So, the operators initially will turn off
18	aux feed water until they can figure out what is safe
19	to do and where can I send my people?
20	So, we model the operators isolate the
21	feedwater aux feedwater to the faulted steam
22	generator.
23	MEMBER STETKAR: The other one typically
24	is they don=t like to be in a situation where you

	[]
1	have an uncontrolled cool down going on. They like
2	to be able to hold temperature and pressure and things
3	in a way, you know, in a regime that they can actively
4	control it and then walk the plant down. So, that=s
5	another.
6	So, that=s I=m going to try to finish
7	this stuff by 10:00 so that we can go on with the
8	rest of it.
9	The other concern that I have regarding
10	steam line breaks now is that, it=s my understanding
11	that what I=ll call small steam line breaks upstream
12	of the MSIVs. Some people might call them spurious
13	opening of main steam safety valves. You can give it
14	any name you want to, but it=s the kind of thing where
15	you can either break the riser off or the main steam
16	safety valve decides that it wants to open spuriously.
17	Those events, as I understand it, are now
18	grouped with general transient. Is that true?
19	MEMBER CORRADINI: I believe so, yes.
20	MEMBER STETKAR: Okay.
21	The concern I have about that is that, if
22	one of those happens, I don=t know whether an
23	automatic reactor trip will occur on this plant
24	because I=m not familiar with all of the trip set

1	points.
2	I kind of know what the capacities of the
3	safety valves are, it depends on where your high power
4	or your turbine versus reactor power trip set points
5	are. You may or may not get an automatic trip is
6	and I=m not sure. Apparently, I don=t know.
7	However, if the plant does trip either
8	manually or automatically, you then have a situation
9	where you=re relieving a fairly good fraction of your
10	rated steam flow out through this stuck open valve.
11	And, you probably will get an over
12	cooling event. You certainly do have a you=ll get
13	a safety injection.
14	You have an uncontrolled cool down. And,
15	if I now go to core melt at high pressure, don=t I
16	have now a high dry low with an open offsite relief
17	path?
18	And, there=s no way for your current
19	models to capture that because it=s all a general
20	transient.
21	So, that=s those are my concerns about
22	steam line breaks. Big steam line break location
23	inside the containment, in summary, and no separate
24	model for whether you want to call it a small steam

	70
1	line break or a stuck open a spuriously open main
2	steam safety valve upstream of the MSIVs not
3	distinguished as a separating initiating event to
4	track.
5	Not so much Level 1, again, but
6	progression through the Level 2 models.
7	The third thing that I wanted to and
8	again, I=ll give you any comments?
9	MR. ROZGA: No.
10	MEMBER STETKAR: Okay. You guys know
11	well enough to just interrupt me when I start lying
12	and making up stuff. And, I=m old enough that I=ve
13	gotten really good at lying and making up stuff.
14	MEMBER CORRADINI: Oh boy, is that true.
15	MEMBER STETKAR: The
16	MEMBER SKILLMAN: John, may I ask a
17	question, please?
18	MEMBER STETKAR: Sure.
19	MEMBER SKILLMAN: To your dissertation
20	here, on the first item that you raised, asymmetry
21	and the preponderance of the risk becomes because of
22	the reactor coolant pump service is being cooled by
23	a particular division of component cooling water.
24	Here=s my question, is that observation

1	an issue where our numbers in the PRA are misleading
2	us? I would have thought intuitively that having the
3	pumps serviced by different divisions would have
4	reduced the frequency.
5	And, you=re theorem is, by the asymmetry
6	that is there, the risk is probably as it should be
7	independent of the fact that the cooling is from, if
8	you will, an asymmetric or nonsymmetric cooling
9	source.
10	The thought that was going through my
11	head is, are we being misled by the PRA in this
12	instance?
13	MEMBER STETKAR: I don=t - I don=t want
14	to get too much internal discussions here with limited
15	time, but we=re not being misled by the PRA provided
16	that the PRA accurately accounts for all of the
17	scenarios that can threaten the pumps seals.
18	I meam, the PRA is supposed to model the
19	plant as its designed and operated and it actually is
20	for the cases that you=re evaluating the seal LOCAs.
21	And the risk comes out to be whatever the
22	risk is. You know, whether it would be higher or
23	lower if you had two pumps off of Division 1 and two
24	pumps off of Division 2, I=m not going to speculate

	⁷²
1	on that right now, because I don=t like talking about
2	numbers, I like talking about, you know, whether the
3	plant the PRA is modeling the plant.
4	So, I don=t think we=re being misled by
5	the PRA here.
6	MEMBER SKILLMAN: And, perhaps my
7	question=s not the right question. I guess what I
8	was really getting at is, presuming that the PRA
9	results are accurate, are we being driven to leave
10	the plant configured as the PRA suggests because we=re
11	not willing to reassign the reactor coolant pumps to
12	different divisions because that could be more
13	beneficial.
14	MR. ROZGA: Could I interject?
15	Again, without talking numbers, if you
16	had one division supplying two reactor coolant pumps
17	and you had another division supplying another two
18	reactor coolant pumps, now, if you have a failure in
19	either division, that=s going to lead to a seal LOCA.
20	As now, if we have a failure in the Dib
21	2 CCW system, we won=t have a seal LOCA. So
22	MEMBER STETKAR: It=s the difference
23	between one division affecting four pumps or each of
24	two divisions, each affecting two pumps.

	73
1	MEMBER BLEY: We shouldn=t we could
2	have something offline on this, but just a real quick
3	close on that, the question you=re trying to phrase
4	has different answers depending on exactly how you
5	put the question.
6	Here, we=re saying, how likely is that we
7	get one out of four having a problem and, if you=re
8	then dependent on two different systems, that=s more
9	likely.
10	If you=re asking the other question, how
11	likely is it we have at least one that doesn=t have
12	a problem, you get a different answer.
13	But, I think we ought to take that offline
14	and
15	MEMBER SKILLMAN: Fair enough.
16	MEMBER BLEY: do some detailed
17	looking.
18	I think generally, our
19	MEMBER CORRADINI: Until you think about
20	it.
21	MEMBER SKILLMAN: Counterintuitive is
22	where I am.
23	MEMBER BLEY: Our intuition isn=t always
24	as finely tuned as we think.

1	MEMBER SKILLMAN: Thank you. John, I
2	apologize for ruining the momentum you had.
3	MEMBER STETKAR: Oh, no, that=s okay.
4	That=s sometimes people need to stop me.
5	The other issue that I wanted to bring
6	up, and this, again, is kind of the nexus between the
7	Level 1 and Level 2 modeling, is that the Level 1
8	steam generator tube rupture event tree does not
9	question the status of steam generator of isolation
10	of the ruptured steam generator.
11	Isolation of the ruptured steam generator
12	is questioned in the Level 2 models. There=s a top
13	event, I don=t remember, SGIS or something like that.
14	And, if it=s isolated, that=s a good
15	thing. The Level 2, if it=s not isolated, that=s not
16	so good for Level 2.
17	The question that I have is that the order
18	in which that isolation is questioned between Level
19	1 and Level 2, if the steam generator is not isolated,
20	if it=s open to the environment, and in particular,
21	one isolation pathway is closing the main steam
22	isolation valve that isolates everything downstream
23	of the main steam isolation valve.
24	Another isolation pathway would be the

1	steam generator blow down lines.
2	And, a third isolation pathway is during
3	the event response, the main steam safety valve, at
4	least one of them, if not more than one, I guess two
5	because there=s two steam lines on each steam
6	generator, will indeed open under steam relief.
7	And, if one of those sticks open, does
8	not reclose as you try to cool the plant down, you
9	now have an unisolated ruptured steam generator and
10	that changes the dynamics of the required operator
11	actions in the Level 1 model to prevent core damage.
12	In particular, if the secondary side of
13	the ruptured steam generator is open to the
14	environment, the only way that the operators can stop
15	the net loss of inventory from primary to secondary
16	is to walk the primary system down to just about
17	atmospheric conditions.
18	Once I get down to atmospheric
19	conditions, I=m not going to have much of a driving
20	head anymore.
21	But, you can=t just stop at a 1,000 pounds
22	in the primary system. So, I think, from what I can
23	see that there may be sources of optimism in the Level
24	1 tube rupture model because the status of isolation

1	of the ruptured steam generator is not questioned in
2	that part of the model.
3	It=s only questioned after the fact,
4	after you have a core damage event already and then
5	questioning, okay, if I got there through a tube
6	rupture scenario, is it isolated?
7	Now, that also is reflected in the steam
8	line break upstream and downstream of the MSIV models
9	and the feedwater line break models because those
10	models also have consequential pressure in these now
11	tube ruptures included in them.
12	So, they have a simplified but not super
13	simplified model for tube rupture response built into
14	those event trees. And, those event trees also don=t
15	seem to care whether or not the secondary side of the
16	ruptured steam generator is isolated. They kind of
17	progress oblivious to that.
18	So, I don=t know if you want to comment
19	on that. That was sort of an observation.
20	He really ought to be up front.
21	(Laughter.)
22	MR. DREMEL: Ray Dremel from Enercon
23	again.
24	And, as you pointed out, the modeling of

1	isolation am I speaking loud enough?
2	MEMBER STETKAR: Yes, you=re on.
3	MR. DREMEL: The modeling of isolation of
4	a steam generator tube rupture for Level 1 had a
5	different focus than Level 2.
6	So, the events we consider failure to
7	isolate for Level 1, if the operators don=t close the
8	main steam isolation valve, and this is all initially,
9	because it=s before core damage, then you have some
10	steam going out which is taking mass out of the steam
11	generator which is limiting to some extent the amount
12	of water from the primary that=s going to over fill
13	the steam generator.
14	So, if the operators fail to close the
15	main steam isolation valve, that makes things better
16	from a Level 1 point of view.
17	Because, the concern in the steam valve
18	tube rupture is to prevent over filling the steam
19	generator, the primary is leaking out, you need to
20	put water on your main steam insolation valves you
21	over fill.
22	MEMBER STETKAR: That=s one concern.
23	MR. DREMEL: So, from a Level 1 point of
24	view, not closing the main steam isolation valve is

1	a good thing. We don=t take credit for failures.
2	Similarly, if steam generator blow down
3	is online and the operators don=t isolate steam
4	generator blow down, then you=re taking water from
5	the bottom of the steam generator, putting it in some
6	place that=s relatively safe. I mean, it=s
7	subprimary water that=s going to the steam generator
8	blow down system and that makes things better from a
9	Level 1 point of view.
LO	The operators have more time to cool down
L1	to prevent over fill. So, that=s why those events
L2	are not modeled in the Level 1 event tree.
L3	Now, as far as the main steam isolation
L 4	valve sticking open
L 5	MEMBER STETKAR: Safety valve.
L 6	MR. DREMEL: Safety, I=m sorry, the main
L7	steam safety valve sticking open, the first event in
L8	the steam generator tube rupture event tree is to
L 9	the operator takes official action to cool down the
20	initial 50 degree cool down to stop the flow from the
21	primary to second to reduce secondary pressure less
22	than primary.
23	So, to do that, the operators have to use
24	the atmospheric dump valve and

	79
1	MEMBER STETKAR: On the intact steam
2	generator?
3	MR. DREMEL: On the intact steam
4	generator, yes.
5	But, if they cool down quickly, then
6	you=re really not challenging the steam generator
7	main steam safety valves because you=re cooling down
8	the whole primary. Because initially
9	MEMBER STETKAR: They don=t they open
10	initially?
11	MR. DREMEL: There is it depends on
12	the trip and what happens. So, until the operators
13	close the main steam isolation valves and the EOP=s
14	directing the operators to initially cool down to the
15	condenser, and use the turbine bypass valves which
16	should open automatically to prevent challenging your
17	safety valves.
18	So, we don=t necessarily credit the
19	turbine bypass valves, but by design, they would open
20	to prevent challenging the main steam isolation
21	valves.
22	MEMBER STETKAR: Safety valves.
23	MR. DREMEL: Safety valves, I=m sorry.
24	MEMBER STETKAR: Okay, thank you.

1	I still think that there=s a hole there.
2	The - I agree with your concern that
3	having a path to put water other than just in the
4	steam generator makes it fill more slowly.
5	I=m more concerned in the long-term that
6	keeping a path open to transfer the IRWST to some
7	place that the TRWST ought not to be is also a
8	concern.
9	Granted that that=s a long time, but if
10	the operators, to stop that, if the only way that
11	they can stop that is to make the primary system close
12	to atmospheric. In other words, cool it down to like
13	close to a 100 degrees C, it=ll take them some time
14	to get there, given their cool down rates, allowable
15	cool down rates.
16	MR. DREMEL: Ray Dremel from Enercon
17	again.
18	And, in the Level 1 steam generator event
19	tree, if the operators over fill the steam generator
20	the faulted steam generator, the next node is, do
21	you cool down to atmospheric and you can get there
22	from a number of ways.
23	MEMBER STETKAR: That=s yes. But, my
24	concern, I the model as it=s laid out is, if you

	81
1	pump the safety valves on the ruptured steam generator
2	open by filling it with water, it=s assumed that they
3	stick open and, indeed, the model walks you down
4	has to walk you down to atmospheric conditions in the
5	primary side.
6	What I=m concerned about is, other ways
7	that before you over fill the steam generator during
8	a cool down that you can get a stuck open safety valve
9	or an open pathway through and MSIV that maybe you
10	didn=t think about other ways that steam could get
11	out or whatever.
12	It=s ust we=ve had enough discussion
13	about it. I=m three minutes over where I said I=d
14	stop, so I=ll stop.
15	CHAIRMAN BALLINGER: I think this is a
16	convenient place to stop for our break. So, we=11
17	recess for until, let=s try to come back at 15
18	minutes after to try to make up a few minutes.
19	I might remind people that, at the rate
20	of slide production, we=ll be here until Saturday
21	afternoon at about 5:00.
22	We=re in recess.
23	(Whereupon, the above-entitled matter
24	went off the record at 10:03 a.m. and resumed at 10:16

1	a.m.)
2	CHAIRMAN BALLINGER: Come back in session
3	please.
4	By my reckoning, we=ve advanced by two
5	slides that weren t discussed.
6	MR. T. HWANG: I present them. Can I
7	start the presentation?
8	CHAIRMAN BALLINGER: Yes, but what I=m
9	saying is I was on slide 22 and there=s 23 and 24.
10	Okay, from there.
11	MR. These slides were covered
12	already.
13	CHAIRMAN BALLINGER: Oh, okay. Got it,
14	okay, sorry.
15	MR. IN: We went back to the yes, 22.
16	The next presentation is 19.1.2 and it=s
17	internal events Level 2 and it=11 be presented by Mr.
18	Hwang.
19	MR. T. HWANG: Thank you.
20	My name is Taehee Hwang and I=m working
21	for the KEPCO E&C Company PRA Group.
22	In this part, I briefly introduce the
23	method approach here of APR1400 DC Level 2 PRA and
24	its recert.

1	In the APR1400 Level 2 PRA, the
2	methodology I will PDS, Plant Damage State and
3	Containment Event Tree with the composition event
4	tree analysis is used.
5	PDS model originally created in the SAREX
6	and PDS event trees used to capture all inner system
7	and intra system dependencies.
8	Following the quantification recert of
9	PDS and containment event tree analysis, the source
10	term variation was propounded for each release
11	category.
12	To develop the APR1400 PRA model, the
13	MAAP 4.0.8 code was used to analyze severe accident
14	progression and system release variation.
15	And, SAREX code was used to develop the
16	Level 2 PRA model
17	Before presenting the Level 2 PRA recert
18	inside, let me briefly explain the severe accident
19	mitigation feature of the APR1400.
20	Which was significantly constructing the
21	Level 2 PRA model
22	First is APR1400 containment. It is
23	designed as a pre-stressed containment with a steel
24	liner plate and it is designed to be large dry type

1	containment.
2	The containment in their pre-volume is
3	approximately 3.1 billion cubic feet.
4	Next, to the reactor cavity for APR1400
5	is designed to mimimize the challenges posed by that
6	containment heating, pure coolant interaction and
7	molten corium concrete interaction.
8	The reactor cavity has a large for
9	express the corium spreading and its coolability.
10	Next is severe accident and mitigation
11	picture, considering the PRA is a capped flooding
12	system.
13	During the severe accident, it functions
14	to minimize or eliminate the corium concrete attack
15	due to MCCI after the reactor vessel breach.
16	And, it also functions to minimize the
17	generation of combustible gas such as the hydrogen
18	and/or carbon monoxide in MCCI.
19	Mind that the design information for
20	severe accident mitigation feature will be, again,
21	addressed in the 19.2 presentation.
22	And, hydrogen mitigation system is
23	designed to limit hydrogen concentration in

	85
1	The hydrogen can be generated from the
2	100 percent cooled clad water reaction and hydrogen
3	mitigation system consisted of 30 PARS and 80
4	igniters.
5	MEMBER REMPE: Before you leave, I
6	apologize, I missed the very first few slides, but I
7	had some questions and this is as a good a time as
8	any.
9	But, when I was looking through the
10	material, there=s discussions of a term called the
11	core debris chamber and a core cavity trap.
12	Is that just the base of the underneath
13	the vessel? I mean, is there something special that
14	makes it a core cavity trap or a core debris chamber?
15	Do you have what=s the definition of those terms?
16	Can you show me on the drawing what you=re talking
17	about?
18	MR. T. HWANG: Yes, the reactor cavity
19	has a cavity chamber to capture the excess core debris
20	and to prevent the high pressure valve ejection or
21	DCHE compartment.
22	And, the reactor cavity has a component
23	to the flow path to the containment compartment.
24	MEMBER CORRADINI: So, do you have a

1	picture?
2	MEMBER REMPE: Yes, that would help.
3	And, are there any things is there anything special
4	in the cavity? Is there any extra liner or anything
5	like that or is it just that region?
6	MR. IN: Yes, we don=t have a picture on
7	these slides.
8	MEMBER CORRADINI: Can you at least tell
9	us where to look? I think we=ve got all the documents
10	somewhere. Or, that=s my problem, but if you just
11	tell us where to look, because I also was a bit
12	confused about what the description meant.
13	MEMBER REMPE: There=s a figure, I guess,
14	under but agaim, it=s a proprietary document, but
15	if you could point it out on a Figure 2.9-2 of your
16	severe accident analysis report, that would help, I
17	think. Just, I want to make sure that I understand.
18	MR. T. HWANG: We=ll look for that.
19	MEMBER CORRADINI: Yes, we can do that.
20	MEMBER REMPE: Sometime, yes, later, yes,
21	it would just help because I was confused about the
22	terminology.
23	MR. B. KIM: Byung Jo Kim, could you
24	explain the detailed design of the reactor cavity?

	87
1	CHAIRMAN BALLINGER: Are we into the
2	proprietary discussion now?
3	MR. B. KIM: No. This is Byung Jo Kim
4	from KEPCO Engineering and Construction Company.
5	In the DCD Figure 19.2.3-1, you can find
6	what is the difference between the reactor cavity and
7	the chamber room and so on.
8	And, the other information for this
9	compartment in the lower region is given in Table
10	DCD Table
11	MEMBER REMPE: Slow down for a second,
12	could you give us that figure number again?
13	MR. B KIM: 19.2.3-1.
14	MEMBER REMPE: I=m looking.
15	MR. B KIM: And, in the Table 19.2.3-2,
16	includes the volume or elevation of the bottom of
17	each subcompartment and height of each compartment
18	including the rear cavity and chamber room, cavity
19	chamber room and as I said and so on.
20	MEMBER REMPE: Okay, so, I=m looking at
21	this figure and it = s just a containment drawing. And
22	so, it is indeed just that whole region under the
23	vessel is the trap or the chamber?
24	MR. B. KIM: Yes.

1	MEMBER REMPE: Okay.
2	MR. B KIM: Actually, the DCD figure is
3	not the whole information for the how the reactor
4	cavity can trap the containment debris. So, this
5	kind of cavity space is not exactly shown in this
6	figure, but you can find the if you can look at
7	the technical report related to it, you can see the
8	variation.
9	MEMBER REMPE: Okay, then, tell me again
10	the table number, too. So, I found the figure and
11	what was the table?
12	MR. B. KIM: Yes, Table 19.2.3-2.
13	MEMBER REMPE: Okay. Thank you.
14	MEMBER SKILLMAN: Joy, it=s also Figure
15	1.2-4 in Tier 2.
16	MEMBER REMPE: And, they actually label
17	it as because this does not have a label on it.
18	MEMBER SKILLMAN: Labeled as ICI Cavity
19	and it shows the reactor cavity.
20	MEMBER REMPE: Okay, but this core debris
21	trap
22	MEMBER STETKAR: Just be careful, because
23	those Chapter 1 things are labeled
24	MEMBER REMPE: Yes, I did yes, they

	89
1	have these funny phrases like chamber and trap that
2	I=m not seeing on the figures and that was my
3	confusion. And, thank you.
4	Actually, I have more questions, too.
5	What type of concrete is used on figure
6	or in slide 28? Is it the salt based or is it
7	limestone concrete? Did you
8	So, in your analyses, did you assume a
9	particular type of concrete in the MCCI evaluation?
10	MR. T. HWANG: Concrete type is limestone
11	concrete, yes.
12	MEMBER REMPE: Okay.
13	MR. T. HWANG: So, it is good to cool the
14	excessive core debris.
15	MEMBER REMPE: Okay, thank you.
16	CHAIRMAN BALLINGER: So, let me repeat it
17	so I finally found the figure. I=m not as fast.
18	So, 19.2.3-1 it kind of looks like a PWR
19	reactor cavity. Is there something unique about it
20	that we need to understand?
21	I mean, you called it the ICI cavity, it
22	just kind of looks like a reactor cavity with in core
23	instrumentation coming out the bottom and going up to
24	the seal table. Is it bigger, smaller, is there

	90
1	something unique about it that we should be aware of?
2	MR. IN: Can we discuss this question in
3	the 19.2 because, you know, they have more
4	CHAIRMAN BALLINGER: Sure.
5	MR. IN: figures there.
6	CHAIRMAN BALLINGER: That=s fine.
7	MEMBER REMPE: Okay.
8	CHAIRMAN BALLINGER: That=s fine.
9	MR. IN: Yes, this Level 2
10	CHAIRMAN BALLINGER: No problem.
11	MR. IN: doesn=t have any figures.
12	CHAIRMAN BALLINGER: No problem.
13	MR. IN: Okay.
14	CHAIRMAN BALLINGER: No problem.
15	MR. IN: Thank you.
16	MR. T. HWANG: Okay, next to severe
17	accident mediation feature constructing Level 2 PRA
18	is a pilot operated safety relief valves. It
19	provides a means to rapidly depressurize the primary
20	system to about 250 PSIA to prevent DCH and induced
21	steam generator tube rupture following the severe
22	accident.
23	And, the three-way valves located in the
24	POSRV discharge path can be used to redirect release

	91
1	point of hydrogen from IRWST to the containment
2	atmosphere.
3	And, the next feature is ECSBS.
4	MEMBER STETKAR: Can I ask a question
5	about the relief path? The I looked at the model
6	for that and the success criteria for rapid
7	depressurization in the Level 2 model, or whatever
8	it=s called, it=s top event SDR
9	MR. T. HWANG: Yes.
10	MEMBER STETKAR: requires that the
11	operators open at least two POSRVs and they redirect
12	the discharge to the steam generator compartment, is
13	that correct?
14	MR. T. HWANG: Yes, right.
15	MEMBER STETKAR: So that
16	MR. T. HWANG: Yes.
17	MEMBER STETKAR: if I do not open the
18	POSRVs I remain at high pressure. And, if I do not
19	direct flow to the steam generator compartment, I
20	remain at high pressure. Is that correct?
21	MR. T. HWANG: Yes, right. If the in
22	our model, the success criteria for rapid
23	depressurization is open is to operate more than
24	two POSRVs and the operation of auxiliary valves.

	92
1	MEMBER STETKAR: How much difference does
2	it make to the hydrogen models if I release into the
3	IRWST compared to into the bulk volume of the
4	containment?
5	So, for example, if the operators open
6	the POSRVs but only direct the flow into the IRWST,
7	how what effect does that have on your hydrogen
8	modeling?
9	MR. T. HWANG: In the IRWST area is
10	relatively closed volume so the if the hydrogen
11	generated from the vessel go to the IRWST area, then
12	the it result in a hydrogen concentration inside
13	the IRWST area.
14	Even if the swing panel in the IRWST upper
15	part, but significantly, hydrogen releases go to the
16	IRWST area, in there it can make a different condition
17	during the severe accident.
18	MEMBER STETKAR: So, I was trying to ask
19	a simple question. Is it worse if you release into
20	the IRWST compared to the containment?
21	MR. T. HWANG: Yes, yes.
22	MEMBER STETKAR: Okay, thank you.
23	MR. T. HWANG: It=s very worse.
24	MEMBER STETKAR: The model right now,

1	then, and this is just a statement of my concern, the
2	model right now is I try to stay away from a word
3	that I don=t like to use the model over predicts
4	the conditional probability of high pressure because
5	failing to realign the three-way valves to the
6	containment, despite the fact that the POSRVs are
7	open will go to high pressure.
8	So, it over predicts high pressure, but
9	it under predicts, perhaps, hydrogen effects in the
10	IRWST because, every time you depressurize, by
11	definition, it must be to the bulk volume of the
12	containment. You never can get a successful
13	depressurization with hydrogen release to the IRWST.
14	MEMBER CORRADINI: Can you say
15	MEMBER STETKAR: Well, that=s
16	convoluted, you can read the
17	MEMBER CORRADINI: Can you say that
18	again?
19	MEMBER STETKAR: you can read
20	MEMBER CORRADINI: Sorry.
21	MEMBER STETKAR: Okay.
22	I, as an operator, can open the POSRVs to
23	depressurize. Okay? I do that, now I have a choice
24	between where do put the flow from those POSRVs? I

	94
1	can either put it into the IRWST or I can put it out
2	into the steam gemerator compartment.
3	Their success criteria for depressurizing
4	requires me to both open the POSRVs and put the flow
5	into the steam generator compartment.
6	If I fail to do either one of those, I
7	stay at high pressure, either one. So, I could open
8	the POSRVs
9	MEMBER CORRADINI: I don=t depressurize
10	or no?
11	MEMBER STETKAR: I can open the POSRVs
12	and keep the flow path aligned to the IRWST. In the
13	model, that is treated as a high pressure case.
14	It doesn=t have to make sense, it=s just
15	a fact.
16	MEMBER CORRADINI: It=s just the way the
17	
18	MEMBER STETKAR: It=s just the way
19	they=ve modeled it.
20	MEMBER CORRADINI: Okay, fine.
21	MEMBER STETKAR: So, that is not good for
22	high pressure because I will actually depressurize if
23	I blow into the IRWST.
24	However, if I go to melt then, I will

	95
1	have, in that flow path, hydrogen released into the
2	IRWST with a higher likelihood of a detonatable
3	mixture in the IRSWT.
4	That detonatable mixture cannot occur in
5	their model because their model requires success to
6	always be into the containment.
7	I know it=s confusing, it=s on the
8	record. I can talk to you later about the logic.
9	MEMBER CORRADINI: I just asked you to
LO	repeat it. Thank you.
L1	MR. RYU: Excuse me.
L2	MR. T. HWANG: Mr. Ryu?
L3	MR. RYU: I am In Chul Ryu from KEPCO E&C
L 4	for severe accident analysis team.
L5	Actually, the way the valve is always
L 6	open, not closed. Just closed direction change. So,
L7	if we operate the POSRVs always we can deliver the
L8	high pressure in the excess pressure.
L 9	So, the we don=t need to operate two
20	valves should be open.
21	MEMBER STETKAR: The and just for
22	MR. RYU: And also, the installation of
23	the three-way valve is not we just we cannot
ЭΔ	say simple release into the TRWST is dangerous because

1	we just want to remove the uncertainty of a hydrogen
2	problem.
3	For example, another plant and if even
4	though the hydrogen concentration is very high in the
5	IRWST, but actually the combustion is required for
6	the oxygen. So, the in that case, a simulating
7	case so the IRWST is also the same.
8	But, why we introduced the three-way
9	valve is the different reason. One is that we don=t
10	argue the dangerousness about the valve.
11	And also, if we have the if we release
12	into the IRWST, then the risk point is the annual
13	severe area of the reactor containment. That area
14	has many accumulations. So, in that area, we may
15	have the diffusion frame.
16	So, you want to leave the environmental
17	condition in that area. So, we change the direction
18	into the steam generator compartment so we installed
19	the three-way valve, not because of the just
20	dangerousness of the IRWST.
21	MEMBER STETKAR: Thank you. I just was
22	making the observation that the model, the way it=s
23	implemented, is as I stated.
24	MR. T. HWANG: Thank you for your comment

1	and I=11 take consideration about that.
2	Next, we
3	MEMBER BLEY: I=m just going to I=ll
4	let John tell me if I=m off track. But, I think where
5	John=s headed on this, he=s telling point now what
6	the model does. But, what=s conservative or okay for
7	one thing you=re thinking about might not be for
8	another thing you re not thinking about at this time.
9	And, if you model it the way it really
L 0	works, you get to cover all those cases when you model
L1	it in a way that takes care of what you=re thinking
L2	about. When you=re doing the modeling, you might be
L3	missing something important elsewhere.
L 4	MEMBER REMPE: And, to beat a dead horse
L5	a bit more, the ERI report did look at that case and
L 6	that you could get higher concentrations if you
L7	considered that case.
L8	MR. T. HWANG: And next mitigation
L 9	feature is the ECSBS. ECSBS provides alternative
20	means for containment spray after 24 hours following
21	the severe accident initiation.
22	It delivers water from external water
23	source to the ECSBS containment spray header and ECSBS
24	will be a pumping device which is independent of

1	normal and emergemcy AC power source.
2	MEMBER CORRADINI: So is that FLEX? Your
3	terminology for FLEX?
4	MR. IN: This was not designed as a part
5	of the FLEX. It was a design previous to the
6	MEMBER CORRADINI: Oh.
7	MR. IN: FLEX.
8	MEMBER CORRADINI: Does it satisfy the
9	FLEX? I mean, that=s what it sounds like.
10	MR. IN: Yes.
11	MEMBER CORRADINI: Okay, fine. Thank
12	you.
13	MEMBER STETKAR: That, by the way, I was
14	trying to look up my notes and, in the interest of
15	time, I won=t quote numbers, but my recollection was
16	that ECSBS is a rather important contribution to your
17	conditional containment failure probability.
18	My recollection was that you did a
19	sensitivity case that, without ECSBS, the conditional
20	containment failure probability increases by
21	something like a factor of five or so.
22	MR. T. HWANG: That=s right. Yes, it=s
23	very
24	MEMBER STETKAR: Okay. So, this is

	99
1	important for you Level 2 folks.
2	MR. T. HWANG: For an internal event, at
3	power
4	MEMBER STETKAR: At power?
5	MR. T. HWANG: Yes.
6	MEMBER STETKAR: At power internal event?
7	MR. T. HWANG: Yes.
8	From now on, I=ll briefly explain the
9	method and approach of APR1400 Level 2 PRA.
10	The first task for Level 2 PRA is the
11	plant damage states analysis.
12	In the PDS analysis, the Level 1 event
13	pre-sequences are extended to be additionally
14	questioned in terms for the Level 2 PRA.
15	For example, the status of containment
16	isolation is an important parameter question in the
17	Level 2 PRA.
18	Also, if not questioned in the Level 2
19	PRA model, the status of containment sprays or the
20	status of a steam generator condition, wet or dry,
21	are also questioned in PDS event trees.
22	The bridge tree
23	MEMBER STETKAR: Can I just stop you here
24	and I promise I=m not going to say much more on Level

1	2.
2	Containment isolation, there was in
3	Chapter 9 of the DCD describes a containment high
4	volume purge system that=s operated during plant
5	shutdown.
6	And, it also describes a containment low
7	volume purge, smaller line, that=s operated, and I
8	quote, when required during plant operation.
9	MR. T. HWANG: Yes.
10	MEMBER STETKAR: Many plants, in my
11	experience, do operate their low volume purge to keep
12	the containment atmosphere relatively clean in case
13	people need to go in there.
14	I donet they don=t necessarily operate
15	it 100 percent of the time, that=s plant specific.
16	My only question is, does the containment
17	isolation model account for isolation of that low
18	volume purge for whatever fraction of the time that
19	it=s open? Is it included in the model?
20	MR. T. HWANG: The APR1400 PRA model the
21	low volume purge line is cleaned out because, as you
22	said, the low volume pressure line is normally closed
23	and can be operated intermittently.
24	But, the line is the line has to be

1	closed during the extent because the containment low
2	volume line is closed by actuation of containment
3	isolation signaler or the containment depressurize in
4	isolation signal.
5	And, the lines of valves are being
6	monitored, will be monitored in the MCI operators.
7	So, we screened out this line has a very low
8	probability of isolation.
9	MEMBER STETKAR: Okay. Many things in
10	the PRA had low probability. The reason I bring this
11	up is that, if that line is open and it is not
12	isolated, it may represent a large enough hole in the
13	containment that removes containment energy, just
14	removes energy.
15	Now, that=s a good thing for not over
16	pressurizing containment. It=s not a good thing for
17	offsite releases.
18	So, here=s another case where assumptions
19	about what may or may not be included in the model
20	can have an effect, depends on the fraction of time
21	that the line is open, depends on the reliability of
22	the isolation signals and so forth.
23	So, I=ll just make that comment, if it=s
24	not in the model, it can do good things for you in

1	terms of not over pressurizing the containment. It
2	can do bad things in terms of increasing the
3	conditional large early release frequency.
4	CHAIRMAN BALLINGER: I need to remind
5	people that we=ve got 80 some odd slides and, right
6	now, they have to be finished, at least by the
7	schedule, at 11:30, which means we have to do it
8	almost like a movie.
9	So, we=ve got to do something about this.
10	MEMBER CORRADINI: I thought I mean,
11	just looking at the schedule, I thought 19.1 goes
12	through the afternoon.
13	CHAIRMAN BALLINGER: But, there=s an NRC
14	presentation 19.1 also.
15	MEMBER CORRADINI: Okay, fine.
16	CHAIRMAN BALLINGER: I=m just just to
17	remind I mean, it=s our fault, not our fault, we=ve
18	been asking good questions.
19	MR. T. HWANG: Is it okay?
20	CHAIRMAN BALLINGER: Optimistic
21	schedule. Keep going.
22	MR. T. HWANG: Yes.
23	Yes, so the bridge tree sequences are
24	grouped into the PDS group based on the similarities

1	in the extent progression based on the PDS grouping
2	parameters such as containment bypass or the status
3	of containment isolation, the LOCA or transient
4	sequences, the ICS pressure and so on.
5	As a Level 2 PDS binning, 108 PDS groups
6	were defined and quantified to capture all Level 1
7	and Level 2 dependencies.
8	To develop the Level 2 containment event
9	tree model, we needed to estimate the APR1400 stress
10	peak containment UPC.
11	In the APR1400 Level 2 PRA, the plant
12	specific containment to the facility was determined
13	by ultimate pressure capacity calculation which
14	approximates the realistic probability for keeping
15	pressure on.
16	For APR1400 containment, two containment
17	failure modes such as loss of power mode and leak
18	power mode determined based on the NUREG-1150 and
19	NUREG/CR-6906.
20	In the Level 2 containment event tree
21	analysis, the various containment failure modes and
22	the major severe accident phenomena are represented
23	a top events of the containment event trees.
24	Detailed variation of the phenomena for

1	each top event of CET is created in the composition
2	event trees.
3	The Level 2 CET considered the following
4	containment challenges, direct containment to bypass,
5	containment isolation, system failure, induced SGTR
6	during the severe accident, high pressure mass
7	ejection and direct containment heating or blow down
8	post steam explosion, hydrogen phenomena, steam over
9	pressurization and MCCI and basemat melt through.
10	In the development of the APR1400 Level
11	CET, the generic data were used.
12	NUREG-1570 was utilized for developing
13	induced ISGTR combustion event tree, including the
14	condition probabilities of induced ISGTR developed
15	for the current generation plants.
16	MEMBER REMPE: So, 1570 was for a
17	Westinghouse plant design.
18	MR. T. HWANG: Yes.
19	MEMBER REMPE: Your steam generator, I
20	would think, would be more like a CE type of steam
21	generator design. How do you justify using those
22	conditional probabilities?
23	Because the geometries are a bit
24	different, right?

	105
1	MR. T. HWANG: Yes, the geometry the
2	1570 plant is different from the APR1400, but the
3	at this time, the plant specific in this ISGTR
4	probability cannot be developed in this design stage.
5	So, we just assumed that the condition
6	probability of this in this ISGTR for NUREG-1570 was
7	used APR1400 event tree.
8	MEMBER REMPE: So, the staff has been
9	working hard looking at CE designs and they have this
10	NUREG-2125 that they issues as a draft and it actually
11	has quite different numbers of the CE designs.
12	Now, they also said things are very
13	design specific, so you=11 need to look at what they
14	did and see if it applies to your design. But, it
15	does have quite higher conditional probabilities for
16	the CE design and you might want to consider it.
17	MR. T. HWANG: Yes, yes, it=s a good
18	comment and we=11 take consideration for another
19	around as your comment directs 2512 and
20	MEMBER REMPE: It=s 2125 and it=s a just
21	NUREG, it=s not a NUREG/CR.
22	MR. T. HWANG: Yes, okay. Okay, thank
23	you.
24	And, NUREG/CR-6475 and NUREG/CR-6109 for

1	induced hot leg rupture probability was referenced
2	for the referenced to the PRA.
3	And, NUREG-1150 and NUREG/CR-4551 were
4	considered for various phenomena such as in vessel
5	core recovery or rocket mode failure or steam
6	explosion and so on.
7	After the quantification of PDS and CET
8	analysis, the number received at the end points is
9	very large, and detailed system analysis for all the
10	CET end points in not feasible.
11	Hence, CET end points are grouped into
12	the system release categories based on the
13	similarities of release characteristics such as
14	magnitude of the timing releases.
15	Source term release calculations are
16	performed using MAAP 4.0.8 code. And, to determine
17	the large release frequency for the APR1400 Level 2
18	PRA, the large release is defined as released of
19	greater than 2.5 percent of volatile or semi-volatile
20	fission products that is iodine, cesium, tellurium.
21	This is a second depiction of large
22	releases in the NUREG/CR-6595.
23	In addition, the APR1400 Level 2 PRA
24	defined all the releases as that the release people,

1	they calculated the evacuation of the surrounding
2	public after the generic emergency declaration.
3	This slide shows the Level 2 PRA result
4	for at power internal events. The conditional
5	probability of an in tank containment is 86 percent
6	of internal CDF.
7	The conditional probability of
8	containment failure, including large releases and
9	small releases is 14 percent.
10	Where the small release categories
11	includes the release categories of basemat melt
12	through or steam generator tube rupture, with the
13	SGTR for scrubbing and so on.
14	Final y, the conditional probability of
15	large releases is 9 percent of internal Level 1 event
16	CDR.
17	The most significant containment failure
18	contributor is the containment bypass which is 6
19	percent of CDF.
20	Uniso ated steam generator tube rupture
21	sequences prior to core damage contributes 5 percent
22	to at power internal events CDF.
23	Severe accident induced SGTR such as
24	severe accident induced SGTR contributes 1 percent to

1	core damage frequency.
2	Level 2 depressurization by using POSRVs
3	is effective to prevent induced SGTR.
4	And, the single tube rupture with pool
5	scrubbing, with wet pool scrubbing, do not result in
6	a large release due to pool scrubbing inside loss of
7	the steam generator.
8	Second dominant containment failure
9	contributor is late containment failure which is 5
10	percent of CDF.
11	ECSBS is effective to prevent containment
12	failure due to steam over pressurization and PARs and
13	flooded cavity by cavity flooding system is operate
14	effective to prevent the buildup of high hydrogen
15	concentration inside the containment so it prevents
16	the containment failure due to hydrogen.
17	This is the end of my presentation.
18	CHAIRMAN BALLINGER: So, can you
19	MEMBER REMPE: I have to correct myself.
20	Professor Ballinger got that I was saying the wrong
21	number, it=s NUREG-2195. I apologize.
22	MR. T. HWANG: NUREG-2195.
23	MEMBER REMPE: Yes, I apologize.
24	MR. T. HWANG: Okay, yes, thank you.

1	Thanks very much.
2	CHAIRMAN BALLINGER: You have a much
3	better memory tham I do.
4	MEMBER REMPE: Yes, well, I forgot.
5	MR. T. HWANG: It is a final issue?
6	MEMBER REMPE: It was a draft issued a
7	while ago, but the final we=re having an ACRS
8	meeting to discuss it this next in two weeks from
9	now. But, there is an earlier draft and the numbers
10	were higher in that draft, too.
11	MR. T. HWANG: Okay.
12	MEMBER REMPE: So, in a week or two you
13	should see a new one.
14	MR. T. HWANG: Thank you very much.
15	MEMBER REMPE: Yes.
16	MR. SCHNEIDER: Ray Schneider,
17	Westinghouse.
18	There was an error in the draft where
19	they treated the CE pumps as Westinghouse pumps. I
20	think we sent them a note to fix that, so there may
21	be some changes coming from.
22	MEMBER REMPE: Okay.
23	MR. IN: Shall we move on to the next
24	presentation?

	110
1	The next presentation is on the seismic
2	assessment and it will be presented by Dongwon Lee.
3	MR. D. LEE: Good morning, ladies and
4	gentlemen. My name is Dongwon Lee from KEPCO E&C PRA
5	team.
6	I=m going to present to you seismic risk
7	assessment.
8	For the seismic risk assessment, we
9	considered three different methodologies.
10	First, a Staff Review Memorandum to SECY-
11	93-087; and second, DC/ISG-020 provides the guidance
12	for the implementation process for performing PRA
13	based SMA. And, three, SSC, structure, systems and
14	the components can be evaluated by either
15	Conservative Deterministic Failure Margin method or
16	Separation of Variables method.
17	Next?
18	For the PRA based SMA, we considered
19	seismic input motion. We certified seismic design
20	response spectra which is from Spectral Reg Guide
21	1.60 enhanced in high frequency.
22	CSDRS anchored to a peak ground
23	acceleration of 0.3g and defined at free field ground
24	surface.

1	For the PRA model assessment, seismic
2	margin earthquake is considered at 1.67 times the
3	CSDRS.
4	Look at the right side of the figures,
5	the blue line is the certified seismic design response
6	spectra and red one is the margin earthquake.
7	Next?
8	APR1400 FSTS, we did design specific
9	capacity. We do the specific coolant capacity.
10	First we do the specific building
11	structures capability analysis such as reactor
12	containment building and the concrete internal
13	structures of the building, EDG and diesel fuel tank
14	room building.
15	And, we considered seven RCS at design
16	specific capacity such as the following.
17	Next?
18	MEMBER STETKAR: On that slide, it struck
19	me as curious that the structural analyses do not
20	include the emergency service water component cooling
21	water heat exchanger building or the tunnels that
22	connect the component cooling water heat exchanger
23	building to the auxiliary building.
24	And, I know that those are not part of

1	the certified design, but the implication is here
2	that they must be much, much stronger than the
3	containment because they never fail in your seismic
4	margin analysis.
5	So, that struck me as curious because
6	now, as a COL applicant, must I build those building
7	much, much stronger than the seismic category one
8	containment to satisfy the seismic margin analysis?
9	Or, will I be surprised when I do my COL
10	seismic margin analysis and discover that if those
11	buildings fail, they could be an important
12	contribution to my seismic risk?
13	MR. D. LEE: I want to introduce Mr.
14	Kyuho from SGH, he might give you the details for
15	that.
16	MR. K HWANG: I=m Kyuho Hwang from SGH
17	to support KEPCO E&C on the seismic evaluation.
18	Is it on?
19	CHAIRMAN BALLINGER: Just a little
20	closer.
21	MR. K. HWANG: All right.
22	Well, actually, the system the yard
23	buildings, the safety related yard buildings are not
24	in the scope of DC certification. So, we just, right

1	now, so those buildings are never designed at this
2	stage. But, we just show that those buildings are
3	seismically rugged so we can screen them out.
4	MEMBER STETKAR: I=m sorry, the reactor
5	containment building, to me, sounds like a
6	seismically rugged building, and yet, you have a
7	specific fragility evaluation. It has it does not
8	have a zero failure probability.
9	So, by implication, these other buildings
10	must be more must be much stronger, much stronger,
11	than the containment. Because they have precisely
12	zero failure probability.
13	MR. K. HWANG: Well, actually, our
14	approach is like a deterministic approach. So, we
15	never enveloped the probability of the failure of
16	those buildings in question.
17	MEMBER CORRADINI: But, just to clarify,
18	so you left it of the analysis? That=s what I
19	hear you really saying. I mean, John is trying to
20	pulse you to say that, but you=ve left out of the
21	analysis, is that fair to say?
22	MR. DREMEL: Ray Dremel from Enercon.
23	And, not the CCW building, the ESW
24	buildings have zero failure probability. We don=t

	114
1	have a plant specific fragility for those, so we
2	assumed that they will have at least a .5g HCLPF.
3	They are included in the seismic margins assessment
4	model.
5	MEMBER STETKAR: I=m sorry, they are not
6	included in the seismic margins model. I could not
7	find them anywhere.
8	MR. DREMEL: Are we talking Rev 0 or Rev
9	1?
10	MEMBER STETKAR: They were screened out.
11	MR. D. LEE: Rev 0.
12	MEMBER STETKAR: Rev 0, they were
13	screened out.
14	MR. DREMEL: They were added in Rev 1.
15	MEMBER STETKAR: Okay. Thank you.
16	MR. D. LEE: Can we move on?
17	Okay, this slide is for approach for
18	HCLPF capacity evaluation.
19	First, the critical failure mode should
20	be identified. First this step, APR1400 design
21	specific report calculations and the drawings should
22	be reviewed.
23	And, potential failure modes by comparing
24	design seismic demand to design capacity already

1	identified areas of design margin.
2	And then, governing failure modes for
3	HCLPF capacity evaluation was selected.
4	For the seismic demand, APR1400 design
5	specific seismic demand were used and CSDRS applied
6	at plant finished grade in the free field for eight
7	generic certified and a fixed base case such as design
8	in Chapter 3, what it is.
9	And, static capacity equations were used
10	coded capacity for ACI 349 and ASME Section III
11	Service Level D Level of EPRI NP-6041-SL Revision 1.
12	And, for the ductile failure mode, we
13	considered inelastic energy absorption capacities.
13 14	considered inelastic energy absorption capacities. And, finally, we conducted the HCLPF
14	And, finally, we conducted the HCLPF
14 15	And, finally, we conducted the HCLPF capacity of SSCS CDF method in EPRI NP-6041 applied
14 15 16	And, finally, we conducted the HCLPF capacity of SSCS CDF method in EPRI NP-6041 applied to demonstrate HCLPF is equal to or greater than
14 15 16 17	And, finally, we conducted the HCLPF capacity of SSCS CDF method in EPRI NP-6041 applied to demonstrate HCLPF is equal to or greater than seismic margin earthquake that is 1.67 times CSDRS.
14 15 16 17	And, finally, we conducted the HCLPF capacity of SSCS CDF method in EPRI NP-6041 applied to demonstrate HCLPF is equal to or greater than seismic margin earthquake that is 1.67 times CSDRS. I=m going to introduce the major HCLPF
14 15 16 17 18	And, finally, we conducted the HCLPF capacity of SSCS CDF method in EPRI NP-6041 applied to demonstrate HCLPF is equal to or greater than seismic margin earthquake that is 1.67 times CSDRS. I=m going to introduce the major HCLPF from the structures. This table shows you the
14 15 16 17 18 19	And, finally, we conducted the HCLPF capacity of SSCS CDF method in EPRI NP-6041 applied to demonstrate HCLPF is equal to or greater than seismic margin earthquake that is 1.67 times CSDRS. I=m going to introduce the major HCLPF from the structures. This table shows you the summary of the building structures.
14 15 16 17 18 19 20 21	And, finally, we conducted the HCLPF capacity of SSCS CDF method in EPRI NP-6041 applied to demonstrate HCLPF is equal to or greater than seismic margin earthquake that is 1.67 times CSDRS. I=m gping to introduce the major HCLPF from the structures. This table shows you the summary of the building structures. As you can see, the results varied from

1	Next?
2	And, this table shows you the RCS
3	component HCLPF and it is varied from 0.51g and 1.31g.
4	The lowest one is the pressurizer and the
5	reactor internals. Reactor internals governed by
6	core support barrel lower flange to primary membranes
7	stress and the pressurizer was governed by
8	pressurizer spray nozzle.
9	Next?
10	The other SEL components, it is related
11	to RAI question 19-73, a. It requests such as provide
12	the basis and justification for the assumption HCLPF.
13	And, second, provide a detailed description of the
14	methodology.
15	So, we provided detailed description of
16	HCLPF and shortages and the basis and the
17	justification for ISGS shortage.
18	The following is the answer for this RAI
19	and HCLPF of ESWIS CCW heat exchanger building and
20	BOP components because the detail of design
21	information is not available in this phase.
22	And, also, the SSCF design spec is a COL
23	item as well in Chapter 3. That=s why we assigned to
24	COL items and assume to have a 0.5g HCLPF.

	117
1	Next?
2	MEMBER STETKAR: Except, the only point
3	I was trying to make, if you went back a couple of
4	slides, is that, you showed that the lowest HCLPF
5	capacity for the buildings in scope that you evaluated
6	was the auxiliary building at .51g.
7	You used a nominal 1g earthquake for your
8	seismic margin evaluation. And, that auxiliary
9	building has a non-zero probability of failure at 1g,
10	hence, the service water and component cooling water
11	building would have a non-zero probability of failure
12	at 1g.
13	MR. D. LEE: Mr. Ray could give you the
14	details.
15	MEMBER STETKAR: And, I think we=ve heard
16	you=re fixing that up in Rev 1.
17	MR. DREMEL: Right. The answer is
18	MEMBER STETKAR: I just wanted to kind of
19	close the loop here.
20	MR. DREMEL: Yes, and the answer is that
21	the values that are being presented here are for
22	Revision 1 of the seismic margins analysis.
23	MEMBER STETKAR: So, that the just to
24	make sure, and we haven=t seen Rev 1, I would expect

	118
1	then for the nominal 1g earthquake that you use to
2	propagate to solve your model, I don=t want to say
3	quantify frequency, but to solve your model that the
4	ESW CCW building and those tunnels will have some
5	measurable probability of failure.
6	MR. DREMEL: Yes, yes.
7	MEMBER STETKAR: Okay, thank you.
8	MR. T HWANG: Okay, continue.
9	MR. D. LEE: Okay.
10	To develop the seismic equipment list,
11	the following three things are considered.
12	First, seismic initiating and the
13	consequential events were defined such as the direct
14	core damage scenarios such as a building collapse,
15	loss of all instrumentation control, SBO, LOCAs,
16	adverse and loss of offsite power.
17	And, the safety functions needed for
18	response were determined such as the following and
19	then steps needed to fulfill safety functions were
20	identified based on internal event PRA and powered by
21	onsite emergency AC sources.
22	Next?
23	Here we designed the logic model. First,
24	the seismic event trees were considered following

1	seismic events, direct core damage and also I&C at
2	the large LOCA, medium LOCA, small LOCA and LOOP.
3	And then, seismic event trees inserted
4	the seismic failures into failure trees and lastly,
5	to the plant level HCLPF, the following will be
6	performed to solve the seismic event tree models.
7	And, through the Min-Max method, the
8	final plant level was developed at 0.5g and beside
9	from that, we assumed the generic failure of SSGS
10	compound building collapse and turbine building
11	collapse was 0.5g HCLPF, as I mentioned earlier.
12	Next?
13	Here is my conclusion, major APR1400 SSCs
14	were evaluated by following ISG-020.
15	APR1400 design specific seismic demands
16	and design data was used.
17	And, CDFM method in EPRI NP-6041-SL Rev
18	1 was adapted for HCLPF capacity evaluation.
19	And, HCLPF capacity over the SSCs for
20	major the SSCs greater than 1.67 times CSGRS.
21	Thank you.
22	MEMBER STETKAR: I have only one
23	observation, I=ll just make this comment quickly.
24	When I went through the results that are

	120
1	documented in Table 19.1-44, I noted several
2	instances of nonsymmetric failures that I could not
3	understand. And, I=ll just list the contributors and
4	point you to them.
5	For example, number 17, 19, 23, 26 and 40
6	involve turbine driven auxiliary feedwater Pump A. I
7	could not find what I would expect, symmetric failures
8	of Pump B anywhere.
9	Similarly, scenarios 28, 29, 31, 33, 34
10	and 44 include seismic combinations of seismic and
11	hardware failures that disable Emergency Diesel
12	General B but I couldn=t find the symmetric
13	combinations with A.
14	So, it just struck me as curious that I
15	didn=t see at about the same number. It=s called a
16	frequency, but the same ranking, let=s call it, those
17	symmetric combinations which may mean that there=s
18	something in the model that didn=t quite get set
19	correctly. I don=t know. I=ll just make that as an
20	observation.
21	MR. D. LEE: Thank you.
22	MR. T. HWANG: Yes, shall we move on to
23	the next presentation? We=ve got three more
24	presentations.

1	CHAIRMAN BALLINGER: Yes, we have what
2	amounts to a hard stop for one of our Members at
3	11:30. So, we=11 have to find a way to stop then at
4	a convenient place and
5	MEMBER STETKAR: The Member can become
6	very arrogant and let the other people wait if we run
7	past.
8	CHAIRMAN BALLINGER: Okay. Like I said,
9	we have a hard stop for one of our Members at 11:30.
10	MR. IN: Okay, the next presentation is
11	the internal fire PRA which will be presented by Mr.
12	Greg Rozga.
13	MR. ROZGA: Again, I=m Greg Rozga from
14	Enercon. We=ll be discussing the internal fire.
15	I=ve put together this presentation based
16	on the PRA tasks numerically. The tasks aren=t done
17	in order, I kind of have it put together in the order
18	of how you actually do the work.
19	The first thing we do is we divide the
20	plant into physical analysis units. There=s
21	approximately 390 PAUs identified for the APR1400.
22	Some of the major highlights is that the
23	auxiliary building has 279 physical analysis units.
24	It=s very highly compartmentalized. And, that

	122
1	results in many, many fires only impacting small
2	amounts of equipment.
3	So, with respect to fire, the
4	compartmentalized design is actually a good design.
5	All of these fire areas are have rated
6	barriers with the exception of separation that we
7	take credit for for the yard transformers.
8	And, actually, the DCD says that they
9	will either be 50 foot separation of there=11 be a 3-
10	hour barrier.
11	And, the low power shutdown model uses
12	the same PAUs. There are some removable barriers.
13	However, those barriers are used for things like if
14	you=re replacing a pump motor or something and those
15	things are very infrequent, rare occurrences and
16	there=s an assumption and a COL item that those
17	barriers will be removed during defueled operations
18	so you don=t have to worry about spreading a fire
19	because of that.
20	Next slide?
21	Tasks 2 and 3 are the equipment and cable
22	selection and the at power fire PRA equipment list is
23	based on the at power internal events PRA equipment
24	list with the addition of some nonmodeled spurious

1	operations and they have been screened out because of
2	low probability in the internal events that they need
3	to be added back in.
4	Same thing with the low power shutdown
5	FPRA. It=s basically the low power shutdown internal
6	events PRA equipment list with the additional cable
7	for the low power shutdown LOCAs. And, that=s the
8	CDCS line, it=s called a JL LOCA, if you=ve seen it
9	in the documentation.
10	The pables for all the equipment is
11	routed most 9 percent of it is based on the
12	referenced plant, Shin Kori 3 and 4.
13	There is some assumed cable routing, the
14	new diesel generators, the ESW and CCW that aren=t
15	part of the referenced plant. We had to assume cable
16	routing.
17	And, $I=11$ just tell you that that is
18	that=s not uncommon even in existing plant PRAs.
19	There=s some cables where they just don=t know where
20	it is and so we assume cable routing.
21	We also the type and number of
22	penetrations between the PAUs is from the reference
23	plant.
2.4	Cables for new equipment, so the

1	additional equipment that was in the database but
2	wasn=t part of the internal events, we were actually
3	able to route that based on the reference plant.
4	Tasks 9 and 10 are the detailed circuit
5	failure analysis and failure mode likelihood
6	analysis.
7	For our fire PRA, we assumed worst case
8	failure modes. So, if a controlled cable failed, if
9	the worst case is that there was a spurious operation,
10	we would assume the spurious operation occurred.
11	If the worst case was that the component
12	wouldn=t operate, we assumed that it wouldn=t
13	operate.
14	There s a lot of fiber optic cable in the
15	plant between the main control room and the group
16	controllers. And, what=s good about that is that you
17	don=t they=re the well, you don=t have spurious
18	operations.
19	Yes, sir?
20	MEMBER BLEY: Is the worst case the same
21	for all possible scenarios in the PRA or did you
22	evaluate worst case on a scenario by scenario basis?
23	MR. ROZGA: In most cases, it=s
24	MEMBER BLEY: Yes, but

	125
1	MR. ROZGA: Yes, yes. For Level 1 PRA,
2	it=s always that, you know, you want flow to happen.
3	So, the worst case would be that you would have a
4	spurious closure.
5	Now, there is the possibility that in
6	Level 2, the worst case might be that you would later
7	on want to close that valve.
8	And, I believe we have that covered but
9	that=s something that we can check into and verify.
10	MEMBER BLEY: Well, just for example,
11	over and under cooling can both affect Level 1. And,
12	but, you assumed oss of flow was the worst case for
13	everything?
14	MR. ROZGA: Yes, yes.
15	MEMBER BLEY: Okay.
16	MR. ROZGA: Yes.
17	MEMBER BLEY: Eventually, you might want
18	to reconsider that.
19	MR. ROZGA: And then, for the spurious
20	operations, we didn=t take credit for clearing of the
21	short. We assumed the short happens at a probability
22	of 1. We didn=t do any analysis.
23	With respect to qualitative screening,
24	there was no qualitative screening done for the at

1	power fire. It was always assumed that you at least
2	have a transient fire in every room and that you will
3	at least have a plant trip.
4	For low power shutdown, there was some
5	qualitative screening. Because the plant=s already
6	shut down, if a fire in the room does not disrupt
7	your shutdown cooling, then we were able to screen
8	out those rooms.
9	MEMBER SKILLMAN: Greg, please
10	MR. ROZGA: Yes?
11	MEMBER SKILLMAN: go back to slide 52.
12	MR. ROZGA: Okay.
13	MEMBER SKILLMAN: Task 9, detailed
14	
14	circuit failure analysis, so you identify for a power
15	
	circuit failure analysis, so you identify for a power cable loss of function control cable failure to operate.
15	cable loss of function control cable failure to
15 16	cable loss of function control cable failure to operate.
15 16 17	cable loss of function control cable failure to operate. For the power cable loss of function, how
15 16 17 18	cable loss of function control cable failure to operate. For the power cable loss of function, how does that apply to a valve, say a motor operated valve
15 16 17 18	cable loss of function control cable failure to operate. For the power cable loss of function, how does that apply to a valve, say a motor operated valve that only functions 50 percent of its intended
15 16 17 18 19	cable loss of function control cable failure to operate. For the power cable loss of function, how does that apply to a valve, say a motor operated valve that only functions 50 percent of its intended direction that is, if it=s to go open and only goes
15 16 17 18 19 20 21	cable loss of function control cable failure to operate. For the power cable loss of function, how does that apply to a valve, say a motor operated valve that only functions 50 percent of its intended direction that is, if it=s to go open and only goes open halfway or if it=s to isolate, go closed, it

1	the PRA is for the valve to change state, open or
2	closed, if the power cable is damaged, we assume that
3	it does not change state.
4	MEMBER SKILLMAN: What I was really
5	asking is, is there another set of scenarios where
6	the devices don=t fail as you=ve predicted, but they
7	actually fail approximately halfway and you=re only
8	stuck because you can=t because of the failure,
9	proceed to isolate or proceed, if you will, to vent
10	or open, you=re stuck halfway?
11	MR. ROZGA: No, no.
12	MEMBER SKILLMAN: That=s just not a
13	feature of the PRA?
14	MR. ROZGA: Yes, yes, correct. Yes, it
15	either doesn=t move to its designed position or it
16	does.
17	And, even if the fire doesn=t damage it,
18	it may randomly fail. The fire PRA doesn=t only
19	include the fire failures, it also looks at the random
20	failure probabilities.
21	MEMBER SKILLMAN: Thank you.
22	MR. ROZGA: Okay, you=re welcome.
23	MEMBER POWERS: I have a question which
24	the answer is probably, no, we didn=t address it.

1	But, I=ll ask anyway.
2	If I have a fire in one of your areas and
3	smoke is distributed into other areas, accumulates at
4	critical contacts, do you attempt to adjust any of
5	your failure probabilities in the PRA for the fact
6	that those contact points and things like that might
7	corrode because of the corrosive nature of the smoke?
8	MR. ROZGA: No, that=s corrosion from
9	smoke, that=s long-term action. If the fire is in
10	the immediate area, that
11	MEMBER POWERS: Not interested in the
12	immediate area.
13	MR. ROZGA: Right, right.
14	MEMBER POWERS: It=s the disbursal beyond
15	that.
16	MR. ROZGA: Yes, yes, we do no, no.
17	The answer is just no.
18	MR. DREMEL: Is that beyond the current
19	state of the art for fire PRA?
20	MEMBER POWERS: You know, an argument
21	would certainly make could be based on that exact
22	argument that it s beyond the current state of the
23	art. But, it=s the state of the art that I tend to
24	mess with. So, I ask and not very critical that you

1	didn=t take it into account. But, it=s a persistent
2	concern.
3	MR. ROZGA: Okay.
4	And, did we do this? We actually already
5	did this one.
6	Task 5, I don=t know if we noted, FIRM is
7	fire induced risk model. That=s just the PRA model
8	with your fire inputs.
9	The at power and low power shutdown FIRMs
LO	are both based directly on their respective internal
L1	events model and then we manipulate that model for a
L2	different fire scenarios.
L3	We identify the equipment that would be
L 4	damaged and we force that equipment failed.
L5	If we impact operator actions, local
L 6	operator actions that may have to take place, et
L7	cetera.
L 8	And, the at power fires in each physical
L 9	analysis unit were assumed to either result in a
20	transient, loss of CD, loss of DC A or B, loss of
21	feedwater LOOP, PLO CCW or a small LOCA and those are
22	all based on the equipment damage in the immediate
23	room that the fire took place.
2.4	No other fire induced initiators were

1	identified. If no PRA equipment or cables in the
2	room were damaged, again, we always assume that you
3	at least have a plant trip, the fire might be bad
4	enough that the operators are going to trip the plant.
5	And, all fire induced failures are
6	assumed nonrecoverable including offsite power. So,
7	we don=t take credit for any recovery.
8	The low power shutdown fire induced risk
9	model screen, POS 7, 8 and 9 and they=11 probably
L 0	discuss this in the low power shutdown. Eight is
L1	defueled, 7 and 9, you=re at high water elevation and
12	the times associated with that boil down are extremely
L3	long.
L 4	We took credit for that same screening
L 5	that was done for the internal events.
L 6	The unscreened low power shutdown fires
L7	are assumed to either result in a loss of CC, the JI
L 8	LOCA which is the CVCS line, spurious operation LOCA,
L 9	loss of 4KV to the operating train, loss of offsite
20	power, the loss of level control event or just the
21	unrecoverable failure of the operating shutdown
22	cooling train.
23	I do want to reemphasize for those who
2.4	are unfamiliar with fire PRA, when we screen

1	something, that fire frequency doesn=t go away. We
2	bring it back in when we look at the multi-compartment
3	analysis.
4	So, there may be a fire in an area and
5	that area doesn=t result in any of these initiating
6	events, so we screened it from the single compartment
7	analysis.
8	However, when we do the multi-compartment
9	analysis, we bring all those back and then we say,
10	well, what happens if the fire spreads from that area?
11	So, screening doesn=t mean it=s
12	completely out. We do look at it again when we look
13	at multi-compartment analyses.
14	Task 6 is calculation of the ignition
15	frequencies. And, they=re based on, again, generic
16	data. And, that generic data is continuously
17	updating.
18	We recognize that there=s a new NUREG-
19	2169 that is part of our PRA that we=ll evaluate.
20	The low power shutdown ignition
21	frequencies are currently based on NUREG/CR-7114.
22	
22	And, for transient fires, there are transient
23	And, for transient fires, there are transient influencing factors and it=s part of this NUREG-6850

Τ	transient fires are going to occur.
2	So, areas were high maintenance areas,
3	areas where you store equipment that might be a
4	transient initiator.
5	Highly populated areas, well, for low
6	power shutdown, we reevaluated those transient
7	initiating factors. And, as an example, you know, we
8	increased all the containment building transient
9	influencing factors because there=s additional work
L 0	that=s done in containment.
L1	And, we did a PAU by PAU assessment and
L2	we made adjustments to those factors.
L3	Task 12 is HRA. The initial HEPs were
L 4	estimated using the NUREG-1921 screening analysis and
L5	then the top HEPs ranked by F-of-Vs were reevaluated
L 6	using your normal THRP, CDBMT, whatever is the
L 7	appropriate methodology.
L 8	The fire PRA HRA used the same level of
L 9	dependency among dependent HFEs. And, the current
20	PRA update is reevaluating all of the HEP human
21	failure events using the detailed HRA methodologies
22	and we=re going to be reevaluating all the
23	dependencies.
24	CHAIRMAN BALLINGER: Okay, I=m not sure

	133
1	whether this is a convenient place to stop. Say
2	again?
3	MR. SISK: There are three slides
4	remaining.
5	CHAIRMAN BALLINGER: Oh, three slides?
6	Okay, continue.
7	MR. ROZGA: Okay.
8	These slides mostly do with fire
9	modeling. Without a plant to walk down, you can=t do
10	any reasonably accurate fire modeling. So, we made
11	some overarching assumptions.
12	We assumed for any single compartment
13	that anything in the compartment burns out every time,
14	no matter the size of the fire, we don=t know the
15	location of the equipment in relation to the fire, so
16	we just assume at time zero, everything has failed.
17	We do our initial CDF quantification,
18	that=s the Task 7 quantitative screening. And,
19	again, I want to reemphasize that things that are
20	quantitatively screened, their CDF doesn=t go away,
21	we just don=t do additional work on them because the
22	CDF is low enough where you want to spend your
23	resources on your higher CDF areas.
24	The initial high CDF areas include the

1	main control room containment, turbine building, and
2	there were about 35 other single compartment physical
3	analysis units.
4	Again, since we couldn=t do detailed fire
5	modeling, the only thing we did is we took credit for
6	automatic suppression.
7	There was a generalized assumption that
8	the design of the if the suppression system was
9	designed to cover this electrical panel, that it=s -
10	- that the design is correct and it would put the
11	fire out.
12	And, again, if there was a failure of the
13	suppression system, then we=d go back to a full room
14	burnout.
15	One other thing I=ll say about
16	suppression, we did credit manual suppression only in
17	cases where we knew there was going to be somebody
18	there. So, we took credit in the main control room.
19	We know what=s comtinuously manned.
20	And, we took credit for prompt manual
21	suppression for hot work fires. You at least have
22	the person that s doing the hot work. There-s
23	generally a fire watch. You=ll also generally have
24	welding blankets or something put out as he=s doing

1	his work.
2	We also have no knowledge of intervening
3	combustibles. So, when it comes to the multi-
4	compartment analysis, we assume that if the barrier
5	between the two compartments fails that any fire in
6	the exposing compartment is sufficient to fail all
7	the equipment in the exposed compartment.
8	The other detailed analysis were the main
9	control room where we have to deal with a control
10	room abandonment scenarios.
11	Containment was high because you have all
12	four trains of instrumentation for RPS SFAS and
13	there=s the potential for small LOCA.
14	Turbine building, it just has a very high
15	ignition frequency because of the size. There=s also
16	offsite power cables in there.
17	And, the other 35 were just various
18	reasons they had higher CDF, multi-compartment
19	analysis is also part of the detailed quantification.
20	Task 13, seismic fire interaction
21	analysis, without a plant to walk down, we just had
22	to do a qualitative analysis based on the current
23	design information.
24	Theres a total of 480 single compartment

1	analyses, and 1,054 multi-compartment analysis
2	scenarios.
3	And then, due to the highly
4	compartmentalized nature of the APR1400, the CDF is
5	generally distributed. Only 24 scenarios are higher
6	than 1 percent, 50 percent of the CDF is in the top
7	eight scenarios. Most of that is the main control
8	room because of the conservative analysis that we
9	did.
10	We don=t have an alternative shutdown
11	procedure at the time the analysis was done.
12	Next?
13	And then, for low power and shutdown,
14	there are 918 single compartment analyses and 6,071
15	multi-compartment scenarios and a low power shutdown
16	scenario is a combination of the initiator and the
17	POS.
18	The initiating event might change based
19	on the POS. And, like at power results, due to the
20	highly compartmentalized nature, the CDF is generally
21	well distributed.
22	MEMBER POWERS: I can=t resist pointing
23	out that you assume you have assumed away the
24	Brown=s Ferry Fire because of your credit for manual

1	suppression.
2	MR. ROZGA: Well, manual suppression can
3	fail. It can fail and, if it failed, then the room
4	continues to burnout, correct, yes.
5	MR. DREMEL: And, Brown=s Ferry was not
6	hot work, Brown=s Ferry was an inspection.
7	MEMBER POWERS: Close enough.
8	(Laughter.)
9	MR. DREMEL: But, from a fire PRA,
10	there=s a big distinction. Transients can happen
11	anywhere, a transient fire source. But, hot work
12	MEMBER POWERS: You=re splitting a hair
13	that I don=t even think needs to be done.
14	MR. DREMEL: We would not have assumed
15	away the Brown=s Ferry Fire because that is a
16	transient. Manual suppression is not credited for
17	transient fires.
18	MEMBER POWERS: Useful information.
19	MEMBER STETKAR: I have one a couple
20	comments on the main control room analyses, I wanted
21	you to get through the whole thing here, the way those
22	were performed, and make sure that I understand it,
23	is that you accounted for manual suppression in the
24	main control room as you said.

	138
1	That time window was assigned for a ten
2	minute time wind w and, that if it was suppressed
3	within ten minutes, abandonment was not required.
4	If it was not suppressed within ten
5	minutes, you assume that
6	MR. ROZGA: Yes.
7	MEMBER STETKAR: people would abandon
8	the main control room.
9	And, from there, it was just .1
10	conditional core damage probability without any
11	further evaluation.
12	MR. ROZGA: Right.
13	MEMBER STETKAR: I=m but, I don=t want
14	to get into why . because that=s a made up number.
15	What I=m more concerned about is the
16	large fraction of the fires that are extinguished
17	within ten minutes, but do damage inside the main
18	control room and could certainly affect subsequent
19	operator performance inside the main control room.
20	Those fires, as best as I can tell, are
21	simply ignored.
22	MR. ROZGA: There are there were some
23	tests done on the main control room enclosure. I
24	don=t remember the NUREG that it=s documented in.

	139
1	And, they had their main control room
2	fire scenarios and the result of that analysis was
3	that the driving force in the control room abandonment
4	was obscuration. It wasn=t necessarily heat or heat
5	flux, it was obscuration.
6	And, it occurred somewhere between 6 and
7	16 minutes.
8	The - that test enclosure was about half
9	of the volume of the APR1400 containment. And, the
10	for transients, we actually assumed eight minutes
11	and that=s the time to the peak heat release rate for
12	transient fire for cabinet fires.
13	We used ten minutes which gets you to
14	about 70 percent of the peak heat release.
15	And, those numbers fell well within the
16	that 6 to 15 minute range given the fact that, you
17	know, the size is smaller.
18	MEMBER STETKAR: Greg, in the interest of
19	time
20	MR. ROZGA: Yes?
21	MEMBER STETKAR: if you=11 allow me to
22	interrupt you, I m not arguing about what criteria
23	you used for me to leave this room, I=m raising a
24	concern about for the fraction of time when the fire

1	is extinguished, don=t have to leave the room.
2	MR. ROZGA: Yes.
3	MEMBER STETKAR: I stay here, but some
4	fraction of this control panel is now burned.
5	Now, that burned fraction of the control
6	panel, first of all, I probably can=t use the controls
7	on that fraction to do anything.
8	Second of all, they may have created
9	spurious signals because of the fire in the control
10	panel.
11	Third of all, maybe my performance isn=t
12	quite the same as it would have been in a plain
13	vanilla reactor trip.
14	And, those are the scenarios that I=m
15	concerned about -
16	MR. ROZGA: Yes.
17	MEMBER STETKAR: is how because I
18	don=t see any accounting for those effects where the
19	people extinguish the fire, whether it=s 8 minutes
20	from a transient or 10 minutes for a cabinet,
21	extinguish it, stay in the control room with some
22	degraded either human performance or degraded ability
23	to manually operate stuff or perhaps with some
24	spurious signals from the fire damage within whatever

1	fraction of the console is.
2	Those seem to be ignored in the model.
3	MR. ROZGA: Yes, we
4	MEMBER STETKAR: I don=t know how
5	important they are, but they seem to be ignored.
6	MR. ROZGA: Yes. We do impact the
7	operator actions. We do for all. We impact all
8	control room fire actions or, I=m sorry, we impact
9	all
10	MEMBER STETKAR: But that=s for fires
11	outside of the comtrol room.
12	MR. ROZGA: Right, right. And, recall,
13	we use the 1921 screening criteria for most of them
14	and then the top ten.
15	Regarding the control panels, most of the
16	fires in the containment, there are a couple of
17	control panels and those control panels are generally
18	away from where the operators I don=t know if you
19	have a
20	MEMBER STETKAR: I don=t want to split
21	hairs on the nomen clature of stuff that contains stuff
22	that controls other things. I know that there are
23	some panels, if you want to call them that, that are

1	consoles, and that I know that you have evaluated
2	fires in those separated panels.
3	I=m talking about fires in the operator
4	console. I=m sitting here at my console right here
5	and a fire in this thing that I=m sitting in front
6	of, whatever you want to call that, I=ll call it a
7	console.
8	MR. ROZGA: Yes, and that the electronics
9	in there consist of a PC and a monitor and a mouse
10	and
11	MEMBER STETKAR: Never seen a phone burn?
12	MR. ROZGA: I have not, but I=ve heard
13	that I=m sure that
14	MEMBER STETKAR: It probably has a DC to
15	DC power converters in it. It=s probably got power
16	supplies for monitors. It probably might even
17	have CPUs in it, I don=t know what=s in those
18	consoles.
19	MR. ROZGA: Yes.
20	MEMBER STETKAR: That=s only an
21	observation.
22	MR. ROZGA: Right. And, also understand
23	that if the if the computer or the monitor or the
24	phone at that station has a fire that there is

1	there is the safety console in the room, there=s
2	from the other operator stations, they can take over
3	some of those actions.
4	And, regarding the smoke, there is the
5	control room does have a main control room smoke HVAC
6	system. So, as time goes on, the, you know, the
7	conditions in the control room would be expected to
8	get better.
9	CHAIRMAN BALLINGER: Okay, well, okay.
10	I think this is a good place to stop for a recess.
11	We=11 recess until 12:30.
12	(Whereupon, the above-entitled matter
13	went off the record at 11:41 a.m. and resumed at 12:30
14	p.m.)
15	CHAIRMAN BALLINGER: Okay. We are back in
16	session.
17	MR. IN: Our next presentation is on the
18	Internal Flooding PRA, and it will be presented by
19	Mr. Ray Dremel.
20	MR. DREMEL: Good afternoon. I=m Ray
21	Dremel with Enercon. I=ll be presenting information
22	about internal flooding, and then I=ll continue on
23	with other external events. So the Internal Flooding
24	PRA, the guidance we use, we try to meet all the

1 supporting requirements of Regulatory Guide 1.200 Revision 2, and the ASME PRE Standard 2009 edition. 2 3 To the extent possible for a plant that doesn=t exist. 4 also tried to meet all the requirements 19.1. Standard Plan For the initiating event 6 frequencies, we used the pipe failure data presented at EPRI-TR-1021086. Next slide. 7 So the APR 1400 design greatly limits the 8 risk from internal flooding. The auxiliary building 9 is designed to have four quadrants. 10 In the basement, 11 the quadrants are sealed to a level of nine feet for 12 flooding, at least nine feet. So there=s almost no propagation from one quadrant to another. Within the 13 14 called emergency quadrants, there was what was 15 overflow lines, which are big holes in the floor that 16 pass a lot of water from one elevation down to 17 And that maintains any water that might be released an upper revelation within the same quadrant 18 19 until it gets down to the basement. 20 in the auxiliary building, most of Also 21 the flood sources are finite volume due to being 22 closed loop. So there=s no essential service water 23 in the auxiliary building. The large volume sources

are fire water, domestic water, and raw water, which

1 have very limited flow rates of a couple hundred to 2 four hundred gallons a minute per pump. So if you 3 have large volume, then the flow rate is limited. 4 But that gives you a lot of time to isolate a break. 5 Also, within any elevation there=s a lot 6 of rooms. So you have a flood in one room, you have 7 big concrete walls just to prevent you from spraying equipment in another room and affecting multiple 8 9 systems or multiple trains of equipment. The turbine building, it=s i|solated from all other buildings. 10 You can=t get from the turbine building to the 11 12 auxiliary building at grade. It=s a large, open 13 There s a large overflow from the grade 14 level to the outside, which is designed to pass 15 hundreds of thousands of gallons per minute. 16 The emergency diesel generator building 17 for the alpha and bravo steam generators - again, it=s isolated from other buildings. 18 The flood sources in there are limited. 19 It=s limited to the 20 diesel lube oil, and some fire diesel fuel oil, 21 protection. The compound building has no 22 equipment in it, and there=s very limited potential 23 for a flood in a compound building to propagate -24 the auxiliary building and cause excuse me to

1 We do have a few scenarios of that happening. 2 It=s because we don=t have design of the 3 as-built plan. If we were actually able to go in and 4 look at a plant, we=d probably say you=re not going 5 to propagate across to the auxiliary building. 6 the water is going to go down. But without having a 7 real plant, we camet do it. And those scenarios are not significant. 8 9 The CCW heat exchanger building, there=s 10 very few active domponents in there. The only large 11 volume source there is ESW. We have a ESW model. 12 The frequency of pipe breaks is very low compared to 13 the random loss of ESW frequency. The ESW building, that only has ESW in the pumps. 14 Because the pumps 15 are located below grade. In order for that to pump any significant 16 17 amount of water that could potentially propagate to other buildings, these large pumps would have to 18 19 operate submerged under many feet of water for a 20 fairly long period of time. So we just don=t consider 21 propagation from an ESW break in an ESW building 22 through the tunnels to anything else to be credible 23 And 4kB motors just don=t run submerged scenario.

under many feet of water.

1	So defining a flood-induced initiating
2	event. It=s an uncontrolled release of any fluid
3	that also fails PRA equipment. Not just water. It
4	could be fuel oil, lube oil, anything that=s liquid.
5	Steam. We define an initiating event as anything
6	that causes an immediate reactor trip or requires a
7	tech spec shutdown within twenty-four hours.
8	So if you have a fail in equipment, and
9	you have tech spec say be shut down within seventy-
10	two hours, we didnet consider that an initiating event
11	if it says be shut down within eight hours. We didn=t
12	include that as an initiating event. We took no
13	credit for recovery there.
14	When we did the flood propagation,
15	because we don=t have a real plant to look at, we had
16	to make some conservative assumptions. So we took
17	credit for flood barriers to remain intact up to their
18	design level. That=s a pretty safe, pretty standard
19	assumption for an existing plant. We did not take
20	credit for any flood mitigation above the design
21	level. So in some of the upper elevations between
22	quadrants or between rooms, you may have a design
23	flood barrier for six inches of water.
2.4	But it=s a concrete wall that hounds a

	148
1	switch gear room. I would not expect to see any
2	penetrations going through there down low. But
3	because we don=t know, we say as soon as you get to
4	six inches, water propagates across that barrier.
5	MEMBER BLEY: You mentioned - excuse me,
6	Ray. You mentioned that you looked at all the other
7	fluids besides water. That gas turbine generator,
8	what fuel does it use?
9	MR. DREMEL: That I don=t know. But that
10	is outside -
11	MEMBER BLEY: It=s on the outside?
12	MR. DREMEL: Yes.
13	MEMBER BLEY: Okay.
14	MR. DREMEL: And failure of that would not
15	have caused a reactor trip. Or require a reactor
16	trip.
17	(Laughter.)
18	MEMBER BLEY: But it=s outside.
19	MR. DREMEL: Yes.
20	MEMBER SUNSERI: You also said a couple
21	of times that you don=t have a real, actual plant to
22	go look at. What about Shin Kori or the Amaritz
23	plants? I mean, those are pretty far along. Aren=t
24	they the same physical layout?

	149
1	MR. DREMEL: They are - I would expect
2	them to be similar. But when we did this analysis,
3	they weren=t in a state that we could have done that.
4	MEMBER SUNSERI: Okay. Because it=s just
5	a plane trip, right?
6	MR. DREMEL: Yes.
7	MEMBER SKILLMAN: Ray, did you confirm -
8	for instance these assumptions that you
9	communicated?
10	MR. DREMEL: I=m sorry?
11	MEMBER SKILLMAN: You communicated that
12	you made assumptions -
13	MR. DREMEL: Yes.
14	MEMBER SKILLMAN: In order to complete
15	this work. Did you confirm that those assumptions
16	are communicated as COL items in the DCD? You=ve
17	made assumptions to give you a success path. That
18	success path needs to be communicated into the design
19	control document.
20	MR. DREMEL: And the assumptions are that
21	the design barriers are as designed. So I don=t
22	believe we have a COL item to confirm that the -
23	MEMBER SKILLMAN: Oh, for the period?
24	MR. DREMELL Yes. Then their design basis

1	for the flood barriers doesn=t change.
2	MEMBER SKILLMAN: Let=s back up. You
3	said we don=t have a plan to look at.
4	MR. DREMEL: Right.
5	MEMBER SKILLMAN: But we=re making
6	assumptions.
7	In my view, that means that the
8	assumptions that you are making must be communicated
9	into the COL items for what will become an as-built
10	plan.
11	MR. DREMEL: Okay.
12	MEMBER SKILLMAN: Are those items there?
13	MR. IN: There isn=t a COL item for the -
14	to verify that, you know. Once the design is in
15	place, it has to be looked at. There isn=t a COL
16	item.
17	MR. SKILLMAN: Is that an ITECH or just a
18	COL item?
19	MR. IN: It=s a COL item. Because it=s
20	not only - they have to re-do the assessment. The
21	PRA assessment.
22	MR. SKILLMAN: Based on what will be the
23	as-built?
24	MR. IN: Yes.

1 SKILLMAN: Okay. Thank you. 2 DREMEL: Okay. Next assumption we MR. 3 made was non-watertight doors are going to fail once water level on one side of them reaches one foot, if 4 5 that failure makes the situation worse. 6 failure of the door helps you, we assume that the 7 doors remain intagt. An example of that would be you have a pipe break in a hallway. You have a door that 8 9 goes down a stairwell within the same quadrant. 10 you have a door that goes across the quadrants to a 11 different quadrant. 12 So even though the door to a different 13 quadrant might be up on a six inch curb, if we did not say the door going down the stairwell would fail 14 remains 15 first. We said, that door intact. 16 Therefore, propadation to the other quadrant would 17 So any barrier failures or propagation that would ameliorate the event - we didn=t consider those. 18 19 We did credit flow through drains, emergency overflow 20 lines, or other pathways to the extent that they are 21 credited in the design basis. 22 So there=s a certain place where the 23 design basis credits flow through a drain up to a 24 certain gallon per minute. Because that=s a design

1 requirement. credited that. The flow through we 2 occurring. The emergency overflow those drains is 3 lines are basically a big hole in the floor that pass 4 a lot of water just down to the next elevations. 5 did credit those. 6 Based on all the accident sequences, we have one hundred and thirty events that we explicitly 7 analvzed. Most of these events are analyzed because 8 9 they are related | we assumed that a manual shutdown Some of them we assumed would have 10 was required. 11 caused a reactor trip. High energy line breaks are 12 a unique case, Regulation Guide 1200 and the ASME Standard says you have to treat high energy line 13 breaks in a conservative manner. 14 15 So within the auxiliary building, 16 auxiliary feed water and steam lines are analyzed 17 inside a HELB barrier that=s designed for a complete severance of that line. So those HELB barriers 18 remain intact up until the design of the HELB. 19

auxiliary feed water and steam lines are analyzed inside a HELB barrier that=s designed for a complete severance of that line. So those HELB barriers remain intact up until the design of the HELB. There are some other HELB barriers, where you have auxiliary steam that runs or operates intermittently for rad waste processing. And for those, we said if you have a break bigger than the design basis, the barrier is going to fail. It=s going to fail everything in that

20

21

22

23

1 room and the first barrier to the next room. 2 conservative assumption, it=s auxiliary steam. 3 it=s consistent with other places we=ve looked at in 4 the industry. It gives you the insight you need. 5 We also assumed that any high energy line 6 break will actuate all the fire protection systems in 7 Steam doesn=t give you anything, but the fire protection will turn things off. The CDF we see 8 is two times ten to the minus seven per year. 9 10 pretty low frequency. And there=s 11 significant event to flooding. Most of the breaks 12 that do contribute to damage are beyond design basis breaks to the fire protection system. 13 design basis break of that pipe is 14 15 the old standard divided by two times the thickness 16 of the pipe divided by two. And we are going beyond 17 We are looking at double ended breaks of the fire protection system. If we had an actual plant to 18 go look at, I would expect the risk would go down 19 20 Because we can now look at the doors. quite a bit. 21 You know, what level will the doors fail. Where are 22 the holes in the walls? Just because a wall is not

a flood barrier, if you have a foot-thick concrete

wall with no penedrations in it, no water is going to

23

1	go across. Or to significant amount of water is
2	going to go across. So if we look at that, I would
3	expect flooding risk to go down.
4	The other thing that is interesting is
5	that most breaks don=t require isolation. Or there
6	is a very long time available to isolate the break.
7	Each quadrant of the auxiliary building can contain
8	hundreds of thousands of gallons of water before you
9	could potentially propagate - or go above nine feet,
10	where we assume propagation could occur. And that is
11	internal flooding in a nutshell.
12	MEMBER STETKAR: You didn=t think you
13	were going to get away unscathed, did you?
14	(Laughter.)
15	MEMBER STETKAR: Just a couple of
16	observations. When I looked at the results, this is
17	again similar to what I mentioned for the seismic
18	analyses. I noticed that there were cut sets that
19	involved flooding in turbine-driven auxiliary feed
20	water pump room D - as in dog - for that. I couldn=t
21	find any for C - Charlie - I don=t know why that is?
22	MR. DREMEL: In the flooding, there are
23	physical asymmetries.
24	MEMBER STETKAR: Okay. That might

1	explain it. That was for the at-power. And in the
2	shutdown, if I look at tables 19.1-107 and 19.1-108
3	and 19.1-10, it=s got all of the flooding. About -
4	if I do a rough cut, table 19.1-107 shows that about
5	ninety-eight percent of the core damage frequency in
6	plant operating states five and eleven comes from
7	prior protection flooding. Which is mostly around
8	the plant.
9	In plant operating state eleven, a very
10	small fraction is in plant operating state five. And
11	the duration of plant operating state five is about
12	three and a half hours longer than plant operating
13	state eleven. And of course, the heat levels are
14	higher in plant operating states. So I was curious,
15	why that asymmetry? That one I couldn=t figure out.
16	That=s just plant operating state, I=m not talking
17	about locations. It=s just this slice. That one I
18	don=t get. So anyway, that=s on the record.
19	MR. DREMEL: It could be because for low
20	power shutdown PRA, we assume in the first half of
21	the outage they are working on one division. And in
22	the second half of the outage, they are working on
23	the other division. So if I have -
24	MEMBER BLEY: Of everything?

1	MR. DREMEL: Yes, yes. So it=s just like
2	consisting with you have a division one outage,
3	division one part of the outage and a division two
4	part of the outage. So if I have a flood in my
5	division two pump room, while I=m working on my
6	division two pump, it contributes nothing to risk.
7	Because that shut down cooling pump is out of service
8	anyway. When you go to the other half of the outage,
9	if I have a flood in my division one pump room, and
10	my division two pump is out of service -
11	MEMBER STETKAR: Just be careful, because
12	the tech specs require you to have both divisions
13	available when level is low. I=m talking
14	particularly about five and eleven which were mid-
15	loop.
16	MR. DREMEL: Okay, but you can work on -
17	there=s other equipment that you can work on.
18	MEMBER STETKAR: That=s okay. I just
19	raised it as an observation. I don=t know the answer.
20	MR. DREMEL: Okay. Now I can move on to
21	other external events. Analysis of most of the other
22	external events is identified as a COL item or COL
23	items. The external events considered identified in
24	DCD chapter table 2.0.1. For transportation

1 accidents, there=s a COL item to confirm that they 2 are not risk significant. Obviously, we don=t have 3 a plant location to analyze. We don=t have a site to 4 analyze. Turbine missiles were looked at. 5 The APR 6 1400 has favorable orientation for turbine а 7 missiles. In DCD chapter 3.5.1.3, the probability of two point one times ten to the minus nine per year of 8 a turbine missile was determined based on a twelve-9 year inspection interval. 10 The events that were 11 analyzed were high winds, including tornadoes. 12 design basis tornedo was two hundred and thirty miles 13 That=s based on region one of Reg Guide per hour. 1.76, region one. That tornado has an exceedance 14 15 frequency of ten to the minus seven per year. So we 16 screened that out as a conservative screening. 17 Similarly, design basis hurricane is two hundred and sixt♥ miles per hour and per Reg Guide 18 19 1.221, every place except Southern Florida - that 20 hurricane has an exceedance frequency of less than 21 ten to the minus seven per year. High winds are not 22 considered a problem. Next. 23 identified for COL items the COL 24 applicant to do. They have to do a site-specific

1	risk assessment for the events on the left. And then
2	for the events on the right, they just have to confirm
3	they are not an outlier. You=re not going to build
4	a nuclear plant next to an unstable mountain or next
5	to a volcano. So there=s a COL item to confirm these
6	events. Based on that, we consider that risk from
7	other external events is going to be a negligible
8	contributor. That=s all I have for other external
9	events.
10	MR. IN: The next presentation is on the
11	low power end shutdown PRA. That will be presented
12	by Mr. Kim.
13	MR. J. KIM: My name is Jae Gab Kim from
	MR. J. KIM: My name is Jae Gab Kim from KEPCO E&C. I=m going to discuss low power shutdown
14	
13 14 15 16	KEPCO E&C. I=m going to discuss low power shutdown
14 15	KEPCO E&C. I=m going to discuss low power shutdown PRA. A key document to follow for shutdown is called
14 15 16	KEPCO E&C. I=m going to discuss low power shutdown PRA. A key document to follow for shutdown is called regulatory industry support. Associated with the
14 15 16 17	KEPCO E&C. I=m going to discuss low power shutdown PRA. A key document to follow for shutdown is called regulatory industry support. Associated with the NRC=s report. Every PRA report is also reported
14 15 16 17	KEPCO E&C. I=m going to discuss low power shutdown PRA. A key document to follow for shutdown is called regulatory industry support. Associated with the NRC=s report. Every PRA report is also reported through the shutdown initiating event. Next slide.
14 15 16 17 18	KEPCO E&C. I=m going to discuss low power shutdown PRA. A key document to follow for shutdown is called regulatory industry support. Associated with the NRC=s report. Every PRA report is also reported through the shutdown initiating event. Next slide. These are touched on in low power
14 15 16 17 18 19	KEPCO E&C. I=m going to discuss low power shutdown PRA. A key document to follow for shutdown is called regulatory industry support. Associated with the NRC=s report. Every PRA report is also reported through the shutdown initiating event. Next slide. These are touched on in low power shutdown. And singularly, the power of plant
14 15 16 17 18 19 20 21	KEPCO E&C. I=m going to discuss low power shutdown PRA. A key document to follow for shutdown is called regulatory industry support. Associated with the NRC=s report. Every PRA report is also reported through the shutdown initiating event. Next slide. These are touched on in low power shutdown. And singularly, the power of plant operating stage development. So detailed analysis

1	guess you put 1300 degrees after the peak clouding
2	temperature instead of 1340. And the basis of 1340
3	was attributed to an ASME standard, which I didn=t
4	have access to. But to the Reg CR report that you
5	cited in the prior slide. If I pull that string,
6	it=s a Surry analysis and it was the clouding
7	temperature where you would have core damage within
8	a short period of time. So basically, that success
9	criteria is based on a Surry analysis if I=m
10	understanding this philosophy. What gives you
11	confidence that forty degrees difference is enough to
12	have for that success criteria?
13	MR. J. KIM: As you said, and as in the
14	standard as in the Reg CR inspection manual report.
15	1300 Fahrenheit is from the report. But these
16	evaluations, that's something that's assumed. 1300
17	Fahrenheit.
18	MEMBER REMPE: I=m sorry. I=m having
19	trouble following. Maybe a little slower and louder.
20	MR. J. KIM: This must be a little
21	continuity assumption. 1300 Fahrenheit is much lower
22	than 1340 Fahrenheit. So, this PR group time is much
23	shorter than 1300 Fahrenheit.

1	degrees is sufficient conservatism, because I would
2	assume APR 1400 is a much higher power plant than
3	Surry.
4	MR. PREMEL: There are also some NRC
5	inspection manual chapters out for shutdown risk
6	assessment. And they reference the 1300 degrees as
7	- keep your temperatures less than 1300 degrees, you
8	should be okay for shutdown. And what we found when
9	we did the success criteria runs, 1300 is here.
10	You=re either way down here, or you=re way up here.
11	MEMBER REMPE: Okay.
12	MR. DREMEL: So it=s really - you can
13	debate, but -
14	MEMBER REMPE: Okay. I was not sure. I
15	didn=t have time to go look through those inspection
16	manuals. So that s comforting that apparently they
17	across the board said 1300 Fahrenheit is fine. And
18	then you=ve done some analyses that make you feel
19	comfortable.
20	MR. DREMEL: Yes. Well, there=s no place
21	where we got, you know -
22	MEMBER REMPE: Real close?
23	MR. DREMEL: Yes.
24	MEMBER REMPE: Okay. Thank you.

1	MR. J. KIM: Next slide. To decide POS
2	division, make use of prior experience with current
3	and next generation analyses. At this table, it=s
4	just to show the Reg CR report. The total number of
5	POS is fifteen. Next slide.
6	CHAIRMAN BALLINGER: Excuse me. We are
7	either being serenaded by the workout in the gym
8	below, or there-s somebody on the phone. We are
9	being serenaded? Okay, we can=t do anything about
10	that.
11	MEMBER CORRADINI: It will stop at one
12	o=clock.
13	(Laughter.)
14	CHAIRMAN BALLINGER: Keep going.
15	MR. J. KIM: Okay. This table is APR 1400
16	Plant Operating States and states definition. Total
17	number of POSs is fifteen, which determined the base
18	they=re on. Our primary system water level and the
19	pressure and the temperature and the TS mode. Which
20	is related to the substance criteria, as related to
21	the variable time after event. And the system
22	arrangement. Next slide.
23	
	APR 1400 Initiating event has been

Reg and NS data, but some specific initiating event from the two, the initiating -- and the APR TR report 1003113. Next slide. So an appropriate combination of generic and design-specific event frequencies used.

MEMBER STETKAR: Can I stop you here? I have several comments on low power shutdown. The first one deals with partly this topic. You have the only event models really documented in the DCD are for plant operating states five and eleven. So I=11 only speak to them, since I know nothing about the others.

There are statements in the DCD that says that one train of shutdown cooling is operating and other is standby. And there are also ih statements in the systems= analyses saying that no changes were necessary for complement cooling water or essential service water from the full power PRA models to the low power and shutdown PRA models. I look at sections of the DCD. For example, 5.4.7 in the DCD, it explicitly says that in the early part of the outage, two trains cool down. Assuming two trains are in service in the early part of the outage, that seems to extend through plant operating state five.

6

7

8

9

10

11

12

13

14

15

16

17

18

19

20

21

22

23

1	There are things in the DCD that
2	explicitly say that in the early part of the outage
3	- this is in chapter nine, section 9.2.2.2.4.2. Four
4	component cooling water pumps in 9.2.1.2.3.2 for
5	essential service water pumps are operating. That is
6	different from the full power model, and it=s
7	different than the configuration that you used in
8	plant operating state five.
9	Now, why do I bring it up now? Well, you
10	have initiating events that says the normally running
11	train of shutdown cooling fails. Or it=s
12	interrupted. That=s S1. And the normally running
13	train fails, that s S2. If both trains are running,
14	those frequencies are much different. The
15	consequences are much different. The recoverability
16	is much different
17	So now I=m confused about what is the
18	actual configuration of running in standby equipment
19	in each of the plant operating states? All the way
20	from plant operating - every plant operating state.
21	And I don=t know what they are. I=m only left with
22	things that are contradictory between the PRA and
23	other parts of the design certification.
24	MR. PREMEL: One point is, and you

1 mentioned section 5.4.7 that talked about a two train 2 So you need - the DCD analyzed as needing cool down. 3 two trains to remove decay deep and cool down so that 4 you can get into refueling. But I believe one train 5 is adequate to remove decay heat. 6 MEMBER STETKAR: I will give you the 7 quote so we have it on the record. The shutdown cooling system or SCS reduces the RCS temperature as 8 Two train cool down, normal operation. 9 follows. Ι 10 can continue to give you all of the temperatures. 11 can continue to give you all the way down to 120 12 degrees Fahrenheit within ninety-six hours. If I look at the timeline for the plant operating states, 13 that takes me out into plant operating state five. 14 15 Now if that=s normal operation, and I=m 16 in the power plant, and I=ve been in power plants, we 17 normally like to get cold kind of as quickly as 18 possible to get the outage started. So we ran pretty 19 much everything that we could do to get cool down. 20 Not so much at the end of the outage. So it might be 21 different in eleven compared to five. But at the 22 front end of the outage, a lot of plants have pretty 23 much everything running. I=mjust making 24 observation. That, by the way, affects both the

initiating event 1 frequencies. You can=t use generic 2 initiating event frequencies because there is no such 3 thing. 4 Ιt allso affects the recoverability 5 because if I now have a common cause failure that 6 affects both of my operating trains, I can=t recover 7 shutdown cooling. I have to go to feed and bleed cooling and so forth. It affects time windows, I 8 9 mean it affects everything. So I=11 just make that The other sections, chapter nine, also 10 observation. 11 indicates that it=s normal operation during the 12 initial cooling. 13 J. KIM: Okay. Next slide. This 14 is the Accident Sequence Analysis. 15 analysis models the combinations of system responses and operator actions that could occur during the 16 17 Event is used to delineate these event. Tree combinations to present these events. 18 This diagram 19 is one example of an accident sequence. Next slide. 20 Success criteria is the ability to be 21 using MAAAP 4 and RELAP5. Considering the initiating 22 event, limiting plant conditions for each POS, and 23 equipment availability specified for each accident 24 And the core damage temperature for the sequence.

1 RDR are 1300 Fahrenheit. Based on the ASME PRA 2 Standard and NRC Inspection Manual. Next slide. 3 At this Level 2 analysis, for POSs with 4 RCS and containment intact, Level 2 conservatively using conditional 5 estimated the full power 6 probability of large release. For POSs with RCS 7 intact but containment hatch open, failure to close hatch assumed to be large release. The successful 8 9 closure of the hatch before boiling evaluated using 10 full power CPLR. 11 And for POSs with RCS head removed, 12 detailed Level 2 RA developed. Also for portions of 13 the analysis, the full power Level 2 methodology are 14 considered conservatively. And LPSD Level 2 Fire 15 modeling are the same as internal events. 16 MEMBER STETKAR: Now, there=s an 17 assumption in the PRA that says isolation or containment demonstrations is assumed to be identical 18 19 to the containment isolation modeling in the Level 2 20 I will tell you that I=m pretty darn sure model. 21 plant shutdown modes, that during the 22 containment, high volume containment purae is 23 operating. That | certainly is not modeled in the 24 full power PRA model.

1	I=11 make the same comment that I made
2	this morning. If that is operating and is not
3	isolated, that=s a big hole. That=s a much bigger
4	hole in the side of the containment which has both of
5	the effects that I mentioned earlier. That it=s good
6	that you might not get an over pressure failure of
7	the containment. It=s bad because it might be a
8	contributor to large releases. So, I=m kind of
9	questioning this notion that you didn=t have to change
10	the containment isolation models from full power to
11	low powering shutdown.
12	MR. J. KIM: Could you show me that?
13	MEMBER STETKAR: Sure.
14	MR. J. KIM: Could you give me more
15	detailed information?
16	MR. LEARY: Jeff Leary with Enercon. The
17	statement you made is true. It=s something we will
18	take a look at. The additional contribution from it
19	is going to be an additional line out of -
20	MEMBER STETKAR: It=s not necessarily an
21	additional line. Remember, this is a big line. So
22	it=s a big enough line - certainly this one is big
23	enough. I don=t know its physical size, because I
24	couldn=t find it in the DCD. But I know it=s big.

1	And it=s certainly big enough to exhaust containment
2	heat. If that line is open, there=s no way you can
3	ever get an over pressure failure of the containment.
4	It just is not going to happen.
5	That=s good - you know, that=s the good
6	news part of it. The bad news is if the line is open,
7	everything=s going out. So it=s different than any
8	of the other small water isolation lines that also
9	have to be is lated to satisfy whatever the
10	containment isolation criteria are. That one behaves
11	differently.
12	MR. LEARY: But your statement is true,
13	that the LPSC model used the same containment
14	isolation model as the F power.
15	MEMBER STETKAR: Okay. Thank you.
16	MR. J. KIM: To continue. Results are
17	dominated by operator recovery failures. And our
18	results indicate, as expected, that the draindown and
19	reduced inventory POSs are highly risk significant.
20	During power shutdown, you cannot use secondary
21	generator, and also the signal is bypassed.
22	MEMBER STETKAR: The two comments I=11
23	make - and I=ll try to be quick - well, I have to
24	make three. Because results indicate, as expected -

	169
1	the results will always indicate, as expected, if
2	that=s where you concentrate all of your activity.
3	Sometimes people are surprised when they look at other
4	plant operating states and find out that they are
5	more important than the mid loop operations. There
6	have been studies that have found that.
7	So as expected is a warning to me that
8	says, well, we thought these were going to be most
9	important. That s why those are the only ones that
10	I can see in the DCD. And that=s why you concentrated
11	all of your effort there. That=s sort of
12	philosophical.
13	Two comments that I had on this notion of
14	the importance of operator actions - I have a lot of
15	comments on the Level 2 models. But when you
16	reevaluate, and I heard earlier that you are
17	reevaluating all of your HRA for the next update.
18	There were several scenarios when I could not
19	understand the relative timing and the success
20	criteria for operator actions.
21	In a particular operator action MI for
22	makeup or isolation of a drain down path, I had no
23	idea how much time was available for the operators to
24	do that. Some things led me to believe that it was

1	four or five minutes. Some things led me to believe
2	that it was a couple of hours. That needs to be
3	clarified and make sure that the HRA is crisp there.
4	There is one combination of things that
5	I was especially puzzled by. And that is in the
6	Level 1 model. There is an operator action - it=s
7	called feed and bleed, but it=s basically makeup to
8	the primary system when you don=t have shutdowr
9	cooling. It=s put more cold water in and you can call
L 0	it feed and boil if you want. Or you can call it
L1	feed and spill - anything. It=s that sort of thing.
12	And there=s a statement in there that
L3	says that the available time window for that action
L 4	is 2.2 hours based on the start of core damage. Ther
L 5	in the Level 2 model, there is a top event called
L 6	melt stop, which requires that the operators start
L7	putting water into the vessel to either prevent core
L 8	damage or stop a melt in progress. It=s not quite
L 9	clear to me which of those two apply. And there is
20	separate credit for that.
21	Now if I as an operator have sat around
22	for 2.2 hours and have not decided to put water in
23	the vessel, and that=s the amount of time before the
24	start of core damage, why am I suddenly going to get

1	really really smart in a relatively short period of
2	time and start putting water in from the same sources.
3	So I was really puzzled. Because there are two
4	distinct actions that happen to be separated by this
5	artificial Level 1 and Level 2 split for the same
6	people putting the water in the same place with the
7	same pumps.
8	(Laughter.)
9	MEMBER BLEY: It=s the kind of thing that
10	if a shift change had occurred maybe that=s -
11	(Simultaneous speaking.)
12	MEMBER STETKAR: This is 2.2 hours. You
13	know, fortuitous maybe.
14	MEMBER BLEY: Twenty-five percent chance
15	of a shift change
16	MEMBER STETKAR: Okay.
17	MR. LEARY: Jeff Leary with Enercon
18	again. The action that you=re referring to in the
19	Level 2 part of it is taking credit for additional
20	indication that would be occurring with the SAMGs
21	when core exit thermal couples reach 1200 degrees
22	Fahrenheit. Taking the credit for additional cues
23	and information that would not have popped up sooner.
24	So there=s a dependency analysis between the actions.

1	MEMBER STETKAR: Yeah, my dependency would
2	have been one, but the problem is the story about FB
3	which is the initial makeup. It also mentions core
4	exit thermal couples and the onset of core damages,
5	the critical condition that would be the end point of
6	that time window. So it=s hard - in principle, I
7	could wait for 2. 19 hours and still win because the
8	core exit thermal couples start to go up for the feed
9	and - whatever we want to call it - feed and boil,
10	feed and whatever.
11	MEMBER CORRADINI: Since John finds these
12	interesting things, is this just a mechanical - a
13	bureaucratic separation of Level 1 and Level 2?
14	MEMBER STETKAR: I believe that it is.
15	MEMBER CORRADINI: That=s what it sounds
16	like.
17	MEMBER STETKAR: The problem is the
18	stories - again if I just read the stories about
19	these actions, the story about melt stop, the later
20	one says, well yeah. We recognize that early on in
21	the event, people could have tried to make up and
22	they might not have, but there would be additional
23	cues. I can buy that, except for the early action
24	seems to consume the entire time until core damage

1	begins. And that time is important, because the time
2	affects the human error probability for that initial
3	action.
4	MR. LEARY: I can say that the dependency
5	was evaluated and it=s something that is -
6	MEMBER STETKAR: I know you said that. I
7	just wanted to raise - that one bothered me in
8	particular. The other one that I mentioned about
9	time available for feed and boil in some scenarios -
10	I call it feed and boil to distinguish from the other
11	thing. And for make up - it=s called make up and
12	isolation, but there are very few that you can
13	isolate. So basically getting water in before
14	something undesired happens. Those time windows, to
15	me, were not documented very well.
16	And I just wanted to raise those because
17	you said you=re re-doing the HRA. And in terms of
18	flags that they raise to me where the HRA people might
19	need some more clarity. The second one being a Level
20	1 to Level 2 issue. The first one all being kind of
21	Level 1.
22	MR. LEARY: Okay, thank you.
23	MEMBER STETKAR: Thanks. And that=s
2.4	important, obviously because as you=ve mentioned, HRA

1	is the whole story on the low power end shutdown.
2	Thank you. Sorry
3	MR. Thank you, that concludes the
4	presentation - all presentations for 2.1.
5	CHAIRMAN BALLINGER: Thank you. Thank
6	you. We=ve got a change in the schedule in that some
7	people have flight schedules this afternoon. And so
8	what we=re going to do is to continue with KHMP to do
9	chapter 19.2. And then we=ll so the staff
10	presentations in order.
11	MR. SISK: Rob Sisk, Westinghouse.
12	Thank you, Chairman. If we can, that would be very
13	helpful. We=ll call our people up and be ready to go
14	in just a minute.
15	CHAIRMAN BALLINGER: Okay, so you=ve just
16	go to change out?
17	MR. SISK: Exactly.
18	(Simultaneous speaking.)
19	MR. B KIM: Good afternoon, ladies and
20	gentlemen. My mame is Byung Jo Kim from KEPCO
21	Engineering and Construction Company. Before I
22	begin, let me introduce my co-workers. In Chul Ryu,
23	he=s the Team Leader of the Central Analysis Team in
24	my company. And Dr. Chan Y. Paik from the Fauske &

1 Associates in Не is the Technical Chicago. 2 Consultant for this project, the main calculation. 3 This morning and in the previous session, we discussed the probabilistic risk assessment for a 4 5 very wide spectrum. This session, I would like to 6 talk about the Chapter 19.2, Severe Accident Evaluation from the deterministic viewpoint. 7 the section overview. 8 9 Today Ι have four technical topics. First one is the severe accident prevention design. 10 11 The second one is the severe accident mitigation 12 features, and the deterministic evaluation method origin, why there are assumptions for the evaluation 13 and the variation. The third topic is containment 14 for MELCOR and analysis, it will be discussed. 15 we will talk about the severe accident management 16 17 framework, and a short summary will be given at the end of my presentation. 18 19 Severe accident evaluation is performed 20 to confirm to APR 1400 design, with the relevant 21 quidance such as the SECY 93-087 and 10 CFR 50.44 and 22 Reg Guide 1.216. | Today=s first topic is the severe accident prevention design. The APR 1400 is designed 23 24 to prevent sever's accidents from the anticipated

1 transient without scram by digital safety system and 2 diverse protection system. 3 Severe accident initiated from the mid-4 loop operation can be prevented by instrumentation or shutdown operation. 5 Shutdown cooling system design, steam generation mozzle dam integrity, and alternate 6 7 decay heat removal method. Severe accident following station blackout will be prevented by alternate 8 current, starting alternate AC, and manually aligned 9 to provide power to Class 1E 4.16 kV when EDGs fail. 10 11 Fire detection, automatic and manual fire 12 suppression and fixed fire prevention are designed in 13 APR 1400 to prevent severe accident following the fire incident. Intersystem loss of coolant can be 14 15 recorded at safety injection system, shutdown cooling 16 system, chemical and volume control system, 17 containment system, and et cetera. Because 18 sections of this system and interfaces are designed to withstand full RCS operating pressure or have a 19 20 leak-test capability, valve position indicators in 21 the control room and high-pressure alarms to warn the 22 operators. 23 So CVCS from ISLOCA can be prevented in 24 APR 1400. There are other features incorporated in

1 APR 1400 to prevent severe accidents, including two 2 independent of turbine-driven feedwater pumps, when 3 AC power is not available. And shutdown cooling 4 pumps can be used as a backup of containment spray 5 pumps during a LOCA event. Feed and bleed operation 6 using safety injection system and pileup operating safe repairs. 7 severe accident 8 Second topic is 9 mitigation to keep up of today=s presentation. 10 already discussed the overview of containment design 11 in terms of severe accident management. And severe 12 accident progression, both in-vessel and ex-vessel. Then I will introduce design features equipped in APR 13 1400 and the performance variation as a result of 14 15 those features. Containment is the role of the rest of 16 17 the severe accident - so it is a more simple kind of structure in the severe accident mitigation. 18 19 containment 1400 is concrete structure 20 cylindrical and dome part. Concrete second is 4.5 21 feet and 6mm thick steel liner plate is installed on 22 the inside of the dome and cylindrical wall to prevent 23 leak-tightness as on the basemat concrete area. 24 Design characteristics of the containment

1	in terms of severe accident management is that it has
2	a large free volume and dry-type containment. In
3	order to accommodate the condensable and non-
4	condensable gases generated during the severe
5	accident. Also inside the containment, natural
6	mixing is achieved throughout the containment
7	atmosphere.
8	Design pressure limit of the containment
9	should be designed to meet the severe accident
10	internal pressurization challenges. In other words,
11	design pressure limit of the containment should meet
12	the factored load category criteria, as noted in Reg
13	Guide 1.2016. I will discuss this issue later.
14	MEMBER REMPE: So is this good time to
15	bring up this question about is there anything special
16	in the cavity? I think the answer is no. It=s just
17	that when I look at the drawings of the containment
18	building. This thing about a debris trapper or a
19	core debris chamber. That=s just an area that=s -
20	there=s nothing special in that area, right?
21	(Simultaneous speaking.)
22	MEMBER REMPE: Okay, thank you.
23	MR. B. KIM: Here you can see the key
24	phenomena in the progression of severe accident for

APR 1400 design. 1 So while there is an initiating insufficient 2 surface begins with in the 3 Then the cores start to heat indications. 4 creating oxidation. Fuel marking and COL information in the lower half | and finally, direct result failure 5 is inevitable if operators recovery has been failed. 6 7 Regarding the vessel failure mode, five events are integrated in 8 mechanical the severe accident code MAAP, such as ejection of a penetration 9 tube, creep rupture of the lower head, and attack of 10 11 vessel wall of overlying metal layer. 12 MEMBER REMPE: So again, I guess I=d like In this accident analysis 13 to interrupt you here. there=s some tables in Appendix D that 14 report, 15 carefully detail the corium composition and mass in the lower plenum for different types of vessel failure 16 17 evaluations. And so I know how much is in the lower plenum, but I domet know how much of the material 18 For example, if you had this attack 19 went ex-vessel. of the vessel wall by the overlying metal layer, would 20 21 you just release the metal and keep the UO2 materials 22 If you have a penetration at the within the vessel? everything goes 23 bottom, Is that out? а true 24 Because I could not find that, but maybe assumption?

1	I missed it in all the documentation.
2	MR. B. KIM: Right. Yes, you are correct.
3	MEMBER REMPE: Okay, good.
4	MR. PAIK: This is Chan Paik from FAI.
5	Whatever the corium debris, above the failure
6	location. Elevation is locating as an initial
7	pressure failure. And then we could have subsequent
8	to creep rupture of the lower half. Whatever is
9	remaining still heats up. So that can have later
10	failure. And then later failure, we assume that
11	failure will cause at that bottom of the vessel and
12	that will locate the rest of the material in the lower
13	plenum.
14	MEMBER REMPE: Okay.
15	MR. PAIK: But we can still have some
16	material left in the core.
17	MEMBER REMPE: Okay. So I=m not sure I
18	found anywhere that told me how much is in the vessel
19	and ex-vessel in some of these analyses.
20	MR. PAIK: There were most sequence, and
21	here is no recovery sequence. So eventually all the
22	corium relocates.
23	MEMBER REMPE: Good.

	181
1	methodology. You just allow for failure of the IVR.
2	MR. PAIK: The IVR is not applied in these
3	sequences.
4	MEMBER CORRADINI: But it=s there.
5	MR. PAIK: It=s feature is there.
6	MEMBER CORRADINI: But you don=t consider
7	it?
8	MR. B. KIM: Yes, in this variation.
9	MEMBER REMPE: Well, that=s something I=d
10	like to discuss later. They don=t take credit for
11	it. But then it is there, so I=m wondering if you
12	can have some is ues because the insulation around
13	the vessel could collapse and you might - I=m not
14	quite sure how you - I mean, you say you don=t take
15	credit for it. But it=s there. Do you ever consider
16	adverse effects because it=s there? You know, like
17	the AP 600 and AP 1000 reinforced the entryway for
18	the water to come in. So did you consider unintended
19	aspects of it? You don=t take credit, but that was
20	something I was going to bring up later. But it is
21	kind of a nuance that they don=t take credit for it.
22	But it=s there.
23	MEMBER CORRADINI: I don=t remember.
24	But there was some previous certification. If I knew

1	who it was, I probably couldn=t say it anyway. But
2	there was a previous certification where the coming
3	applicant basically said that their mitigation
4	measures were not credited. And they showed that
5	with the presence of the mitigation measures, it
6	didn=t make it any worse than essentially ignoring.
7	That=s what I think is being said here.
8	MR. PAIK: Similarly in APWR, even though
9	they -
10	MEMBER CORRADINI: In which one?
11	MR. PAIK: APWR.
12	MEMBER CORRADINI: Oh, okay.
13	MR. PAIK: Yes. They have similar
14	features, but not critically.
15	MEMBER POWERS: Why does the metal float
16	over the uranium dioxide?
17	MR. PAIK: The current - when you have -
18	MEMBER POWERS: Can you show me a single
19	experiment that=s ever been done to show that it
20	happens?
21	MR. PAIK: I think there is some
22	experiment that shows that light matters. It=s kind
23	of moving upward. MASK experiment.
24	MEMBER POWERS: MASK experiments were

1	explicitly done to show that it did not.
2	MR. PAIK: I have to get back on that with
3	the particular experiment that has that.
4	MEMBER POWERS: Only when they
5	deliberately constructed the oxide phase to have no
6	- to be hyper-stoichiometric could they get the metal
7	to float. How do you guarantee that your oxide phase
8	is hyper-stoichid metric? When you=ve got zirconium
9	metal that=s incompletely oxidized?
LO	MR. FAIK: The current model assumes the
L1	light metal layer is floating above oxide.
L2	MEMBER POWERS: What are the consequences
L3	of being wrong on that assumption?
L 4	MR. PAIK: If you credit the in-vessel or
L 5	ex-vessel cooling, then that becomes an issue. That
L 6	was one of the reasons this ERVCs -
L7	MEMBER POWERS: If you look at the heat
L 8	transfer to the ex-vessel cooling, how thin does the
L 9	wall have to be in order to get a boiling flux
20	outside?
21	MR. PAIK: I think it=s typical when the
22	ERVCs are available, the vessel wall can go down to
23	two to three centimeters.
2.4	MEMBER POWERS: So any kind of -

	184
1	MR. PAIK: High pressure sequence -
2	MEMBER POWERS: Any kind of collapse in
3	material, it will fail?
4	MR. PAIK: I mean, as long as there is
5	two to three centimeters, it is still strong enough
6	to retain the corium in low pressure.
7	MEMBER POWERS: Yes, but if the internals
8	collapses?
9	MR. PAIK: The internal plenum still is a
10	relatively cold.
11	MEMBER POWERS: What I=m asking is, that=s
12	a pretty good radiation heat flux coming off the melt
13	up into the upper internals. If they collapse and
14	hit the bottom of the vessel when it=s only two or
15	three centimeters thick, that still holds together?
16	MR. PAIK: If you do the ERVC, then corium
17	temperature can get very hot and that radiation can
18	raise the internal temperature. And that kind of
19	thing potentially could happen. But at least in APR
20	1400, the ex-vessel cooling is not credited.
21	MEMBER CORRADINI: So can I ask Dana=s
22	question a little bit differently? So the
23	orientation of where the metal is compared to where
24	the oxide is - since you=re not crediting the ex-

1	vessel in-vessel retention, it=s of no consequence?
2	MR. PAIK: Right. It=s not that
3	important.
4	MEMBER CORRADINI: That=s what I think
5	what you were trying to get at. The uncertainty -
6	the stuff comes out regardless. Because they are not
7	crediting and thus a retention.
8	MEMBER POWERS: The failure modes they
9	have explicitly recognize the orientation. If you
10	don=t have that orientation, you=ve got a different
11	problem. And for instance, if I have a metal melt
12	streaming on the lower head, it fails instantly. If
13	I fail because of the metal attack low instead of
14	high, drain everything out instantly. It=s a little
15	different problem.
16	MEMBER CORRADINI: Right. But I=m not
17	answering for them. On the other hand, what I thought
18	Chan was saying is that given that they didn=t credit
19	the in-vessel cooling, it all comes out eventually.
20	The rate would change as to what comes out first. Is
21	that your point? And the chemical reactions are
22	related with that rate.
23	MEMBER POWERS: Yeah, you have a different
24	situation. And I=m uncertain of what the

1	consequences are.
2	MR. B. KIM: Upon vessel failure, the MAAP
3	progression moves to the ex-vessel with the following
4	key parameters. RCS suppression, corium vessel
5	failure mode and timing, corium releasing
6	characteristics, cavity floor concrete type,
7	availability of cavity flooding at the time of vessel
8	failure. And during its vessel phase, the various
9	events can cause the containment failure, such as the
10	high pressure melt ejection and direct containment
11	heating, ex-vessel steam explosion, molten core-
12	concrete interaction, and hydrogen combustion.
13	Ex-vessel, EVSE, contains considerable
14	core uncertainty. In order to reduce the uncertainty
15	related to the ex-vessel event, the following
16	approaches are applied in severe accident evaluation.
17	Ex-vessel steam explosion, initial conditions are
18	established for the realistic case. The sensitive
19	cases need bounding parameters.
20	For direct containment heating, the
21	sampled input is prepared by Latin Hyperbolic
22	Sampling technique. And for molten core containment
23	and hydrogen risk, we use conservative input to
24	increase concrete ablation depth and hydrogen

	187
1	generation. And commonly, for the selection of the
2	ex-vessel sequences, we used a combination of
3	probabilistic and deterministic approaches in the
4	variation.
5	MEMBER POWERS: When you did your DCH
6	analysis, you say sampled input values. I=m unclear
7	what you mean by that. What input values do you
8	sample?
9	MR. B. KIM: There are known key
10	parameters. Each has a dominant effect on the DCH
11	measurement, such as the ICS pressure or the
12	containment as shown. And we can determine the
13	allowable band of each parameter. The pressure is
14	from the low-band and higher-band, which is available
15	in the APR 1400 -
16	MEMBER POWERS In the case of this
17	particular -
18	MR. B. KIM: We collect random data from
19	each parameter and prepare it for than more than one
20	thousand data points. And we variate these randomly
21	established input - like that.
22	MEMBER CORRADINI: Can I ask Dana=s
23	question a little differently? There are some old
24	experiments done at Argonne and then at Sandia about

	188
1	co-ejection of melt with water. Forget about the
2	pressure. So I=m trying to decide what happens with
3	the presence of water in the cavity. And is that
4	considered in the DCH? Is that considered?
5	MR. B. KIM: No.
6	MEMBER CORRADINI: Okay. Because if
7	memory serves me, it kind of matters.
8	MR. B KIM: I=m sorry?
9	MEMBER CORRADINI: The presence of water
10	matters. So if you have water there, it kind of
11	turns into a pressurization event, if I remember the
12	old Argonne and Sandia experiments. That to me would
13	be an interesting input variable, or variation that
14	I=d be curious about. I mean, to put it in a
15	different way, DCH dry - interesting but of no
16	consequence.
17	DCH with water -
18	MR. PAIK: I think that these rapid steam
19	generation due to these ejections can raise the
20	pressure. But still does not reach containment
21	failure.
22	MEMBER CORRADINI: Okay. So that bounding
23	calculation was done?
24	MR. PAIK: I don=t know if it was

1	officially done.
2	MEMBER CORRADINI: Okay.
3	MEMBER KIRCHNER: Well, you=re trying -
4	you know, the natural thing you=re trying to do is
5	get as much water into these scenarios as possible.
6	So there=s going to be a large amount of water to
7	generate steam. And then, with your reactor vessel
8	melt through, it doesn=t have to be a violent result
9	and a fairly significant pressurization of the
10	containment.
11	MEMBER POWERS: I=m not even talking
12	violent. That s why I asked if a bounding
13	calculation was done.
14	MEMBER KIRCHNER: Yeah, if they bounded
15	that.
16	MR. PAIK: For the containment performance
17	calculation actually, we used a mechanistic
18	calculation of what those re-entering the pool and
19	generating the steam and hydrogen. And then the
20	effect on pressurization. That was considered.
21	MEMBER POWERS: It seems to me that for
22	this particular design, for the direct containment
23	heating, a dominant uncertainty is the amount of
24	expelled core debris that gets ejected up around the

vessel and into 1 dome. And it seems to me that 2 that=s a fairly complicated process. If you estimate 3 why wouldn=t that transport, you sample the 4 parameters affecting that? Rather than just 5 input parameters? 6 MR. B. KIM: The approach used in the DCH evaluation is by following the Reg Guide. 7 So this is talked about later. Again, I can give you more 8 9 detailed information at a later time. 10 MEMBER POWERS: What I=m driving at 11 would you have sampled things - of these things, how 12 much melt gets expelled? What metal fraction of it is, what the driving pressure is? And those are all 13 admittedly uncertain, and you can formulate some sort 14 15 of distribution. And the nice thing is, nobody=s 16 going to be able to prove you wrong on those. 17 that=s not what dictates the pressurization for you. What dictates the pressurization for you in this is 18 19 how much pre-existing hydrogen you have, and how much 20 of the debris comes up around the vessel and goes up 21 into the dome. 22 Because it=s only that debris that goes 23 up in the dome that can fully impart its energy to 24 the pressurization of the atmosphere.

1	process of expelling debris and having it come up
2	into the dome region involves particles bouncing off
3	things, going up through channels and what not.
4	There are lots of things that I personally don=t know
5	how to mechanistically calculate. So if I were
6	having to do it, I would have to do some sort of an
7	uncertainty analysis or bounded like Mike does on
8	everything he ever encounters.
9	(Laughter.)
10	MEMBER POWERS: In some way, look at a
11	range of things. But apparently, you only sampled
12	over the inputs and nothing associated with that
13	discharge up into the dome region. And I=m just
14	trying to understand why?
15	MR. FAIK: I don=t remember every detail
16	of the DCH calculation. But actually how much can go
17	through the analysis to the dome - we probably have
18	done some analytical calculation to provide us some
19	of those values.
20	MEMBER POWERS: I would think that would
21	be a first order in importance. Because, I mean,
22	sampling the input values - I think that=s great.
23	And I=m sure you put in distributions that we can
24	argue over until the cows come home and it won=t make

1	any difference. It=s fine, whatever you did. That=s
2	not the crucial thing. The crucial thing is how much
3	energy you put into the atmosphere, and that seems
4	like it=s challenging. And I think, particularly for
5	this design, it=s crucial.
6	MEMBER CORRADINI: I=m trying to find the
7	Sandia report, but Marty Pilch did a series of Sandia
8	reports for the NRC to try to think of these effects
9	that Dana has mentioned. So that=s, I guess, is
10	where I would start.
11	MEMBER POWERS: Yeah, I mean that=s
12	certainly exactly right. That=s where I would start.
13	They=ve done their time pressure, and they spent all
14	their time looking at Westinghouse designs and things
15	like that. Here, you=ve got a substantially
16	different situation because what=s in there is
17	different. I meam, there=s just a lot of things that
18	are different.
19	And what goes on below the operating deck
20	really doesn=t matter for containment pressurization.
21	It=s what you get up into the dome. And the amount
22	of pre-existing hydrogen that you have up there that
23	can get ignited. In your case, you might not have
24	very much because you=ve got your igniter, your

	193
1	passage systems, and things like that. So you=re in
2	good shape to start with.
3	MR. PAIK: The methodology certainly
4	follows the Sandia results.
5	MR. B KIM: Okay now, let=s move to the
6	mitigation features of APR 1400. First to be
7	discussed here is hydrogen control systems. Hydrogen
8	control system is designed to accommodate the
9	hydrogen generation from one hundred percent metal
10	water reaction and to limit the hydrogen
11	concentration less than ten percent, as required in
12	these two criteria.
13	The mitigation features of hydrogen risk
14	is - the first one is containment. The second one is
15	pressure recombiners, and the third one is igniters.
16	Containment tests large free volume, as I told you
17	previously. Rather than the three million cubic
18	feet. And thirty PARS and eight igniters is
19	installed throughout the containment with the seismic
20	category 1 requirement.
21	MEMBER POWERS: When you think about your
22	severe accident, and you say gee - I=ve got melt down
23	interacting with concrete. And concrete always has
24	a certain amount of gypsum in it. So I=m getting

1	sulphur-bearing casses coming off of that. Do you
2	look at the poisoning by the PARS by those sulphur-
3	bearing gasses?
4	MR. FAIK: That particular thing was not
5	considered. But the effectiveness of the PARS would
6	be reduced to about fifty percent. Yes. The base
7	would be twenty-five reduction of PAR capability. So
8	in order to consider this time of consulting -
9	MEMBER POWERS: What I=m - I mean that=s
LO	great, except I don=t know where the twenty five -
L1	why wouldn=t it be one hundred percent if I=m putting
L2	up volumes of hydrogen sulfide? If you=ve ever done
L3	a melt concrete experiment, you know they stink of
L 4	hydrogen sulfide.
L5	MR. B. KIM: Yeah, I don=t remember seeing
L 6	the actual PAR data using those things yet. But
L7	instead of a mechanistic model, the chemicals reduce
L8	the effectiveness of PARS. It=s one way of trying to
L 9	address some of our uncertainties.
20	MEMBER POWERS: Well, the difficulty I
21	have is reducing if the potential reduction is one
22	hundred percent and I take twenty-five percent, then
23	I haven=t done anything. That=s the dilemma I run
2 Д	into I certainly donet know Teve never but a PAR

1	in the presence of a melt concrete interaction. And
2	it may well be, though unlikely in this particular
3	geometry, that the hydrogen all burns up the melt
4	concrete interaction for all I know.
5	But I do know - what I absolutely know -
6	is that most of the PARS that are used, that are
7	proposed for use in nuclear power plants were
8	originally developed for use on diesel engines. And
9	they had to require people use low-sulphur diesel,
L 0	because the sulphur irreversibly poisons the
L1	palladium-platinum alloy.
L2	MR. PAIK: In APR 1400, when you have an
13	MCCI, we still have about seven or eight meters of
L 4	water pool on top of the corium. So whatever the
L5	off-gas from MCCI and aerosol generation has to go
L 6	through these seven or eight meter of water pools.
L7	And most of them, especially aerosols, will be
L 8	scrubbed. Some gas can escape.
L 9	MEMBER POWERS: I would recommend that you
20	bubble hydrogen sulfide into water and sniff over the
21	top.
22	MR. B. KIM: Three, hydrogen control
23	system performance. We applied MAAP 4.08 code. And
24	with highly probable sequences from PRA Level 1 study

1 is represented deterministic sequences including five 2 major initiatives. Such as three LOCAs and station 3 blackout, and total loss of feedwater. 4 Regarding the hydrogen source, besides 5 the hydrogen mass! you can bound it to the one hundred 6 percent MWR inside the in-vessel, as criteria 7 requires. An additional generation of during each vessel phase, such as the MCCI were also 8 9 considered in the variation. 10 So in MEMBER REMPE: your accident 11 analysis report, you discuss the sub-nodal method 12 that=s in MAAP. Could you talk about that a little 13 Because you mention that seems very helpful in 14 matching the data such as the HDR tests. I also 15 appreciated the fact that you said, although this 16 matches here, there=s a lot of uncertainty when we 17 extrapolate to a 1 arge scale facility or containment. But could you talk a little bit about that? Because 18 19 I think MAAAP or melt core doesn=t have such a sub-20 nodal method, and so I was curious on how it helps. 21 MR. B. KIM: Right. MAAP has two or 22 actually three models. The typical lump -23 parameter core doesn=t have. One is, it has a 24 counter-current flow. So when we have a heavier or

1	colder gas on top of a lighter gas, then the heavy
2	gas will come down and light gas goes up. So we have
3	a counter current flow. In terms of sub-nodal
4	physics, a model is essentially - we are modeling a
5	plume rising.
6	Let=s say we have a hollow LOCA and
7	hydrogen coming out. And then a plume will generate
8	going through the low compartment, steam compartment
9	to upper compartments. So essentially, using these
10	plume paths, we can push some of the lighter gas to
11	the top portion. That=s one aspect of sub-nodal
12	physics.
13	Second aspect of sub-nodal physics is
14	like a couple kind of features. One is if a lighter
15	gas is trying to come down. And let=s say it goes
16	below this table. Then only a portion of it will be
17	covered by lighter gas. It=s not mixing all of the
18	way. Then a lump of the parameter, that cannot be
19	modeled. So we use a sub-nodal physics model to
20	check if the lighter gas only penetrates the certain
21	length. And it doesn=t really contribute to the
22	overall nature of circulation.
23	So depending on that condition,
24	essentially we shut off the junctions to prevent these

	198
1	numerical mixing. So you have the sub-nodal physics
2	pushing to one, shut off the junction to prevent these
3	lighter gasses mixing to the lower part. And second
4	part is let the lighter gas plume rise to the top.
5	MEMBER REMPE: Okay. Thank you.
6	MR. B. KIM: Once the hydrogen steam and
7	air mixture conditions are calculated for all
8	containment in use from the MAAP study, the flame
9	acceleration, and different operation to deflagration
10	detonation rendition, DDT, is analyzed by applying
11	the sigma criterion and seven lambda criteria,
12	respectfully.
13	Another possible hydrogen bonding mode
14	inside the containment is a slow deflagration. The
15	pressure prediction for this slow deflagration is
16	analyzed on the conservative assumptions and bounding
17	pressure predicted by the adiabatic isochoric
18	complete combustion approach.
19	So here, we again applied a hydrogen
20	source to the one hundred percent method of the
21	reaction. Hydrogen control analysis results indicate
22	that awareness of containment must be achieved, and
23	leave less than ten percent hydrogen concentration.
24	Also, there is no potential for DDT and pressure by

	199
1	AICC assumption meets the FLC requirement of the
2	containment integrity, as discussed later.
3	MEMBER POWERS: I find that no possibility
4	of flame acceleration or DDT remarkable. It=s just
5	because you never get high enough concentration of
6	hydrogen to satisfy the seven lambda requirement?
7	MR. B. KIM: Yes.
8	MEMBER POWERS: Assuredly in your dome,
9	seven percent hydrogen lambda is on the order of half
10	a meter or something like that? Am I remembering
11	that roughly correctly?
12	MR. FAIK: I don=t know the exact lambda
13	value.
14	(Simu taneous speaking.)
15	MR. PAIK: What the TSMP did is they
16	applied these OECD - the standard methodology for
17	flame acceleration and also lambda defined the
18	geometry, defined in -
19	MEMBER POWERS: So I suspect you just
20	always fell below the initiating criteria? I suspect
21	that=s what happened. Assuredly, the dimensions in
22	the lambdas are okay, but they cut that off. And
23	there=s no good reason to cut it off. We=ve just
24	never done experiments that are in that regime.

1	MR. B. KIM: The second accident issue is
2	molten core concrete interaction. The goal of MCCI
3	mitigation is to secure the basemat liner integrity
4	by minimizing the corium concrete attack and removing
5	it from the core debris in the reactor cavity. So
6	mitigation features of APR 1400 for MCCI is the
7	reactor cavity and cavity floor concrete area, and
8	cavity floating system CFS.
9	APR 1400 cavity is designed with cavity
L 0	floor concrete and almost to the empty space. And to
L1	achieve the complete corium spreading on the floor,
12	we dug out any obstacles for spreading. And
L3	protective concrete layer is installed in the basemat
L 4	liner plate. Cavity floating system is designed to
L 5	flood the cavity with water from the IRWST initiated
L 6	by operation of the time of the severe accident entry.
L7	MEMBER CORRADINI: Can you explain that
L 8	part? I=m kind of curious where you=re going to send
L 9	the operator when I have severe accident open valves.
20	Tell me the procedure that has to be done by the
21	operator to go open a valve at this point in a severe
22	accident to flood the cavity.
23	MR. B. KIM: Yes. When the accident goes
ЭΔ	to the CFS the operator tries to open the MOV in the

1	cavity flooding system. Once the MOV is open, then
2	IRWST - water in the IRWST starts to flow into the
3	cavity by the -
4	MEMBER CORRADINI: I get that part. But
5	the way - maybe I m misunderstanding. I didn=t read
6	this section, I=1 admit it. It says manual. So
7	what=s the timing and where=s the manual operation
8	occurring?
9	MEMBER POWERS: How do they know?
10	(Laughter.)
11	(Simultaneous speaking.)
12	MR. B KIM: Core temperature exceeds one
13	thousand two hundred degrees Fahrenheit.
14	MEMBER CORRADINI: So is this the same
15	manual operation for the IVR?
16	MR. B. KIM: No.
17	MEMBER CORRADINI: I would think it has to
18	be. If the water is going to the same place, isn=t
19	it?
20	MR. B KIM: Yes, but the -
21	MEMBER CORRADINI: Do you know what I=m
22	asking? I=m trying to understand the logic.
23	MR. PAIK: If they open the MOV, what
24	happens is the volume of the tank and cavity level

	202
1	will be similar. And that level is below the vessel.
2	So you cannot have these expressive coolings. So if
3	they will not do an IVR, then you have to - the valve
4	is not open and you have to inject using the shutdown
5	cooling pump - in ect the water into the cavity. So
6	the cavity to whole - whatever HVT -
7	MEMBER CORRADINI: Ah, so this valve is
8	connecting the HVT to the cavity?
9	MR. PAIK: Yes. Right.
10	MEMBER CORRADINI: Okay.
11	(Simultaneous speaking.)
12	MEMBER CORRADINI: Okay. All right. So
13	that was my mistake. So now I=ve got a valve between
14	the HVT and the cavity, and how does the operator get
15	to it?
16	MR. B. KIM: MOV.
17	MEMBER CORRADINI: MOV? So it=s a manual
18	actuation? So I=ve got DC power? Okay, fine. All
19	right, I misunderstood you. Thank you. And this
20	floods into a level below the reactor vessel bottom
21	area?
22	MR. B. KIM: Right.
23	MEMBER CORRADINI: Got it. And - I=m
24	sorry. And so you = re not crediting an IVR, but if it

1	were an IVR, you would pump it in?
2	MR. PAIK: Then they have to close the
3	valve.
4	MEMBER CORRADINI: Right. Okay.
5	MR. B. KIM: By using the CFS, we applied
6	to free-floating strategic power to the vessel. So
7	analysis of the MCCI by using MAAP studies performed
8	with conservative approaches with a supporting MCCI
9	and CORQUENCH. So MAAP 4.08 incorporates two MCCI
L 0	motors. One is the jet breakup, and the other one is
L1	a heat removal to override water pool in order to
L2	mimic the water integration effect. So to decide the
L3	usually dependent key parameters of MAAP motor - for
L 4	these two kinds of motors.
L5	The supplemental study using CORQUENCH is
L 6	done by Dr. Mitch Farmer at Argonne National Lab. Sc
L7	Dr. Farmer evaluates the very conservative operation.
L 8	That=s under the assumption of full core relocations
L 9	at once. And without jet breakup in case of large
20	LOCA sequence. So the conservative CORQUENCH studies
21	project ablation depths of .27 meter. So MAAF
22	parameters related to the these two MCCI motors is
23	then decided to get a comparable ablation depth with
24	CORQUENCH study for the conservative Large LOCA case.

1	The selective MAAP model parameters used
2	for all of the last test on sequence variation. This
3	is the conservative variation. So the MAAP study
4	result credits that the highest tabulation depths of
5	.24 meters from the Large LOCA case, which is
6	obviously less than the thickness of the LCS concrete,
7	which is nineteen centimeters. So therefore, we have
8	compounded the integrity of basement liner plate
9	against an MCCI event.
10	MEMBER KIRCHNER: May I ask, what=s the
11	pressure rise in the containment in this scenario?
12	How high does the pressure go?
13	MR. B. KIM: Yes. Of course, the
14	pressure goes up due to the continuing steam
15	evaporation from the cavity. It=s of importance, so
16	we look at the pressure behavior due to the MCCI for
17	long-term. And we found that it=s not - it does not
18	go over to the design barrier.
19	MEMBER KIRCHNER: Is it close?
20	MR. B. KIM: No. It=s lower than the
21	containment performance requirement.
22	MEMBER KIRCHNER: I understand that it
23	might be lower. But how close does it get to the
24	yield plate? Or your containment pressure?

	205
1	(Simultaneous speaking.)
2	CHAIRMAN BALLINGER: The design pressure
3	is about sixty psi?
4	MEMBER KIRCHNER: That=s normal.
5	CHAIRMAN BALLINGER: Normal? Yeah. But
6	how close does it get?
7	MR. B. KIM: The criteria, the pressure
8	limit of the containment is not sixty psi. It=s much
9	higher than the design pressure. It=s more than one
10	hundred twenty psi. I don=t remember the exact
11	barrier of the pressurization on the inside, but -
12	MEMBER KIRCHNER: Is it sixty or a hundred
13	psi?
14	MR. PAIK: One hundred ten psi.
15	MEMBER KIRCHNER: Okay. So now it raises
16	the question of how well mixed this core collapse is
17	with the water. Because that could change the rate
18	at which the steam is generated and the pressure pulse
19	that you get. Do you see what I=m saying? That you
20	can get a pressure, a fairly significant pressure
21	pulse from a collapse of the corium into the water
22	pool.
23	MR. B. KIM: Okay. I think your concern
24	is more related to the steam explosion, not the -

	206
1	MEMBER KIRCHNER: More to the pressure.
2	The pressure that is generated inside the
3	containment.
4	MEMBER CORRADINI: I think Dr. Kirchner is
5	asking, you=re getting a quasi-steady pressurization
6	with time. Do you ever get to the failure pressure
7	of one hundred and ten? Or does it just happen or
8	occur days later?
9	MR. FAIK: Yes, this one hundred and ten
10	psi occurs in twenty-four hours.
11	(Simultaneous speaking.)
12	MR. PAIK: At the time of pressure
13	failure, we will have a pressure spike. But that
14	spike is typically low. Initially it goes up and
15	then it comes down, and then we will have a gradual
16	increase.
17	MEMBER KIRCHNER: Increase, okay. Is that
18	pressure - is the pressure time history, is that a
19	function of your assumptions for how well-mixed the
20	corium is as it comes through the vessel and
21	collapses?
22	MR. PAIK: Yes.
23	MEMBER KIRCHNER: So do you look at a span
24	of bounding calculations without getting too wrapped

1	up in exactly how it jets down. Do you see where I=m
2	going with this? Do you just mix that corium with
3	the water pool to see the amount of surface area that
4	is available for quick pressurization?
5	MR. PAIK: The current MAAP 4 model, as
6	heat transfer is a factor as it is coming down and
7	generating, or transferring heat to the water and
8	generating steam. Once the corium contacts the
9	cavity, then that particulate generated is mixed with
10	the remaining corium. So that particulate was not
11	tracked.
12	MEMBER KIRCHNER: No, I was just curious.
13	A simple experiment. If you ever take a thermos and
14	put hot water in - just very near boiling water -
15	shake up the thermos and try to lift the top off, and
16	you=ll see the kind of pressure spike you get from
17	that. And I=m just curious what kind of pressure
18	spike you might get, depending on how the vessel
19	ruptures and the orium is just dumped into the pool.
20	MR. PAIK: I think that depends on the
21	vessel pressure, and how deep the water pool is. And
22	then we typically use a kind of a jet entry using an
23	aid that can get to our fuel bar or pressure spike.
	Π

1	state when this happens? Is it pretty low?
2	MR. PAIK: The - I mean, as I mentioned
3	earlier, the pressure is gradually increasing.
4	MEMBER KIRCHNER: It=s gradually going up.
5	Okay, all right. Thank you.
6	MR. B. KIM: Okay. The third severe
7	accident issue is high pressure melt ejection and
8	direct containment heating. The goal is to prevent
9	early containment failure and minimizing entrained
LO	debris to upper containment. So the mitigating
11	feature for HPME, DCH, and for the APR 1400 is rapid
L2	depressurization system and reactor cavity with
L3	convoluted flow path. So RCS pressure reduction
L 4	system performance is analyzed by using MAAP 4.08
L5	code and DCH event is analyzed by following the
L 6	NUREG/CR-6338 methodology.
L7	Analysis results indicate that the
L8	present pressure reduction system can make the RCS
L 9	pressure less than the DCH pressure of 250 psi at the
20	time of vessel breaching. And conditional
21	containment failure probability in APR 1400
22	containment by DCH event is calculated less than .01
23	percent.
24	The fourth issue is fuel coolant

1 interaction. For a steam explosion in both in-vessel 2 and ex-vessel. The first step of analysis 3 initial boundary methodology is to set uр the 4 conditions. For the base case and sensitivity cases. 5 Second step is $t \phi$ evaluate the energetic loads by 6 using the TEXAS- \forall code. Then finite element modal 7 code is employed to investigate the vessel load head and the cavity wall response against those steam 8 9 explosion energy. will 10 indicate The analysis that 11 integrity of the lower half and the cavity were 12 In addition, the effect of the in-vessel preserved. 13 retention and external reactor vessel cooling, IVR-ERVC, stretches on the ex-vessel steam explosion. It 14 15 will be assessed by COL time by applicant as described 16 in the item 19.2. 17 fifth The issue is the equipment The proposal of ES assessment 18 survivability, or ES. 19 is to conform the equipment and instrumentation can 20 operate under the severe accident environment over 21 the required time window. So the first step of ES 22 assessment is to identify and to restore the equipment 23 and instrumentation used in the severe accident 24 is mitigation. And second step evaluation

1	environmental conditions of those equipments by using
2	MAAP 4.08 code for selected sequences.
3	Then, we can decide what is the bounding
4	temperature, pressure, and radiation for each
5	increment from the MAAP calculation. Lastly, the
6	instrument survivability is assessed by comparing
7	them with suppliers= test data or experimental test
8	data by thermal lag analysis.
9	MEMBER REMPE: So I had a couple questions
10	on this. First of all, is there a cutoff frequency?
11	You have here that you used MAAP3 code for selected
12	sequences. How did you select the sequences? Did
13	you have a cutoff frequency where you said, okay - I
14	mean, you could really have a bad sequence if you
15	don=t have a cutoff frequency. So, how did you select
16	those sequences. That=s one of my questions.
17	And then the other question is that you
18	have hot junction thermal couples and core exit
19	thermal couples that are type Ks. And in the accident
20	analysis report, it claims that you have data - KHNP
21	has data that says that type Ks can withstand up to
22	1533k for long durations, which amazed me. Because
23	I just don=t know of any type Ks that can do that.
24	What kind of sheath does it have? Because usually,

1	there=s chromium or something in the sheath that will
2	migrate through and attach to the thermal elements.
3	And they=11 cause those thermal couples to degrade.
4	So I was real curious on what thermal couples you had
5	that could withstand that high of temperatures.
6	MR. B. KIM: Okay, for the first
7	question. We selected accidents by following the
8	required 1.216. Simply, I can say we chose accident
9	sequences which correspond to more than ninety
10	percent of coding frequency. And in addition, we
11	also applied them to the accident sequences,
12	initiated by the dominant sequences.
13	MEMBER REMPE: Okay. Okay.
14	MR. B KIM: And for the second question,
15	some thermal couple K-types can survive that
16	temperature, elevated temperatures for a long time.
17	I need to check from the physical description for
18	that information.
19	MEMBER REMPE: Yes, please. It actually
20	stated that in your report. And so I was real puzzled
21	about that one, because -
22	MEMBER POWERS: Well I would think that it
23	ll en
	would depend on what you mean for a long time. The

	212
1	effusion. So it = relatively slow. The question is
2	- I mean, you=re not looking for a particularly
3	accurate measurement here. So the degradation is
4	slow, but I mean
5	MEMBER REMPE: It just goes downhill when
6	I=ve run thermal couples in furnaces.
7	MEMBER POWERS: I had -
8	MEMBE REMPE: - Eleven hundred. And we=ve
9	had a large number of different types.
10	MEMBER POWERS: I=ve had them do
11	everything known to man. Up, down, sideways, open,
12	and what not. But if all you=re looking for is an
13	indication, the temperatures are very hot and you
14	don=t care about how hot, then yes. They can do it
15	for a while. If you=re interested in three days,
16	you=re in trouble. If you=re interested in three
17	minutes or three hours, probably it=s okay.
18	MEMBER REMPE: It said long duration. So
19	I=d be curious about the definition.
20	MEMBER POWERS: Yes, what=s the definition
21	of long?
22	(Laughter.)
23	MEMBER REMPE: What data they have to
24	support that claim?

1	MEMBER POWER: Yeah, I mean - I=ve run
2	type Ks in obnoxious environments and used every bit
3	of the 1327 you=ve got.
4	MR. B. KIM: The containment conditions
5	will never reach that high.
6	MEMBER REMPE: Well, this is the core
7	exit temperature in a hot junction thermal couples
8	that are used for water level measurement in the
9	vessel.
10	MR. B. KIM: Basically, the thermal couple
11	is only - we expected can survive the continual onset
12	of the core damage. So beyond this time span, if the
13	thermal couple survives, it is okay. But we don=t
14	take credit for a long time.
15	MEMBER REMPE: Okay. It was on page five
16	hundred out of six fifty-nine of your accident
17	analysis report. And so I=d be curious on the data
18	that supports that claim, okay?
19	MR. B KIM: Okay. I will check for you.
20	So because the major assessment is related to the
21	suppliers= or the vendors= data, so the sections for
22	ES just gives those instrumental lists. And how we
23	do the ES assessment based on the reference plant
24	experience. And what expected bounding environmental

1	conditions are. So the rest part of the ES assessment
2	will be done later as addressed in the first core
3	item of 19.2.
4	The containment performance - containment
5	withstands to the severe accident challenges is
6	performed to confirm to containment performance.
7	Criteria for the containment is given in SECY 93-087
8	and Reg Guide 1.216. As per Reg Guide 1.216,
9	applicant needs to show the containment integrity
10	against the pressure load from the hydrogen
11	combustion and more likely, severe accident
12	challenges. Positions two and three, respectfully.
13	Containment integrity regarding the
14	position two - the hydrogen burning load are varied
15	conservatively under the key assumptions to hydrogen
16	mass from one hundred percent MWR, and no credit of
17	recombiners and igniters, and AICC bonding
18	methodology. In addition, the various initial
19	impression is considered to get the maximum AICC
20	pressure under the given condition.
21	So, determined AICC pressure is a
22	bounding value of hydrogen, deflagration is a 123.7
23	psi is then applied be an input value for containment
24	response. So finite element modal, FEM, studies

1 indicate that the maximum strength of the liner plate 2 not reach the allowable limit. Therefore, 3 conservative hydrogen combustion load meets the 4 factored load category, FLC, requirement. 5 Regarding the position three, the 6 pressure from more likely severe accident challenges 7 evaluated. \$0 according to the commission=s recommendation addressed in the Reg Guide, accidents 8 9 are selected to be ninety percent of cumulative CDF 10 from PRA Level In addition, study. the five 11 representative initiators such as Large and Small 12 LOCA, station blackout, SGTR, and total loss 13 feedwater are taken into account in the light of deterministic approaches with conservative accident 14 15 progress. 16 a MAAP 4.08 study was done Then, 17 bounding pressure profile determine а and pressure with realistic [ESA] appropriation, such as 18 19 the success of cavity flooding system and RCS pressure 20 emergency containment spray backup reduction and Determined bounding profiles then again 21 system. 22 applied to the three dimensional finite element modal 23 study of containment structure. 24 MEMBER CORRADINI: Can I just make sure of

1	something? So, you don=t have to pull it up. But
2	on slide thirty-six for the Level 2 PRA Section 19.1,
3	this connects up to these dots. Which is, you delay
4	containment failure with the ECSPS and with cavity
5	flooding, you delay any sort of over pressurization
6	so late in time. So you have no early failures in
7	the first day or two?
8	MR. B. KIM: Yes. We dealt with
9	containment.
10	MEMBER CORRADINI: Okay. And so the
11	dominant contributors to the fourteen percent
12	containment failure probability is containment bypass
13	and delaying all failures until late times. So, all
14	the other stuff we were talking about and quizzing
15	you about are much smaller fractions of containment
16	failure. In other words, of the - I don=t know how
17	to ask this properly, but - of the fourteen percent,
18	I=m worrying about DCH and explosions, et cetera, et
19	cetera, et cetera.
20	It=s small fraction of everything we=re
21	talking about. It=s really the operation of the
22	ECSBS cavity flooding delaying pressurization that
23	dominates that late fourteen percent containment
24	failure. Do I have that correctly? Do you

_	understand my question:
2	MR. T. HWANG: My name is Taehee Hwang
3	from KEPCO & ENEC. He is right, the containment
4	failure is probably based on internal events. This
5	contributes to fourteen percent of CDF. Opposed to
6	containment containment bypass, SGTR including
7	severe accident induced SGTR. And then second
8	containment failure modules or rate containment
9	failure due to low pressurization and/or the hydrogen
10	-
11	MEMBER CORRADINI: Yeah. So let me ask my
12	question this way. If tomorrow magically explosions,
13	direct containment heating, the other things we were
14	asking about all went to zero probability - would
15	fourteen percent go to thirteen percent?
16	[Simultaneous speaking.]
17	MEMBER CORRADINI: Do you understand my
18	question? There s a fourteen percent containment
19	failure probability. If all these physical processes
20	were wrong and zero probability, does fourteen become
21	thirteen? I think the delta change is very small.
22	I=m trying to get an idea of what the delta change
23	is. Am I making sense? No? Member Stetkar says
24	no. I=m just trying to understand the contribution

	218
1	of all -
2	MEMBER STETKAR: I know what you=re
3	trying to ask. But the way you=re asking is not
4	making sense. I don=t know how to ask it, is the
5	problem.
6	MR. PAIK: What=s the containment failure
7	frequency when ESPSBS is not available?
8	MR. LEARY: Excuse me. If I may, Jeff
9	Leary with Enercon. I believe the question that
10	you=re trying to express is the significance of or
11	contribution to containment failure from DCH and
12	steam explosions?
13	MEMBER CORRADINI: Yes. Let=s take those
14	two as an example.
15	MR. IEARY: Yeah, I don=t have the exact
16	percentages. But it=s not a significant
17	contribution.
18	MEMBER CORRADINI: Okay. It=s a small
19	fraction of the fourteen percent, is what I was trying
20	to estimate.
21	MR. LEARY: That=s correct.
22	MEMBER CORRADINI: So I=m curious about
23	the timing of the failures. Does the timing of the
24	failures, as long as it=s beyond - I=m not sure

1	exactly what you call long - but a day or two, does
2	it matter after that in terms of large release
3	frequency? Or it also is - because the other thing
4	I was going to ask you is going back to slide thirty-
5	six, I was trying to understand the difference between
6	the fourteen percent for conditional containment
7	failure probability and nine percent for large
8	release frequency. So there=s five percent going
9	away, and I=m trying to figure out physically why
10	there=s a difference there. And it must be timing of
11	the failure.
12	MR. LEARY: I=m sorry. The five percent
13	or so is a small containment failure.
14	MEMBER CORRADINI: So it=s leaking, but
15	it=s just not leaking fast enough?
16	MR. LEARY: Including things like basalt
17	and things that are not large. So the nine percent
18	that you saw on there is large releases, and the
19	fourteen percent is all. So large and small combined
20	together.
21	MEMBER CORRADINI: But the difference is
22	really leakage at lower rates?
23	MR. LEARY: By rates, you mean?
24	MEMBER CORRADINI: Percent per day.

1	Through out of the containment or its leakage paths.
2	I think that=s what you=re saying.
3	MR. LEARY: It=s a total integrated at
4	the end is what determines large versus small, but
5	yes.
6	MEMBER CORRADINI: Okay. Fine. Thank
7	you.
8	MR. LEARY: Thank you.
9	MEMBER CORRADINI: I=m just trying to
10	figure out how much I have to worry about all the
11	things we ask you.
12	MR. B. KIM: The last part of 19.2 is
13	severe accident management framework. Accident
14	management encompasses those actions taken into
15	during the course of accident by the plant operating
16	and technical staff. The first step is to prevent
17	core damage. The second step is to terminate the
18	progress of core damage. The third step is to
19	maintain containment integrity as long as possible.
20	And the last step is to minimize the offsite release.
21	At each step, operator will try to act
22	what he can do according to the accident management
23	guidelines. For example, operator tries to recover
24	the RCS inventory by safety injection. And if safety

1 injection has failed, he will try to open POSRVs to 2 depressurize RCS and to allow injection 3 shutdown cooling or containment spray pump. **ERVC** 4 strategy can be achieved by flooding using shutdown 5 cooling pump to remove the heat on the outer surface 6 of the vessel. 7 MEMBER REMPE: I have a question about this slide. Because this is what I was thinking 8 9 about with the vessel retention. The staff doesn=t review the severe accident management guidelines, 10 11 So you=re going to include them in the 12 quidance to the operators. And how does this work? 13 Because it=s like something that=s out there, we don=t take credit for it. And that was my question earlier 14 15 about - you know. Do you reinforce it so you know it 16 works? 17 I kndw the AP 1000 and at least the AP 600 had to change the design to make sure that the 18 19 insulation was robust. And you=re chugging all that

I know the AP 1000 and at least the AP 600 had to change the design to make sure that the insulation was robust. And you=re chugging all that water through and generating the vapor for the external reactor vessel cooling. So you=ve got this mitigating strategy in your design that=s being credit for, so I guess the staff doesn=t review it very much. How does something like that work? And

20

21

22

23

24

1	how are you going to come up with the guidance with
2	late term water addition, and things like that? When
3	we=ve been talking about flecks - is this something
4	that - you know. If this plant were built in the
5	U.S., would it be part of the PW Owner=s group? And
6	this would be something that=s considered by the PW
7	Owner=s Group?
8	MR. PAIK: I think in the APR 1400, they
9	are looking at the ERBC plus the water injection.
10	Because AP 1000 and ERBC is just a passing. But the
11	APR 1400 and ERBC is you need a pump to inject the
12	water. And if you have a pump that=s available, the
13	question is why not inject into the vessel? Why only
14	inject on the outside? So what they need, what they
15	want to do is it takes about thirty to forty minutes
16	to fill up the cavity.
17	In the meantime, ICS will be
18	depressurized. So as soon as they finish the cavity
19	flooding, then they can switch to the injecting into
20	the vessel. So I don=t know the details, but I think
21	that that=s the kind of approach they will go use.
22	So not only the express cooling, but also trying to
23	inject after the RCS is depressurized.
24	MEMBER REMPE: Well it=s just something

	223
1	I=m not quite sure how the staff will deal with that.
2	Is this something - well, they don=t. What if the
3	guidance is not optimum? And who reviews that
4	guidance?
5	MEMBER CORRADINI: I don=t want to speak
6	for the staff, but my understanding is as long as
7	it=s there, that=s it.
8	MEMBER REMPE: I hope that it=s done
9	right.
10	It sounds like it = s unreviewed. I mean, this is a
11	different thing that=s not standard in the existing
12	fleet and although it is - I guess in the AP 1000 -
13	they are supposed to have it. And I just am kind of
14	curious about this long-term phenomena. You want to
15	inject in the vessel. It seems like a reasonable
16	thing to do. If the vessel has - if it=s at a high
17	pressure. I hope they would have the right criteria
18	for doing it. I guess I=ll leave it at that.
19	And then I didn=t hear anything about,
20	did you consider how much you need to reinforce that
21	insulation? Like the folks did for the AP 1000? How
22	much scrutiny did the design have? I mean, the
23	staff=s not reviewing it. So I=m asking. Did you
24	consider, did you have sufficient opening for water

	224
1	to get in and for the steam to go out of this vessel
2	retention capability?
3	MR. RYU: But for reference, we make some
4	change to enhance the flow rate in the cooling
5	channel. Each situation the design is varied.
6	MEMBER REMPE: Is it in the Shin Kori
7	design? It is? Okay.
8	MR. RYU: This is in Shin Kori.
9	MEMBER REMPE: Okay.
10	MR. B. KIM: Regarding the accident
11	management framework, detailed development
12	implementation and maintenance of accident management
13	plan is clarified in 19.2. It is time to close my
14	talk with some summaries from 19.2. The severe
15	accident prevention and mitigation features of APR
16	1400 are designed to confirm to associated criteria
17	and requirements. Hydrogen risk, MCCI, DCH, and ES
18	are investigated, and we found the requirements are
19	satisfied. Containment integrity or containment
20	performance is confirmed according to the Reg Guide
21	1.216. And accident management plan will be
22	developed and established as described in COL 19.2.
23	This is the end of my presentation. Thank you for
24	your kind attention.

1	MEMBER STETKAR: Before KHNP vacates the
2	premises, I just wanted to make a couple of comments.
3	I know I was pretty critical of a few items this
4	morning. I just wanted to, for the record, say that
5	my review of this particular design certification PRA
6	- in my opinion it is much, much better than the
7	vast majority of design certification PRAs than we
8	have seen over the nine and a half years I=ve been on
9	the committee. And I=ve looked at five or more design
10	certifications.
11	In particular, not so much the Level 1
12	internal events because everybody sort of does the
13	same thing there. But I think your treatment of
14	fires is much more coherent. Your treatment of
15	internal flooding is much more coherent. Your low
16	power and shutdown models, you actually have low power
17	and shutdown models. And the fidelity of the way
18	that you did and presented the PRA base size
19	margins. So I hope this - from the staff=s
20	perspective is a good example going forward to any
21	other designs that we might see. Because it=s a heck
22	of a lot better than what I=ve seen, anyway.
23	CHAIRMAN BALLINGER: That=s a big
24	compliment.

1	(Laughter.)
2	CHAIRMAN BALLINGER: He doesn=t say that
3	to all of us. In fact, that=s the first time I=ve
4	ever heard him say it.
5	MEMBER CORRADINI: Are we sure it=s him?
6	(Laughter.)
7	MEMBER POWERS: And once again, he=s
8	probably wrong again.
9	(Laughter.)
10	CHAIRMAN BALLINGER: Well thank you very
11	much. What we will do now is we will recess for
12	fifteen minutes. Well, until quarter of. And then
13	we will pick up with the staff.
14	(Whereupon, the above-entitled matter
15	went off the record at 2:28 p.m. and resumed at 2:47
16	p.m.)
17	MR. STECKEL: My name is Jim Steckel, and
18	I=ve had the privilege of working with this PRA team
19	for the last couple of years.
20	A couple of things Lynn Mrowca is over
21	on this side. She is the branch chief who will,
22	sadly, soon be leaving the agency. I wanted to make
23	sure everyone knew that.
24	MEMBER POWERS: Is it because she doesn=t

1	like us?
2	MEMBER BLEY: That=s pretty much it. I
3	heard it was one person.
4	(Laughter.)
5	MEMBER POWERS: Okay. Well, I=ve done
6	my share of harassing on her, I=ll have to admit.
7	MR. STECKEL: One and done.
8	The technical staff will be up here to
9	make the presentations for their particular sections
LO	that they have reviewed. These are the names and
11	their areas where they work and their titles, and of
12	course Jeff Cioco is lead. I=m Jim Steckel, the
L3	chapter PM. And these will be the actual areas of
L 4	review that each of the members has taken on.
L5	And just for your clarification, this is
L 6	what we call Chapter 19, consists of 19.1 and 19.2.
L7	And we have considered the rest of the 19s to be
L8	separate chapters, at least during the review process
L 9	and the SER preparation.
20	So you may hear me or someone refer to
21	Chapter 19.3 when we get to the phase 6 where
22	everything there are no more open items, et cetera.
23	I believe everything will be consolidated under one
Э Д	Chapter 19 with those different sections 19 1

1	through 19.5. But the rest of it will be tomorrow.
2	We are going to get all of these reviewers
3	to come up here and participate, which means there
4	will be some seat swapping going on. We will try to
5	keep that to a minimum a minimum disruption for
6	the proceedings.
7	And I m going to ask the staff to please
8	leave your name tags here. Chris will either collect
9	them or they need to be here for us tomorrow, and I
10	believe he wants to retain those for the future.
11	So with that, we are ready to proceed for
12	our first reviewer, which is Mr. Hanh Phan. He is
13	the senior reviewer for PRA.
14	MR. PHAN: Good afternoon. My name is
15	Hanh Phan. I am the lead reviewer for APR1400 design
16	certification.
17	MEMBER BLEY: Could you speak a little
18	more directly into the mike? It=s hard to hear over
19	here.
20	MR. PHAN: Okay. Better now? Thank
21	you.
22	First, on behalf of the staff
23	participating in the review of the APR1400 PRA severe
24	accident evaluation, we=d like to thank all of you

1	for the opportunity to share with you our phase 2
2	SECY reviews and any comments you have on our
3	assessment.
4	We=d also like to take this opportunity
5	to recognize the guidance from our branch chief, Mrs.
6	Lynn Mrowca, and the lead project manager, Mr. Jeff
7	Ciocco, since both of them are going to retire late
8	this month or early next month.
9	Next slide, please.
10	This slide outlines the staff today
11	presentations for Chapter 19.1. In this
12	presentation, the staff will cover internal events,
13	Level 1 and 2; internal fires, Level 1 and 2; internal
14	flooding, Level and 2; PRA-based seismic margin
15	assessment, and other external events.
16	This PRA covers both at-power and during
17	low power and shitdown operations. The staff will
18	also present you the reviews of the PRA quality and
19	the use of this PRA during the design certification
20	stage. For each technical area, the staff will
21	briefly present you the depth of our review and the
22	key technical issue. It should be noted that for
23	this presentation it only covers the information
24	provided in the DCD Revision 0, and any support

information for this revision. 1 2 The staff is totally aware and on top of 3 the PRA update being conducted by the applicant. 4 However, because the DCD revision was -- is not yet 5 available to us; therefore, it is immature at this 6 point to make any conclusion on the PRA adjustment. 7 Next slide, please. The first topic for 8 today=s PRA 9 presentation is on the quality of APR1400 PRA. The applicant addressed the qualities of the PRA 10 conducting peer reviews and provide stratifications 11 12 in Section -- DCD Sections 19.1.2, and specifically in Table 19.1.1, that the PRA is sufficient to support 13 this application. 14 15 Following the guidance provided in the SRP, the staff ensured that the levels of details, 16 17 the scope, and the PRA qualities, including PRA update and upgrade are reasonable and acceptable. 18 The staff 19 estimates the peer review=s report to an audit to 20 ensure that any deficiencies identified from these 21 peer reviews would not have any significant impacts 22 Due to the issues identified in the on the PRA. 23 staff evaluation report with open items, at this point

we are unable to make any conclusion that the PRA

24

1	quality of APR1400 is acceptable.
2	Next slide, please.
3	Under the quality, two topics we=d like
4	to present to you. The first one is the PRA
5	conversions from SAREX to CAFTA. During phase 1=s
6	review, the applicant notified the staff that they
7	had intended to convert their models from SAREX to
8	CAFTA.
9	The duration for this conversion taking
10	place from June 2015 through July last year. During
11	the conversion, the applicant incorporates some of
12	the peer review findings, some of the staff findings,
13	and their self-identified issues.
14	During the public meetings last year,
15	they sent to us their preliminary results from the
16	CAFTA models. The staff noted that those two models
17	not identical; however, the difference is from the
18	CDF, the LRF, CCFF, and the PRA insights are not much
19	different, and they are just minor difference.
20	In addressing the staff concerns, the
21	applicant agreed to complete the following tasks
22	during the staff phase 2 review, including perform
23	self-assessment om the CAFTA model, notify the staff
	soll assessment on one offilm model, needly one seall

1	revisit all of the sensitivity studies using the
2	SAREX, and revise the DCD.
3	Next, please.
4	The next topic is on the peer review. I
5	mentioned previously the applicant justified their
6	quality the quality of their PRA. They conducted
7	a peer review prior to the submittal.
8	This was performed during the week of
9	June 24, 2013, against the ASME/ANS PRA standard.
LO	The peer reviews were conducted by a team of six PRA
L1	experts with over 170 years of diverse PRA experience.
L2	The scope of this review included at-
L3	power internal events, Level 1; at-power internal
L 4	flooding, Level 1; and loss release frequency
L5	modelings.
L 6	This peer review resulted in 90 facts and
L7	observations. Within those F&Os, 59 are findings, 27
L 8	are suggestions, and four are best practices.
L 9	The peer report concluded that, and I
20	quote it directly from that report, that the PRA1400
21	PRA substantially meets both the ASME PRA standard
22	and the draft ALWR standard at capability 2 or better
23	for 88 percent of the applicable supporting
2.4	requirements, with 90 percent met at capability 1 or

1	better.
2	Next slide, please.
3	MEMBER KIRCHNER: Could you just for the
4	non-PRA practitioners, I find it interesting that
5	it=s 88 percent of the applicable supporting
6	requirements. Is that just you just tabulate all
7	of the requirements in the standard and then match
8	the PRA against it?
9	I mean, what does it mean to be 88 percent
10	or 90 percent or better? Is that like an A, or is it
11	a good vintage, or is it or a lot of work left to
12	be done? It doesn=t sound like it. So I=m just
13	curious. Is this the way these peer reviews are
14	typically done?
15	I=m having a little fun, Mr. Chairman.
16	MR. PHAN: In the
17	MEMBER KIRCHNER: It=s interesting that
18	the peer reviewers used percentages to grade it. I=m
19	just
20	MR. PHAN: In the PRA standard, there are
21	327 supporting requirements. Based on their initial
22	evaluation, they believe that 49 of them is not
23	applicable, like sub-requirement for dual unit. For
24	those that may not applicable to them, at this point

1	they take that out from the 327 SR.
2	And for the rest of that 278 remaining
3	SR, they say that 245 of them, or 88 percent I
4	mentioned here are the capability 2 or higher, which
5	means that those supporting requirements sufficient
6	to support risk-informed application. But that is
7	not the case here. This is the design certification.
8	So according to the SRP, capability 1s
9	would be sufficient for this application. So with
10	that, they say 90 percent of 278 supporting
11	requirements met the capability 1.
12	MEMBER KIRCHNER: Now I will be a little
13	more serious. You know, in the construction
14	management business, one is always concerned about
15	percent complete because you could count milestones,
16	but not all milestones are created equal. So in lay
17	terms, plain English terms, what=s your assessment of
18	the what does that mean when it=s 88 percent or 90
19	percent?
20	This is quite good. It would
21	MR. PHAN: Yes.
22	MEMBER KIRCHNER: seem to indicate
23	that it=s a mature a relatively mature PRA at this
24	point, given where they are in the design.

	[] 235
1	MR. PHAN: The 88 percent would not tell
2	anything.
3	MEMBER KIRCHNER: Right.
4	MR. PHAN: The staff taken that to ensure
5	that for those that not met, the applicant, they have
6	to justify why not met, and what the impact is on the
7	application.
8	MEMBER KIRCHNER: Okay.
9	MR. PHAN: Secondly, the staff focused on
10	the findings not met are not met at this point,
11	because the finding would tell us any there are,
12	you know, issues with the PRA models, and that=s where
13	the staff paid the attention on.
14	MEMBER KIRCHNER: Thank you.
15	MR. PHAN: And for your information, we
16	asked the applicant to resolve all of the findings
17	and give us their resolutions by the end of phase 4
18	review.
19	MEMBER KIRCHNER: Thank you.
20	MR. PHAN: Yes.
21	MEMBER BLEY: Just for members of the
22	Committee who haven=t been here the last many years,
23	in a series of letters over at least five years, maybe
24	going on 10, the Committee has been urging the staff

1	to actually ask that the design cert PRA be a category
2	2, except in cases where it is not possible because
3	of the state of construction. They haven=t agreed
4	with us.
5	MR. PHAN: Okay. Through the regulatory
6	audit, the staff had the opportunity to estimate the
7	peer reviewers' report, and open insights with the
8	PRA has been assigned to the capability of the PRA
9	standard.
10	For the staff, this peer review was used
11	to identify the strength and the weakness of the PRA
12	and get confidence in the PRA models and results.
13	Based on our initial review and the audit, the staff
14	finds that the applicant had not completely
15	dispositioned all the 59 findings.
16	Some of those findings the applicant
17	assessed by perform such DCD study. And,
18	furthermore, we found inconsistencies of the
19	information provided in the report and the
20	information provided in the DCD.
21	In response to the staff concerns, the
22	applicant agreed to disposition all 59 findings and
23	update the DCD to incorporate the findings into their
24	model and the DCD during phase 4 review.

	237
1	And that is the end of the PRA quality.
2	The next topic is on the internal events at-power
3	Level 1 PRA. And I will introduce Mr. Ayegbusi and
4	Ms. St. Peters.
5	MR. AYEGBUSI: All right. Next slide.
6	All right. Good afternoon. My name is
7	Ayo Ayegbusi, and I was responsible for reviewing the
8	initiating events, success criteria, and accident
9	sequence analysis, and the quantification section of
10	the DCD.
11	All right. So my review was performed in
12	accordance with the SRP-19.0 acceptance criteria
13	while using the PRA standard as well as a guide. As
14	Hanh mentioned, he had already talked about the peer
15	review. So because the applicant had a peer review
16	performed, I was able to perform a less detailed
17	review and focus on issues of the design and the
18	consistency between the DCD and the PRA notebooks.
19	I was also able to audit the PRA notebooks
20	for my sections in detail, partly because the DCD was
21	light on information. In addition, my review
22	included ensuring the applicant appropriately used
23	the data from NRC, NUREGs, and other sources that
24	they referenced, as they were applicable to the

1	applicant=s design.
2	Subsequent to that, I was I used RAIs
3	for areas that were not adequately described in the
4	DCD as expected by the SRP acceptance criteria or
5	areas that, based on our experience, we felt needed
6	to be covered in the DCD.
7	Overall, the applicant=s responses to my
8	RAIs were acceptable, and the RAIs are now
9	confirmatory items.
L 0	Next slide, please.
L1	So now I would like to discuss some items
L2	of interest that came up during my review, and they
L3	are mainly under the initiating events analysis and
L 4	the success criteria analysis section of the DCD.
L5	What I identified was that some
L 6	initiating events, such as very small LOCA, were not
L7	screened during the analysis, even though that was -
L8	- it=s one of the initiating events that is identified
L 9	in NUREG-6928, and in the applicant=s application
20	they mentioned that they had used that in developing
21	and performing the analysis.
22	We also did not identify any new or unique
23	events. The applicant didn=t. We looked at it from
Э Д	our point of view and we also didn=t identify any

1	All right. To move on to success
2	criteria, so for this
3	MEMBER STETKAR: Before you get to
4	success criteria, I=ll ask you the same question I
5	asked the applicant. It=s really curious to me why
6	I don=t see many support system initiating events,
7	and why the support system initiating events that I
8	can see are in lockstep with that NUREG.
9	Did you review the initiating event
10	notebook and the initiating event grouping? And let
11	me ask you a couple of questions. Are you okay with
12	the fact that failure of the main transformer is a
13	general transient initiating event?
14	MR. AYEGBUSI: Which question would you
15	like me to answer first?
16	MEMBER STETKAR: Both of well, the
17	first one you can answer first.
18	MR. AYEGBUSI: Okay. So I did review
19	both notebooks. Well, I did review the initiating
20	event analysis notebook.
21	MEMBER STETKAR: Are you okay with the
22	fact, then, that failure of the main transformer is
23	a general transient initiating event?
24	MR. AYEGBUSI: I did not identify any

1	issues with main transformer failure being a general
2	transient initiating event.
3	MEMBER STETKAR: Thank you.
4	MR. AYEGBUSI: Okay.
5	MEMBER STETKAR: I completely disagree
6	with your finding. Are you okay with the fact that
7	spurious opening of a main steam safety valve is a
8	general transient initiating event?
9	MR. AYEGBUSI: I have to go back and look
10	at that.
11	MEMBER STETKAR: Okay.
12	MR. AYEGBUSI: I don=t recall off the top
13	of my head.
14	MEMBER STETKAR: Did you look at the fact
15	that there are many failures, valve failures, that
16	can give you spirious isolation of all component
17	cooling water to all four reactor coolant pumps?
18	And that if you use the valve failure
19	rates in NUREG/CR-6928, the frequency of that event
20	would be comparable to the total frequency of partial
21	loss of component cooling water. That to me sounds
22	like it=s a design-specific initiating, support
23	system initiating event. Did you look at that?
24	MR. AYEGBUSI: So for the in looking

1	at the design-specific initiating events, I was
2	trying to identify if any were there. As far as
3	support system initiating events, what I looked at
4	was the fault trees that developed for each support
5	system, and what frequencies they developed there and
6	compared that to what the NUREG initiating event
7	frequencies were and to see what they eventually used.
8	MEMBER STETKAR: Do you have any idea
9	what the configuration of the component cooling water
10	system in the NUREG is that gave them those
11	frequencies in that NUREG?
12	MR. AYEGBUSI: I don=t have that off the
13	top of my head.
14	MEMBER STETKAR: No, you don=t, because
15	it=s an amalgam of chunk.
16	MR. AYEGBUSI: Okay.
17	MEMBER STETKAR: Okay? The particular
18	thing that I was trying to mention here is that it=s
19	nothing to do with pumps failing. It is valves
20	closing spuriously that isolate all component cooling
21	water to all four reactor coolant pumps. And this is
22	this does not depend on whether the pumps are split
23	between division 2 or division 2. It=s strictly the
24	plumbing in the plant.

1	The frequency that I can calculate using
2	data from the same NUREG that you referred to gets me
3	a larger fraction of the total frequency that they
4	use that ostensiby accounts for pumps failing. But
5	I don=t know whether it=s pumps failing because, you
6	know, we don=t know what=s in that NUREG frequency;
7	do we?
8	Greg, do you want to add something?
9	MR. ROZGA: Greg Rozga from Enercon. Is
10	this on?
11	MEMBER STETKAR: Yes, it is.
12	MR. ROZGA: Okay.
13	MEMBER STETKAR: Well, speak into it.
14	MR. ROZGA: When you did your
15	calculation, did you also need to fail seal injection
16	cooling?
17	MEMBER STETKAR: No, no. That=s I=m
18	sorry. If I fail component cooling water to all four
19	reactor coolant pumps, I will have an initiating
20	event. I will have no reactor coolant pumps running
21	because the operators will shut them down.
22	MR. ROZGA: Correct. I=m sorry. I
23	thought
24	

1	themselves.
2	MR. ROZGA: you were referring to a
3	seal LOCA.
4	MEMBER STETKAR: No. I didn=t say seal
5	LOCA; I said initiating event.
6	MR. ROZGA: My error. Sorry.
7	MEMBER STETKAR: Okay. Thanks.
8	Last question I have for initiating
9	events is and ==m trying to keep these as concise
10	as I can. The LOCA initiating event frequencies in
11	this magic NUREG that we have to use the numbers from
12	have a small LOCA size of .5 inches to two inches, a
13	medium LOCA size of two inches to six inches, and a
14	large LOCA size of greater than six inches.
15	And that is from the January 2012 version
16	of NUREG/CR-6928, just to give you a NUREG. It is
17	actually listed as Update 2010, but if you look at
18	the footer of the page it=s January 2012.
19	How do we know that those are the
20	appropriate LOCA size ranges for this nuclear power
21	plant?
22	MR. AYEGBUSI: So the if I remember
23	correctly, that was the initial looking at the
24	looking through the notebooks, right, there was

1	and that was something I was going to get to under
2	success criteria there was some inconsistency
3	between the DCD and the notebook, right?
4	And so I don=t recall if it was a question
5	that was asked via the RAI process or a question that
6	was asked during pur audit, but that was a question
7	that was asked. And what we got back from the
8	applicant through their analysis was that those break
9	sizes were applicable to this design.
10	And so what I did then was look at the
11	results of what was provided. I believe some of the
12	results were provided in the in this I want to
13	say the success criteria notebook, in one of the PRA
14	notebooks, and that was I found that acceptable,
15	so
16	MEMBER STETKAR: Did you find I mean,
17	did they do a systematic typically, the break sizes
18	are based on physics and thermal hydraulics. You
19	know, what is the largest break that cannot directly
20	remove decay heat determines the upper end of the
21	small LOCA size range. That depends, in my notion,
22	on how big a power plant you have.
23	MR. AYEGBUSI: It=s not just a two-inch
24	piece of pipe. The size break between medium and

1	large LOCA depends on the ability of low-pressure
2	injection alone to prevent core uncovery, not to be
3	careful about core uncovery, to allow reflood. That
4	also depends on the plant design.
5	MEMBER STETKAR: So did the success
6	criteria notebook do that? If I have a 300 megawatt
7	plant compared to a 1,500 megawatt plant, my break
8	sizes are going to be much different.
9	MR. AYEGBUSI: I agree.
10	MEMBER STETKAR: Okay. So that=s,
11	again, why because the magic generic NUREG/CR-6928
12	gives me frequencies for a half-inch to a two-inch
13	break, why is that an appropriate small LOCA frequency
14	for this particular plant?
15	MR. AYEGBUSI: So when we looked at that
16	probably over a year ago, the analysis that I recall
17	bounded the break sizes in NUREG-6928. So I don=t -
18	- so, for example, such as for large LOCA, I don=t
19	recall specific - the specific details of what was
20	done, but I do recall that that analysis was done to
21	determine the threshold between small and medium and
22	medium and large.
23	MEMBER STETKAR: Okay. Thank you.
24	MR. AYEGBUSI: Okay. So moving on to

1	success criteria, in one instance during our review
2	we identified the Chapter 19 success criteria for SI
3	pumps in response to a large LOCA was more
4	conservative than the Chapter 15 success criteria.
5	We also found that there were similar inconsistencies
6	between the DCD and the PRA notebooks during our
7	audit.
8	In discussions with the applicant, these
9	items were resolved, and they have been closed to
10	confirmatory actions confirmatory action items.
11	On the final bullet that I have, the PRA
12	model software conversion, so the applicant is
13	they are converting the model, the PRA model, and we
14	are expecting them to incorporate some of the issues
15	that they identified during that were identified
16	during the PRA review, some of the issues that we
17	have raised and resolved by the RAI and audit process.
18	And once that=s done, and I guess later
19	revisions to the DCD is sent in, I will have to review
20	those changes and then determine if there is any
21	impact on the PRA results and insights.
22	MEMBER MARCH-LEUBA: Can you give us an
23	example of those success criteria that were more
24	conservative?

	11 247
1	MR. AYEGBUSI: All right. So I=ll just
2	
3	MEMBER MARCH-LEUBA: Just one example.
4	MR. AYEGBUSI: Okay. So, for example,
5	as you=re aware, chapter 19 is the accident analysis,
6	right? And in Chapter sorry, did I say Chapter 19?
7	Chapter 15.
8	MEMBER MARCH-LEUBA: You said 19; you
9	meant 15.
10	MR. AYEGBUSI: 15, yes. So, in
11	Chapter 19, the success criteria for large LOCA for
12	the safety injection pump was three out of four pumps,
13	right? In Chapter 15, it was two out of four pumps,
14	right? And, you know, typically, with Chapter 19 and
15	the PRA, we are expected to be more realistic, right?
16	So
17	MEMBER MARCH-LEUBA: And do you expect
18	that that was because they did a preliminary
19	Chapter 19 before they actually had a design, and
20	then didn=t come back to fix it?
21	MR. AYEGBUSI: I have no idea.
22	MEMBER MARCH-LEUBA: But they=re fixing
23	it now?
24	MR. AYEGBUSI: That is correct.

1	MEMBER MARCH-LEUBA: Okay. Thank you.
2	MR. AYEGBUSI: That=s all I have, unless
3	there are any questions.
4	MS. ST. PETERS: Good afternoon. My name
5	is Courtney St. Peters. I also reviewed part of the
6	internal events at-power. I was responsible for
7	reviewing data analysis, system analysis, and human
8	reliability analysis.
9	Next slide, please.
10	This slide just goes over my review
11	approach. As you can see, I revised part of the peer
12	review report, a sampling of the PRA and system
13	notebooks during the audit, but during my audit I
14	also asked RAIs if I needed additional information,
15	and I also asked questions during the audit as well
16	and had technical topic discussions at the public
17	meeting.
18	I also had to ensure consistency with
19	other DCD chapters, because some of my sections
20	covered things that were in other chapters, such as
21	human factors and digital I&C. I reviewed the key
22	assumptions which involved following up on some of
23	those. And in the course of my review, I found my
24	DCD sections were mostly acceptable, but I do have

1	some confirmatory items, along with an open item.
2	Next slide.
3	So one of the technical topics that I=ll
4	be talking about was digital I&C. This is one of the
5	this is the open items that I do have. During my
6	review, there was a lack of information regarding
7	digital I&C, in particular the common cause failure
8	analysis relating to their digital I&C system.
9	At the time of writing my SC, I still did
L 0	not have enough information. After the SC was
L1	issued, we did hold a public meeting with KHNP and
L2	KEPCO staff, and they committed to providing
L3	additional information, and we do have an approach to
L 4	closing out this open item.
L 5	So, if you go to the next slide, the next
L 6	slide highlights the staff commitments from KHNP and
L7	KEPCO. Some of those where they plan to discuss the
L 8	COMMON Q software similarities with Westinghouse,
L 9	they are going to evaluate the level of detail of
20	the model detail that they currently provide. There
21	are also plans to evaluate the architecture of the
22	digital I&C compared to the reference plant.
23	They will be adding the software common
24	cause failure events to their PRA, and this

	250
1	information will be incorporated into their next PRA
2	update, and they are going to plan to update the DCD.
3	During these updates, I am in communication as well
4	with the digital I&C staff to ensure that this is
5	consistent with what their information is as well.
6	Next slide?
7	The other technical topic I had to
8	highlight was related to RCP seal LOCAs, which I know
9	was discussed ear lier.
10	No, no. I was hoping you guys already
11	had all the questions out of the way.
12	So during the course of my review, and
13	along with other reviewers, the question related to
14	RCP seal LOCAs came up. It was evaluated by KHNP and
15	KEPCO as a model uncertainty, a sensitivity analysis,
16	and it was a key assumption as well.
17	During our review, we noticed they have
18	the failure probability of $1\mathrm{E}^{-3}$ per pump, which was
19	based on engineering judgment. Before they performed
20	their seal LOCA model, we requested additional
21	justification. In the course of that, they did
22	provide their seal model testing results, which was
23	proprietary information, but the results did support
24	their assumption.

	II 251
1	They plan to review and revisit the model
2	uncertainty and their sensitivity analysis during
3	their PRA update, and this item is considered a
4	confirmatory item.
5	MEMBER STETKAR: I read the RAI response,
6	and I won=t quote any numbers from it because it=s a
7	proprietary document.
8	MS. ST. PETERS: Yes.
9	MEMBER STETKAR: It raised several
10	questions in my mind, and I would does the staff
11	have the WCAP report?
12	MS. ST. PETERS: Yes.
13	MEMBER STETKAR: You do?
14	MS. ST. PETERS: During the audit, yes,
15	we=ve had access to it.
16	MEMBER STETKAR: No, I=m sorry. Do you
17	have it in hand?
18	MR. PHAN: We don=t have that report.
19	MEMBER STETKAR: We would like to have,
20	somehow, access to that WCAP report. I would anyway.
21	I don=t know how we make that happen because it=s not
22	submitted on the docket. But I will tell you that
23	numbers in that RAI response, especially given what
24	we=ve learned about other pumps= designs and other

1	claims for reliability of advanced seals, are
2	suspect.
3	So I would like to have the opportunity
4	to somehow be able to read the source document and
5	see what types of engineering, what types of design,
6	and in particular what amount of testing has been
7	done on those seals under what conditions.
8	MR. SCHNEIDER: Excuse me, but I=d like
9	to basically add - Ray Schneider, Westinghouse. I=d
10	like to add some information.
11	MEMBER STETKAR: This is, by the way, an
12	open meeting, so be careful about what you say.
13	MR. SCHNEIDER: Right.
14	MEMBER STETKAR: This is a public
15	meeting.
16	MR. SCHNEIDER: I understand. But I=m
17	going to basically do is just try to put everything
18	in perspective, because I think there is a
19	misinterpretation as to which seal design we are
20	looking at.
21	The RCP seal design used in the KNGR plant
22	is a derivative of the combustion engineering design,
23	which is totally different than the which is a
24	hydrodynamic seal design, which is totally different

than the design of those typical Westinghouse seals. 1 2 The hydrodynamic designs typically -- and 3 this design has been evaluated by the NRC, and an 4 approved consensus guidance document for a very 5 similar kind of construction in 2004 applied to the 6 CE fleet. 7 And the version of this seal that is being used for the KNGR design is a three-stage. 8 9 stage is fully \- full pressure stages. They=re dynamic seal stages, so they -- all stages have to 10 11 fail sequentially in order for a substantial leak 12 above this by -- | bf qpm above about 10 qpm to occur 13 per pump. 14 In the testing on the old versions of a 15 parallel seal design, not the KSB design, years ago, 16 which just tested these to 72 hours under station 17 blackout conditions. We recently completed testing of the KSB seal design in Germany for the advanced 18 seal version of the type F seal, which is going to be 19 20 going into these plants. 21 The type F seal was a modified redesign 22 of the KSB pump seal, specifically for the intent of 23 with station blackout scenarios. dealing They 24 modified some very small interference, so the seal

1 able and contract grow any 2 interference or distortion. 3 reevaluated redesigned They and or 4 rerequired the composition of the elastomers such 5 that the elastomers would be able to take -- been tested to at least 72 hours at -- in the 560 degree 6 7 range without any impact. And there was a full-scale test also completed a few months back, which basically 8 9 shows that operation for 120 hours, of which 72 remain station blackout conditions, had minimum leakage. 10 11 And we also looked at the possibility of 12 going to low subcoolings to find out if there is 13 impact to pop opening, and we couldn=t see 14 observable pop open, which we didn=t expect to see 15 anyways, but we had them do that special test. 16 provide -- based on this 17 information, a ne₩ topical was written which slightly modified the existing information that was part of 18 19 the old combustion engineering plant topical, which I believe is in the hands of the NRC now. 20 21 And these values will basically show that 22 the failure rates dropped a little bit based on these 23 new enhancements, but they are in the 10^{-3} range. 24 this typical what you see in the combustion of

	255
1	engineering fleet, and this was also tied to the
2	question you had with the with how they may have
3	been treating these seal leakages in the
4	consequential steam engineering and tube rupture
5	report.
6	So it s a different design. There=s a 10
7	leaking seal, and I just wanted to basically make
8	that clear, so we re not mixing apples and oranges.
9	MEMBER BLEY: Do you know if you are
10	submitting that topical?
11	MR. SCHNEIDER: I=m putting
12	MEMBER BLEY: You don=t know. That=s
13	okay.
14	MEMBER CORRADINI: But I thought John=s
15	initial question was, can we get the topical?
16	MEMBER STETKAR: It=s not a topical
17	report. It=s simply a it=s a
18	MEMBER CORRADINI: A technical report.
19	MEMBER STETKAR: it=s a WCAP technical
20	report.
21	MEMBER CORRADINI: Technical report.
22	MEMBER STETKAR: It has not been
23	submitted on the docket.
24	MR. OH: This is Andy Oh, KHNP,

	<u> </u>
1	Washington office. That WCAP document is not
2	submitted to the NRC, but it is admitted to the
3	electronic reading room, and the staff can audit and
4	see that document.
5	MEMBER MARCH-LEUBA: So do ACRS members
6	have access to the electronic reading room? Or can
7	we get access?
8	MEMBER STETKAR: We don=t need to work
9	out the logistics at this subcommittee meeting. This
10	is just a request.
11	MR. CIOCCO: This is a document that we
12	requested. This is a document that we audited. So
13	we don=t that s as far as we=re going with it.
14	And, I mean, if you have a request for the document,
15	I guess you could provide it to KHNP. But for the
16	staff, it=s an audit document.
17	MEMBER STETKAR: We=11 work through the
18	I think we did, but it=s on the record. They can
19	say no.
20	MEMBER MARCH-LEUBA: Courtney, back to
21	digital I&C, once you put the common cause failures
22	on software, my gut feeling is that the reliability
23	is going to be achieved through the watchdog and not
24	through the software itself. And there is going to

1	be a big reliance on the watchdog, which we will
2	review under Chapter 17, how it=s implemented.
3	I=m just giving you a heads-up that
4	whenever this PRA gets done of the whole digital I&C
5	system, please make sure to review the watchdog
6	implementation and how it=s built into the PRA,
7	because that=s what is going to give the numbers.
8	MS. ST. PETERS: Okay. And I=ve been
9	talking quite frequently with the Chapter 7
10	reviewers, and we=ve been communicating on the
11	information we had and what we=ve seen. And so I=ll
12	definitely keep that in mind.
13	MEMBER MARCH-LEUBA: Just make sure the
14	PRA evidence is the watchdog.
15	MS. ST. PETERS: Okay.
16	MEMBER MARCH-LEUBA: Because that=s
17	where the numbers are going to come from.
18	MEMBER REMPE: So I think I should have
19	asked this for Odunayo instead of you, but did you -
20	- were you present earlier today when we talked about
21	the use of the NUREG-1570 Westinghouse conditional
22	consequential steam generator tube rupture
23	probabilities?
24	MR. AYEGBUSI: Yes, I was.

1	MEMBER REMPE: So you heard my question
2	about using Westinghouse data for CE, and you=re aware
3	of the staff=s work in research on NUREG-2195?
4	MR. AYEGBUSI: I=m not aware of the I
5	wouldn=t say that I heard your question and was able
6	to follow your question. Neither am I aware of the
7	NUREG you mentioned.
8	MEMBER REMPE: So I did I think I
9	believe I heard KHNP say, AYes, we will be looking at
10	this, and that we might want to change those values.@
11	And I think it would behoove the staff to also look
12	at that report and think about whether the conditional
13	probabilities for consequential steam generator tube
14	rupture should be changed.
15	MR. AYEGBUSI: Understood. We=11 take a
16	look at that.
17	MEMBER REMPE: Thank you.
18	MR. AYEGBUSI: Thank you.
19	MS. ST. PETERS: So if there=s no other
20	questions, that=s the end of my presentation, and I
21	believe the end of Level 1 at-power.
22	MR. NAKANISHI: Good afternoon. My name
23	is Tony Nakanishi, and I=ll be discussing the internal
24	fire and flood review. This morning I think the

	259
1	applicant provided a good summary of the individual
2	tasks that are performed for both Level 1 floods and
3	fires. So I=d like to focus more on kind of the
4	high-level staff thinking relative to how the fire
5	and floor PRA is supporting the design certification
6	application.
7	Can you go to the next slide, please?
8	So, overall, we=re finding that the fire
9	PRA we=re fair y comfortable with the applicant=s
10	approach and assumptions that are being used. You
11	know, we have a few questions related to mainly
12	with respect to documentation and the DCD.
13	But, overall, you know, the staff
14	we=re finding that the applicant used the you know,
15	the industry standard approach, NUREG-6850, and
16	applied it to the extent practical and appropriate
17	for design certification stage by, you know, assuming
18	appropriate assumptions like, you know, full room
19	burnout for most of the fire compartments, assuming
20	at least, you know, transient, general transient,
21	given a fire cable, you know, in lieu of doing a
22	detailed cable or circuit analysis, you know,
23	assuming sort of a, you know, bounding approach.
24	So at this point, you know, I think we=re

1 comfortable with the methodology and 2 assumptions. Ι will say that Hanh had mentioned 3 they=ve gone through a conversion activity, and we 4 need to sort of circle back and make sure the results 5 -- kind of confirm the results. 6 verall we are finding that the But 7 applicant is also, you know, using risk insights to, you know, propose things that need to carry through 8 9 design and the operation, like, you know, in 10 particular the routing of the transformer cable was judged to be placed outside the turbine building, for 11 12 example. 13 have identified some cables that 14 need to be protected to ensure the risk profile, which 15 leads to my next slide, if you could -- so one item 16 to highlight that -- you know, the that we do want 17 applicant had memtioned this also I think in the morning presentation, but they have identified in 18 19 risk-significant fire compartments certain 20 cables that need to be either, you know, protected 21 or, you know, can be shown later that it won=t affect 22 the component that it controls. 23 ensure that this sort of carries So to 24 the applicant to identify a COL through, we asked

1	item to make sure that, you know, this key PRA
2	assumption remains in place.
3	So, again, overall, you know, we are
4	fairly comfortable with the fire PRA approach. And
5	if you have no questions, I can move on to the
6	flooding analysis
7	MEMBER STETKAR: I have questions. You
8	asked them a question about why they didn=t model
9	fire-induced if we want to call it spurious safety
10	injection or a fire-induced safety injection, and
11	their response was, well, the normal reactor coolant
12	system pressure is higher than the shutoff pressure
13	of the safety injection pump, so it=s not a problem.
14	In my experience, a safety injection is
15	a lot more than just starting the safety injection
16	pumps. It=s isolation of the containment. It=s
17	other things that get isolated, like main feedwater
18	gets isolated.
19	So for spurious safety injection, we only
20	care about whether the pumps can pump water into a
21	higher pressure.
22	MR. NAKANISHI: So that=s a good point.
23	MEMBER STETKAR: Okay.
24	MR. NAKANISHI: We=ll look at that and

1	make sure
2	MEMBER STETKAR: What I=m trying to probe
3	here, by the way, is the level of detail that the
4	staff thought about these types of initiating events,
5	not just looking at some NUREG someplace and accepting
6	what somebody says with a focus on pump deadheading.
7	So, okay, thank you.
8	The second question I had on the fires -
9	- you heard were you here this morning?
L 0	MR. NAKANISHI: I was.
L1	MEMBER STETKAR: Okay. Or this
L2	afternoon, whenever the heck it was. Why are you
L3	okay with the way they treated main control room
L 4	fires, given the fact that I put out the fire in 9.9
L5	minutes and have some amount of damage on the thing
L 6	that I=ve taken to be calling a control of console to
L7	avoid confusion with something that somebody else
L 8	might call a cabinet?
L 9	MR. NAKANISHI: So you gave me something
20	to think about a so there. We=ll look at that and
21	see if there needs to be any adjustments.
22	MEMBER STETKAR: And, finally, something
23	that I didn=t know reading anything in the DCD or
Э Д	looking at the models or looking at success criteria

1	or reading about human reliability analysis until I
2	got to the staff=s review of the fire stuff is that
3	apparently one of the two motor-operated valves in
4	the line for each pressurizer POSRV is normally
5	deenergized and somebody has got to run out and
6	connect power to you know, close a breaker or
7	something like that, in order for the operators in
8	the control room to initiate feed and bleed cooling.
9	MR. NAKANISHI: That=s correct. We
10	didn=t know that initially either.
11	MEMBER STETKAR: It=s interesting it=s
12	not documented anywhere. Did the staff look at all
13	at the human reliability analysis? And now, because
14	I didn=t learn about this until fire, but it applies
15	during power operation, and it applies even during
16	low power and shutdown.
17	MR. NAKANISHI: Absolutely. Actually,
18	we
19	MEMBER STETKAR: Do you look at how that
20	affects the human reliability analysis for
21	MR. NAKANISHI: Right. So we
22	MEMBER STETKAR: those actions?
23	MR. NAKANISHI: That=s exactly the
24	question that=s outstanding still.

1	MEMBER STETKAR: It is?
2	MR. NAKANISHI: Yes. We actually
3	noticed it as part of the internal flooding analysis
4	where there was some inconsistency and assumptions
5	where during internal events well, let=s see, for
6	flooding they have an assumption where for
7	external you know, operator actions external to
8	the control room will basically fail.
9	Now, that may be a potential thing that
10	needs to be looked at if the feed and bleed will
11	require ex-control room action. So we have an RAI to
12	kind of figure out you know, figure out that
13	assumption.
14	MEMBER STETKAR: But and I read that
15	for both the internal fires where I first learned
16	about this and the internal flooding that you just
17	mentioned. Did you also try to follow up on how they
18	treated it during a plain vanilla loss of feedwater
19	initiating event that propagates this is full power
20	operation, loss of main feedwater, internal
21	initiating event, that eventually gets to feed and
22	bleed cooling?
23	MR. NAKANISHI: Right. So
24	MEMBER STETKAR: It strikes me that the

1	human error probability for failure to initiate feed
2	and bleed on this particular design would be higher
3	than the human error probability for a design where
4	the operator simply has to walk up to the control
5	board and open the valves.
6	MR. NAKANISHI: So we did look at the HRA
7	notebook, and, you know, their methodology identifies
8	that particular step as
9	MEMBER STETKAR: They do.
10	MR. NAKANISHI: external to control
11	room action. So they=ve considered that.
12	MEMBER STETKAR: Okay. Thank you. Do
13	you know how many operators they have to dispatch to
14	given the distribution of things throughout the
15	auxiliary building, I=m assuming that these they
16	have to connect - they have to close breakers in
17	four separate rooms.
18	MR. NAKANISHI: I don=t know.
19	MEMBER STETKAR: Okay. By the way, if
20	KHNP wants to answer this, you can come up and get it
21	on the record.
22	MR. J OH: Yes. This is Andy Oh, KHNP,
23	Washington office. In order to implement a POSRV
24	feed and bleed operation for circuit breaker for

1	the belt should be closed in a local area. That
2	is based on my memory, that is located in second
3	floor of the aux building, and that takes time for -
4	- within 30 minutes operator can close the circuit
5	breaker, and then the NCR, the POSRV belt can be open,
6	and then implemented to the feed and bleed.
7	The reason that we the design of that
8	feature is inadvertent open for the POSRV makes some
9	LOCA. So in order to prevent that inadvertent just
10	per function of opening valve in on the NCR, that
11	leads to the direct LOCA. So that=s the reason we
12	just made some of the redundant features to the to
13	make some circuit is in different location.
14	MEMBER STETKAR: Thank you. You didn=t
15	answer how many people do this. Is it single operator
15 16	answer how many people do this. Is it single operator or
16	or MR. J. OH: Yes. Per I think that one
16 17	or
16 17 18	or MR. J. OH: Yes. Per I think that one single people car dispatch to that place that can
16 17 18 19	or MR. J. OH: Yes. Per I think that one single people car dispatch to that place that can close the circuit breaker. MEMBER STETKAR: Okay. When you say
16 17 18 19 20	or MR. J. OH: Yes. Per I think that one single people can dispatch to that place that can close the circuit breaker. MEMBER STETKAR: Okay. When you say Athat place, @ it=s I know the rooms they have to
16 17 18 19 20 21	or MR. J. OH: Yes. Per I think that one single people can dispatch to that place that can close the circuit breaker.

	<u> </u>
1	whatsoever in the DCD, and it=s a different design
2	feature than
3	MR. ROZGA: Greg Rozga from Enercon.
4	Yes, there is two rooms. There is an I&C equipment
5	room, Div 1 and Div 2, that they have to go to.
6	They=re in the Alpha and Bravo quadrants. Whether
7	it=s on the second or third level, that I don=t
8	recall.
9	MEMBER STETKAR: But this says the power
10	is disconnected to the motor-operated valve, there=s
11	four POSRVs, so I=m assuming there=s four motor-
12	operated valves. And maybe I=m wrong; I was just
13	assuming that one would be in each of the four AC or
14	DC divisions. But I don=t even know if they=re AC-
15	or DC-powered motor-operated valves.
16	MR. ROZGA: They are correct me if I=m
17	wrong, they are AC motor-operated valves, but they
18	have a DC power supply through an inverter.
19	MEMBER STETKAR: Okay.
20	MR. ROZGA: Is that correct?
21	MEMBER STETKAR: Well, I don=t want to -
22	- time on the details, but
23	MR. ROZGA: Thank you.
24	MR. NAKANISHI: So we=11 move on to

	268
1	internal flooding. If you could just the other
2	way.
3	So, again, internal flooding you know,
4	overall the staff finds that the applicant basically
5	used the industry standard approach, you know,
6	consistent with the ANS standard and the staff=s SRP.
7	As Hanh mentioned, this model was peer
8	reviewed also. This is one of the other models that
9	was peer reviewed, and basically the peer review team
LO	found that, you know, the PRA essentially meets
L1	capability category 1.
12	There was one finding relative to
13	uncertainty or certain assumptions being not
L 4	documented and things like that. But overall, you
L5	know, I think the applicant provided a lot of detail
L 6	in terms of characterizing the flood scenarios. You
L7	know, the partitioning represents the design, and so,
L8	again, we=re fairly comfortable with the overall
L 9	methodology and assumptions.
20	One thing, if you=d go to the next slide,
21	one item of potential interest is regarding the
22	maintenance-induced floods. The applicant initially
23	screened out this as a potential initiating event
Э Д	where an operator would inadvertently operate a

1	component leading to a flooding event. And there was
2	a quantitative approach that we felt that wasn=t quite
3	defensible.
4	So the applicant identified a COL item
5	for the the CO applicant or holder to do a plant-
6	specific analysis when more details in terms of
7	procedures and things like that are available. So
8	we=re thinking that=s an acceptable approach.
9	So that=s it in terms of internal
10	flooding. Are there any questions? Thank you.
11	MR. WAGAGE: My name is Hanry Wagage.
12	I=ll be discussing the results for internal events,
13	internal fire, and internal flood at-power Level 2
14	PRA.
15	MEMBER MARCH-LEUBA: Do you have your
16	light green?
17	MR. WAGAGE: My name is Hanry Wagage.
18	I=m discussing my review of internal events, internal
19	fire, and internal flood at-power Level 2 PRA.
20	I reviewed DCD Section 19.1 related to
21	Level 2 using SRF 19.0 guidance. Reviewed Level 2
22	methodology, demonstrates containment event trees,
23	decomposition event trees, and release categories.
24	Some of these informations were missing or discussed,

1	for example, how the decomposition event trees were
2	analyzed, were not discussed. So then I discussed -
3	- I asked the applicant during audit or issued RAIs
4	and got changes to DCD adding this information.
5	Audited APR1400 PRA notebooks related to
6	this area, and I looked at the review topics in this
7	large release frequency in the PRA review report.
8	Discussed as I said, I discussed technical issues
9	with the applicant during audit and during public
10	meetings.
11	To highlight one of the areas I review -
12	- I have described, when we noticed that there are
13	two source term categories in internal events PRA,
14	they differ only by 10 percent release area. One is
15	containment leakage, .1 cubic foot opening, and other
16	one contains a breach, one cubic foot area.
17	So when they looked at the source term,
18	cesium iodine, which represents iodine release, we
19	found that it does not justify the significant change
20	from the area because the release was so high. And
21	we asked the applicant to explain.
22	Finally, the applicant explained that the
23	reason was that for one case, STC-17, containment
24	pressure stays high because the leak containment

	271
1	pressures stays high. Because of that natural
2	circulation, cooling is high. So because of that,
3	there is less revaporization of isotopes in the
4	pressurizer. That=s the reason that the STC-17 data
5	load found this justification acceptable and
6	reasonable.
7	Next slide?
8	Internal fire and internal flood Level 2
9	PRA, there wasn=t much information in DCD to bring it
10	to a Level 2. But applicant described Level 1/
11	Level 2 PRA for internal events, but not much for
12	internal fire and internal flood.
13	So I asked the applicant to provide this
14	information, and applicant updated proposed
15	updates to DCD providing this information. Applicant
16	stated that applicant used the same methodology used
17	for internal events for internal fire and internal
18	flood Level 2 PRA. We find that acceptable because
19	initiating events would not affect how the
20	containment would behave in Level 2.
21	Next slide? Next?
22	MS. NEUHAUSEN: Good afternoon. My name
23	is Alissa Neuhausen. I=m a technical reviewer in the
24	Structural Engineering Branch. I was responsible for

1	the review of the PRA-based seismic margin
2	assessment. In addition to myself, Robert Roche and
3	Hanh Phan also contributed to the review.
4	The intent of the review was to ensure
5	that the applicant=s size of margin assessment is
6	reasonable and acceptable. To reach a conclusion,
7	the staff reviewed the scope, level of details, and
8	technical adequacy of the applicant=s approach. The
9	staff followed guidance in ISG-20, implementation of
10	a PRA-based seismic margin analysis for new reactors,
11	and SECY 93-087.
12	The staff focused on information provided
13	in DCD Section 19 1.5.1, seismic risk evaluation, and
14	Table 19.1-43, seismic fragility analysis results
15	summary. The number on the slide is incorrect. It
16	should say 43.
17	In the next two slides, I will discuss
18	the applicant=s seismic fragility evaluation and the
19	status of the plant level, high confidence of low
20	probability of failure, or HCLPF capacity.
21	The applicant=s initial submittal, Rev 0,
22	included HCLPF capacities for structures and
23	components based on the reference plant design
24	response spectra. Based on this submittal, the staff

1 eight clarify the SMA fragility RAIs to evaluation approach. 2 3 The fragility evaluation HCLPF capacities 4 are referenced in the APR1400 CSDRS, thereby ensuring 5 an adequate mardin of design based on DCD level 6 information. 7 applicant applied the conservative deterministic failure margin approach to determine 8 9 the HCLPF capacities. The staff found that the fragility evaluation is in accordance with guidance 10 11 in ISG-20. The ||fragility evaluation demonstrated 12 that site-independent structure HCLPF capacities are 13 greater than or equal to .5 q, component HCLPF 14 capacities are gleater than or equal to .5 g, and 15 site-dependent structure HCLPF capacities are greater than or equal to 1.67 times the GMRS PGA. 16 17 For the at-power seismic margin assessment, the staff found that the method used was 18 19 For low power and shutdown modes, the acceptable. 20 PRA-based SMA was not addressed in the DCD. The 21 additionally, staff, requested seismic-induced 22 dominant mixed cutsets containing seismic failures, 23 random failures, and operator actions in sequence 24 level HCLPF capadities during at-power and low power

1	shutdown modes, before a conclusion can be made on
2	the acceptability of the PRA-based SMA.
3	That=s the end of this portion of the
4	presentation, if there are no questions.
5	MR. PHAN: Thank you, Alissa.
6	The next topic is on other external
7	events. For other external events
8	MEMBER KIRCHNER: Hanh, before you go on,
9	Mr. Chairman, can I ask a couple of questions, at
10	risk of backtracking?
11	CHAIRMAN BALLINGER: You can ask more
12	than a couple.
13	MEMBER KIRCHNER: While the presenters
14	are here. The first one is on sensitivity analysis.
15	I just I looked at that, and you had some cases
16	where, without going into numbers because I think
17	this must be proprietary, the GSI-191 sensitivity
18	case showed a significant increase on CDF, and then
19	the statement, AWell, this is well within the
20	Commission=s goal @
21	So what do you do when you look at these
22	sensitivity analyses? What do you and I think
23	that statement is made several times. So I was left
2.4	somewhat perpleyed as to what the takeaway is on

1	sensitivity analysis.
2	MR. PHAN: I would ask Courtney or Ayo
3	to
4	MEMBER KIRCHNER: Yes, we lost Courtney
5	already. Sorry.
6	MEMBER MARCH-LEUBA: They=re hiding
7	behind the
8	MEMBER KIRCHNER: They=re hiding from me.
9	MR. AYEGBUSI: Can you please repeat the
10	question? Because some
11	MEMBER KIRCHNER: Yes. My question was
12	on sensitivity analyses. You had five or six cases
13	I will not go into the numbers because I believe
14	this is proprietary, but at least one case GSI-191
15	showed a significant increase in CDF.
16	But then the tag line was although that
17	appears significant, it=s well within the
18	Commission=s goal, and that was stated several times.
19	So what are you looking at when you look at these
20	sensitivity analyses?
21	(Pause.)
22	CHAIRMAN BALLINGER: We=ve got a little
23	too much dead air here. How about we refer this?
24	MEMBER KIRCHNER: Okay. And then I=m

1 information, so I=m one or two 2 I was -- I wanted to go back to presenters behind. 3 the case of the release of fission products. The 4 explanation given was that, in part, the -- you had a significant, lalger opening in the containment, and 6 I expected that to be the culprit. 7 then you go on to say that containment pressure 8 reduction in made natural convection cooling of the pressurizer less effective, 9 so you had revaporization of iodine. How much versus 10 the -- how much was that a factor versus the opening 11 12 size? I would have thought that would be in the I=m just intuiting that the pressurizer 13 temperature isn=t going to be a lot different. 14 15 MR. PHAN: Actually, the applicant used 16 a natural circulating heat transfer correlation. 17 plugged the numbers to point out that when 18 pressure is high, then it increases heat transfer by 19 a factor of three or -- I don=t remember the exact 20 I found that that was reasonable explanation number. 21 for significant change in release, although the area 22 is not --23 MEMBER MARCH-LEUBA: You=re talking 24 about the pressure in the containment air?

1	MR. PHAN: Yes. We have one case
2	MEMBER MARCH-LEUBA: You said one
3	MR. PHAN: of this containment air
4	pressure. In one case, it=s leakage .1 cubic foot.
5	It does not drop the pressure in the containment. In
6	the other case, in one case it=s 1.1 square foot area.
7	The other case it s one square foot area. You drop
8	the containment pressure significantly. When the
9	pressure is low, density of air is low.
10	MEMBER KIRCHNER: I understand all that,
11	but the thermal imertia of the pressurizer and the -
12	- and what=s going through it is going to dominate
13	the temperature, not the external cooling of it. I
14	suspect it was more the area than this phenomenon,
15	but I
16	MR. PHAN: Actually, area only could not
17	explain this. Area change is 10 times. That release
18	is 357 times. So that=s why we got the applicant to
19	explain it. Applicant provided
20	MEMBER KIRCHNER: They=re blowing down
21	the containment with a bigger area. As you said, it
22	depressurizes the containment. That=s going to take
23	a lot more out with it.
24	MR. PHAN: That=s right. That case

	[] 278
1	viewed the higher release. Because the
2	depressurization dropped the pressure, then it does
3	not provide sufficient cooling for the pressurizer,
4	then revaporizes happen in the pressurizer, in that
5	case only at high release dose.
6	MEMBER KIRCHNER: Thank you, Mr.
7	Chairman.
8	CHAIRMAN BALLINGER: Where are we?
9	MR. PHAN: We are on the other external
10	events, Slide 32. For the other external events, the
11	staff reviews ensured that the applicant=s assessment
12	is comprehensive in scope, the approach used for
13	evaluating and screening out the external events
14	conforms to the guidance, the screening criteria and
15	the justifications used to support the screening out
16	of these external events are rational, and the
17	external events treatments are reasonable.
18	The applicant assessed the external
19	events following the guidance in Part 6 of ASME/ANS
20	PRA standard, specifically in Appendix 6-A, which
21	identifies the external events that require
22	considerations and supporting requirement EXT-B1,
23	which is the initial preliminary screening for
24	screening out an external event. And to the staff

1	this is acceptable.
2	Next, please.
3	The staff review finds that the applicant
4	did not follow the SRMs on the SECY-93-087 to perform
5	quantitative or bounding analysis for the external
6	events, such as high winds, hurricanes, tsunami, and
7	so on.
8	In addition, the DCD Revision 0 does not
9	discuss how the main control room would cope with the
10	external fires. Furthermore, the COL information
11	item 19.1(8) is not complete, missing events,
12	tsunami, and others.
13	Therefore, at this point, the staff
14	concludes that the external event assessment, that
15	appears in the DCD Revision 0 is incomplete.
16	In addressing the staff findings, the
17	applicant agrees to revise the DCD to include the
18	quantitative or bounding analysis and address the
19	main control room = s issues. In addition, applicant
20	will revise the revise the COLs information items
21	19.1(8) to include those missing events.
22	Up to this point, we have presented you
23	the PRA during at-power. The next topic is on the
2.4	PRA during low power at shutdown.

1	MS. POHIDA: Good afternoon. My name is
2	Marie Pohida, and first I=ll be discussing the
3	approach that I took for evaluating the low power and
4	shutdown PRA for internal events.
5	Consistent with the SRP and the draft low
6	power and shutdown standard, I reviewed the plant
7	operating state definitions for completeness. All
8	POSs were defined, including reduced inventory
9	operations, water solid conditions, and cavity
10	flooded conditions.
11	For each POS, the time to boiling and the
12	time to core uncovery was determined, along with the
13	status of all open RCS penetrations, RCS level, and
14	decay heat. I reviewed the event trees for each POS.
15	They were not included in Revision 0 of the DCD, but
16	they will be added to the DCD Revision 1. Okay?
17	I also reviewed the implementation of
18	Generic 88-17 regarding RCS level and temperature
19	instrumentation, the availability of pumped
20	injection, the installation of steam generator nozzle
21	dams, the potential for vortexing of the shutdown
22	cooling pumps, and containment closure during reduced
23	inventory conditions.
24	I also reviewed the risk insights to

	281
1	identify what SSEs should be considered for potential
2	tech specs, LCOs under Criterion 4 of 50.36. An
3	example of that would be containment closure during
4	reduced inventory conditions.
5	We did perform a confirmatory calculation
6	of the applicants low power and shutdown MAAP
7	analyses for source terms, and Jason will be
8	addressing that topic later this afternoon.
9	And also made sure that significant
10	operational assumptions were included as risk
11	insights or tech specs, as applicable. And an
12	example of that would be the order of nozzle dam
13	installation, you know, such as the hot leg nozzle
14	dams, they=re always installed last, and the steam
15	generator or hot leg nozzle dams are always removed
16	first.
17	MEMBER STETKAR: Before you flip to the
18	next slide, I=ll ask this one here now. I noticed
19	when I read the SER that there was some discussion
20	about interfacing system LOCAs during low power and
21	shutdown, and that apparently the applicant will
22	provide a DCD update to state that once a primary
23	event is established there is a negligible IS LOCA
24	vulnerability.

1	It sounds to me like that whole
2	discussion focused only on the classic narrow focus
3	of overpressurizing a low pressure piping system.
4	When shutdown cooling is operating, they have a low
5	pressure letdown flow path open.
6	That indeed does not go through the flow
7	path that is discussed, at least what I could read in
8	the SER, and yet if that flow path is open, and
9	charging is not available to put water back in, that
10	to me is an interfacing system LOCA. More water is
11	going out of the reactor coolant system than is going
12	in, and where it=s going to is outside of the
13	containment.
14	So I was curious, since you=re happy with
15	the fact that they don=t have any IS LOCAs, how do
16	you disposition that? In fact, it=s called
17	initiating event L, but that=s strictly pipe breaks.
18	I=m talking about other things that can happen that
19	keeps water draining out and not going in.
20	MS. POHIDA: Okay. I=m going to this
21	is going to be a reach of my memory here. I may have
22	to go and take that question back.
23	MEMBER STETKAR: Okay. That=s
24	MS. POHIDA: JL breaks I believe were

1	evaluated in the Level 2 portion of the SER, but to
2	the details I=m going to have to go back and check on
3	that.
4	MEMBER STETKAR: JL but my point is,
5	JL is a break, and I don=t care about pipe breaks.
6	MS. POHIDA: I understand.
7	MEMBER STETKAR: I care about flow paths
8	that deliver water outside of the containment, and no
9	water going back in. That to me is an interfacing
10	system LOCA. I don=t have to have a pipe rupture.
11	MS. POHIDA: Operator-induced flow
12	diversions
13	MEMBER STETKAR: No, no, no. I didn=t
14	say operator-induced; did I?
15	MS. POHIDA: Okay. Not
16	MEMBER STETKAR: This is a normal flow
17	path that is open, such that if the water is going
18	out and no water is going back in, the water goes out
19	and goes away and doesn=t go back in.
20	MS. POHIDA: Yes.
21	MEMBER STETKAR: Now, that can happen for
22	a variety of different causes that are not related to
23	overpressurizing a system or operators or anything.
24	Operators could be part of it. It=s hard to

1	overpressurize it when there=s no pressure, but
2	MS. POHIDA: Okay.
3	MEMBER STETKAR: And all of everything
4	that I read in terms of rationalizing why that type
5	of phenomenon was not important dealt with things
6	like, well, we have orifices, and those are high
7	pressure orifices as well. This line connects
8	downstream of those high pressure orifices. In fact,
9	those high pressure orifices are isolated when you=re
10	shut down because you can=t get any flow through them
11	at low pressure.
12	So just take I just wanted to make
13	that comment to see if you had thought about it.
14	That=s all I have on this one. You can go to the
15	next slide.
16	MS. POHIDA: Thank you. I=d like to take
17	that question back and evaluate that.
18	May I go on to the second slide, please?
19	MR. ANDERSON: Excuse me, Marie?
20	MS. POHIDA: Yes, sure.
21	MR. ANDERSON: If I could hi, Ross
22	Anderson with Enercon. We deliberately included
23	diversion events in our review and development of
24	initiating events. We took a look at industry

1	history of diversion events of any sort, not
2	necessarily to another system, but water being taken
3	out of the primary, put elsewhere, and, therefore,
4	you have what could be called a LOCA, called a
5	diversion event, because we don=t see much in the way
6	of pipe breaks with the system depressurized and
7	cooled down.
8	But there were a number of events,
9	typically not always high volume, where a lot of water
10	was removed from the primary system, and that was the
11	basis for our what was our small LOCA term ESL,
12	Sierra Lima initiator.
13	So we did include that, and we judged at
14	the time, because we reviewed the issue of intersystem
15	LOCA, we thought we were covered by the diversion
16	since
17	MEMBER STETKAR: But on the other hand,
18	Sierra Lima events are inside the containment.
19	MR. ANDERSON: We didn=t limit the
20	definition that way. We called them a diversion of
21	any sort to anywhere. So could be in, could be out.
22	In terms of the Level 2 implication, I
23	can=t address that for you. But in terms of the
24	Level 1 impact, it=s covered.

	1
1	MEMBER STETKAR: You think you=re covered
2	on Level 1 in terms of the scope of
3	MR. ANDERSON: Yes.
4	MEMBER STETKAR: that particular
5	initiating event.
6	MR. ANDERSON: Yes.
7	MEMBER STETKAR: Okay. I=11 have to
8	think about that. Level 2 is you=re right, Level
9	2 can be a different issue because that=s
10	MR. ANDERSON: It=s a different table.
11	MEMBER STETKAR: that is a release
12	pathway, but okay. Let me think about that one.
13	Thank you.
14	MS. POHIDA: Shall I continue?
15	MEMBER STETKAR: Yes.
16	MS. POHIDA: Thank you. Okay. Based on
17	staff questions, the applicant added or augmented the
18	following tech specs and DCD descriptions. One is
19	regarding containment closure when the RCS is open
20	via the pressurizer manway until the refueling cavity
21	is flooded, 23 feet above the reactor vessel flange.
22	Two trains of safety injection are
23	operable in hot shutdown, cold shutdown, and
24	refueling, when the refueling cavity is less than 23

1	feet above the reactor vessel flange. Midloop
2	operation was defined as taking place greater than 96
3	hours post-shutdown.
4	The availability of the PARs and igniters
5	during shutdown was documented as a risk insight in
6	Chapter 19. And procedures to ensure that a steam
7	generator or hot leg manway is open to prevent a rapid
8	loss of inventory when any cold leg penetrations exist
9	was included as a risk insight.
10	So I found the applicant=s approach to be
11	consistent with our guidance, subject to closure of
12	the open and confirmatory items.
13	MEMBER STETKAR: One that I=m honestly
14	really I=m not trying to I=m really puzzled
15	about this one. In the low power shutdown model
16	now talking Level 2, low power shutdown, get you
17	oriented. The models right now say, AWell, in plant
18	operating state 33 and 4A, the equipment hatch may be
19	open.@
20	MS. POHIDA: That is correct.
21	MEMBER STETKAR: And that to isolate the
22	containment, personnel need to reclose the equipment
23	hatch and at least secure it with a minimum of four
24	bolts.

1	MS. POHIDA: Yes.
2	MEMBER STETKAR: Okay. I got that. One
3	question is, in the DCD, it says something to the
4	effect, and I can=t find the quote right at the
5	moment, but if a station blackout occurs, no AC power
6	whatsoever, that activity is failed. In other words,
7	it=s assumed they can=t reseal can=t move the
8	equipment hatch in place.
9	It strikes me that I don=t know the plant
10	design, but most plants I have looked at have one
11	power supply for a crane that can move the equipment
12	hatch not for independent safety-related power
13	supplies. So it s not clear to me why that = s only
14	impossible if I have a station blackout, why it=s not
15	impossible when I have failure of power at some bus.
16	So I don=t know if you=ve looked at that,
17	which might be a lot more likely than station
18	blackout.
19	MS. POHIDA: Okay. Could you please
20	restate the question?
21	MEMBER STETKAR: Okay. The statement in
22	the DCD and I can=t find the quote right now; I
23	can find it later is that that activity is
24	failed

1	MS. POHIDA: Yes.
2	MEMBER STETKAR: if you have a station
3	blackout
4	MS. POHIDA: Yes.
5	MEMBER STETKAR: meaning no AC power
6	anywhere. In my experience, it might be different
7	for this plant design. In my experience, you do not
8	have four independent safety-related power supplies
9	to a crane that can move the equipment hatch. You
LO	typically have one power supply, and it often is not
L1	safety-related.
L2	So my question is: does the model
L3	actually account for the real power supply to that
L 4	crane, and where is it powered from? Because I would
L 5	bet I could be wrong that it is not does not
L 6	have redundant power supplies from all four safety
L 7	buses.
L 8	MS. POHIDA: Okay. In POS 3B, that is -
L 9	- let=s see, that is hot shutdown.
20	MEMBER STETKAR: I=m not I don=t care
21	about POS here.
22	MS. POHIDA: Okay.
23	MEMBER STETKAR: I care about the power
24	what let me phrase this very explicitly. What

	290
1	is the power supply to the crane that can move the
2	equipment hatch? Is that clear enough?
3	MS. POHIDA: Mm-hmm. I
4	MEMBER STETKAR: If I know the answer to
5	that question, I will then know how vulnerable you
6	are to not being able to move the equipment hatch.
7	MS. POHIDA: Okay.
8	MEMBER STETKAR: So what is the power
9	supply to that crane?
10	MS. POHIDA: I will have to go back and
11	check on that.
12	MEMBER STETKAR: More importantly,
13	though, is there is a discussion in the DCD and I
14	didn=t stumble across this until I found it in the
15	SER, which is good in the SER it says according to
16	tech spec I=ll get you the right number 3.6.7,
17	POS 4B, 6, 10, and 12A may have the equipment hatch
18	open. So that got my attention because it=s assumed
19	that it=s closed in those plant operating states in
20	the model.
21	So I went and looked up the tech specs,
22	and indeed the tech specs say that containment
23	integrity is required during modes 1, 2, 3, and 4.
24	Section 3.6.7 indicates that the hatch must be closed

	291
1	and secured with at least four bolts. One door in
2	each personnel airlock must be closed, and the
3	containment isolation valves must be closed or
4	operable, during reduced inventory configurations in
5	mode 5 or 6, which is consistent with what you have.
6	Section 3.9.3 further requires those same
7	containment integrity conditions whenever fuel is
8	being moved in mode 6. However, other than that, the
9	tech specs are silent regarding the need to have the
10	containment hatch closed at any other condition
11	during mode 5 or mode 6.
12	The SER says, well, the question is
13	considered closed, but issues remain unresolved and
14	related to RAI 8546, question 16-149. So I dutifully
15	went to look at that, and it seems that question
16	pertains only to tech spec requirements during those
17	reduced inventory configurations.
18	So my real question is: according to the
19	law, can the equipment hatch be open in POS 4B, 6, 7,
20	8, 9, 10, and 12A?
21	MS. POHIDA: Thank you for bringing up
22	this question because we spent a lot of time on this
23	during the review. When I initially reviewed
24	Revision 0 of the DCD, there was an inconsistency

1	between the Level 2 portion of the PRA that said we
2	defined we built one containment event tree to
3	describe shutdown operations when the pressurizer
4	manway is open and when the refueling when the
5	reactor vessel head is off.
6	And so in the Level 2 section, Level 2
7	portion of the PRA I=m going to speak very slowly
8	so I make sure I get this right from POSs 4A and
9	to, you know, POS 12, one containment event tree was
10	used, and it was predicated back that the containment
11	hatch and all penetrations were closed.
12	I went back and looked at Chapter 16 of
13	the tech specs tech spec, you know, 3.6.7, and it
14	says reduced inventory operations. Reduced inventory
15	operations is defined in Generic Letter 88-17 as three
16	feet below the reactor vessel flange. Okay? That
17	leaves a gap. Okay? Because 4B covers those POSs
18	for that one containment event tree that was built,
19	cover operations during vessel head removal and
20	reinstallation.
21	So if you read the letter of the law,
22	there is you know, there was a technical
23	inconsistency between tech specs and the Level 2
24	portion of the DCD for shutdown. So we asked a bunch

1	of RAIs, and tech specs were modified, and they were
2	modified they were modified, and this is still
3	confirmatory. I believe it=s still an open item, to
4	change the applicability for tech spec 3.6.7 so it
5	includes hatch closure during reactor vessel head
6	removal operations and installation operations.
7	So that=s and that is identified and
8	being resolved through RAI 16-149, the change in
9	applicability for tech spec 3.6.7. Does that help?
10	MEMBER STETKAR: Yes, I am confused. I
11	
12	MS. POHIDA: Yes. How can I help?
13	MEMBER STETKAR: I have a simple
14	question.
15	MEMBER CORRADINI: Some of the members
16	enjoy confusion om his part. Let=s just let him sit
17	there for a minute.
18	(Laughter.)
19	MEMBER STETKAR: Can the equipment hatch
20	be open in what the PRA calls POS 4B, POS 6, POS 7,
21	POS 8, POS 9, POS 12A, POS 12B, and maybe a little
22	bit of 13? That is a simple question. Do the tech
23	specs allow the equipment hatch to be open under any
24	of those conditions?

1	MS. POHIDA: Okay. Based on DCD
Τ	MS. POHIDA: Okay. Based on DCD
2	Revision 0 or the changes that we=re expecting in
3	Revision 1 of the DCD?
4	MEMBER STETKAR: I don=t know, because
5	the follow up question is, if I=ve got to have the
6	containment hatch closed during the whole outage, I
7	don=t want to work in that plant. I=m trying to find
8	out the how the tech specs and what somebody may
9	or may not be committing to for closing and sealing
10	the containment hatch line up to the condition of the
11	containment hatch that is assumed in the PRA model.
12	And right now, from what I can read, those do not
13	align.
14	And what Marie has said is the staff has
15	identified that inconsistency, but I don=t know how
16	the tech specs are being revised. And if they=re
17	only being revised to when they=re removing or
18	installing the head, that still does not satisfy all
19	of the other plant operating states that I identified
20	that the model now assumes that the hatch is sealed.
21	MEMBER BLEY: Okay. So the question
22	arose because in the PRA model you see assumptions
23	about requiring the hatch be sealed.
24	MEMBER STETKAR: Yes. The PRA model

1	strictly says only in something called 3B and 4A the
2	hatch can be open and
3	MEMBER BLEY: Yes.
4	MEMBER STETKAR: that=s the only
5	MEMBER BLEY: That=s the assumption in
6	the PRA, but my question is sort of the other way
7	around. The PRA doesn=t govern operation of the
8	plant, although if we=re using the PRA it ought to
9	match operation of the plant. But I don=t recall
10	that that anything like that that was in any tech
11	specs I=ve seen.
12	MEMBER STETKAR: Well, they have actually
13	instituted a tech spec on this plant, which I think
14	it=s kind of a risk-informed tech spec that says at
15	midloop operation they want the containment equipment
16	hatch closed with four bolts in place. It=s not
17	fully bolted
18	MEMBER BLEY: Okay.
19	MEMBER STETKAR: because they feel
20	they are more risk-sensitive during those
21	MEMBER BLEY: And I=ve seen other people
22	implement something similar
23	MEMBER STETKAR: Right.
24	MEMBER BLEY: although I didn=t think

	<u> </u>
1	it was in the tech specs, but this plant
2	MEMBER STETKAR: This is actually in the
3	tech specs.
4	MEMBER BLEY: Okay.
5	MEMBER STETKAR: It=s tech spec 3.6.7.
6	They have the
7	MEMBER BLEY: It=s not a bad idea.
8	MEMBER STETKAR: No. And they have the
9	standard one that says whenever you=re moving fuel,
10	which is actually what they call POS 7 and POS 9 here,
11	it also has to be in place with four
12	MEMBER BLEY: Need to close quickly.
13	MEMBER STETKAR: No. It=s got to be in
14	place with four bolts.
15	MEMBER BLEY: Okay.
16	MEMBER STETKAR: And that=s also pretty
17	standard. What I m interested in is the other ones.
18	The reason I=m interested in the other ones is that
19	the human error the inability to reclose that
20	equipment hatch is a big contributor to large releases
21	during those two relatively short plant operating
22	states when it=s open.
23	So if it actually is can be open
24	during

1	MEMBER BLEY: More.
2	MEMBER STETKAR: more, then the PRA
3	model is wrong. On the other hand, if they=re going
4	to write tech specs saying that it=s got to be closed
5	the whole time, I probably don=t really want to have
6	an outage in that plant.
7	MEMBER BLEY: And I guess the related
8	piece and I haven=t seen a tech spec on this either
9	is in times when it=s allowed to be open in other
10	plants I don=t know what they=ve got here it is
11	often open in such a way that you aren=t going to
12	close it for hours because there=s cables and tubing
13	and all kind of stuff running through.
14	MEMBER STETKAR: Here they well, you
15	can get into the timing and stuff like that. That
16	was the first question I had about they say, well,
17	you can=t close it. If you have a complete loss of
18	all AC power, you can=t close it. My allegation is
19	that if you don=t have AC power at some bus, you can=t
20	close it.
21	They claim that it=s supposed to be clear
22	enough that you can get it closed within whatever
23	time window they have to close it, and they have some
24	criteria in the PRA that says, you know, what triggers

1	that motion.
2	So I don=t know if we=ve discussed it
3	enough. I just want to understand what if the
4	tech specs are being changed, that=s fine. I mean,
5	we=ll pick it up in Rev, you know, whatever the heck
6	it is, one of the PRA and whatever.
7	MS. POHIDA: But this point is very
8	important because
9	MEMBER STETKAR: Yes.
10	MS. POHIDA: you know, times to
11	boiling are exceptionally quick. You know, the time
12	to boiling, whether you=re at we do at midloop or
13	with reduced invertory operation, which is defined as
14	three feet below at flange
15	MEMBER STETKAR: Early on.
16	MS. POHIDA: or at the flange. It=s
17	only minutes. So the goal of this RAI was to ensure
18	that what was modeled in the Level 2 portion of the
19	PRA was consistent with tech specs. And so 16-149 is
20	supposed to tweak tech specs, so that the tech specs
21	are consistent with Level 2 of the shutdown PRA.
22	MEMBER BLEY: But John is also bringing
23	up, should the applicant overtweak the tech specs,
2.4	they can=t operate this plant.

1	MEMBER STETKAR: It=s going to make life
2	difficult to actually move stuff inside and out of
3	the containment when you
4	MEMBER BLEY: Like you need to do during
5	the outage.
6	MEMBER STETKAR: Somebody is shaking
7	their head, so let=s get feedback from them.
8	MR. ANDERSON: Hi. Ross Anderson with
9	Enercon again. Just wanted to weigh in. Per tech
10	spec, hatch is closed modes 1 through 4.
11	MEMBER STETKAR: Yes.
12	MR. ANDERSON: Below 4, reduce inventory
13	or hatch is closed. Otherwise, it can be open,
14	and I believe that =s a standard tech spec convention,
15	so there shouldn=t be any surprises there.
16	MEMBER STETKAR: That=s right.
17	MR. ANDERSON: Again, I haven=t gone
18	through to verify that that has been integrated into
19	the Level 2 analyses, but nothing unusual about tech
20	specs and the analyses should be consistent.
21	MEMBER STETKAR: Good. From what I just
22	heard, then, unless something is going to change, the
23	hatch can be legally open in POS 4B, 6, 8, 10, 12A,
24	12B, and maybe part of 13, because 13 is kind of

	300
1	you=re coming out of mode 5 and 13. It=s a
2	transition-type POS. So I can give up on mode 13
3	or POS 13.
4	But if it can legally be fully open in
5	4B, 6, 8, 10, 12A, and 12B, that condition is not
6	modeled in the current PRA. It=s assumed that it=s
7	closed in the current PRA.
8	MR. ANDERSON: I want to be careful with
9	what I say because I haven=t inspected these parts of
10	the model. But the way they were defined is that it
11	was consistent with tech specs or it should be.
12	MEMBER STETKAR: The POSs that I read,
13	4B, 6, 8, 10, 12A, 12B, use the standard containment
14	event tree from the full power PRA, which assumes
15	that the containment hatch is closed because it=s
16	closed during full power.
17	MR. ANDERSON: And you folks may want to
18	revisit that.
19	MEMBER STETKAR: You may want to revisit
20	that. A big deal is made out of that narrow window
21	of 3B and 4A. Special analyses are done. A special
22	analysis says I=m exposed to having the equipment
23	hatch open, and I need to close it if only in those
2.4	two plant operating states.

	301
1	The amalysis for 5 and 11 says that it=s
2	closed with four bolts, and because of that there is
3	a higher conditional probability for overpressure
4	failure of the containment because it=s not sealed as
5	tightly.
6	It, similarly, is closed in 7 and 9, which
7	are the two when you=re actually moving fuel
8	MS. POHIDA: For alteration tech specs.
9	MEMBER STETKAR: Right. And those plant
10	operating states are basically ignored in the low
11	power and shutdown PRA because the refueling pool is
12	full of water. So they=re not even addressed in the
13	low power and shutdown PRA, and that=s why I=m
14	concerned about 4B, 6, 8, 10, 12A, and 12B. And I
15	think I=m not going to say it again.
16	MEMBER SUNSERI: Yes. I=ll just add one
17	thing from my plant operating experience. And maybe
18	the staff found this or you=ll learn this from KHNP,
19	but the last few outages I=ve been in in the last
20	couple of plants I was at, the utility had to
21	demonstrate that they could close that hatch within
22	30 minutes or meet the time to blow requirements,
23	including having a temporary generator stage, if
24	necessary, for the electric hoist. And we ran drills

1	every outage multiple times to demonstrate compliance
2	with that requirement.
3	MEMBER STETKAR: And, indeed, in POS
4	just to follow up on this, in POS 3B and 4A, the
5	models explicitly evaluate whether people can get it
6	closed within whatever time window. And, indeed, you
7	know, like everything in PRA, it=s not guaranteed
8	failed, and it=s mot guaranteed success.
9	The failure probability that=s in there
10	is a relatively large contribution to large releases
11	in those particular plant operating states. In fact,
12	it=s the largest contribution to large releases in
13	those, too.
14	If the hatch was closed with the same
15	conditional I=m sorry, if the hatch was open with
16	the same conditional probability for getting it
17	closed in all of the other plant operating states
18	that I mentioned, the overall large release frequency
19	during low power and shutdown would be much higher
20	than it currently is.
21	MEMBER SUNSERI: Yes. John, I wasn=t
22	challenging. I was just giving some direction or
23	some advice to the staff of where they could look.
24	MEMBER STETKAR: okay.

1 POHIDA: So the intent is that it=s 2 -- this discrepancy between the tech specs and the 3 PRA resolved through will be changing the tech spec 3.6.7, 4 applicability of vou 5 containment closure. So that single containment 6 event tree that emcompasses plant operation state 4B all the way to 12 is reasonable. 7 MEMBER STETKAR: Well, that=s one way to 8 9 do it. That=s making my life as a plant operator more miserable because you want the plant to emulate 10 11 The other way is to make my life what I=d 12 like it to be and make the PRA emulate what the plant You have either of those options. Usually, we 13 want people to operate the plants the way that they 14 15 can manage an outage and get things done, and make the PRA consistent with that, meaning the models, the 16 17 Level 2 models for those plant operating states would need to change, rather than changing the tech specs. 18 19 Anyway, I think the issue is clear. 20 just a matter of what KHNP -- my concern is that this 21 has been punted off into a Chapter 16 issue, and I 22 want to make sure that however it gets resolved that 23 it circles back to the PRA because it has now been 24 punted out of the PRA into Chapter 16, which is tech

1	specs, with apparently the presumption that the tech
2	specs will be changed such that that Level 2 model
3	that=s in there now is valid.
4	MS. POHIDA: Yes.
5	MEMBER STETKAR: Yes. So we=11 let KHNF
6	struggle with that one.
7	MS. POHIDA: Okay.
8	CHAIRMAN BALLINGER: Can we continue?
9	MS. POHIDA: I=m completed with my
LO	presentation. Are there any more questions or
L1	well, thank you very much for your time.
L2	MEMBER SKILLMAN: Yes, I do have a
L3	question, please.
L 4	MS. POHIDA: Oh, I=m sorry.
L5	MEMBER SKILLMAN: I=m on page 19-78 of
L 6	the safety evaluation. And the text here is as
L7	follows, AThe staff also recognized that installed
L8	reactor internals did shorten the time to core boiling
L 9	given possible limited communication between the RCS
20	inventory around the core and inventory in the
21	refueling cavity.
22	And the RAI is requesting action, and one
23	of the items is an evaluation documenting the time to
2.4	core damage given an extended loss of the decay heat

1	removal function with and without installed reactor
2	internals.
3	MS. POHIDA: Yes.
4	MEMBER SKILLMAN: And my question is:
5	the reactor internals that that action item is
6	referring to is the plenum or that piece that fits
7	above the core in this design? Is that what that is?
8	MS. POHIDA: Okay. Now
9	MEMBER SKILLMAN: This is part of the low
10	power shutdown.
11	MS. POHIDA: Oh, I understand.
12	MEMBER SKILLMAN: It=s in POS 7 and POS
13	9.
14	MS. POHIDA: Yes. And this the reason
15	why this question was asked is that all plant
16	operational states were evaluated in the PRA before
17	POSs 7 and 9 were quantitatively screened. We asked
18	the applicant for some, you know, thermal hydraulic
19	analysis to identify the time to, you know, core
20	damage when reactor vessel level is 23 feet above the
21	reactor vessel flange.
22	As you said, two sensitivity studies were
23	performed, one with installed reactor internals and
24	one without, to look at the differences of the time

1	to core damage. And I=m trying to think if my
2	mind is drawing a blank here to everything that
3	constitutes the reactor internal package.
4	But I do know that they are installed;
5	before they are removed that they can limit the
6	communication between water in the reactor vessel
7	cavity and what=s in the core.
8	If you want a list of the specific
9	components, I would have to go and take that back.
10	MEMBER SKILLMAN: No. I think what this
11	is referring to is what is known as the plenum or the
12	I don=t know what the device is called in the
13	APR1400. But it is the device that really rests
14	above the core. You remove the head and you remove
15	that piece, and if it=s that piece then I understand
16	it=s the chimney of the heat coming up from the fuel
17	up to the refueling canal. I understand that.
18	I was just my first reaction was I
19	don=t think you can have a core without internals
20	because the internals hold the core. But I think
21	this is just a nomenclature issue about this device
22	that rests on top of the fuel.
23	MS. POHIDA: May I take that back?
24	MEMBER SKILLMAN: Please.

	307
1	MS. POHIDA: Thank you.
2	MEMBER SKILLMAN: Yes. I was just trying
3	to get clarification. Again, it=s on page 19-78 of
4	the safety evaluation.
5	MS. POHIDA: Okay. Thank you.
6	MEMBER SKILLMAN: Thank you. Okay.
7	MS. POHIDA: Are there any additional
8	questions? Thank you for your time.
9	MR. NAKANISHI: Good afternoon. This is
10	Tony Nakanishi again, and I just want to quickly cover
11	the staff review of internal fire and floor during
12	low power and shutdown.
13	So I did want to mention that there
14	currently is no staff-endorsed guidance for
15	performing low power shutdown internal fire or flood.
16	But basically the at-power approach can be applied
17	for shutdown conditions, and that=s exactly what the
18	applicant did. And NUREG/CR-7114 provides a little
19	more guidance in terms of how one might take the 68.50
20	approach and apply it to low power shutdown.
21	We went through the underlying
22	documentation within you know, during our audit,
23	and basically the staff confirmed the approach that
24	was taken, and we find it that it=s a reasonable

1	approach.
2	One thing that=s important for low power
3	shutdown fire and flood is the integrity of the
4	barrier, and that we wanted to
5	make sure there are adequate provisions to make sure
6	there are controls.
7	For example, you know, having so the
8	COL items actually cover ensuring appropriate, you
9	know, fire barrier management procedures,
10	configuration control procedures that will ensure
11	that, you know, risk-significant doors and such are
12	monitored with a fire watch or a watch.
13	So, overall, we think that the applicant
14	approach the shutdown fire and flood in a
15	reasonable manner
16	So that=s all I had, if there=s any
17	questions.
18	MR. PHAN: The last topic in this PRA
19	presentation is on the use and application of the
20	PRA. As listed on this slide, the APR1400 PRA was
21	used as an input for many DCD chapters, including
22	Chapter 19.6, physical security; Chapter 14.3, ITAAC;
23	Chapter 16, technical specifications; Chapter 17.4,
24	reliability accuracy programs; Chapter 18, human

1	factor engineering; Chapter 19.2, severe accident
2	evaluations; and also in the environmental report,
3	SAMDA.
4	Note that there are no risk-informed
5	initiatives included in this application. In
6	conformance with the policy statements on the use of
7	the PRA, the applicant did use the PRAs to improve
8	the design, such as the numbers the numbers of the
9	diesel generators and the battery=s depletion time to
10	optimize the plant safety.
11	The staff reviews ensure that the APR1400
12	PRA is commensurate with the issues and the
13	applications, the inputs used for the programs is
14	sufficient, and the information in Chapter 19 and
15	other chapters are consistent.
16	The staff expected that during phase 4
17	the applicant will revisit these chapters and update
18	the PRA input with the PRA final models and final
19	resource.
20	Next slide?
21	In conclusion, due to the phase 2
22	findings, the staff is currently unable to accept and
23	make final conclusions on the APR1400 PRA in of
24	appropriate scope, level of detail, and technical

-	
1	adequacies. And also the APR1400 PRA reasonably
2	reflects the as-designed, as-to-be-built, and as-to-
3	be-operated plant.
4	This is the end of our presentation on
5	APR1400 PRA. At this point, I would ask, do you want
6	us to continue with 19.2, severe accident evaluation,
7	or we should stop here for additional questions on
8	the PRA?
9	CHAIRMAN BALLINGER: I have another
10	question. Do we think we need a short break? Okay.
11	I think we=ll take a 10-minute break, come back at
12	five of. We=ll be in recess.
13	(Whereupon, the above-entitled matter went off
14	the record at 4:46 p.m. and resumed at 4:55 p.m.)
15	CHAIRMAN BALLINGER: Okay. We=re back in
16	session. I don=t know which one is going to be which,
17	but whichever one it is, please start.
18	MR. WAGAGE: My name is Hanry Wagage.
19	I=ll be presenting leading off Section 19.9 on
20	severe accident evaluation. We have several
21	reviewers presenting this, but first I will go ahead.
22	I will be presenting severe accident prevention.
23	And using the recommendation of SECY-90-
24	016 and SECY-93-087, applicant addressed severe
<u>_</u> 1	ord and blor sollow, appricant addressed severe

1	accident prevention issues, anticipated transient
2	without scram, midloop operation, station blackout,
3	fire protection, and interfacing steam loss of
4	coolant accident.
5	I have some highlighting issues
6	specifically on station blackout. This morning,
7	also, applicant discussed how the applicant addressed
8	station blackout by having diverse power systems, or,
9	in addition to that, increasing two emergency diesel
10	generators to four. They added more diverse systems
11	to address the station blackout.
12	MEMBER STETKAR: Hanry, why is the
13	staff and don t give me SECY numbers because I
14	know the SECY numbers, but why technically is the
15	staff concerned with these, and only these, severe
16	accident prevention issues for any new plant that we
17	may review?
18	MR. WAGAGE: Prevention
19	MEMBER STETKAR: Let me ask you, why are
20	we not questioning steam generator tube rupture?
21	MR. WAGAGE: That comes on this
22	interfacing system loss of coolant.
23	MEMBER STETKAR: Okay. We=ll talk about
24	that later then. My question is that these were

	312
1	derived from a limited number of PRAs that were
2	performed in the late 1980s and early 1990s for
3	currently operating plants at that time, and said,
4	AGee, these things look like they would be important
5	to risk. You=d better pay attention to them.@
6	What relevance does that necessarily have
7	for any new plant that might come into us? In other
8	words
9	MR. WAGAGE: To address these, some of
10	the new plans address some other issues. For
11	example, some of the plants address ex-vessel steam
12	explosion issues. This one, the plant design is that
13	the issues are addressed differently. The steam
14	explosion applicant is doing analyses, ensuring that
15	they can prevent by containment threat by design
16	in the containment. But these aren=t ones the
17	applicant addressed.
18	MEMBER STETKAR: We can go on. I=m
19	just it was a rhetorical question, that the staff
20	was spending time looking at these and only these
21	because of some SECY that was written 25 years ago.
22	And you may be missing other more important things to
23	severe accidents because you=re focusing only on
24	these.

1	MR. WAGAGE: Other issues that applicant
2	addressed by designing for example, the applicant
3	on the mitigation, we will be talking about other
4	issues.
5	Interfacing system loss of coolant
6	accident, there were two methods recommended
7	having low pressure systems designed to full RCS
8	pressure and providing means of testing pressure
9	isolation valves and indications.
10	Applicant identified the systems
11	interfacing with the RCS, and what I found is that
12	the shutdown cooling system it was not clear how
13	the applicant had it, because in one place applicant
14	said that the shutdown cooling system is designed to
15	have full pressure or leak test capability, and also
16	it mentioned eliminating interfacing lines.
17	And it was not clear which way it is doing
18	with eliminating interfacing or having design for
19	full pressure. Then applicant clarified that
20	eliminating unnecessary interfacing lines.
21	Next, I will be discussing severe
22	accident mitigation progression and features. Severe
23	accident mitigation there is a severe accident
24	analysis report that provides details of how

1 applicant addressed severe accident. Four of the 2 areas I reviewed was MELCOR concrete interactions and 3 core debris coolability, and decontam in heating and 4 high pressure melt ejection. 5 There was a question this morning how the applicant -- how much melt was going to occur to the 6 upper containment. 7 Applicant used the area ratio, area of the annulus and area of the cavity flow area, 8 to determine how much melt would go to the upper 9 10 containment. 11 Τn severe accident analysis 12 applicant identified input parameters but did not give the input values. And I asked -- we are going 13 14 provide the input values, and found 15 reasonable, will update the severe and accident 16 analysis report. 17 In-vessel and ex-vessel steam explosions and containment bypass -- there was a question this 18 19 morning about condrete type used in this containment. 20 There is a sump in these -- the containment floor. 21 The sump is closer -- the bottom of the sump is closer 22 to the liner, and also recall it is a constricted 23 It can accumulate melt to a higher depth. area. 24 Because of that, general melt and core concrete

1	interactions would not work because it=s a
2	significant higher melt depth.
3	And applicant mentioned that report Dr.
4	Pilch, Marty Pilch, analyzed that, and I reviewed
5	I audited that report on ERR. And I found that the
6	sump being having a higher melt depth, it has
7	to the cooling or quenching of melt is not
8	guaranteed for basaltic concrete because other
9	type two types of concrete are limestone and
LO	limestone common sand.
L1	Those two types of concrete, gas
L2	generation from the ablation was significant to break
13	the melt crust on the top, but it could not have
L 4	sufficient justification for breaking the crust for
L 5	basaltic concrete. Because of that, that those
L 6	analyzed type of concrete, I asked the applicant to
L7	identify that the DCD the DCD is going to be
L 8	updated to limit the type of concrete to basalt and
L 9	to limestone and limestone common sand.
20	MEMBER REMPE: I somehow missed that in
21	your SC that you asked them that as an RAI. It=s in
22	there?
23	MR. WAGAGE: This is during audit. Audit
24	we are we asked that, then applicant provided that

1	report.
2	MEMBER REMPE: Okay. So it=s not
3	included in this Chapter 19 anywhere? Because I
4	didn=t see that. I wouldn=t have asked the question
5	if I had seen it earlier. Is it in what we reviewed
6	in your Chapter 19?
7	MR. WAGAGE: I stated that I reviewed
8	sump evaluation, but I did not discuss it further.
9	MEMBER REMPE: Okay. Thank you.
10	MEMBER POWERS: One point the applicant
11	made in his discussion was the amount of ablation of
12	the concrete when melt streams down onto it versus
13	the depth of the liner below the concrete. And he
14	has assumed limestone concrete, limestone aggregate
15	in his concrete.
16	Since the ablation depth is dependent on
17	the heat of the fusion of the concrete, the limestone
18	concrete has a much, much higher heat effusion than
19	does a basaltic concrete. And the differences are on
20	the order of a factor of two, which means that a small
21	ablation in the case of limestone concrete would be
22	much bigger in the case of basaltic concrete. Is
23	that a point of issue here?
24	MR. WAGAGE: I didn=t catch the last part

Τ	or your
2	MEMBER POWERS: Is that a point of issue
3	here? That whereas his analysis on streaming
4	suggested that he would ablate a small fraction of
5	the concrete. I mean, it will be roughly roughly
6	speaking, twice that much. And you would get to the
7	point where the concrete may not be able to sustain
8	the load on it, and he would in fact fracture out
9	whatever remaining concrete is and expose the
10	embedded liner directly. Is that an issue to
11	consider?
12	MR. WAGAGE: I think the issue that is
13	the cavity filled with water when it transfers heat
14	toward it, not calculate much less ablation, and
15	MELCOR calculates higher-than-MAAP ablation rate for
16	water-filled cavity. This is a water-filled cavity
17	because of that, and there have been melt spread in
18	large area, and the thickness of melt layer is small,
19	and that it does not have
20	MEMBER POWERS: No matter how much you
21	spread it, or how much you try to quench it, if you
22	get any concrete ablation you will get more ablation
23	with a siliceous concrete than you will with a
24	calcareous concrete, simply because the heat effusion

1	is so much less in the case of the siliceous concrete.
2	And whereas they ablated like a foot with the
3	limestone concrete, you will ablate like two feet
4	with a siliceous concrete.
5	MR. WAGAGE: I mean, siliceous concrete
6	is not going to be used in this plant.
7	MR. PAIK: This is Chan Paik from Fauske
8	and Associates. The difference between the siliceous
9	concrete and limestone or a limestone common sand has
10	limestone has a lot higher decomposition kind of
11	energy to require
12	But the main issue here with the water is
13	the gas generation, and this gas generation
14	essentially, like an eruption, so this gas is going
15	through the accordion floor and entering the molten
16	core into the outside become a particle, and that
17	particle can be cooled by water.
18	So the main difference between the
19	siliceous concrete and limestone, limestone common
20	sand, would be the water. It=s a decodable gas-
21	induced eruption mechanism for coolability.
22	MEMBER POWERS: If you get any ablation
23	at all thermally, you will get more with siliceous
24	concrete than you will with calcareous concrete,

1	simply because of the heat it takes to I mean,
2	you=ve got to decompose the calcium carbonate, and
3	that is an extremely energy-intensive process.
4	I=m just wondering if that=s an issue.
5	If the application specifies, AThou shalt use
6	calcareous concrete,@ okay, fair enough. If it=s
7	left as is conventional to whatever is locally
8	available, about a third of your sites have a
9	siliceous aggregate commonly used in construction.
10	MR. WAGAGE: Actually, it is limited by
11	because of the sump mainly because sump is has
12	a larger thickness of melt to break the melt from
13	melt solidifying melt, you need to produce some
14	gas. Siliceous concrete was not producing that gas
15	because
16	MEMBER POWERS: I defy you tell in
17	looking at a mel concrete interaction, you cannot
18	tell the difference between calcareous and siliceous
19	concrete based on gas generation because in the
20	siliceous case you are decomposing a larger volume of
21	concrete, and so you get steam; whereas, in the
22	calcareous you also get steam and carbon dioxide.
23	They look about the same.
24	If you sit down and calculate, the molar

1	generation of gas is about twice as much in the case
2	of calcareous concrete per unit of concrete evolved.
3	But you decompose twice as much with a siliceous
4	concrete. So you get about the same amount of gas
5	generation. I mean, it=s not exact, but it=s roughly
6	the same.
7	MR. WAGAGE: In addition to gas
8	generation, it was that the calculation found that
9	if each of the line line of failure, it would kind
10	of guarantee the failure of preventing line of
11	failure. Line is three feet below. Siliceous
12	concrete showed line of failure if sued within certain
13	time.
14	So that=s why that applicant decided to
15	limit types of concrete to limestone and limestone
16	common sand.
17	Next I will be talking about in-vessel
18	steam explosions. A while ago, the NRC had studies
19	and those studies found that threat to the containment
20	by in-vessel steam explosion is minor. However, the
21	applicant performed analysis with TEXAS-V computer
22	code and used ABAQUS code to do structure analysis
23	and found that it is still sticking.
24	Ex-vessel steam explosion is an open item

321 because of several 1 reasons. The applicant used a 2 one-dimensional TEXAS computer code, one-dimensional 3 meaning it can take radius in vertical direction but 4 not in horizontal direction. The radial direction conditions are assumed to be the same. It=s mixed -- well mixed in the radial direction. 6 7 In that case, if one uses much larger radial distance of radial pool of water, then it can 8 9 quench the melt, and there will be less energy of 10 someone uses much smaller area of explosion. Ιf 11 water pool, cross sectional area, then there will be 12 so much steam generation, then melt will not be in the vicinity of water to produce any. 13 14 means between there is optimal That 15 For in-vessel steam explosion, the applicant value. 16 showed that applicant will use the optimal value

during higher energy release. But for ex-vessel, you are revealing that you -- that applicant -- how the applicant is just if ying that.

Other area of review is that opening of how the pressure is attenuated, this computer code calculates the pressure. And after it calculates the pressure in the given calculation area or volume, it has to attenuate the pressure and get the -- calculate

17

18

19

20

21

22

23

24

1 structures to the 2 structures. 3 I found there was an error in the equation 4 By the way, for in-vessel steam explosion, 5 that equation was not used; only for ex-vessel. in-vessel 6 means steam explosion that attenuate 7 pressure, attenuation was not used. Whatever the maximum pressure dalculator was applied to the bottom 8 9 of the vessel, but ex-vessel, you know, is attenuation 10 and there was an error in the of pressure used, 11 equation that I am discussing with the applicant. 12 Staff is reviewing the structural 13 evaluation of cavity structures. We this morning also discussed that 14 in-vessel retention system, 15 ex-vessel external reactor vessel cooling system 16 operation. 17 wasn=t much information There 18 The question came about installation. We 19 found that mentioned in DCD Tier 2, Section 5.3.5. 20 That is on shipment and installation. There is one 21 read. AThe installation for the sentence I can 22 reactor vessel is designed to have an annular flow 23 path suitable fbr the external reactor vessel 24 cooling, RVC, operation during the

Τ	accident.
2	I was not concerned about the external
3	reactor vessel cooling because applicant did not take
4	credit in the PRA, and I assume that system is not
5	working.
6	When the applicant does not take credit,
7	there is no reason for me to ask how good is the
8	system, how whether it=s going to work. For
9	example, I was not concerned about how the
10	installation is going to work because applicant did
11	not assume it=s going to work. That system is going
12	to work.
13	However, for the ex-vessel steam
14	explosion, there was a concern it=s the opposite.
15	Our thinking was that, yes, the applicant did not
16	take credit, but during a severe accident when
17	operator sees this, operator is attempting to use
18	this to flood the cavity to cover part of the reactor
19	vessel, and with the intention of quenching melt
20	inside the vessel so it will not come out.
21	However, there is a possibility that melt
22	will be unfrozen the layer on the top, that that
23	melt layer can keep attacking the vessel and vessel
24	may fail, giving a much larger MELCOR. But that

1	MEMBER CORRADINI: So can I ask a
2	question? This goes back to the AP1000.
3	MR. WAGAGE: Yes.
4	MEMBER CORRADINI: Right? The AP600 in
5	fact. Exactly the same analysis was done for AP600
6	and 1000. But my memory is that the person who did
7	it claimed and I think it was certainly
8	accurate is the MELCOR rate would actually be
9	smaller, not larger.
10	MR. WAGAGE: No, no.
11	MEMBER CORRADINI: So why would it be
12	larger?
13	MR. WAGAGE: No. It=s much larger.
14	It=s I think I I think it=s much larger because
15	assume that it=s going to open like a clamshell and
16	pour a much larger actually, AP600 did analysis
17	for that situation and found the cavity is going to
18	fail but containment would stay intact.
19	MEMBER CORRADINI: So you=re looking at
20	the whole thing on Zippy.
21	MR. WAGAGE: Yes. Not whole thing like
22	opening like a clamshell that
23	MEMBER CORRADINI: Like a
2.4	MR. WAGAGE: for significant amount of

1	melt.
2	MEMBER CORRADINI: Like an upside-down
3	tin can, like an upside-down soup can.
4	MR. WAGAGE: Like Pacman opening, yes.
5	Then AP600 did structural analysis for that and found
6	that cavity is going to fail, but they do not detail
7	the containment. But this APR1400 has not gone that
8	far.
9	MEMBER CORRADINI: But they didn=t do the
10	analysis.
11	MR. WAGAGE: They did not do the
12	analysis. They did not take credit. But we are
13	debating whether to oh, then many odd questions -
14	_
15	MEMBER CORRADINI: So now I was going to
16	ask you the binary question. If it went away, does
17	it matter? And if it was there, does it matter, in
18	terms of the overall containment failure probability?
19	MR. WAGAGE: Okay. Applicant did
20	sensitivity and -
21	MEMBER CORRADINI: Before you make them
22	go through this excruciating analysis, does it
23	matter?
24	MR. WAGAGE: Actually, the one for which

1	applicant did sensitivity analysis for the
2	operating the system and found that it did not matter
3	much to the system. So they did sensitivity
4	analysis. Even if the system works, that does not
5	buy much.
6	MEMBER REMPE: If you claim it=s not
7	there, if you really want to prove that it doesn=t
8	hurt things, do you assume an adiabatic out-of-
9	surface on the vessel? Because your what was the
L 0	heat transfer epefficient they assumed on the
L1	exterior surface of the vessel to the you know,
L2	through the insulation into the cavity area, because
L3	with it there you are hoping that you=re going to
L 4	have nice heat transfer from the ERVC, and they aren=t
L5	taking credit for it.
L 6	So what did they assume for the heat
L7	transfer coefficient off a vessel? Because if it
L8	adversely affected things, if you couldn=t get water
L 9	in between the vessel and this insulation for ERVC,
20	then you would have a very reduced heat transfer and
21	you might actually cause the vessel to fail earlier.
22	So did they assume an adiabatic outer
23	surface if they didn=t take credit for it?
24	MR. WAGAGE: Actually, they did not

	327
1	assume the cavity being filled to cover the vessel.
2	The ex-vessel external reactor vessel cooling was
3	not considered because they did not take credit.
4	They did not show any calculation for that one, though
5	it did not
6	MEMBER REMPE: So, basically, they assume
7	an adiabatic, or do they have natural convection to
8	the wall? I mean, they would have to the thing
9	is, one of the things we worried about with AP600
10	was, you know, if it wasn=t sufficiently robust, and
11	you mentioned in Chapter 5 apparently they=re saying
12	they have a good flow area, so they have considered
13	this, but, you know, if you had some sort of collapse
14	of that flow path that it would limit the flow of
15	water down there, and could you have a heat transfer
16	condition on the outer surface that is
17	MR. WAGAGE: Our situation was that
18	because the applicant did not take credit, there was
19	no reason for us to ask how good the system was. Now,
20	with the opposite
21	MEMBER REMPE: Right.
22	MR. WAGAGE: applicant does take
23	credit. However, the operator may use the system.
24	Then what happens? That=s what I was

1	MEMBER CORRADINI: I=m trying to remember
2	back for AP1000. But if my memory serves me, AP1000
3	there was an estimate by ERI. I=m looking for the
4	gentleman; he has left.
5	MR. AYEGBUSI: Hossein is sitting in the
6	back of the room. He did that work.
7	MEMBER CORRADINI: Hossein did it, but
8	that isn=t the person in charge. But my memory was
9	it=s a fractional amount that was estimated that the
10	IVR wouldn=t work. It was something like about 17 or
11	24 percent. And in that time period you assume you
12	go to film boiling, and you essentially create a hole.
13	I don=t remember the whole hole unzipping. I
14	remember that was the bounding calculation to get
15	them so that it=s not a problem.
16	So are you asking the applicant to do
17	some sort of bounding calculation, or just consider
18	this and it=s up to them to figure out what to do?
19	MR. WAGAGE: Actually, when asked the
20	question, applicant proposed a COL
21	MEMBER CORRADINI: That=s a copout.
22	MR. WAGAGE: information item telling
23	that it has
24	MEMBER CORRADINI: Sorry.

	329
1	MR. WAGAGE: that COL applicant will
2	be addressing ex-vessel steam explosions if SAMDA
3	uses this system.
4	MEMBER CORRADINI: Okay.
5	MEMBER REMPE: And then it will already
6	be a certified design, and we don=t look at the AMGs,
7	and so it=s it=s not evaluated.
8	MEMBER CORRADINI: Well, I=m back to
9	I=m back to I don=t mean to be so brutal, but I=m
10	back to, why do I care? I either care because of
11	accident management guidelines, or I care because it
12	affects the containment failure probability. So if
13	it doesn=t affect the containment failure
14	probability, then I don=t care. Does it affect the
15	accident management guidelines?
16	Those are the only two reasons I would do
17	this analysis. Otherwise, I just wouldn=t do it.
18	It=s interesting. I find it fascinating. But I
19	wouldn=t do it unless it affects one of those two
20	items.
21	MR. WAGAGE: I think if you put
22	probability here, then I think it would be a much
23	more probability because it has to
24	MEMBER CORRADINI: It would be what? I=m

1	sorry.
2	MR. WAGAGE: It must be small probability
3	for the
4	MEMBER CORRADINI: But I think Dr.
5	Rempe=s question is a fair one. If you=re asking the
6	applicant to do his, and they can already show by
7	essentially binary, either it=s there and I get a
8	failure of cavity but it doesn=t do anything to
9	containment, or it=s not there and that change is
L 0	delta is so small as to the overall containment
L1	failure probability it only comes down to the accident
L2	management guidelines is where it matters. I think
L3	that=s where Joy was going with it.
L 4	MEMBER REMPE: Well, if you can I
L 5	think what I remember is more AP600-based, but they
L 6	basically finally said there is too much uncertainty,
L7	and so they did do the bounding and say, ADoesn=t
L8	matter. If you can make them do that, that=s cool.@
L 9	But right now, it s kind of like out there and we=re
20	not really analyzing it.
21	So then I start wondering about adverse
22	effects. You aren=t taking credit, but then you need
23	to think about that there=s something in this cavity
2 4	and containment area that and show that it doesn=t

	331
1	adversely affect things. So I would prefer that a
2	bounding calculation show that it can=t you know,
3	it doesn=t affect things, and there=s no adverse
4	effects.
5	But I=m not sure how one I mean, we
6	can write something about it in the letter, but I
7	don=t know what the staff could do. Mike, is there
8	something?
9	MEMBER CORRADINI: I just want to
10	understand what Hanry is forcing them into.
11	MR. WAGAGE: No, I=m not right now
12	that is
13	MEMBER CORRADINI: Oh, you=re giving them
14	a choice.
15	MR. WAGAGE: That=s the status.
16	Actually, I proposed that COL information item and -
17	-
18	MEMBER CORRADINI: That=s acceptable.
19	Okay.
20	MR. WAGAGE: we are reviewing it with
21	the that=s right. We are reviewing it right now.
22	MEMBER CORRADINI: But I guess
23	MR. WAGAGE: We don=t have a position
24	which way to go.

	332
1	MEMBER CORRADINI: But I think, to clean
2	it up, since the AP1000 part of this open, they can
3	just look and see what was done there, right? Okay.
4	MR. WAGAGE: Yes.
5	MEMBER REMPE: It seems like that would
6	be making it a COLA item is kind of I don=t
7	know, that doesn=t seem as satisfactory.
8	MR. WAGAGE: Thank you. I am done with
9	
10	CHAIRMAN BALLINGER: We should move on.
11	MR. WAGAGE: this part of the
12	presentation.
13	CHAIRMAN BALLINGER: Maybe we shouldn=t
14	move on.
15	MEMBER STETKAR: In your presentation
16	this afternoon, you didn=t address one of the bullet
17	items on your Slide 50, and in particular that would
18	be containment bypass. And we=re not going to talk
19	about it anywhere else, so I=m going to talk about it
20	now.
21	In the SER, there is a section that does
22	address containment bypass. And in the interest of
23	brevity, let=s just say it says two types of accident
24	scenarios that are of interest are steam generator

1 tube rupture and interfacing system LOCA. 2 There is then a discussion of an exchange 3 between the staff and the applicant regarding tube 4 ruptures, both as an initiating event and as a 5 consequential tube rupture. And it basically cites 6 the fact that for consequential tube ruptures they 7 can open up the POSRVs and depressurize the primary And for initiating events, they can do the 8 9 standard steam gemerator tube rupture response. And the final conclusion of the staff 10 11 is -- and here=s where I will quote -- AGiven the 12 design features described above, @ which is all of the tube rupture stuff I just summarized, Aand evaluated 13 Section 19.2 2.5 of this report, which is a 14 15 discussion of interfacing system LOCA initiating 16 are consistent with SECY-90-016 events, which 17 recommendations, the staff concludes that 18 containment bypass is not a significant contributor to severe accidents for the APR1400 design.@ 19 20 To me, that=s really interesting because 21 in the DCD I learn that 49 percent of the large 22 release frequency just slightly less than half, is 23 from containment bypass from tube rupture, both

initiating event and induced, where most of it is

24

1	actually from the consequential.
2	For those of you interested in whatever
3	is going down around in that cavity, that is
4	invisible. Twenty-seven percent comes from a late
5	rupture with no containment sprays, 12 percent is
6	from a containment rupture prior to core damage.
7	That=s energy release overpressure early
8	I know. I know you=re fascinated by it.
9	I heard that you are.
10	And then there is 10 percent from
11	containment leakage and, I don=t know, it gets really
12	small after that. So my curiosity is the staff is
13	saying, well, containment bypass is no big deal on
14	this plant, and yet it=s half
15	PARTICIPANT: More than half.
16	MEMBER STETKAR: No, it=s 49 percent.
17	PARTICIPANT: Oh, 49.
18	MEMBER STETKAR: Forty-nine percent.
19	It=s actually a little less than half.
20	Of their large release frequency. I=m
21	curious. This comes back to my initial question
22	about, why do you focus on only those things that
23	were identified back in some SECY paper 25 years ago,
24	and not focus on what is important for this plant?

1	And is there anything that can be done to make the
2	stuff that=s important less important?
3	They have already accounted for
4	everything that you cite in your discussion, and yet
5	even accounting for all of that it=s still half of
6	the large release frequency. I=m not going to say
7	any more. It=s on the record.
8	MR. WAGAGE: I=ll take that question
9	back.
10	CHAIRMAN BALLINGER: Let=s continue.
11	MS. GRADY: Good afternoon. I=m Anne-
12	Marie Grady, and I=m here to address the severe
13	accident mitigation feature of equipment
14	survivability.
15	CHAIRMAN BALLINGER: Is your light on?
16	MS. GRADY: It=s green. Does that sound
17	better?
18	CHAIRMAN BALLINGER: Yes.
19	MS. GRADY: Okay. The objective of
20	equipment survivability comes from SECY-93-087, and
21	it requires mit gation features be designed to
22	operate in the severe accident environment for which
23	they are intended over the timespan for which they
2.4	are needed.

1	10 CFR 50.44(c)(3), which covers
2	combustible gas control, requires containments to
3	establish and maintain safe shutdown and containment
4	structural integrity with systems and components
5	capable of performing their functions during and
6	after exposure to the environmental conditions
7	created by the burning of hydrogen equivalent to that
8	of a fuel clad and coolant interaction involving 100
9	percent of the fuel cladding. That is an additional
10	condition over severe accident mitigation.
11	Severe accident mitigation is after any
12	severe accident. This is an additional condition put
13	on it by the burning of hydrogen.
14	Staff finds hold on. I guess I=ve got
15	to read that. Okay. The applicant selected accident
16	scenarios from the most probable core damage
17	sequences in the Level 1 PRA and from several LOCAs.
18	The applicant then identified mitigation functions of
19	reactor coolant system inventory, reactivity control,
20	and containment integrity as the mitigation functions
21	that needed to be satisfied.
22	The applicant in the DCD specified
23	specific equipment which would be needed to achieve
24	those functions, and it=s found in DCD

1	Table 19.2.3-4. entitled Systems and Equipment and
2	Instrumentation Required for Equipment Survivability.
3	Staff agreed with the equipment that was
4	identified in that table, and in addition requested
5	two other items be added. One of them is the
6	emergency containment spray backup system check valve
7	that is sitting in side the containment, and the other
8	one is the integrity of the containment isolation
9	penetrations.
10	The containment isolates much earlier in
11	an accident than this, but this is just to maintain
12	integrity of the penetrations where the containment
13	isolation valves are.
14	The applicant has agreed to add those two
15	items to the existing list, and we agree with the
16	equipment that has been identified.
17	The accident conditions characterized by
18	the applicant and the environmental conditions for
19	equipment survivability establish sufficient guidance
20	to demonstrate compliance with 50.44(c)(3) and 10 CFR
21	50.34(f). The temperature profiles were confirmed in
22	the staff confirmatory calculations, and the
23	applicant=s AICC pressure of 110 psia bounded the
24	staff=s confirmatory pressures.

1	Additionally, the applicant calculated
2	the severe accident radiation dose of 4.4E+05 Gy or
3	4.4E+07 rad using a MAAP dose code. Staff did not do
4	a confirmatory calculation on the dose, but rather
5	compared the dose calculated by the applicant with
6	other advanced light water reactors of similar size
7	and design and fuel type, and found them comparable.
8	MEMBER POWERS: This is dose over some
9	period of time?
10	MS. GRADY: Twenty-four hours.
11	MEMBER POWERS: Twenty-four hours.
12	MS. GRADY: Yes.
13	MEMBER POWERS: Okay.
14	MS. GRADY: Staff also found the
15	containment atmospheric assessments of temperature,
16	pressure, and radiation described in DCD Section
17	19.2.3.3.7 acceptable for evaluating equipment
18	survivability.
19	There was, and still is, a COL
20	information item whereby the COL applicant will then
21	take the equipment identified, the conditions of the
22	severe accident, and then ascertain, once they=ve
23	specified this equipment, and once they=ve purchased
24	it, they will do the evaluation to show that that

1	equipment can in fact last for the time period it
2	needs to and function in that time period. But that
3	is a COL item.
4	So this is basically a partially complete
5	evaluation. This is what staff has this is what
6	the applicant has proposed. This is what we have
7	agreed to.
8	MEMBER POWERS: This is this dose is
9	a severe accident dose, and it is for a 24-hour
10	period, but it=s not going to be radically different
11	than the design basis dose because it=s dominated by
12	the noble gases.
13	MS. GRADY: I=m sorry. Would you repeat
14	that last part of the question?
15	MEMBER POWERS: The dose you get for
16	severe accidents is not radically different than the
17	design basis dose, because it=s dominated by the noble
18	gases.
19	MS. GRADY: Okay.
20	MEMBER POWERS: And so that the equipment
21	that must survive to deal with the design basis dose
22	must deal with a much larger total dose, because it
23	has to last for 30 days; is that correct?
24	MS. GRADY: You said 30 days. I don=t

	340
1	know where that requirement would have come from.
2	But it could be longer than 24 hours, yes.
3	MEMBER POWERS: Yes. Okay. So
4	MS. GRADY: But it depends on what you
5	need the equipment for and for how long you need it.
6	All it has to do is survive and function. Yes, I
7	agree with you.
8	That=s all I have to say unless somebody
9	has a question.
10	MR. SCHAPEROW: I=m Jason Schaperow with
11	the Office of New Reactors, and I would like to
12	present to you our MELCOR independent confirmatory
13	analysis that we did for Chapter 19.
14	MEMBER REMPE: Jason, could you kind of
15	explain to me when you say Athe independent
16	calculations you did,@ I know there was a calc
17	notebook, which I actually looked through that ERI
18	created, but that=s just the model description.
19	Where does one find the calculation results
20	documented?
21	MR. SCHAPEROW: Okay. I think it should
22	be a reference in the draft SC that you received.
23	MEMBER REMPE: The only place I=ve seen
24	plots with MELCOR

]
1	MR. SCHAPEROW: And it=s in ADAMS.
2	There=s a reference to the SC that you received; it=s
3	in ADAMS.
4	MEMBER REMPE: I=d like to see a copy.
5	The only place =ve seen calculations are those
6	combustible gas ones that was or an ERI document,
7	but maybe I missed
8	MR. SCHAPEROW: This is actually an SPRA
9	Branch document that we produced.
10	MEMBER REMPE: Okay. And it=s dated
11	2015. And, you=re right, I missed that. I
12	apologize. Okay
13	MR. SCHAPEROW: So the objective of our
14	confirmatory analysis was to confirm the applicant=s
15	use of MAAP for the PRA and for the severe accident
16	analysis, Chapter 19. Our approach was to perform
17	independent analysis for select scenarios, so we did
18	we took a sample of scenarios.
19	We ran the calculation for the MELCOR,
20	and then we compared the MELCOR results with the MAAP
21	results for these scenarios.
22	MEMBER REMPE: Jason, I take it back.
23	I=m sorry to keep interrupting you, but that was a
24	meeting that Walt showed me. It says it=s to be

]
1	developed in the draft SC, the calculations. If I
2	look at that last reference, it says this report is
3	under development. SPRA, is that
4	MR. SCHAPEROW: We finished it in
5	November 2016. So it=s possible that you have the
6	SC version you have is
7	MEMBER REMPE: That must be what we
8	have is outdated, because
9	MR. SCHAPEROW: I=ll get it to you. I=ll
10	get it to you.
11	MEMBER REMPE: Yes. I would like a copy
12	is the bottom line, please.
13	MR. SCHAPEROW: Yes. Especially I and
14	Sean Campbell from Research, the two of us put it
15	together in November.
16	MEMBER REMPE: Okay. Yes, I
17	MR. SCHAPEROW: He was on rotation. That
18	was the first thing he did when he got there was to
19	put the report together because we wanted to have a
20	document of the calculations.
21	Okay. I just want to note up front that
22	there is two remaining issues after this work that we
23	did. One is the applicant has committed to assess
24	the impact of their sensitivity calculations they did

1	in response to our RAI on their SAMDA analysis. And
2	the second one is that the applicant is revising their
3	shutdown analysis with MAAP, and I=ll get into that
4	a little more on my last slide.
5	Okay. Next slide, please?
6	Okay. We reviewed the DCD and the
7	supporting documents that we had access to in the
8	electronic reading room in order to select scenarios,
9	and this graph shows the this chart shows the five
10	scenarios that we analyzed with MELCOR for our
11	confirmatory analysis.
12	The first four rows are at-power
13	scenarios. These scenarios are very similar, with
14	the exception that they have different new these
15	new severe accident features are different. So for
16	the Q03 scenario, there is no it=s a really plain
17	vanilla station blackout, nothing works. And then as
18	you go up higher on the chart, then we start adding
19	systems that they have for severe accident
20	mitigation.
21	Finally, the last row of the chart, we
22	actually did a calculation for a shutdown accident,
23	and this is for scenario POS 5.
24	Next slide, please?

1	So we did the calculations, and when we
2	compared the results we found that we actually had a
3	couple of assumptions a little bit different than
4	what was in the MAAP calculations. The assumptions
5	that we used for MELCOR were based on what we read in
6	the DCD, but we learned a little more when we did the
7	comparison and we said, AWell, why is this a little
8	different?@ and they said, AWell, it=s because we did
9	this.@
10	Some of the differences MELCOR had
11	we had modeled the safety injection tanks in the
12	MELCOR calculation where in the MAAP calculation they
13	didn=t have that included.
14	For the second row here, we had a hot leg
15	creep rupture included in our model, but for the one
16	calculation that we looked at from KHNP, which was
17	the high pressure calculation, they assumed that
18	there was no creep rupture of the hot leg.
19	Similarly we assumed that there was seal
20	leakage and failure. This is a holdover kind of from
21	the sort of work that we did. For MAAP, they assumed
22	no seal leakage or failure.
23	And the last two rows deal with timing of
24	operator actions. From what I saw in the DCD, it

1	looked to me like they were going to perform these
2	operator actions ppening the POSRV, and opening the
3	three-way valves and the cavity flooding valves. I
4	thought this would be done when the core-exit
5	thermocouple hit 922K.
6	Again, when we got to comparing the
7	results, we found out this wasn=t what was done with
8	MAAP. For opening the POSRVs, the operator opened
9	them. They assumed the operator opened them after
LO	the first life of the POSRVs, which was consistent
L1	with their feed and bleed procedures.
L2	And, similarly, for opening three-way
L3	valves and the cavity flooding valves, we found that
L 4	they actually assumed a delay, that they thought it
L5	would take a little while until those valves got open.
L 6	Next slide, please?
L7	As a result of our comparisons, KHNP went
L8	back and they ran some sensitivity cases to look at
L 9	these differences and assumptions. And for the cases
20	that we looked at, for the source term categories,
21	for example, they decided they concluded that the
22	new MAAP calculations didn=t really make any
23	difference in the PRA.
2.4	We took a look at that also, and we

1 extended that look at other parts of the other 2 source term categories beyond source term categories 3 11 -- 10, 11, and 16. We looked at all of the other 4 source term categories to see if we thought the differences in the calculations would be significant. 5 6 Regarding large release frequencies, we 7 scaled the releases to account for the sensitivity calculations, and we decided that it wouldn=t --it 8 9 wouldn=t change ally small release to a large release, so we figured that wouldn=t be a difference. 10 11 We also looked at the SAMDA analysis, 12 again, scalling the cesium releases by 13 differences that we saw, we didn=t think it was going to affect the SAMDA analysis because SAMDA analyses 14 15 do have typically quite large margins in them, and this one did. 16 17 Regarding quantification of the CET, the Case 003 was used in the containment event tree to 18 19 look at containment pressures. And while they did 20 get a little different containment pressure when they 21 did sensitivity calculations with Case Q03 with MAAP, 22 it didn=t make that big a difference, especially in 23 the ultimate containment failure comparison with pressure, which is 162.7 pounds gauge. 24

1	Next slide, please?
2	MEMBER POWERS: Jason, that containment
3	failure fragility number there, that=s a membrane
4	failure, right?
5	MR. SCHAPEROW: It=s listed in the
6	document as the median ultimate containment failure
7	pressure. I don=t know what it=s based on, though.
8	MEMBER POWERS: But it=s the
9	MR. SCHAPEROW: The structural folks
10	would know.
11	MEMBER POWERS: it=s the rupture of
12	the steel liner as a membrane.
13	MEMBER STETKAR: It=s actually around the
14	equipment hatch is where they fail it. So it=s not
15	MR. SCHAPEROW: It=s used within the PRA
16	as part of their determination of the likelihood of
17	overpressure failures, and they use these MAAP
18	calculations to decide what the likely they enter
19	this table of failure pressure to figure out what
20	the likelihood of each of these calculations
21	resulting in containment failure.
22	MR. ROCHE-RIVERA: This is Robert Roche,
23	Structural Engineering Branch in NRO, and I agree
24	with Jason=s last point. I think it did contain not

1	only liner failure limits, but it looked at other
2	aspects such as rebar, tendon, failure limits for the
3	rebar, tendon, and even like leakage failure criteria
4	to come up with the combined median ultimate pressure
5	capacity.
6	MR. SCHAPEROW: We also used MELCOR to
7	simulate a midloop accident. The deck that we
8	started with was an at-power deck, but we made the
9	changes needed to make it mimic a shutdown accident.
LO	In particular, we wanted to do a calculation for a
L1	plant operating state 5, which was a big part of the
L2	core damage frequency for this design. So we reduced
13	the decay heat.
L 4	We assumed the accident happened during
L5	POS 5, which was after a bit after shutdown. We
L 6	added nozzle dams by blocking flow paths. We added
L7	an open manway on the top of the steam generator. We
L 8	took the safety injection tanks away by isolating
L 9	them, and then we changed the RCS pressure temperature
20	and water level to mimic the start of an accident for
21	midloop.
22	We did comparisons. We looked at the
23	MAAP results. We compared them with the MELCOR
24	results. We asked a lot we asked a number of

1	questions to the applicant, and the applicant has
2	decided to revise their MAAP model for this for
3	the POS 5 calculations. And last I saw, they had
4	actually redone several of these calculations and
5	they were documenting them and folding them back into
6	the PRA.
7	They also did find a code bug as part of
8	the as a result of the questioning, and they told
9	us about that as well.
10	CHAIRMAN BALLINGER: Continue. Next?
11	MR. SCHAPEROW: Finished.
12	CHAIRMAN BALLINGER: Thank you.
13	MS. NEUHAUSEN: Good afternoon again.
14	My name is Alissa Neuhausen, and I=m a technical
15	reviewer in the Structural Engineering Branch. I was
16	responsible for the review of the containment
17	performance capability, along with Robert Roche.
18	Next?
19	The staff review ensures that the
20	applicant meets the Commission=s deterministic
21	containment performance goal as described in SECY-90-
22	016 and 93-087. The staff focused on information
23	provided in DCD Section 19.2.4, containment
24	performance capability.

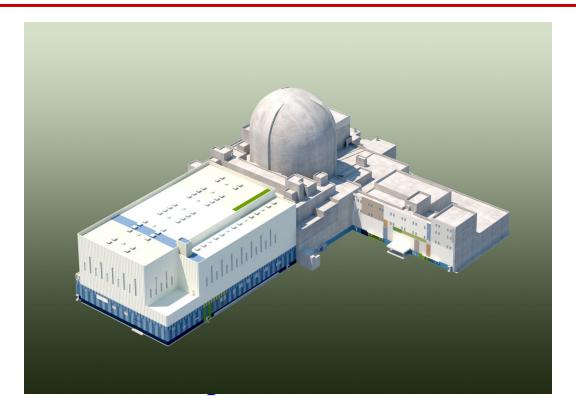
	350
1	The staff also reviewed the applicant=s
2	finite element analysis of containment subjected to
3	severe accident pressure and temperature loadings.
4	The staff followed guidance provided in Regulatory
5	Guide 1.216, Regulatory Position 3, for severe
6	accidents.
7	The staff confirmed that the ASME factory
8	load category for concrete containments are met for
9	severe accident leading. The staff has completed the
10	review of the deterministic containment performance
11	goal.
12	Next, please? Thanks.
13	The deterministic containment
14	performance goal establishes that the containment
15	used to maintain its role is a reliable leak-tight
16	barrier for approximately 24 hours following the
17	onset of core damage and continue to provide a barrier
18	against the uncontrolled release of fission products
19	after 24 hours.
20	The applicant=s approach was to select a
21	conservative severe accident load. The applicant
22	demonstrated that the most significant pressure
23	loading history is generated from a large loss of
24	coolant accident, station blackout, and total loss of

	351
1	feedwater events are bounded by the selected severe
2	accident load.
3	The applicant demonstrated that for the
4	selected severe accident load the strains in the liner
5	plate do not reach the allowable limit strain values
6	as defined by ASME Code Section 3, Division 2,
7	subarticle CC-3720, factor load category.
8	If there are no questions, that=s all I
9	have.
10	MEMBER CORRADINI: So there=s a stylized
11	pressure temperature history that bounds those three?
12	MS. NEUHAUSEN: The pressure bounds those
13	three.
14	MEMBER CORRADINI: And along with some
15	temperature.
16	MS. NEUHAUSEN: Along with some
17	temperature.
18	MEMBER CORRADINI: Okay.
19	CHAIRMAN BALLINGER: Thank you.
20	MR. WAGAGE: My name is Hanry Wagage.
21	I=ll conclude with phase 2 staff findings that due to
22	the remaining issues, the staff is unable to make
23	final conclusions on the severe accident evaluation
24	of the APR1400 design.

1	MEMBER CORRADINI: Pending open items.
2	CHAIRMAN BALLINGER: Thank you.
3	MR. PHAN: Ladies and gentlemen, that=s
4	the end of our presentation on PRA and severe accident
5	evaluation, understanding that there are outstanding
6	questions that the staff will provide you with
7	additional evaluations and information. But for now,
8	again, we thank you for all of your comments and your
9	advice, and the staff will incorporate those in the
10	next phase of our review.
11	And with that, if you have any additional
12	questions, please raise them at this point.
13	CHAIRMAN BALLINGER: Any questions?
14	Now, should we maintain the line open? I=m not sure
15	anybody is on it.
16	So any comments from anybody in the room?
17	Anybody want to - hearing none, the line is open.
18	Is there anybody out there? If there is, can you
19	identify yourself or say that you=re there?
20	MEMBER BLEY: Just ask for comments.
21	CHAIRMAN BALLINGER: Any comments from
22	people on the line? Hearing none, thank you very much.
23	I think that I haven=t heard anything
24	about needing a closed session. We had on the

	353
1	schedule something here and a note I don=t think
2	we have it, so we don=t need it.
3	That being the case, we have gone from
4	likely to be very late to being five minutes early.
5	So, in that case, we are adjourned, released,
6	recessed.
7	(Whereupon, the above-entitled matter
8	went off the record at 5:55 p.m.)

APR1400 DCA Chapter 19.1: Probabilistic Risk Assessment



KEPCO/KHNP April 19, 2017





Overview of Chapter 19 (1/2)

Section Overview

Section	Section Title		
19.0	Probabilistic Risk Assessment and Severe Accident Evaluation		
19.1	Probabilistic Risk Assessment	Young In	
19.1.1			
19.1.2	Quality of PRA		
19.1.3	Special Design/Operational Features		
19.1.4	Safety Insights from the Internal Events PRA for Operations at Power		
19.1.4.1	Level 1 Internal Events PRA for Operations at Power	Greg Rozga	
19.1.4.2	Level 2 Internal Events PRA for Operations at Power Tae-H		
19.1.5	Safety Insights from the External Events PRA for Operations at Power		
19.1.5.1	Seismic Risk Evaluation	Dong-Won Lee	
19.1.5.2	5.2 Internal Fire Risk Evaluation Greg		
19.1.5.3	3 Internal Flooding Risk Evaluation		
19.1.5.4	Other External Events Risk Evaluation	Ray Dremel	
19.1.6	Safety Insights from the PRA for Other Modes of Operation		
19.1.6.1	Level 1 Internal Events PRA for Low Power and Shutdown Operations		
19.1.6.2	Level 2 Internal Events PRA for Low Power and Shutdown Operations	Jaegab Kim	
19.1.6.3	3 Internal Fire PRA for Low Power and Shutdown Operations		
19.1.6.4	Internal Flooding PRA for Low Power and Shutdown Operations		
19.1.7	PRA-Related Input to Other Programs and Processes Young In		
19.1.8	Conclusions and Findings		

Overview of Chapter 19 (2/2)

Section Overview

Section	Title	Presenter	
19.2	Severe Accident Evaluation		
19.2.1	1 Introduction		
19.2.2	2 Severe Accident Prevention		
19.2.3	3 Severe Accident Mitigation Byungjo I		
19.2.4	nment Performance Capability		
19.2.5	Accident Management		
19.2.6	Consideration of Potential Design Improvement under 10 CFR 50.34(f)		
19.3	Beyond Design Basis External Event		
19.3.1	Introduction	Chan-Eok Park	
19.3.2	NTTF Tier 1 Recommendation		
19.3.3	NTTF Tier 2 and 3 Recommendation		
19.4	Loss of Large Area		
19.4.1	Introduction and Background	ckground Cory Hoyner	
19.4.2	Gary Hayne		
19.4.3	Conclusions		
19.5	Aircraft Impact Assessment		
19.5.1	Introduction and Background	_	
19.5.2	Scope of the Assessment Randy James		
19.5.3	Assessment Methodology		
19.5.4	Conclusions		



Overview of Chapter 19.1

Section Overview

17.0 I TOUAUTIISHE KISK ASSESSITIETH AND SEVERE ACCIDENT LIVATUATIO	19.0	Probabilistic Risk Assessment and Severe Accident Evaluation
---	------	--

- 19.1 Probabilistic Risk Assessment
- 19.1.1 Uses and Applications of the PRA
- 19.1.2 Quality of PRA
- 19.1.3 Special Design/Operational Features
- 19.1.4 Safety Insights from the Internal Events PRA for Operations at Power
- 19.1.4.1 Level 1 Internal Events PRA for Operations at Power
- 19.1.4.2 Level 2 Internal Events PRA for Operations at Power
- 19.1.5 Safety Insights from the External Events PRA for Operations at Power
- 19.1.5.1 Seismic Risk Evaluation
- 19.1.5.2 Internal Fire Risk Evaluation
- 19.1.5.3 Internal Flooding Risk Evaluation
- 19.1.5.4 Other External Events Risk Evaluation
- 19.1.6 Safety Insights from the PRA for Other Modes of Operation
- 19.1.6.1 Level 1 Internal Events PRA for Low Power and Shutdown Operations
- 19.1.6.2 Level 2 Internal Events PRA for Low Power and Shutdown Operations
- 19.1.6.3 Internal Fire PRA for Low Power and Shutdown Operations
- 19.1.6.4 Internal Flooding PRA for Low Power and Shutdown Operations
- 19.1.7 PRA-Related Input to Other Programs and Processes
- 19.1.8 Conclusions and Findings
- 19.1.9 Combined License Information





19.1 APR1400 PRA Scope

Opera	tion Mode	Level 1	Level 2
	Internal Events	0	
A 4 -2 0 -2 -2 -2	Internal Fire	О	O
At-power	Internal Flooding	О	
	Seismic*	О	-
	Internal Events	0	0
Low Power and Shutdown	Internal Fire	О	О
SIMUU WII	Internal Flooding	О	Δ

^{*} PRA-based SMA, \triangle Bounding approach





19.1 PRA Methodology & Tools

- Small Event Tree & Large Fault Tree Approach
 - Linked Fault Tree
- Computer Tools
 - KEPCO E&C SAREXTM
 - KAERI FTREXTM
 - EPRI CAFTA*
 - EPRI HRA Calculator 5.1 (2017 PRA Update)
 - MAAP 4.0.8
 - RELAP5/Mod3
 - MACCS2





^{*} For LPSD Internal Fire and Internal Flooding Level 1, and LPSD Level 2. The PRA updates planned in 2017 will be using CAFTA.

19.1.7 Risk Applications

- Current Applications (DC Phase)
 - Reliability Assurance Program (RAP)
 - Severe Accident Management Design Alternative (SAMDA)
 - Environmental Report
- Future Applications (COL Phase)
 - Reactor Oversight Program
 - MSPI, SDP, etc.
 - Maintenance Rule





19.1.7 Design Improvements from Risk Insights

- EDG: two (2) EDGs to four (4) EDGs
- AAC: from Diesel Generator (DG) to gas turbine generator (GTG)
- 125V DC Batteries: Increased capacities
- Technical Specifications 3.6.7: equipment hatch closure in Mode 5
- Cables to be protected: cables for 75 components in 59 fire compartments





19.1.8 Overall Results

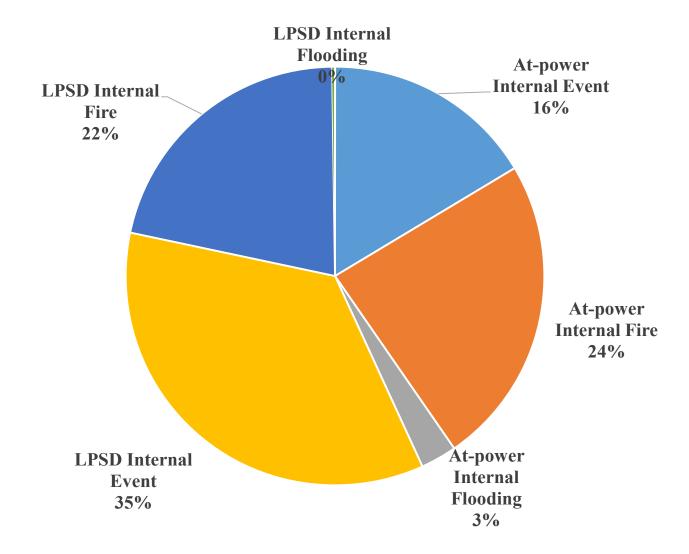
Operation Modes	Hazards	Level 1 (per yr)	Level 2 (per yr)
At-Power	Internal Events	1.3E-06	1.1E-07
	Internal Fire	1.9E-06	1.7E-07
	Internal Flooding	2.2E-07	1.7E-08
LPSD	Internal Events	2.6E-06	1.2E-07
	Internal Fire	1.7E-06	1.3E-07
	Internal Flooding	1.8E-08	
Total		7.9E-06	5.5E-07

Note: The CDF and LRF values are point-estimates.





19.1.8 Overall CDF Profile







19.1.4.1 Internal Events Level 1





19.1.4.1 Initiating Event Analysis

- Identification of Potential Initiating Events
 - Generic industry information sources
 - NUREG/CR-6928, 5750, 3485, GL 88-20, NUREG-1335, EPRI NP-2230
 - Information from similar plants
 - Plant-specific operating experience: N/A
 - Systematic review of the APR1400 design a high level FMEA
- Grouping of Initiating Events
 - Impacts of initiating events on core protection functions and plant responses
 - Group of initiators expected to have a common core damage accident progression and success criteria
 - Comparison with Generic Source such as NUREG/CR-5750
- Calculation of Initiating Event Frequencies
 - Use generic industry data in NUREG/CR-6928 and Initiating Event
 Data Sheets Update 2010
 - Criticality factor 0.95 assumed





19.1.4.1 Initiating Event Analysis

- LOCAs
 - Large, Medium, Small, ISLOCA and RVR
 - SGTR
- Transients
 - General Transient
 - Loss of Main Feedwater
 - Loss of Condenser Vacuum
 - Large Secondary Side Breaks (MS and MFW)
 - Loss of Support Systems (IA, DC, CC, SX)
- Loss of Offsite Power Events (Plant, SWYD, Grid and Weather Related)
- Induced Initiators
 - Not true initiators, but rather unique events induced post-initiator by certain plant response failures
 - ATWS
 - Grid Disturbance LOOP/SBO
 - Station Blackout (SBO)
 - Stuck Open POSRV LOCA





19.1.4.1 Accident Sequence Analysis

- Key Safety Functions
 - Reactivity, RCS Inventory, RCS Pressure, Decay Heat Removal,
 Containment Heat Removal
- Develop Event Trees
 - Define key functional requirements
 - To reach a safe, stable state and prevent core damage, as well as identify the systems and operator actions for accident mitigation
 - Define accident sequences
 - In a manner consistent with plant system design, operating procedures, plant response, etc.
 - Apply T/H analyses to determine the accident progression parameters
 - Identify impacts of initiators to mitigating systems (dependency)
 - Success/failure of preceding systems, functions, human actions
 - System alignments, time-phased, phenomenological conditions
 - Develop Fault Trees: Small Event Tree/Large Fault Tree, Fault Trees are linked to Event Trees





19.1.4.1 Success Criteria

- Definition of Core Damage
 - Consistent with SR SC-A2 of ASME/ANS PRA Standard
 - Peak node temperature exceeds
 - 1204°C (2200°F) for a code with detailed core modeling (RELAP)
 or
 - 982°C (1800°F) for a code with simplified core modeling (MAAP)
- Based on Best Estimate Analyses
 - Utilize MAAP 4.0.8 and RELAP5/mod3
 - Review FSAR Chapter 15 for consistency





19.1.4.1 Internal Events at Full Power

- Key PRA Assumptions
 - The Internal Fire, Internal Flooding and Seismic Assessment
 - Based on the APR1400 design information
 - The SKN 3&4 design information is used, if the design information is not available
 - Digital I&C system
 - Uses the hardware model from the SKN 3&4 design
 - MLOCA
 - Assumed not to require Hot Leg Injection to prevent boron precipitation
 - RCP Seal LOCA Probability
 - Modeled based on the engineering judgment
 - **GSI-191**
 - Sump plugging modeled, but chemicals effect is not modeled since there no fibrous materials in the containment





19.1.4.1 Systems modeled in PRA

Front Line Systems

- Auxiliary Feedwater (AF)
- Containment Spray (CS)
- Shutdown Cooling (SC)
- Safety Injection (SI)
- Chemical & Volume Control (CV)
- Main Feedwater (FW)
- Main Steam (MS)
- Safety Depress. and Vent (SDVS)
 - Reactor Coolant (RC) & Gas Vent (RG)
- Reactor Protection (RP)

Supporting Systems

- Component Cooling Water (CC)
- Essential Service Water (SX)
- Essential Chilled Water (WO)
- Electrical Systems (AC, DC, EDG, AAC)
- Heating, Ventilation and Air Conditioning (HVAC)
- Instrumentation Air (IA)
- T/G Bldg Open Cooling Water (WH)
- T/G Bldg Closed Cooling Water (WT)
- Engineered Safety Feature Actuation (EF)





19.1.4.1 Data and CCF Analysis

- Data Source used in internal level 1 full power PRA
 - Component Unreliability Data
 - 2010 update for NUREG/CR-6928
 - Vendor specific data (e.g., Sempell Co.) for POSRV
 - Alternate industry sources (e.g., IEEE STD-500)
 - Component Unavailability Data
 - 2010 update for NUREG/CR-6928
 - NUREG/CR-5500, Vol. 2, 3, 10, and 11
 - Engineering judgment
 - Common Cause Failure Data
 - 2010 Update for NUREG/CR-5497
 - Special Events Data
 - NUREG/CR-6890 for LOOP non-recovery probabilities





19.1.4.1 Human Reliability Analysis

The HRA model

- Type A: Pre-initiating event human interactions (errors that can occur during test and maintenance)
 - ~ 60 pre-initiators are modeled
 - Based on the test and maintenance procedures from the reference plants
 - Will need to be verified when the detailed test and maintenance procedures become available during COL stage
- Type B: Initiating event related human interaction (if not completed correctly may cause an initiating event)
 - Not explicitly modeled
 - Assumed implicit in the IEFs obtained from Operating Experience
- Type C: Post-initiating event human interaction (evaluated to determine the likelihood of error)
 - ~ 70 operator actions are modeled
 - Dependencies among the operator actions were evaluated





19.1.4.1 Human Reliability Analysis

Methodology

- Re-quantify model with HRA valves set to a value near 1.0
 - This is done to ensure that all risk significant HRA combination are addressed.
 - The combination of HRA probabilities when not set to a high value can be truncated and therefore not addressed by the dependency analysis
- Analyze the HRA combinations for dependency
 - The HRA events are analyzed the same procedure usage
 - The HRA events are analyzed to ascertain if the failure of one events will fail the other HRA events in the combination.
 - The HRA events are analyzed to ascertain the affect of one event on the operator and whether the other events will be attempted.
- Dependency Level Evaluation
 - Dependency level is determined by dependency level decision tree in NUREG-1921, "EPRI/NRC-RES, Fire HRA Guidelines"
 - Decision Tree Branches: Intervening Success / Crew / Cognitive / Cue Demand / Manpower / Location / Sequential Timing / Stress
- The EPRI HRA Calculator provides the tools to perform the dependency analysis (being used for 2017 PRA update)





19.1.4.1 Quantification

- Quantification Process
 - Quantification performed using SAREX and CAFTA
 - 10⁻¹³ is applied as cutoff value for CDF quantification
 - Use of flag events
 - To consider various IE conditions, both house event and double initiators are used together
 - Use of delete-term logic in the model
 - To remove unrealistic MCS combinations, delete-term logic is used in quantification process
 - Logical loop treatment
 - Circular logic in the supporting system were broken at DC batteries.





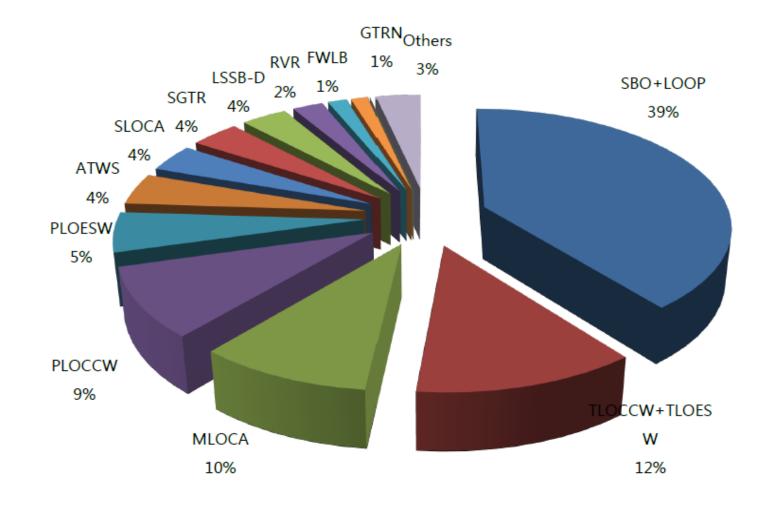
19.1.4.1 Quantification

- Quantification Process
 - Cutset recovery process using recovery file
 - HRA dependency rules, double counted events, transferred initiators with tag events are replaced with meaningful event names





19.1.4.1 Internal Events CDF by Initiating Events







19.1.4.1 Uncertainty Analysis

- Parametric uncertainty
 - State of Knowledge Correlation (SOKC) will be addressed.
 - Selected sensitivity cases to be re-performed (e.g., HEPs and CCF factors)
- Modeling uncertainty
 - Design-specific sources of uncertainty
 - Based on key assumptions
 - Generic sources of uncertainty
 - NUREG-1855, EPRI 1009652
 - Uncertainty characterization
- Selected sensitivity analyses performed





19.1.4.1 Summary and Insights

- The CDF from internal events for at-power operation is low 10⁻⁶ per reactor year.
- The CDF contribution from LOOP and SBO is dominant.
- For final PRA model, 2017 update is in progress.





19.1.4.2 Internal Events Level 2





19.1.4.2 Level 2 PRA Methodology

- Plant Damage State, Containment Event Tree and Decomposition
 Event Tree (CET/DET) methodology is used.
- Model originally created in SAREX and utilized PDS bridge trees to capture all inter-system and intra-system dependencies.
- Computer Codes
 - MAAP 4.0.8 for analyzing severe accident progression and source term release
 - SAREX 1.3 for developing Level 2 PRA model





19.1.4.2 Severe Accident Mitigation Features (1/3)

- Containment Building
 - Pre-stressed concrete containment with a steel liner plate, Large Dry Containment
 - Containment Net Free Volume: 3.1x10⁶ ft³
- Reactor Cavity Design
 - Minimize challenges posed by DCH, FCI, MCCI
 - Convoluted Flow Path to decrease the amount of ejected core debris that reaches the upper containment
 - Large cavity floor area for corium debris spreading and coolability





19.1.4.2 Severe Accident Mitigation Features (2/3)

- Cavity Flooding System (CFS)
 - Minimize or eliminate corium-concrete attack due to MCCI
 - Minimize or eliminate the generation of combustible gases due to MCCI
- Hydrogen Mitigation System (HMS)
 - HMS limits hydrogen concentration in containment, generated from a
 100-percent fuel clad-coolant reaction less than 10 v/o
 - HMS consists of 30 PARs and 8 Igniters





19.1.4.2 Severe Accident Mitigation Features (3/3)

- Pilot-Operated Safety Relief Valves (POSRVs)
 - Provides a means to rapidly depressurize the primary system to about
 250 psia to prevent DCH and induced SGTR following severe accidents
 - Three-way valves located in the POSRV discharge path can be used to redirect the release point of hydrogen from IRWST to the containment atmosphere via SG compartment
- ECSBS (Emergency Containment Spray Backup System)
 - An alternate means of providing containment spray water after 24 hours following severe accidents
 - Deliver water from external water source to the ECSBS containment spray header
 - Use mobile pumping device independent of normal and emergency AC power sources





19.1.4.2 Plant Damage States (PDSs)

- Level 1 event tree sequences are extended to be additionally questioned important for Level 2 PRA. For example,
 - Containment Isolation?
 - Containment sprays? (if not asked for heat removal in Level 1)
 - Steam Generator status? (if not asked in Level 1)
- Bridge Tree (i.e., Extended Level 1 ET or PDS ET) sequences are grouped into PDSs based on similarities in the accident progression by PDS grouping parameters (Bypass, Containment Isolation, LOCA or Transients, etc.)
- As a result of PDS binning, 108 PDSs were defined and quantified to capture all the Level 1 Level 2 dependencies.





19.1.4.2 Containment Structural Analysis

• An Ultimate Pressure Capacity (UPC) calculation approximates the realistic failure pressure of the containment.

• Two containment failure modes (i.e., Rupture and Leak) are determined based on NUREG-1150 and NUREG/CR-6906.





19.1.4.2 Containment Event Tree

- The various containment failure mode and the major severe accident phenomena are represented as top events of the CET. Detailed evaluation of phenomena for each top event of CET is treated in Decomposition Event Trees (DETs).
- The Level 2 CET considered following containment challenges.
 - Direct Bypass (SGTR and ISLOCA)
 - Containment Isolation System Failures
 - Induced SGTR during the severe accident
 - HMPE/DCH or Blowdown Forces (rocket mode failure)
 - Steam Explosions (In-vessel and Ex-vessel)
 - Hydrogen Phenomena (slow combustion/detonation)
 - Steam Over-pressurization
 - Molten core-concrete interaction, including Basemat melt-through





19.1.4.2 Generic Data Used in Level 2

- NUREG-1570 for ISGTR, including the conditional probabilities of ISGTR developed for current generation plants.
- NUREG/CR-6475 and NUREG/CR-6109 for induced hot leg rupture.
- NUREG-1150 and NUREG/CR-4551 were consulted for various phenomena (in-vessel recovery, rocket mode failure, steam explosion, etc.)





19.1.4.2 Source Term Evaluations

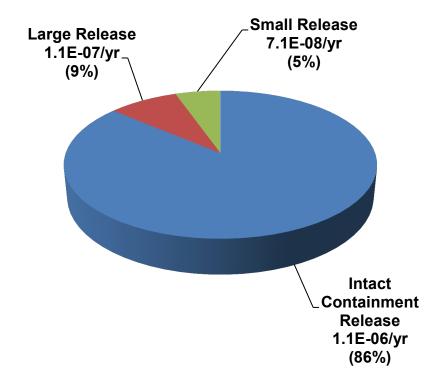
- CET end points are grouped into the source term categories (or release categories) based on similarity of release characteristics (magnitude and timing).
- Source term release calculations are performed using the MAAP 4.0.8 code.
- Definition of a Large Release is ≥ 2.5% of volatile/semi-volatile
 (Iodine, Cesium, Tellurium) fission products (NUREG/CR-6595).
- Definition of early is before effective evacuation of the surrounding public after the general emergency declaration.





19.1.4.2 Level 2 Results for internal events

- Intact containment = 86 % of CDF
- Containment failure (including large and small release) = 14 % of CDF
- Large Releases = 9 % of CDF







19.1.4.2 Level 2 PRA-based Insights

Level 2 Insights (for at-power internal events)

Containment Performance for APR1400

- Containment failure frequency : 1.8E-07/yr (conditional probability : 14 %)
- Large Release Frequency: 1.1E-07/yr (conditional probability: 9 %)

Dominant Contributors for CFF/LRF

- 1st dominant contributor : Containment Bypass (6 % of CDF)
 - SGTR prior to core damage : 5 % of CDF
 - Severe accident-induced SGTR: 1 % of CDF
 - Rapid depressurization is effective to prevent the severe accident-induced SGTR.
 - SGTR sequences with wet SGs do not result in a large release due to pool scrubbing
- 2nd dominant contributor : Late Containment Failure (5 % of CDF)
 - ECSBS is effective to prevent containment failure due to steam overpressure
 - PARs and flooded cavity (by CFS) are effective to prevent the build-up of hydrogen to the high concentration inside the containment





19.1.5.1 Seismic Assessment





19.1.5.1 The Results of Fragility Analysis for PRA-Based SMA

1. Methodology

- > Staff Review Memorandum to SECY-93-087
- ➤ DC/ISG-020 provides guidance for implementation process for performing PRA-based SMA
- > Structures, systems, and components (SSCs) can be evaluated by either Conservative Deterministic Failure Margin (CDFM) method or Separation of Variables (SOV) method

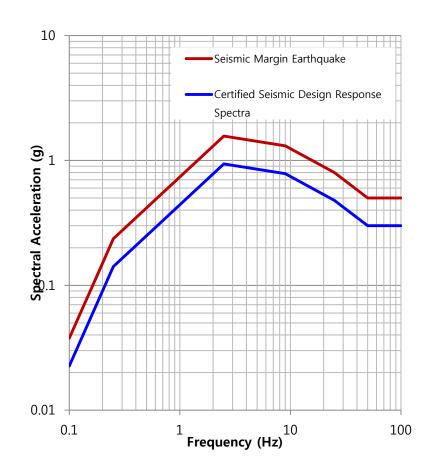




19.1.5.1 The Results of Fragility Analysis for PRA-Based SMA

2. Seismic Input Motion

- Certified seismic design response spectra
 - Spectral shape of Reg.
 Guide 1.60 enhanced in high frequency
 - anchored to a peak ground acceleration of 0.3g
 - defined at free field ground surface
- Seismic margin earthquake is equal to 1.67 times CSDRS







19.1.5.1 The Results of Fragility Analysis for PRA-Based SMA

3. APR1400 SSCs with design-specific HCLPF capacities

- ➤ <u>Building structures</u>
 - Reactor containment building
 - Concrete internal structure
 - Auxiliary building
 - Emergency Diesel Generator (EDG) building
 - Diesel Fuel Oil Tank (DFOT) room building

- Reactor Coolant System (RCS)
 components
 - Reactor vessel & support
 - Reactor internals
 - Control element drive mechanism
 - Steam generators
 - Pressurizer
 - Reactor coolant pumps
 - RCS piping





4. Approach for HCLPF capacity evaluation

- ➤ Identification of critical failure modes
 - Reviewed APR1400 design-specific reports, calculations, and drawings
 - Identified potential failure modes by comparing design seismic demand to design capacity, i.e., design margin
 - Selected governing failure modes for HCLPF capacity evaluation
- Seismic demands
 - Used APR1400 design-specific seismic demands
 - ➤ CSDRS applied at plant finished grade in the free field for 8 generic soil sites and a fixed base case
- > Static capacity equations
 - Used code capacities per ACI 349, ASME Section III Service Level D allowable, or EPRI NP-6041-SL Rev.1





4. Approach for HCLPF capacity evaluation (cont'd)

- Considered inelastic energy absorption capabilities associated with ductile failure modes
- Evaluation of HCLPF capacities of SSCs
 - CDFM method in EPRI NP-6041-SL Rev. 1 applied to demonstrate HCLPF is equal to or greater than Seismic Margin Earthquake, i.e., 1.67 times CSDRS





5. HCLPF capacities of building structures

Building Structure	HCLPF (pga)	Critical Failure Mode
Reactor Containment	0.94g	Tangential shear failure near the base
Reactor Containment Concrete Internal	1.09g	Tangential shear failure of secondary shield wall near the base
Auxiliary Building	0.51g	Shear failure of Wall 15 at the basemat
Emergency Diesel Generator Building	0.87g	Shear failure of Wall 26 at the basemat
Diesel Fuel Oil Tank Room Building	0.73g	Shear failure of Wall 26.1 at the basemat
Stability of NI Structure	0.52g	Sliding toward the turbine building





6. HCLPF capacities of RCS components

RCS Component	HCLPF (pga)	Critical Failure Mode	
Reactor Vessel	0.92g	Column support due to axial compression and biaxial bending	
Reactor Internals	0.51g	Core support barrel lower flange due to primary membrane stress	
Control Element Drive Mechanism	0.64g	Binding of control extension shaft with the upper pressure housing	
Pressurizer	0.63g	Skirt support	
	0.51g	Pressurizer spray nozzle	
Steam Generator	0.60g	Snubber lever support assembly	
	0.54g	Steam generator economizer nozzle	
Reactor Coolant Pump	1.31g	Upper horizontal column support	
RCS Piping 0.55g		Large loss of coolant at surge line nozzle Small loss of coolant at spray nozzle	





7. HCLPF capacities of other SEL components

> Related to RAI Q. 433-8363, 19-73, a)

- ➤ ESWIS, CCW Hx Building, and BOP components
 - Detailed design information is not available in DC phase
 - Assigned to COL items (COL 19.1(7)) and assumed to have 0.5g HCLPF





8. Seismic Equipment List

- Define Seismic Initiating and Consequential Events
 - Direct to core damage scenarios such as building collapse
 - Loss of all Instrumentation and Control
 - Station Blackout (SBO)
 - LOCAs
 - Anticipated transient without SCRAM (ATWS)
 - Loss of offsite power (LOOP)
- Determine Safety Functions Needed for Response
 - Reactivity control
 - Reactor coolant system pressure control
 - Reactor coolant system inventory control
 - Decay heat removal
 - Containment isolation and integrity
- Identify Systems Needed to Fulfill Safety Functions
 - Based on internal events PRA
 - Powered by onsite emergency AC sources





9. Seismic Logic Model

- Seismic Event Trees
 - Direct Core Damage
 - Loss of I&C
 - ATWS
 - LLOCA
 - MLOCA
 - SLOCA
 - LOOP
- Inserted Seismic Failures Into Fault Trees
- Plant-Level HCLPF
 - Solved Seismic Event Tree Models
 - Min-Max Method
 - HCLPF = 0.5g
 - Generic Failure of SSCs
 - Compound Building Collapse
 - Turbine Building Collapse





10. Conclusion

- ❖ Major APR1400 SSCs were evaluated by following ISG-020
 - ➤ Used APR1400 design-specific seismic demands and design data
 - ➤ CDFM method in EPRI NP-6041-SL Rev. 1 was adapted for HCLPF capacity evaluation
- ❖ HCLPF capacities of the SSCs are greater than 1.67 times CSDRS





19.1.5.2 Internal Fire PRA





- 390 Physical Analysis Units (PAUs) identified
 - PAUs are based on Fire Areas with rated barriers
 - Majority are 3 hr rated barriers, but some are 1 or 2 hr barriers
 - Separation <u>may</u> only be credited for yard transformers
 - DCD 8.2.1.4 50 ft separation OR 3 hour barrier
 - ~279 PAUs in Auxiliary Building highly compartmentalized
 - PAUs are mainly single rooms, but may contain 2 or more rooms
 - No credit for PAU internal barriers because walkdowns cannot be performed to determine whether the internal barriers would "substantially contain the adverse effects of fires"
 - LPSD Model uses same PAUs
 - Removable barriers assumed only used during LPSD POS 8 (defueled), so no impact on LPSD CDF or LRF
 - Used for large equipment replacement which is rare





- At-power FPRA equipment list based on At-power internal events PRA, and all LPSD FPRA equipment list based on LPSD internal events PRA
 - At-power equipment identified for non-modeled spurious operations
 - Additional equipment for LPSD "LOCAs" were identified
- Cables for all internal events equipment are routed
 - Cable database is based on reference plant (SKN 3&4)
 - Added assumed routing for 2 new EDGs, AAC, ESW and CCW HX Buildings, and Offsite Source Permissive (OSP) cables
 - Number and type of penetrations (for MCA) are directly from reference plant
 - Cables for new equipment were routed based on reference plant data, and incorporated into the At-Power and LPSD fire risk models (FIRMs)





- No Task 9 Detailed Circuit Failure Analysis
 - All cables assumed to lead to worst case failure modes
 - Power cable loss of function
 - Control cable worst of failure to operate or spurious operation
 - Fiber-Optic Cable loss of function/failure to operate (e.g., no spurious operation)
- No Task 10 Circuit Failure Mode Likelihood Analysis
 - All spurious operations assumed to occur with a conditional probability of 1.0
 - No credit taken for clearing of hot shorts
 - No credit taken for recovery of spuriously operated valves





- No qualitative screening for at-power FPRA
 - Minimum general transient assumed for any fire in any PAU
 - Lack of knowledge in the design stage makes it difficult to support claim that a fire in the plant will not result in at least a trip
- LPSD Qualitative Screening
 - POS 1, 2, 14 and 15 screened in Task 5 (subset of at-power fires with CDF ~1% of at-power fire CDF due to short POS durations)
 - Since plant is already tripped in POS 3A 13, fire must impact shutdown cooling, or result in loss of level control, if not, then no LPSD initiator
 - Different from at-power which assumes every fire has a CDF impact
 - 137 unscreened PAUs analyzed for POS 3A 13
 - Differs from NUREC/CR-7114 qualitative screening criteria which says to include all PAUs which contain credited equipment even if there is no initiator
 - Really only applicable in POS 1, 2, 14 and 15 which are screened





- At-power and LPSD FIRMs both based directly on their respective internal events models
 - In some cases surrogate events were used for spurious operations if the impact is the same (e.g., failures to close (FTC) basic event may be used as surrogate for spurious operation (SO)).
 - Basic events added for non-modeled spurious operations
- At-power Fires in each PAU assumed to result in either GTRN, LOCV, LODCA, LODCB, LOFW, LOOP, PLOCCW or SLOCA based on equipment damage
 - No other fire-induced initiators were identified
 - If no PRA equipment/cables are damaged it is assumed to result in at least a trip which is modeled as a general transient
 - All fire induced failures are assumed non-recoverable including OSP





- LPSD FIRM screens POS 7, 8, 9 (same basis as LPSD internal events model)
- Unscreened LPSD PAU fires assumed to result in either CC, JL, KV, LP, S2 or SL based on scenario equipment damage AND the POS
 - Loss of support system on operating train dependent upon POS
 - Assumed outage schedule is basis for operating trains and T/M schedule
 - Due to assumed outage schedule, PAU initiator may be different for each POS, e.g., "A" SC train assumed operating during POS 3A 6, "B" train assumed operating during 10 13, so a PAU only damaging the "B" SC train results in S2 event only during POS 10 13, no initiator during POS 3A 6
 - All fire induced failures are assumed non-recoverable including OSP





- At-Power Ignition Frequencies based on NUREG/CR-6850 (and Supplement 1) counting and apportioning methodology and EPRI 1016735, "Fire PRA Methods Enhancements: Additions,
 Clarifications, and Refinements to EPRI 1011989" for frequencies
 - Not currently updated to NUREG-2169
- LPSD Ignition Frequencies from NUREG/CR-7114
- Transient Influencing Factors for LPSD based on At-Power TIFs with adjustments based on Engineering Judgement
 - e.g., All Containment Building TIFs increased from low to high (1 to 10) for all LPSD POS due to increased work in containment
 - No effort was made to do a POS by POS adjustment





- Initial HFE HEPs estimated using NUREG-1921 Screening Analysis
- Top 10 HEPs (ranked by F-V) were re-evaluated using detailed HRA methodologies
- Fire PRA HRA used same level of dependency among dependent HFEs as at-power models
- Current PRA update is re-evaluating all HFEs using detailed HRA methodologies, and re-evaluating the dependency among fire HFEs





19.1.5.2 Internal Fire PRA – Tasks 7, 8 & 11

- No/limited knowledge of the ignition source target locational relationships
 - No way to perform "reasonably accurate" fire modeling
 - Full room burnout scenarios for PAUs for Quantitative Screening
 - Initial high CDF areas include the MCR, Containment, Turbine Building and 35 other single compartment PAUs
 - For "important" PAUs, the only detailed fire analysis involved:
 - Credit for automatic suppression systems
 - Credit for manual suppression in MCR and for hotwork fires
 - No fire modeling performed if suppression fails, then back to full room burnout scenario
- No knowledge of intervening combustibles
 - No screening of even the smallest ignition sources
 - Main impact is that all unscreened MCA scenarios are assumed to be possible





- Task 11 Detailed Analysis
 - Main Control Room
 - Abandonment scenarios
 - Containment
 - SLOCA potential and all 4 trains of instrumentation
 - Turbine Bldg.
 - Very Large IEF and OSP cables
 - 35 Other Single Compartments
 - Based on high initial CDF
 - Multi-Compartment Analysis
- Task 13 Seismic-Fire Interaction Analysis
 - All qualitative based on design documents





19.1.5.2 Internal Fire PRA – Results (At-power)

- At Power total of 480 SCA and 1054 MCA Scenarios
- Due to highly compartmentalized nature of the APR1400, CDF is generally well distributed
 - Only 24 scenarios are higher than 1% CDF
 - 50% of CDF in top 8 scenarios, 90% of CDF in top 45 scenarios
 - CDF concentrated in MCR, EDG and Electrical Equipment Rooms
 - MCR is ~1/3 of CDF due to conservative analysis
 - No alternative shutdown (ASD) procedure (CCDP assumed 0.1)





19.1.6.3 Internal Fire PRA – Results (LPSD)

- LPSD total of 918 SCA and 6071 MCA Scenarios
 - LPSD Fire Scenario defined by both IE and POS
- Like the at-power results, due to highly compartmentalized nature of the APR1400, CDF is generally well distributed
 - Only 22 scenarios are higher than 1% CDF
 - 50% of CDF in top 10 scenarios, 90% of CDF in top 59 scenarios
 - CDF concentrated in EDG and Electrical Equipment Rooms, and
 Ultimate Heat Sink (UHS) Building





19.1.5.3 Internal Flooding PRA





19.1.5.3 Internal Flooding PRA

Guidance

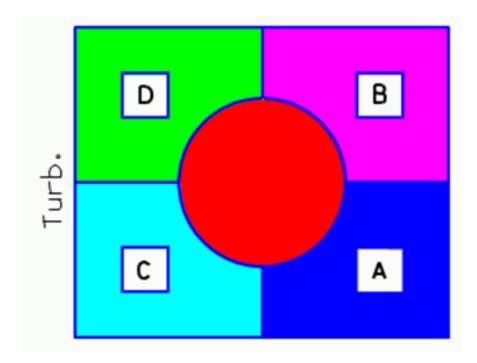
- RG 1.200 Revision 2
- ASME/ANS RA-Sa-2009, "PRA Standards"
- SRP 19.1
- EPRI 1021086, "Pipe Rupture Frequencies for Internal Flooding Probabilistic Risk Assessments" Revision 2





19.1.5.3 APR1400 Characteristics

- Auxiliary Building
 - Quadrant Design
 - Emergency overflow lines limit accumulation on upper elevations.
 - Limited flood sources







19.1.5.3 APR1400 Characteristics

- Turbine Building
- EDG Building (A/B)
- Compound Building
- CCW Heat Exchanger Building
- ESW Building





19.1.5.3 APR1400 Internal Flooding Analysis

- Flood-induced initiating event
 - Uncontrolled release of fluid that also fails PRA-related equipment.
 - Considers failures that result in reactor trip or require Technical
 Specification required shutdown within 24 hours.
- Flood propagation
 - Design flood barriers prevent propagation up to design level
 - Non-watertight doors fail at level of 1-foot if failure exacerbates accident,
 otherwise, doors remain intact (in general)
 - Barrier failures or other propagation pathways that ameliorate event are not considered.
 - Flow through drains, EOLs, other open pathways considered





19.1.5.3 APR1400 Internal Flooding Analysis

- Accident Sequence Analysis
 - Based on Internal Events Sequence
 - Over 130 events explicitly evaluated
 - Most events related to manual shutdown or assumed reactor trip
 - High Energy Line Breaks
 - Conservative treatment
 - HELB barriers intact up to design HELB
 - Break greater than design fail first barrier and actuates fire protection





19.1.5.3 Flooding Insights

- No one significant event
- Most events are related to beyond-design-basis fire protection breaks.
- Propagation potential expected to be less if as-built plant could be analyzed
 - Door failure potential
 - Design flood barrier height
- Most breaks do not require isolation or time available is long





19.1.5.4 Other External Events





19.1.5.4 Events Considered

- Most External Events Identified as COL Items
 - Reference DCD Table 2.0-1
- Transportation Accidents
 - COL Confirm
 - RG 1.76, 1.91, SRP 3.5.1.6
- Turbine Missiles
 - Favorable orientation
 - DCD 3.5.1.3 2.1E-09 per year with 12-year inspection interval
- Events Analyzed
 - High winds (including tornadoes)
 - External floods





19.1.5.4 COL Item

Site-Specific Risk Assessment

- Aircraft crash
- External flooding
- Extreme winds and tornadoes
- Industrial or military facility
- Lightning
- Pipeline accident
- Release of onsite chemicals
- River diversion/flooding
- Toxic gas
- Transportation accidents
- Storm Surge

Confirm No Outliers

- Avalanche
- Biological events
- Coastal erosion
- Dam failure
- Drought
- Forest fire
- High summer temperature
- Hurricane
- Landslide
- Low lake/river water level
- Low winter temperature
- Sandstorm
- Tsunami
- Volcanic activity





19.1.6 Low Power and Shutdown





19.1.6 Key Documents

- Regulatory
 - Trial ANS standard for shutdown PRA quality (March 2015)
 - RG 1.200 Revision 2
 - SRP 19.1
 - NUREG/CR-6144
- Industry
 - Approved submittal for AP1000
 - Submittals for EPR and US-APWR
- Support
 - EPRI shutdown initiating event data (TR-1003113)





19.1.6 LPSD Analysis Strategy

- Major Tasks
 - Plant Operating State Development
 - Initiating Events Analysis
 - Accident Sequence Analysis
 - Success Criteria Analysis
 - Systems Analysis
 - Data Analysis
 - Human Reliability Analysis
 - Analysis of Large Release
 - Quantification
- Same as at-power, plus POS development





19.1.6 Analysis philosophy of POSs

Make use of prior experience with current and next-generation analyses such as US-APWR and EPR: POSs Definitions from Various Sources

NUREG/CR-6144 Section 3.5 (June 1994)				
(1) Low Power Operation & Reactor Shutdown				
(2) Cooldown with Steam Generators to 345°F				
(3) Cooldown with Residual Heat Removal to 200°F				
(4) Cooldown to Ambient Temperatures (using RHR)				
(5) Draining the RCS to Mid-loop				
(6) Mid-loop Operation				
(7) Fill for Refueling				
(8) Refueling				
(9) Draining the RCS to Mid-loop After Refueling				
(10) Mid-loop Operations After Refueling				
(11) Refill RCS Completely (After Mid-loop Operation)				
(12) RCS Heatup Solid and Draw Bubble				
(13) RCS Heatup to 350°F				
(14) Startup with Steam Generators				
(15) Reactor Startup and Low Power Operation				





19.1.6 Analysis philosophy of POSs

APR1400 Plant Operating States

POS	Description	Primary System Water Level(1)	Primary System Pressure & Temperature	TS Mode
1	Reactor trip and Subcritical operation		2250 psia, 548-585°F	1, 2
2	Cooldown with Steam Generators to 350°F	In Pressurizer	2250-450 psia, 548–350°F	3
3A	Cooldown with Shutdown Cooling System to 212°F		450-15 psia, 350–212°F	4
3B	Cooldown with Shutdown Cooling System to 140°F		450-15 psia, 212–140°F	5
4A	Reactor Coolant System drain-down (pressurizer manway closed)		Slight positive pressure or dep ressurized; <140°F	5
4B	Reactor Coolant System drain-down (manway open)	Below Reactor Flange	Depressurized; <140°F	5
5	Reduced Inventory operation and nozzle dam installation	Below Reactor Fluinge		5
6	Fill for refueling			6
7	Offload	Cavity flooded		6
8	Defueled	N/A	N/A	Defueled
9	Onload	Cavity flooded	Depressurized or slight vacuu m during refill; <140°F	6
10	Reactor Coolant System drain-down to Reduced Inventory after refueling			6
11	Reduced Inventory operation with steam generator manwa y closure			5
12A	Refill Reactor Coolant System (pressurizer manway open)	Below Reactor Flange		5
12B	Refill Reactor Coolant System (manway closed)		Depressurized, or at a slightly elevated pressure; <140°F	5
13	Reactor Coolant System heat-up with Shutdown Cooling S ystem isolation at 350°F		15-450 psia, 140–350°F	4
14	Reactor Coolant System heat-up with steam generators	In Pressurizer	450-2250 psia, 350–548°F	3
15	Reactor startup		2250 psia, 548-585°F	2, 1

⁽¹⁾ When level changes during a POS, the minimum level is listed.





19.1.6 Initiating Event Selection

APR1400 uses a consistent set when compared to other current and next-generation PWRs

Event	Initiating Event Description	# of Events	# of Demands	Time (yrs)		degrees of freedom		Lower Confidence Limit	Error Factor
		n	D	Т	PE	f	UCL	LCL	EF
S1	Recoverable Loss of Shutdown Cooling System (*)	9		66.9	1.4E-01	19	2.25E-01	7.56E-02	2
S2	Unrecoverable Loss of Shutdown Cooling System	1		66.9	2.2E-02	3	5.84E-02	2.63E-03	5
S0	Over-drainage During Reduced Inventory Operation	2	874		2.9E-03	5	6.33E-03	6.55E-04	3
SL	Operation	1		5.1	2.9E-01	3	7.66E-01	3.45E-02	5
LL	Large LOCA	Generic NRC data used							
ML	Medium LOCA	Generic NRC data used							
	Small LOCA above reduced inventory	2		72	3.5E-02	5	7.69E-02	7.95E-03	3
SL	Small LOCA at reduced inventory	11		72	1.6E-01	23	2.44E-01	9.09E-02	2
	Small LOCA in transition modes	Generic NRC data used							
JL	Unrecoverable LOCA (CVCS Letdown Line)	NUREG/CR-6144 estimate used							
PL	POSRV Fails to Reclose	Generic NRC data used							
RL	LTOP Relief Valve Fails to Reclose	Generic NRC data used							
LP	Loss of Offsite Power	Generic NRC data used							
LX	Station Blackout	Transfer from LOSP fault tree							
CC	Partial Loss of Component Cooling	At-power fault tree used							
TC	Total Loss of Component Cooling	At-power fault tree used							
ES	Partial Loss of Essential Service Water	At-power fault tree used							
TS	Total Loss of Essential Service Water	At-power fault tree used							
KV	Loss of 4 kV Emergency Bus (SCS Power Supply)	2		72	3.5E-02	5	7.69E-02	7.95E-03	3
DC	Loss of 125 VDC Bus	At-power fault tree used							
SG	Steam Generator Tube Rupture	Generic NRC data used							

IE Point Estimates from TR-1003113 Data Since 1994





19.1.6 Initiating Event Point Estimates

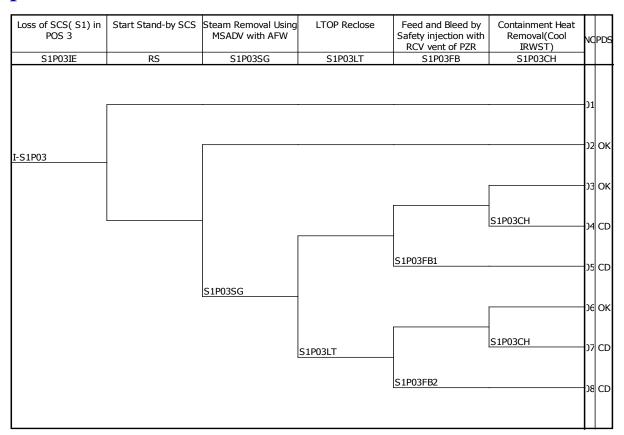
- An appropriate combination of generic and designspecific initiating event frequencies used
- Design-specific initiating events used fault tree development for the point-estimates





19.1.6 Accident Sequence Analysis

- The AS analysis models the combinations of system responses and operator actions that could occur during the event
- Event Tree analysis is used to delineate these combinations to present these events

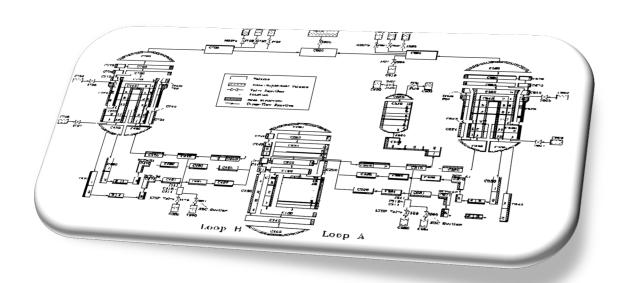






19.1.6 Success Criteria

- Using MAAP 4.0.8 and RELAP5/mod3
- Considering the initiating event, limiting plant conditions for each POS, and equipment availability specified for each accident sequence
- Core Damage is defined based on the ASME PRA Standard and NRC Inspection Manual Chapter 0609 (2005)







19.1.6.2 LPSD Level 2 Analysis

- For POSs with RCS and containment intact, Level 2 conservatively estimated using the full power conditional probability of large release (CPLR)
- For POSs with RCS intact but containment hatch open, failure to close hatch assumed to be large release. Successful closure of hatch before boiling evaluated using full power CPLR
- For POSs with RCS head removed, detailed Level 2 PRA developed. For portions of the analysis, the full power Level 2 models are conservatively used as bounding estimates.
- LPSD Level 2 Fire modeling same as internal events





19.1.6 LPSD Insights

- Results are dominated by operator recovery failures
- Results indicate, as expected, that the draindown and reduced inventory POSs are highly risk significant





AAC	alternate alternating current
AC	alternating current
AF	auxiliary feedwater
ANS	American Nuclear Society
APR1400	Advanced Power Reactor 1400
ASME	American Society of Mechanical Engineers
ATWS	anticipated transient without scram
BOP	balance of plant
CC	component cooling water
CCDP	conditional core damage probability
CCF	common cause failure
CCW	component cooling water
CDF	core damage frequency
CET	1) containment event tree, 2) core-exit thermocouple
CFF	containment failure frequency
CFS	cavity flooding system
COL	combined license
CS	containment spray
DC	direct current
DCD	Design Control Document
DCH	direct containment heating
DET	decomposition event tree
DG	diesel generator
ECSBS	emergency containment spray backup system
EDG	emergency diesel generator





EOL	emergency overflow line
EPRI	Electric Power Research Institute
FCI	fuel-coolant interaction
FIRM	fire risk model
FMEA	failure modes and effects analysis
GTRN	general transient
HCLPF	high confidence of low probability of failure
HELB	high-energy line break
HEP	human error probability
HFE	human failure event
HVAC	heating, ventilation, and air conditioning
I&C	instrumentation and control
IRWST	in-containment refueling water storage tank
ISLOCA	interfacing systems loss of coolant accident
KEPCO	Korea Electric Power Corporation
KEPCO E&C	KEPCO Engineering & Construction Company
KHNP	Korea Hydro & Nuclear Power Company
LOCA	loss-of-coolant accident
LOCV	loss of condenser vacuum
LODCA	loss of dc power (Train A)
LODCB	loss of dc power (Train B)
LOFW	loss of main feedwater
LOOP	loss of offsite power
LPSD	low power and shutdown
LRF	large release frequency
MAAP	modular accident analysis program





MCA	multiple compartment analysis
MCCI	molten core-concrete interaction
MCR	main control room
MFW	main feedwater
MSPI	mitigating systems performance index
NRC	U.S. Nuclear Regulatory Commission
NUREG	NRC technical report designation
NUREG/CR	NRC technical report designation – performed by contractor
OSP	offsite source permissive
PAR	passive autocatalytic recombiners
PAU	physical analysis unit
PDS	plant damage state
POS	plant operational state(s)
POSRV	pilot-operated safety relief valve
PRA	probabilistic risk assessment
RCP	reactor coolant pump
RCS	reactor coolant system
RG	Regulatory Guide
RPV	reactor pressure vessel
RVR	reactor vessel rupture
SBO	station blackout
SC	1) success criteria analysis, 2) shutdown cooling
SDP	significance determination process
SEL	seismic equipment list
SG	steam generator
SGTR	steam generator tube rupture





SI	safety injection
SLOCA	small break loss of coolant accident
SMA	seismic margin analysis
SOV	solenoid operated valve
SRP	Standard Review Plan
SSCs	structures, systems, and components
SX	essential service water system
UPC	ultimate pressure capacity





APR1400 DCA

Probabilistic Risk Assessment and Severe Accident Evaluation : Chapter 19.2



KEPCO/KHNP April 19, 2017





Overview of Chapter 19 (1/2)

Section Overview

Section	Title	Presenter
19.0	Probabilistic Risk Assessment and Severe Accident Evaluation	
19.1	Probabilistic Risk Assessment	Young In
19.1.1	Uses and Applications of the PRA	
19.1.2	Quality of PRA	
19.1.3	Special Design/Operational Features	
19.1.4	Safety Insights from the Internal Events PRA for Operations at Power	
19.1.4.1	Level 1 Internal Events PRA for Operations at Power	Greg Rozga/ Ray Dremel/ Robert Lichtenstein
19.1.4.2	Level 2 Internal Events PRA for Operations at Power	Tae-Hee Hwang/ Jeff Leary
19.1.5	Safety Insights from the External Events PRA for Operations at Power	
19.1.5.1	Seismic Risk Evaluation	Dong-Won Lee/ Kyu-Ho Hwang/ Ray Dremel
19.1.5.2	Internal Fire Risk Evaluation	Greg Rozga
19.1.5.3	Internal Flooding Risk Evaluation	Ray Dremel
19.1.5.4	Other External Events Risk Evaluation	
19.1.6	Safety Insights from the PRA for Other Modes of Operation	
19.1.6.1	Level 1 Internal Events PRA for Low Power and Shutdown Operations	Jaegab Kim/ Ross
19.1.6.2	Level 2 Internal Events PRA for Low Power and Shutdown Operations	Anderson/ Jeff Leary
19.1.6.3	Internal Fire PRA for Low Power and Shutdown Operations	
19.1.6.4	Internal Flooding PRA for Low Power and Shutdown Operations	
19.1.7	PRA-Related Input to Other Programs and Processes	Young In
19.1.8	Conclusions and Findings	



Overview of Chapter 19 (2/2)

• Section Overview

Section	Title	Presenter		
19.2	Severe Accident Evaluation			
19.2.1	Introduction			
19.2.2	Severe Accident Prevention			
19.2.3	Severe Accident Mitigation	Byung Jo Kim		
19.2.4	Containment Performance Capability			
19.2.5	Accident Management			
19.2.6	Consideration of Potential Design Improvement under 10 CFR 50.34(f)			
19.3	Beyond Design Basis External Event			
19.3.1	Introduction	Chan-Eok Park		
19.3.2	NTTF Tier 1 Recommendation	Onun Zon I um		
19.3.3	NTTF Tier 2 and 3 Recommendation			
19.4	Loss of Large Area			
19.4.1	Introduction and Background	Gary Hayner		
19.4.2	Scope of the Evaluation			
19.4.3	Conclusions			
19.5	Aircraft Impact Assessment			
19.5.1	Introduction and Background			
19.5.2	Scope of the Assessment	Randy James		
19.5.3	Assessment Methodology			
19.5.4	Conclusions			

Overview of Chapter 19.2

Section Overview

- 19.0 Probabilistic Risk Assessment and Severe Accident Evaluation
- 19.1 Probabilistic Risk Assessment
- 19.2 Severe Accident Evaluation
- 19.2.1 Introduction
- 19.2.2 Severe Accident Prevention
- 19.2.2.1 Anticipated Transient Without Scram
- 19.2.2.2 Mid-Loop Operation
- 19.2.2.3 Station Blackout
- 19.2.2.4 Fire Protection
- 19.2.2.5 Intersystem Loss-of-Coolant Accident
- 19.2.2.6 Other Severe Accident Preventative Features
- 19.2.3 Severe Accident Mitigation
- 19.2.3.1 Overview of Containment Design
- 19.2.3.2 Severe Accident Progression
- 19.2.3.3 Severe Accident Mitigation Features
- 19.2.4 Containment Performance Capability
- 19.2.4.1 Containment Performance Goal
- 19.2.4.2 Containment Performance Analysis
- 19.2.5 Severe Accident Management Framework
- 19.2.5.1 Severe Accident Management Framework
- 19.2.6 Consideration of Potential Design Improvements under 10 CFR 50.34(f)
- 19.2.7 Combined License Information





19.2.1 Introduction

- Regulation Considerations
 - Severe Accident evaluation for APR1400 design is consistent with the applicable guidance:
 - SECY-93-087
 - 10 CFR Part 100
 - 10 CFR Part 50 Appendix A,
 - 10 CFR 50.34 (f)
 - 10 CFR 50.44
 - RG 1.216
 - SECY-90-016





19.2.2 Severe Accident Prevention (1/2)

- Anticipated Transient Without Scram
 - Digital safety system and diverse protection system
- Mid-Loop Operation
 - Instrumentation for shutdown operation, SCS design,
 SG nozzle dam integrity, Alternate decay heat removal methods
- Station Blackout
 - AAC automatically start and is manually aligned to provide power to a Class 1E 4.16 kV when EDGs fail
- Fire Protection
 - Fire detection, automatic and manual fire suppression, and fixed fire barriers





19.2.2 Severe Accident Prevention (2/2)

• Intersystem LOCA

- ISLOCA can be occurred at SIS, SCS, CVCS, CSS, etc.
- All sections of the system and interfaces are designed to withstand full RCS operating pressure, or have a leak-test capability, valve position indicators in the control room, high pressure alarms to warn operators

• Other SA preventive Features

- Two independent turbine driven AFPs when on/off-site AC power are not available
- SC pumps can be used as a backup of CS pumps during LOCA event
- Feed-and-Bleed operation using the SIS and POSRVs





19.2.3 Severe Accident Mitigation

- 19.2.3.1 Overview of Containment Design
- 19.2.3.2 Severe Accident Progression
- 19.2.3.3 Severe Accident Mitigation Features





19.2.3.1 Overview of Containment Design

Generals

- Prestressed concrete structure with cylindrical and dome part
- Cylinder wall thickness: 1.37 m (4 ft 6 in)
- Steel liner plate with 6.0 mm thickness on the inside of the dome and cylindrical wall to provide leak-tightness
- Design characteristics in terms of SA management
 - Large free volume and dry-type containment
 - Accommodation of condensable and non-condensable gas
 - Natural mixing throughout the containment atmosphere

• Pressure limits

- Design to meet SA internal pressurization challenges
- Meet the FLC requirements for a period of 24 hours from the onset of core damage, and following this initial 24 hour period





19.2.3.2 Severe Accident Progression (1/3)

In-Vessel melt progression

- Core heatup resulting from loss of adequate cooling
- Metal-water reaction and cladding oxidation, core damage
- Melting and relocation of cladding, structural materials, and fuel
- Formation of melt pool and crust, and failure of crust in core region
- Drainage of molten material to the lower head
- Formation of melt pool and crust in the lower plenum
- Reactor vessel breach

Five vessel failure mechanism in MAAP code

- Local ablation of vessel wall by molten jet impingement
- Melt ingress into a penetration tube
- Ejection of a penetration tube
- Creep rupture of the lower head
- Attack of the vessel wall by overlying metal layer





19.2.3.2 Severe Accident Progression (2/3)

- Ex-Vessel melt progression
 - Key parameters:
 - RCS pressure, vessel failure mode and timing, corium releasing characteristics, cavity floor concrete type, availability of cavity flooding, etc.
- Events can cause the containment failure:
 - HPME and DCH
 - High RCS pressure at the time of vessel breach
 - EVSE
 - Dynamic load generated from rapid mixing with water in the cavity
 - MCCI
 - Containment basemat melt-through
 - Pressurization from evolved steam and non-condensable gases
 - Production of combustible gases
 - Hydrogen combustion
 - Dynamic explosion or deflagration





19.2.3.2 Severe Accident Progression (3/3)

- Effort to reduce uncertainty considered in ex-vessel accident progress
 - EVSE:
 - Base case with realistic input parameters
 - Sensitivity cases with bounding input parameters
 - DCH:
 - Sampled input values by Latin Hyperbolic Sampling technique
 - MCCI and H₂ risk:
 - Conservative input values to increase concrete ablation depth and hydrogen generation
 - Selection of accident sequences:
 - Combination of probabilistic and deterministic approach





19.2.3.3 Severe Accident Mitigation Features (1/8)

- Hydrogen Generation and Control
 - Criteria: 10 CFR 50.34(f), 10 CFR 50.44(c)
 - Generation: 100% metal-water reaction (MWR)
 - Control: less than 10% of H₂ concentration inside the containment
 - Mitigation features: Containment, PARs, Igniters
 - Large free volume containment
 - 30 PARs and 8 igniters throughout the containment
 - Meet the Seismic Category I
 - Analysis methodology: Generation and Distribution of H_2
 - MAAP4.0.8
 - Highly probable sequences from PRA Level 1 study && Representative deterministic sequences (LLOCA, MLOCA, SLOCA, SBO, and TLFOW)
 - 100% MWR in "in-vessel phase" + additional source in "ex-vessel phase"





19.2.3.3 Severe Accident Mitigation Features (2/8)

- Hydrogen Risk (cont'd)
 - Analysis methodology: Flame Acceleration and DDT possibility
 - H₂-steam-air mixture for all containment nodes from MAAP study
 - Applying σ -criterion for FA, 7λ -criterion for DDT
 - Analysis methodology: Slow deflagration
 - Hydrogen source equivalent to 100% MWR
 - Conservative and bounding pressure by AICC assumption
 - Analysis results
 - Achieving a well-mixed containment atmosphere
 - Achieving a H₂ concentration less than 10 %
 - No possibility of FA and DDT occurrence
 - AICC pressure meets the FLC requirement (see 19.2.4.2)





19.2.3.3 Severe Accident Mitigation Features (3/8)

- MCCI and Core Debris Coolability
 - Goal: Secure the basemat liner integrity
 - Minimize corium-concrete attack
 - Remove heat from the core debris
 - Minimize generation of gases
 - Scrub fission products
 - Mitigation features: Reactor cavity, cavity floor concrete, CFS
 - Cavity with large floor area and no obstacles for corium spreading
 - Concrete layer on the basemat liner with 3 feet thickness
 - Flooding the water from IRWST initiated by manual opening of MOVs at the time of severe accident entry
 - Supplying the sufficient water to cavity by gravity driven flow





19.2.3.3 Severe Accident Mitigation Features (4/8)

- MCCI (cont'd)
 - Analysis methodology: Conservative preparation of model parameters
 - MAAP4.0.8's user-dependent key parameters:
 - Jet breakup
 - Heat removal to overlying water pool
 - CORQUENCH study for conservative Large LOCA sequence
 - High decay heat, full core relocation, no jet breakup
 - Very conservative ablation depth is predicted (0.27 m or 0.86 ft)
 - Decision of MAAP model parameters
 - To get a comparable ablation depth from CORQUENCH study for conservative Large LOCA sequence
 - Analysis results:
 - Large LOCA: 0.24 m (0.79 ft) << 0.91 m (3 ft)
 - Therefore the integrity of basemat liner can be preserved





19.2.3.3 Severe Accident Mitigation Features (5/8)

HPME and DCH

- Goal: Prevent early containment failure by DCH
 - Provide reasonable depressurization system to prevent HPME
 - Minimize entrained debris to upper containment compartments
- Mitigation features: Rapid depressurization system, reactor cavity
- Analysis methodology:
 - Rapid depressurization analysis using MAAP 4.0.8 code
 - DCH analysis using NUREG/CR-6338 methodology
- Analysis results
 - RCS pressure at reactor vessel failure: less than DCH cutoff pressure (17.6 kg/cm² [250 psi])
 - CCFP in APR1400 containment: less than 0.01 percent (0.0001)





19.2.3.3 Severe Accident Mitigation Features (6/8)

- FCI (In-vessel / Ex-vessel steam explosion)
 - Analysis methodology
 - Setup the initial conditions
 - IVSE: single and multi-jets configuration
 - EVSE: base case & sensitivity cases based on MAAP prediction
 - Evaluation of energetic loads
 - TEXAS-V code
 - Assessment of structural integrity
 - Vessel load head and cavity wall response using FEM code
 - Analysis results
 - Integrity of the lower head and the cavity wall are preserved
 - EVSE under IVR-ERVC: COL 19.2(3)





19.2.3.3 Severe Accident Mitigation Features (7/8)

- ES (Equipment Survivability)
 - Purpose
 - Provide reasonable assurance that the equipment and instrumentation can operate under severe accident environment over the required time span
 - Assessment methodology
 - Identification of required equipment and instrumentation
 - Evaluation of severe accident environmental conditions
 - Using MAAP4.08 code for selected sequences
 - Determination of bounding conditions for equipment
 - Containment gas temperature, pressure, radiation
 - Assessment the survivability
 - Comparison with equipment suppliers' test data
 - Comparison with equipment survivability test data
 - Analytical methodology: Thermal lag analysis
 - Alternative means





19.2.3.3 Severe Accident Mitigation Features (8/8)

- ES (Equipment survivability) (cont'd)
 - Assessment results
 - Site-specific equipment survivability assessment: COL 19.2(1)
 - COL 19.2(1): The COL applicant and/or holder is to perform and submit site-specific equipment survivability assessment in accordance with 10 CFR 50.34(f) and 10 CFR 50.44 which reflects the equipment identified and the containment atmospheric assessments of temperature, pressure and radiation described in Subsection 19.2.3.3.7.





19.2.4 Containment Performance Capability

- 19.2.4.1 Containment Performance Goal
- 19.2.4.2 Containment Performance Analysis





19.2.4.1 Containment Performance Goal

- Criteria for Containment
 - SECY 93-087
 - For the first 24 hours, containment maintain its role as a reliable, leak-tight barrier (meets the FLC requirement) under the more likely severe accident challenges
 - Following initial 24 hours, containment should continue to provide a barrier against the uncontrolled release of fission product
 - RG 1.216
 - Position 2, Combustible Gas Control Inside Containment
 - Pressure load from H_2 mass and energy releases generated from a 100% MWR accompanied by the burning of H_2
 - Position 3, Commission's Severe Accident Performance Goal
 - Pressure load from more likely severe accident challenges





19.2.4.2 Containment Performance Analysis (1/2)

- Combustible Gas Control (RG 1.216 Position 2)
 - Analysis methodology
 - H₂ mass from 100% MWR and ignoring PARs, igniters
 - Adiabatic Isochoric Complete Combustion (AICC) approach
 - Various steam fraction is considered to get a maximum pressure
 - Analysis results
 - Predicted AICC pressure (123.7 psia) is applied to FEM study
 - FEM study indicates maximum strain of liner plate do not reach the allowable limit
 - Therefore, conservative H₂ combustion load meets FLC requirement





19.2.4.2 Containment Performance Analysis (2/2)

- More likely SA challenges (RG 1.216 Position 3)
 - Accident selection (Position 3.1 a)
 - Sequences are selected to cover around 90% of cumulative CDF from PRA Level 1 study (draft)
 - 5 representative initiators (Large and Small LOCA, SBO, SGTR, LOFW) are taken into account in the light of the deterministic approach with having conservative accident progress
 - MAAP 4.0.8 calculation for the selected sequences (Position 3.1 b)
 - CFS and POSRVs assumed to be operable
 - ECSBS operates at 24 hours from the onset of SA
 - Determine a bounding pressure profile and peak pressure
 - 3-dim. finite element model study (Position 3.1 c)
 - Maximum strain in the liner plate remains in elastic region
 - Therefore, SA load does not threat the containment integrity





19.2.5.1 SA Management Framework (1/2)

- Actions taken during the course of an accident to
 - prevent core damage,
 - Ex) non-LOCA:
 - Secondary side cooling by two MD and two TD AFW pumps.
 - If secondary cooling failed, once-through cooling of the core using SI and SC or CS pumps after depressurization by POSRVs
 - terminate the progress of core damage if it begins and retain the core within the reactor vessel, including ERVC strategy,
 - Ex) Try to inject water by SI. If SI failed, open POSRVs to depressurize RCS and allow injection using SC or CS pumps
 - ERVC may be achieved by using SC pumps to submerge the reactor vessel lower head in water
 - maintain containment integrity as long as possible, and
 - Ex) isolation the containment, operation of CFS to terminate MCCI,
 - minimize offsite releases.
 - Ex) operation of CS to remove fission products by CS/SC pumps or ECSBS





19.2.5.1 SA Management Framework (2/2)

- COL applicant is to develop and submit an AM plan (COL item 19.2(3)) that addresses
 - a systematic evaluation of plant functions during potential SA,
 - implementation of the necessary enhancements,
 - severe accident management guidelines and training,
 - In Vessel Retention-External Reactor Vessel Cooling strategy





Summary of Chapter 19.2

- APR1400 Severe Accident Evaluation
 - SA prevention and mitigation features are designed to conform to associated Criteria and Requirements
 - H₂ risk, MCCI, FCI, DCH, ES are investigated and meet the relevant requirements
 - Containment integrity is consistent with RG 1.216
 - AM plan will be established (COL19.2(3))





Attachment: Acronyms & Abbreviations

AAC	Alternative Alternating Current
AICC	Adiabatic Isochoric Complete
	Combustion
AFP	Auxiliary Feedwater Pump
ATWS	Anticipated Transient Without Scram
CCFP	Conditional Containment Failure
	Probability
CDF	Core Damage Frequency
CFS	Cavity Flooding System
CVCS	Chemical Volume Control System
CS	Containment Spray
DCH	Direct Containment Heating
DDT	Deflagration-to-Detonation Transition
ECSBS	Emergency Containment Spray Backup System
EDG	Emergency Diesel Generator
ES	Equipment Survivability
EVSE	Ex-Vessel Steam Explosion
FA	Flame Acceleration
FCI	Fuel Coolant Interaction
FEM	Finite Element Model
FLC	Factored Load Category
НРМЕ	High Pressure Melt Ejection
IRWST	In-containment Refueling Water Storage Tank
IVR-ERVC	In-Vessel Retention and External Reactor Vessel Cooling





Attachment: Acronyms & Abbreviations

IVSE	In-Vessel Steam Explosion
LHS	Latin Hypercube Sampling
LOCA	Loss Of Coolant Accident
LOFW	Loss Of Feed Water
LOOP	Loss Of Offsite Power
MCCI	Molten Core Concrete Interaction
MD	Motor Driven
MOV	Motor Operated Valve
MWR	Metal Water Reaction
PAR	Passive Autocatalytic Recombiner
POSRV	Pilot Operated Safety Relief Valve
PRA	Probabilistic Risk Assessment
RCS	Reactor Coolant System
SA	Severe Accident
SAMDA	Severe Accident Mitigation Design
	Alternatives
SBO	Station BlackOut
SCS	Shutdown Cooling System
SGTR	Steam Generator Tube Rupture
SIS	Safety Injection System
TCE	Two Cell Equilibrium
TD	Turbine Driven
TLOFW	Total LOFW







Presentation to the ACRS Subcommittee

Korea Hydro & Nuclear Power Co., Ltd (KHNP) and Korea Electric Power Corporation (KEPCO)

APR1400 Design Certification Application Review

Safety Evaluation Report with Open Items

Chapter 19.1 - PROBABILISTIC RISK ASSESSMENT Chapter 19.2 - SEVERE ACCIDENT EVALUATION

Staff Review Team



Technical Staff

- ♦ Hanh Phan (Lead), Senior Reliability and Risk Analyst, PRA & Severe Accidents Branch
- ◆ Odunayo Ayegbusi, Reliability and Risk Analyst, PRA & Severe Accidents Branch
- ♦ Anne-Marie Grady, Reactor Systems Engineer, Containment & Ventilation Branch
- ◆ Tony Nakanishi, Reliability and Risk Analyst, PRA & Severe Accidents Branch
- Alissa Neuhausen, General Engineer, Structural Engineering Branch
- Marie Pohida, Senior Reliability and Risk Analyst, PRA & Severe Accidents Branch
- ◆ Robert Roche-Rivera, Structural Engineer, Structural Engineering Branch
- ◆ Jason Schaperow, Senior Reliability and Risk Analyst, PRA & Severe Accidents Branch
- ◆ Courtney St. Peters, Reliability and Risk Analyst, PRA & Severe Accidents Branch
- Hanry Wagage, Senior Reactor Engineer, Containment & Ventilation Branch

Project Managers

- ◆ Jeffrey Ciocco, Lead Project Manager
- ◆ James Steckel, Chapter Project Manager

Presentation Outline



Chapter 19.1 - Probabilistic Risk Assessment (PRA)

- 1) Quality of APR1400 PRA (Phan)
- 2) Internal Events At-Power Level 1 PRA (Ayegbusi, St. Peters)
- 3) Internal Fire and Flood At-Power Level 1 PRA (Nakanishi)
- 4) Internal Events, Fire, and Flood At-Power Level 2 PRA (Wagage)
- 5) PRA-Based Seismic Margin Assessment (Neuhausen, Roche-Rivera, Phan)
- 6) Other External Events Evaluation (Phan)
- 7) Internal Events During Low-power and Shutdown Levels 1 and 2 PRA (Pohida)
- 8) Internal Fire and Flood During Low Power and Shutdown Levels 1 and 2 PRA (Nakanishi)
- 9) Uses and Applications of PRA (Phan)
- 10) Results and Conclusion (Phan)



Quality of APR1400 PRA

Hanh Phan

Quality of APR1400 PRA



- Ensured the applicant's justification is reasonable and acceptable
 - Scope
 - Level of details
 - ♦ Technical adequacy
 - PRA maintenance and upgrade
- Focused on the information provided in DCD Section 19.1.2 and Table 19.1-1
- Examined the results from the peer review
- Confirmed that the deficiencies would not significantly impact the PRA results and risk insights
- The staff is currently unable to finalize its conclusion on the acceptability of PRA scope, level of details, technical adequacy

PRA Conversion from SAREX to CAFTA



- Initiated during Phase 1 review, June 2015
- Completed in July 2016
- Incorporated:
 - Some of 59 findings from the peer review
 - ♦ Some of the staff findings
 - ♦ KHNP/KEPCO self-identified issues
- The staff finds:
 - SAREX model and CAFTA model results are not identical
 - Differences between CDFs, LRFs, CCFPs, and risk insights are minor
- Applicant agreed to:
 - Perform self-assessment on the CAFTA model
 - Notify the staff on the changes and results
 - Update PRA notebooks
 - ♦ Revisit all sensitivity studies & RAI responses using CAFTA model
 - Revise the DCD

Peer Review



- Peer review was performed during the week of June 24 28, 2013, against the PRA Standard, ASME/ANS RA-Sa-2009
- Conducted by a team of 6 PRA experts with over 170 years of diverse PRA experience
- The scope included at-power IEs Level 1, at-power IF Level 1, and LRF
- Peer review resulted in 90 Fact & Observations (59 "Findings," 27 "Suggestions," and 4 "Best Practices")
- Peer review report concluded that "The APR1400 PRA substantially meets both the ASME PRA Standard and the draft ALWR Standard at Capability Category II or better for 88% of the applicable Supporting Requirements, with 90% met at Capability Category I or better"

Peer Review (continued)



- The staff obtained insights of the degree to which the APR1400 PRA has been assigned to the capability categories of ASME/ANS Standard
- Together with the staff safety review, the peer review was used to identify the strengths and weaknesses of the PRA and to gain confidence in the PRA model and results
- The staff finds:
 - ♦ Peer review "Findings" have not been completely dispositioned
 - Some "Findings" were addressed by performing sensitivity studies
 - ♦ Several inconsistencies between the DCD and the peer review report
- The applicant agreed to:
 - Disposition all "Findings" and update the DCD during Phase 4 review



Internal Events At-Power Level 1 PRA

Odunayo Ayegbusi Courtney St. Peters



Internal Events (IEs) At-Power Level 1 PRA

Initiating Events, Success Criteria, Event Sequences, and Quantification

Odunayo Ayegbusi

IEs PRA - Initiators, Success Criteria, Event Sequences, and Quantification



- Reviewed APR1400 DCD Section 19.1.4.1.1 in accordance with SRP 19.0 acceptance criteria (SRP 19.0.II.7)
- Reviewed peer review report and planned resolution which led to less detailed review of the PRA
- Audited APR1400 PRA notebooks at varying levels of detail (audited 70% of each notebook)
- Reviewed DCD references for applicability and use
- Held public meetings with KHNP/KEPCO staff about technical issues and RAIs leading to proposed DCD markups
- The staff found these DCD sections mostly acceptable

Initiating Events and Success Criteria



- New or unique initiating events to the APR1400 design
 - ♦ KHNP/KEPCO did not identify new or unique events
 - ♦ A few NUREG/CR-6928 initiating events initially not evaluated
 - RAI issued and closed to confirmatory action item
- APR1400 success criteria
 - ◆ Chapter 19 success criteria more conservative than Chapter 15
 - ♦ KHNP/KEPCO evaluated inconsistencies and revised DCD
 - RAI issued and closed to confirmatory action item
- PRA model software conversion
 - New platform will incorporate peer review findings and observations
 - Potential impact on PRA modeling and results
 - ♦ RAI issued to review changes and impact on current DCD revision



Internal Events At-Power Level 1 PRA

Data Analysis, System Analysis, and Human Reliability Analysis

Courtney St. Peters

IEs PRA - Data Analysis, System Analysis, and Human Reliability Analysis



- Reviewed applicable APR1400 DCD sections in 19.1
- Reviewed peer review report
- Reviewed a sampling of PRA and system notebooks during audit
- Discussed questions during audit and RAIs if additional information was needed for staff findings
- Discussed technical topics at public meetings
- Ensured consistency with other DCD chapters (e.g. I&C, human factors)
- Reviewed key assumptions and followed up on additional justifications (i.e., room heatup/HVAC)
- The staff found these DCD sections mostly acceptable

Digital Instrumentation and Controls



- The staff review found a lack of detail regarding digital I&C system modeling in the PRA including, but not limited to:
 - System description
 - Key assumptions
 - CCF analysis of both hardware and software
 - Failure effects
- Staff has no findings currently due to continued lack of information
- Public meeting with KHNP/KEPCO staff was held on March 17, 2017, where KHNP/KEPCO committed to provide additional information and an approach to close out this open item

Digital Instrumentation and Controls (continued)



- KHNP/KEPCO staff committed to:
 - ♦ Discuss COMMON Q software similarities with Westinghouse
 - Evaluate level of model detail currently provided in the PRA
 - ♦ Evaluate architecture of digital I&C compared to reference plant
 - Add software CCF events to the PRA
 - Incorporate information provided into next PRA update and update the DCD

RCP Seal LOCA



- RCP seal LOCA is evaluated as a model uncertainty and sensitivity analysis
- KHNP/KEPCO assumed a failure probability 1×10⁻³ per pump based on engineering judgement before performing a seal LOCA model
- Staff requested additional justification
- APR1400 RCP Seal Model testing results (proprietary information) supported this assumption
- KHNP/KEPCO will revisit model uncertainty and sensitivity analysis as part of the PRA update



Internal Fire and Flood At-Power Level 1 and Level 2 PRA

Tony Nakanishi

Internal Fire Level 1 PRA



- Reviewed the extent to which applicant's FPRA information is consistent with the applicable methods in NUREG/CR-6850
 - ◆ Certain tasks were not performed or used simpler analyses since design details are unknown at design certification stage (e.g., specifics of cable routing, ignition sources, and target locations)
- Review focused on methodology and assumptions since significant model changes in conjunction with PRA model conversion were expected

Cable Protection



- In certain risk-significant compartments, cables were assumed to be either protected (e.g., circuits rerouted or redesigned to prevent failure), or can be shown through detailed circuit analysis to not result in the modeled failure mode
- Applicant identified a COL item to ensure that fire protection features required for preventing fire-induced damage of the PRA-credited components will be properly incorporated in the cable design for the as-built condition

Internal Flood Level 1 PRA



- Reviewed the extent to which applicant's internal flood PRA information is consistent with ASME/ANS standard requirements
- Staff considered results peer review, which found that the internal flood PRA generally met the ASME/ANS requirements for at least Capability Category I
- Staff confirmed detailed identification and characterization of flood areas and flood sources, systematic development of flood scenarios

Maintenance-Induced Floods



- Applicant screened out flooding initiating events caused by inadvertent operation or erroneous operation of a plant component during maintenance
- In response to staff RAI, applicant identified COL Item for COL applicant/holder to demonstrate that maintenanceinduced floods are negligible contributors to flood risk when plant-specific information is available



Internal Events, Internal Fire, and Internal Flood At-Power Level 2 PRA

Hanry Wagage

Internal Events Level 2 PRA



- Reviewed APR1400 DCD Section 19.1 related to Level 2 internal events PRA in accordance with SRP 19.0
- Reviewed Level 2 methodology (PDS, CET/DET, and Release Categories)
- Audited APR1400 PRA Notebooks
- Reviewed peer review report
- Discussed technical issues with the applicant during public meetings

Release Category Analysis



- Csl release fraction for STC-21 is 357 times higher than that for STC-17 (5.0 versus 0.014 percent of total core inventory) while the release opening area was only 10 times larger (1.0 versus 0.1 ft²)
- The applicant found a lack of re-vaporization of fission products for STC-17 caused by high pressure in the containment providing better cooling of external surface of the pressurizer
- The staff found that the applicant's justification for the difference reasonable and acceptable

Internal Fire and Internal Flood Level 2 PRA



- In response to staff RAIs, the applicant stated that the quantification process for Level 2 internal fire and internal flooding is the same as that for Level 2 internal events and proposed DCD changes
- The staff finds that the applicant's evaluation of Level 2 internal fire and internal flooding acceptable



PRA-Based Seismic Margin Assessment (SMA)

Alissa Neuhausen Robert Roche-Rivera Hanh Phan

PRA-Based SMA



- Ensured the applicant's seismic margin assessment is reasonable and acceptable
 - ♦ Scope
 - Level of details
 - ♦ Technical adequacy
- Focused on the information provided in DCD Section 19.1.5.1 and Table 19.1-47
- Examined the results of the seismic margin assessment (HCLPF calculations report is available for audit)
- Status of plant level HCLPF capacity

Seismic Fragility Evaluation



- The staff examined DCD Section 19.1.5.1
 - ♦ Initial submittal included HCLPF capacities for structures and components based on reference plant design response spectra
- The applicant clarified approach to SMA fragility evaluation
 - Applicant provided fragility calculations
 - Conservative Deterministic Failure Margin Approach
 - ♦ HCLPF capacity referenced to APR1400 CSDRS
- The staff finds:
 - Seismic fragility evaluation is in accordance with guidance in DC/COL-ISG-20
 - ♦ Site-independent structure HCLPF capacities >= 0.5g
 - Component HCLPF capacities >= 0.5g
 - ♦ Site-dependent structure HCLPF capacities >= 1.67xGMRS PGA

PRA-based SMA Scope and Method



- The method used to assess the at-power seismic margins is acceptable
- The PRA-based SMA during LPSD was not addressed in the DCD
- Staff requested seismic-induced dominant mixed cutsets containing seismic failures, random failures, and operator actions, and, the sequence-level HCLPF capacities during at-power and LPSD modes



Other External Events Evaluation

Hanh Phan

Other External Events



- Staff ensured that:
 - ♦ The applicant's assessment is comprehensive in scope
 - ◆ The approach used for the screening conforms to the guidance
 - ◆ The screening criteria and/or justification used to support the screening out of an external event are rational and acceptable
 - ♦ APR1400 external hazard treatment is reasonable
- ASME/ANS PRA Standard, Part 6, "Requirements for Screening and Conservative Analysis of Other External Hazards At-Power"
 - ◆ Appendix 6-A, "List of External Hazards Requiring Consideration"
 - Supporting Requirement EXT-B1, "Initial Preliminary Screening for screening out an external hazard"

Incomplete assessment



- The staff finds:
 - No quantitative or bounding analyses for the external hazards specified in the SRM on SECY-93-087
 - No discussion as to how the main control room would cope with an external fire, i.e., smoke
 - ◆ COL Information Item 19.1(8) is not complete (e.g., missing aircraft crash event, tsunami)
- The applicant agreed to revise:
 - ♦ DCD to include quantitative/bounding analysis and address the main control room issue
 - ♦ COL Information Item 19.1(8)



Internal Events (IEs) During Low-power and Shutdown Levels 1 and 2 PRA

Marie Pohida

IEs LPSD Levels 1 and 2 PRA



- Reviewed POS definitions for completeness:
 - Time to boiling and core uncovery
 - ♦ Status of RCS penetrations, RCS level, decay heat
- Reviewed Event Trees for each POS
- Reviewed GL 88-17 implementation regarding RCS level and temperature instrumentation, availability of pumped injection, installation of nozzle dams, vortexing, and containment closure during reduced inventory conditions
- Reviewed risk significant equipment considered for TS LCO under 10 CFR 50.36(c)(2)(ii)(D)
- Performed confirmatory calculation of applicant's LPSD MAAP analyses for source terms
- Reviewed significant operational assumptions included as risk insights or TS as applicable

LPSD TS and DCD Additions



- Applicant added the following TS and DCD descriptions based on staff questions:
 - Containment Closure when RCS open via pressurizer manway until refueling cavity water level 23 feet above the reactor vessel flange (TS LCO 3.6.7)
 - ♦ Two trains of SI are operable in hot shutdown, cold shutdown and refueling with refueling cavity water level less than 23 feet above reactor vessel flange (TS LCO 3.5.3)
 - Midloop operation defined in TS requires >96 hrs post shutdown (DCD Chapter 16)
 - Availability of PARs and igniters during LPSD documented as risk insight (DCD Chapter 19)
 - Procedures to open hot leg manway to prevent rapid loss of inventory when cold leg penetrations exist included as risk insight (DCD Chapter 19)
- Staff finds applicant's approach consistent with guidance, subject to successful closure of open and confirmatory items



Internal Fire and Flood During Low-power and Shutdown Levels 1 and 2 PRA

Tony Nakanishi

Internal Fire and Flood LPSD Levels 1 and 2 PRA



- No staff-endorsed guidance on performing LPSD internal fire or internal flood PRA
- NUREG/CR-7114 provides framework for performing LPSD fire PRA
- Staff review focused on changes made relative to the fullpower fire and flooding and the internal events LPSD PRA models (e.g., induced initiating events, barrier integrity), and on adequacy of COL item addressing key assumptions



Uses and Applications of PRA

Hanh Phan

Uses and Applications of PRA



- PRA Results and Insights were used as an input to
 - ◆ Chapter 13.6, "Physical Security"
 - ♦ Chapter 14.3, "ITAAC"
 - ♦ Chapter 16, "TS"
 - ♦ Chapter 17.4, "RAP"
 - ♦ Chapter 18, "HFE"
 - ♦ Chapter 19.2, "SA"
 - Environmental report, "SAMDA"
- Influenced the selection of design features, i.e., four EDGs and battery depletion time
- Ensured that:
 - PRA is commensurate with the uses and applications
 - Input used for above programs is sufficient
 - ♦ Consistency between Chapter 19 and other Chapters



Results and Conclusion

Hanh Phan

Phase 2 Staff Findings



- The outstanding issues are:
 - Appropriate scope, level of detail, and technical adequacy of APR1400 PRA for its identified uses and applications
 - ♦ The reasonableness of APR1400 PRA to reflect the asdesigned, as-to-be-built, and as-to-be-operated plant



Section 19.2

Severe Accident Evaluation

Presentation Outline



Chapter 19.2 - Severe Accident Evaluation (SAE)

- 1) Severe Accident Prevention (Wagage)
- 2) Severe Accident Mitigation (Wagage, Pohida, Grady)
- 3) MELCOR Confirmatory Analysis (Schaperow, Campbell)
- 4) Containment Performance Capability (Roche-Rivera, Neuhausen)
- 5) Conclusion (Wagage)



Severe Accident Prevention

Hanry Wagage

Severe Accident Prevention



- Reviewed prevention issues:
 - Anticipated transient without scram
 - Mid-loop operation
 - Station blackout
 - ♦ Fire protection
 - Interfacing system loss-of-coolant accident

Station Blackout



- Provides one alternate ac (AAC) source, which is independent and diverse from the Class 1E EDGs
- Design change from two EDGs to four EDGs
- Extension of 125 Vdc battery life to 16 hours from 8 hours
- Successful startup of the AAC together with turbine-driven auxiliary feedwater pumps would prevent core damage during SBOs

Interfacing System Loss of Coolant Accident



- SECY-90-016 recommends low-pressure systems to be designed to withstand full RCS pressure or to provide means of testing pressure isolation valves and indications
- SIS, SCS, and CVCS are directly connected to the RCS:
 - SIS and SCS interfaces are designed to withstand full RCS operating pressure or have a leak-test capability
 - ◆ CVCS letdown and charging lines each has a high-pressure alarm to warn the operator when the pressure is approaching the low-pressure system design pressure
- Designing SCS lines to reduce ISLOCA was not clear as DCD stated designing for RCS full pressure or leak test capability and eliminating interfacing lines. In response to audit question, the applicant proposed updating DCD to clarify that deletion of unnecessary interfaces (e.g., the purification return line)



Severe Accident Mitigation "Progression and Features"

Hanry Wagage

Severe Accident Mitigation



- Reviewed DCD Section 19.2 and APR1400-E-P-NR-14003-P, "Severe Accident Analysis Report"
 - ♦ MCCI and Core Debris Coolability
 - DCH and HPME
 - ♦ FCI: In- and Ex-Vessel Steam Explosions
 - Containment Bypass
- Audited the sump evaluation, "Ex-Vessel Severe Accident Analysis for the APR1400 with the MELTSPREAD and CORQUENCH Codes"
- Reviewed severe accident mitigation features identified by the applicant using SRP 19.0 and SECY-90-016

In-vessel Steam Explosions



- The FCI expert review group concluded in NUREG-1116 and NUREG-1524 that the probability of containment failure was vanishingly small or physically unreasonable
- The applicant used one-dimensional TEXAS-V computer code for calculating steam explosion loading
- The staff asked for justification for the chosen crosssectional area of the pool for TEXAS calculation
- The applicant used ABAQUS 6.10 code for structural analysis and Shockey criteria of 11% plastic strain for allowable limit

Ex-vessel Steam Explosions



The remaining issues are as follows:

- Cross-sectional area of the pool used for one-dimensional TEXAS computer code calculations
- Calculation of impulse on cavity structures using TEXAS results
- Structural evaluation of cavity structures
- Impact of IVR/ERVC operation of steam explosion loading

Ex-vessel Steam Explosion: Impact of IVR/ERVC operation



- The SCS provides water from the IRWST for active cavity flooding to perform ERVC strategy that leads to flood water to appropriate elevation
- The applicant did not assume the operation of IVR/ERVC system for DCD Chapter 19 analysis
- Although the active flooding may cool the core melt in-vessel, a
 possibility exists for the vessel bottom to fail on side causing a larger
 melt jet that would generate higher steam explosion energy than
 analyzed
- The applicant proposed a COL information item to analyze the above condition under accident management plan



Severe Accident Mitigation Equipment Survivability

Anne-Marie Grady

Equipment Survivability



Objective:

- ♦ SECY 93-087 requires mitigation features be designed to operate in the severe-accident environment for which they are intended and over the time span for which they are needed
- ◆ 10 CFR 50.44(c)(3) requires containments to establish and maintain safe shutdown and containment structural integrity with systems and components capable of performing their functions during and after exposure to the environmental conditions created by the burning of hydrogen equivalent to that generated from a fuel cladcoolant reaction involving 100 % of the fuel cladding

Equipment Identified



- Applicant selected accident scenarios from the most probable core damage sequences in the Level 1 PRA, and, from several LOCAs
- Applicant identified required mitigation functions of RCS inventory control; RCS heat removal; reactivity control; and containment integrity
- Applicant identified specific equipment required to achieve each function in DCD Tier 2, Table 19.2.3-4, "Systems and Equipment/Instrumentation Required for Equipment Survivability Assessments"
- Staff agreed with equipment identified, but requested addition of ECSBS-V1014, and, CIV and penetration integrity (applicant agreed)

Accident Conditions Characterized



- Staff finds the methodology, identification of equipment required for accident mitigation, and environmental conditions for equipment survivability establishes sufficient guidance and input for the COL applicant to demonstrate compliance with 10 CFR 50.44(c)(3) and 10 CFR 50.34(f)
- The temperature profiles were confirmed in the staff confirmatory calculations
- The applicant's AICC pressure of 110 psia bounded the staff confirmatory pressures

Accident Conditions Characterized (continued)



- The applicant calculated the severe accident radiation dose of 4.4E+05 Gy (4.4E+07 rad) using the MAAP4-DOSE code
- Staff compared these results to those from other ALWR's of similar size, design and fuel type, and severe accident scenarios, and found the containment doses comparable
- Staff also found the containment atmospheric assessments of temperature, pressure and radiation described in DCD section 19.2.3.3.7 acceptable for evaluating equipment survivability
- COL Information Item 19.2(1) will be revised to state that the COL applicant and/or holder is to perform and submit site specific equipment survivability assessment based on the above equipment and containment atmospheric assessments



MELCOR Independent Confirmatory Analysis

Jason Schaperow Shawn Campbell

MELCOR Confirmatory Analysis



- To confirm applicant's use of MAAP for PRA and severe accident analysis
- To perform independent analysis for select scenarios using MELCOR and compare with MAAP results
- Remaining issues
 - ♦ The applicant is assessing impact of MAAP at-power sensitivity calculations on the SAMDA analysis
 - ♦ The applicant is revising MAAP shutdown analyses

MELCOR Confirmatory Analysis



MAAP Case	Objective of MAAP Case	Accident Initiator	New Reactor Severe Accident Feature		
			Rapid Depressur- ization	Cavity Flooding	ECSBS at 24 hours
STC10	Source term for containment leakage	LOCCW	✓	√	√
STC11	Source term for basemat melt-through	LOCCW	√		√
STC16	Source term for containment leak at 24 hours	LOCCW	✓		
Q03	Containment pressure for dry cavity	SBO			
POS5*	Time to core damage, lower head failure	Loss of SDC and injection			

^{*} Mid-loop accident

At-power Accidents



Comparison of MELCOR and MAAP results led to identifying differences in assumptions

Assumption	MELCOR	MAAP
SITs	✓	
Hot leg creep rupture	✓	
RCP seal leakage/failure	✓	
Operators open POSRVs	CET = 922K (SAMG value)	After first automatic lift (feed & bleed procedure)
Operators open 3-way valves and cavity flooding valves	CET = 922K (SAMG value)	30 minutes after CET = 922K (assumed delay)

CET - core-exit thermocouple

At-power Accidents



- The applicant ran MAAP sensitivity cases to address differences in assumptions
- Staff scaled the cesium releases in the DCD by the differences between DCD Cases STC10, STC11, and STC16 and the Cases STC10, STC11, and STC16 sensitivities
 - ◆ LRF scaling the cesium releases does not change the release from small to large for any source term category
 - ♦ SAMDA scaling the cesium releases is unlikely to affect the SAMDA analysis given its margins
- CET quantification
 - ◆ The containment pressure differences between Case Q03 sensitivities in the RAI response and Case Q03 in the DCD are unlikely to affect CET quantification, because the median ultimate containment failure pressure is 162.7 psig

Mid-loop accidents



- Staff modified the MELCOR at-power deck to simulate a midloop accident
 - Reduced decay heat to account for time until reactor is in mid-loop configuration
 - Simulated nozzle dams by blocking flow paths connecting the steam generators to the hot legs and cold legs
 - Added open manway at top of pressurizer
 - Isolated the SITs from the RCS
 - ♦ Set initial RCS pressure, temperature, and water level to 14.7 psia, 330K, and hot leg mid-plane, respectively
- The applicant is revising its MAAP analysis and documentation
 - More realistic modeling of RCS and containment configuration
 - Code bug



Containment Performance Capability

Robert Roche-Rivera Alissa Neuhausen

Containment Performance Capability



- Ensured the applicant meets the Commission's deterministic containment performance goal as described in SECY 90-016 and 93-087
- Focused on the information provided in DCD Section 19.2.4
- Compared the applicant's evaluation to staff guidance
- Examined the results of the applicant's finite element analysis
- Confirmed that the ASME Factored Load Category criteria are met for severe accident loading
- The staff has completed the review of the deterministic containment performance goal

Factored Load Category



- Deterministic containment performance goal
 - ♦ Containment maintains its role as reliable leak-tight barrier
 - Containment stresses do not exceed ASME service level C limits/Factored Load Category for 24 hrs following onset of core damage
 - Containment continues to provide a barrier against the uncontrolled release of fission products after 24 hrs
- The applicant selected a conservative severe accident load
- The applicant demonstrated that the most significant pressureloading histories: LLOCA, SBO, TLOFW are bounded by the severe accident load selected for the FLC
- The applicant demonstrated that the strains in the liner plate do not reach the allowable limit strain values
- Staff concludes strain limits meet ASME Code



Conclusion

Hanry Wagage

Phase 2 Staff Findings



Due to the remaining issues, the staff is unable make final conclusions on the severe accident evaluation of the APR1400 design

ACRONYMS



- ACRS Advisory Committee on Reactor Safeguards
- AICC adiabatic isochoric complete combustion
- ALWR advanced light-water reactor
- ANS American Nuclear Society
- ASME American Society of Mechanical Engineers
- CCF common-cause failure
- CCFP conditional containment failure probability
- CDF core damage frequency
- CET containment event tree or core-exit thermocouple
- CFR Code of Federal Regulations
- CFS cavity flooding system
- CIV containment isolation valve
- COL combined license
- CSDRS certified seismic design response spectra
- CVCS chemical and volume control system
- DC design certification
- DCD design control document

- DCH direct containment heating
- DET decomposition event tree
- ECSBS emergency containment spray backup system
- EDG emergency diesel generators
- EE external events
- ERVC external reactor vessel cooling
- FCI fuel-coolant interaction
- FLC factored load category
- GMRS ground motion response spectra
- HCLPF high-confidence-and-low-probabilityof-failure
- HFE human factors engineering
- **HPME** high-pressure melt ejection
- HVAC heating, ventilation, air conditioning
- **HVT** holdup volume tank
- I&C instrumentation and control
- **IE** initiating event

ACRONYMS (continued)



- IF internal flood
- IRWST in-containment refueling water storage tank
- ISLOCA interfacing system loss-of-coolant accident
- ITAAC inspections, tests, analyses, and acceptance criteria
- IVR in-vessel retention
- KEPCO Korea Electric Power Corporation
- KHNP Korea Hydro and Nuclear Power Co.
- LCO limiting condition for operation
- LLOCA large-break loss-of-coolant accident
- LOCA loss-of-coolant accident
- LOCCW loss of component cooling water
- LPSD low power and shutdown
- LRF large release frequency
- MAAP modular accident analysis program
- MCCI molten core-concrete interaction

- PARs passive autocatalytic recombiners
- PDS plant damage state
- PGA peak ground acceleration
- POS plant operational state
- PRA probabilistic risk assessment
- RAI request for additional information
- RAP reliability assurance program
- RCP reactor coolant pump
- RCS reactor coolant system
- RPV reactor pressure vessel
- SA severe accident
- SAE severe accident evaluation
- SAMDA severe accident mitigation design alternatives
- SAMG severe accident mitigation guidelines
- SBO station blackout
- SCS shutdown cooling system
- SDC shutdown cooling

ACRONYMS (continued)



- SI safety injection
- SIS safety injection system
- SIT safety injection tank
- SMA seismic margin assessment
- SRM staff requirements memorandum
- SRP Standard Review Plan
- STC source term category
- TLOFW total loss of feedwater
- TS technical specifications